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**On-line instrumentation in wastewater  
treatment processes: How to get the right  
information at the right moment and efforts  
to spend concerning the maintenance**

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These are preliminary lecture notes, intended only for distribution to participants



# On-Line Instrumentation in Wastewater Treatment Processes : How to Get the Right Information at the Right Moment and Efforts to Spend Concerning the Maintenance

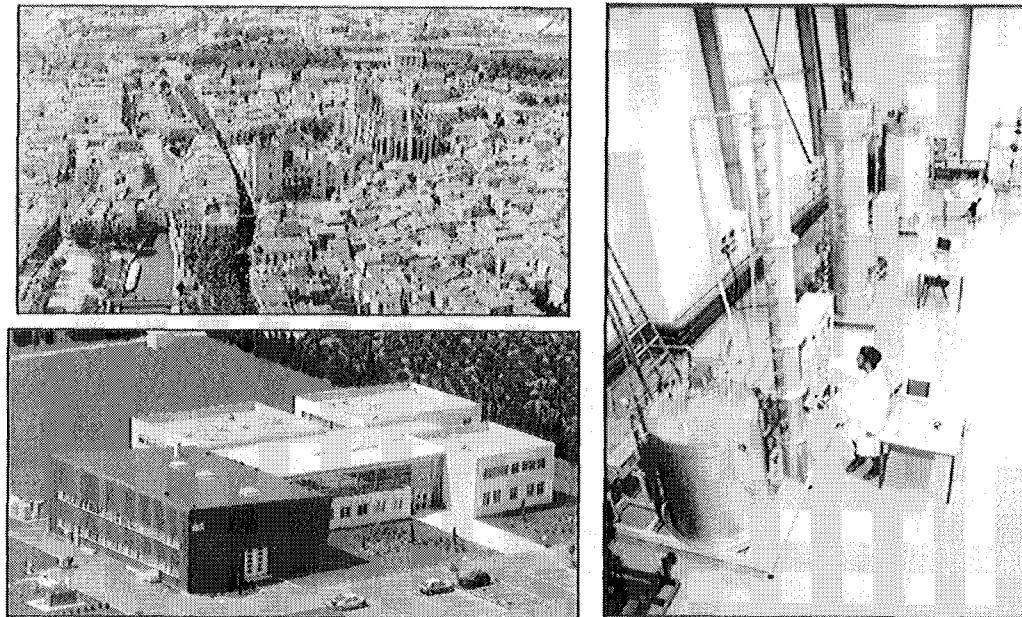
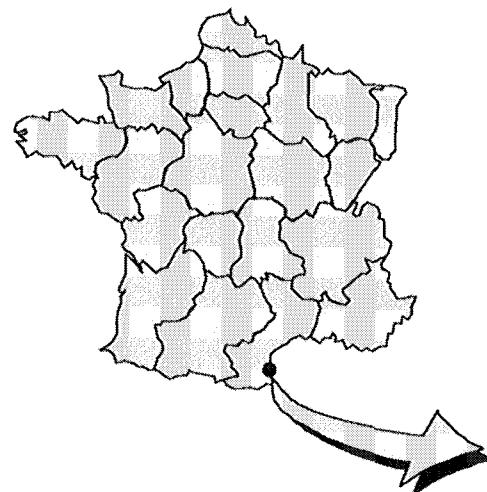
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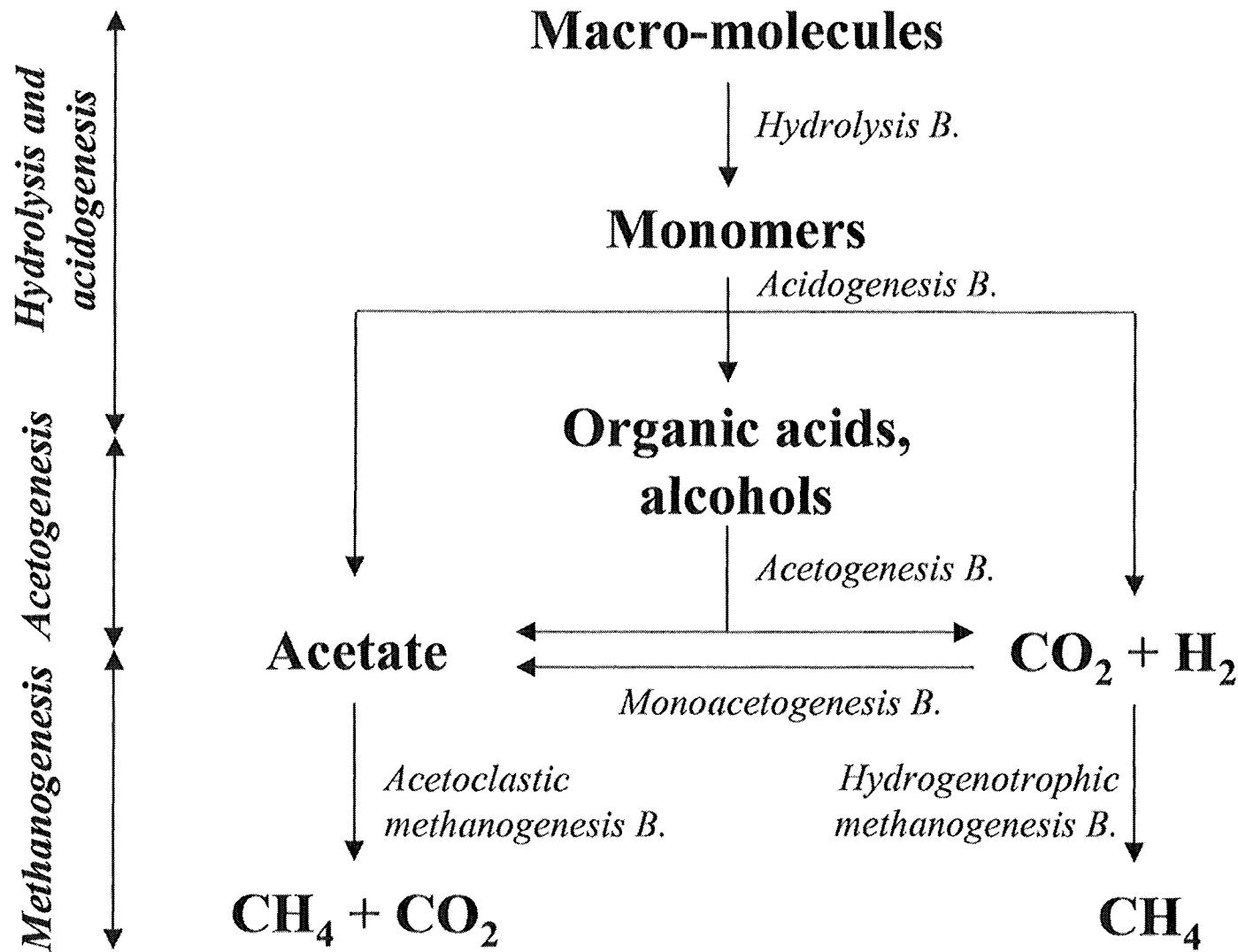


# *Contents of the Presentation*

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- 1) The anaerobic digestion process*
- 2) Some examples of (off-line) sensors*
- 3) Practical illustration of on-line sensors*
- 4) Benefits from on-line instrumentation*

# *The Anaerobic Digestion Reaction Scheme*



# *Applications of Anaerobic Digestion*

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- ✓ Carbon removal of wastewater
- ✓ Production of energy (biogas)
- ✓ Reduction of sludge production
- ✓ Treatment of solid wastes (agricultural, industrial, urban)
- ✓ Decontamination of soils (organochlorine)
- ✓ Discolouration of effluents

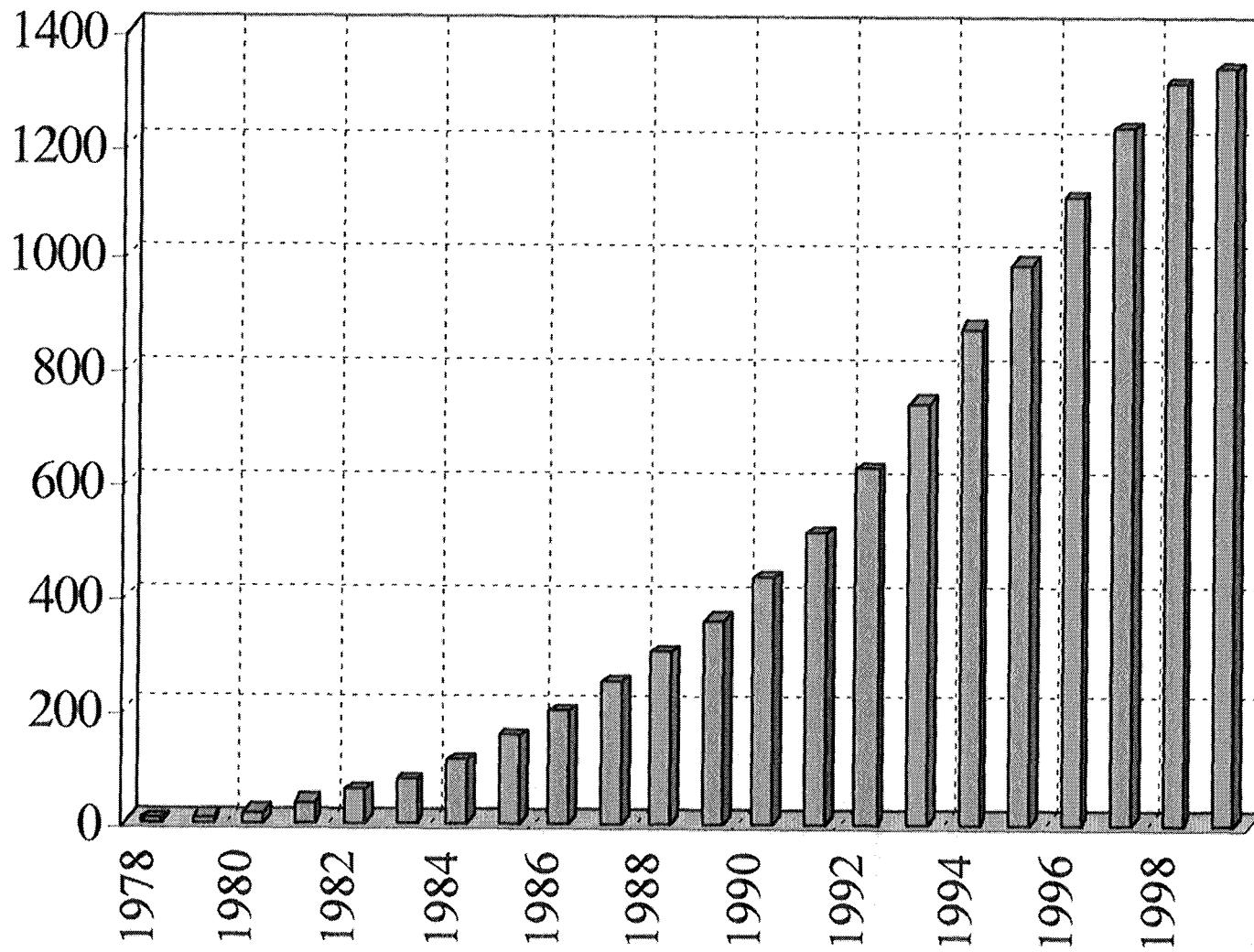
## ↳ Advantages

- ✓ Naturally present in the environment
- ✓ No need of energy
- ✓ Production of valorizable biogas
- ✓ High loading rate achievable (up to 100 kg of COD/m<sup>3</sup>/d)
- ✓ Low sludge production
- ✓ Works with effluents with low N/COD and P/COD ratio
- ✓ High efficiency (80 to 98 % removal of COD)

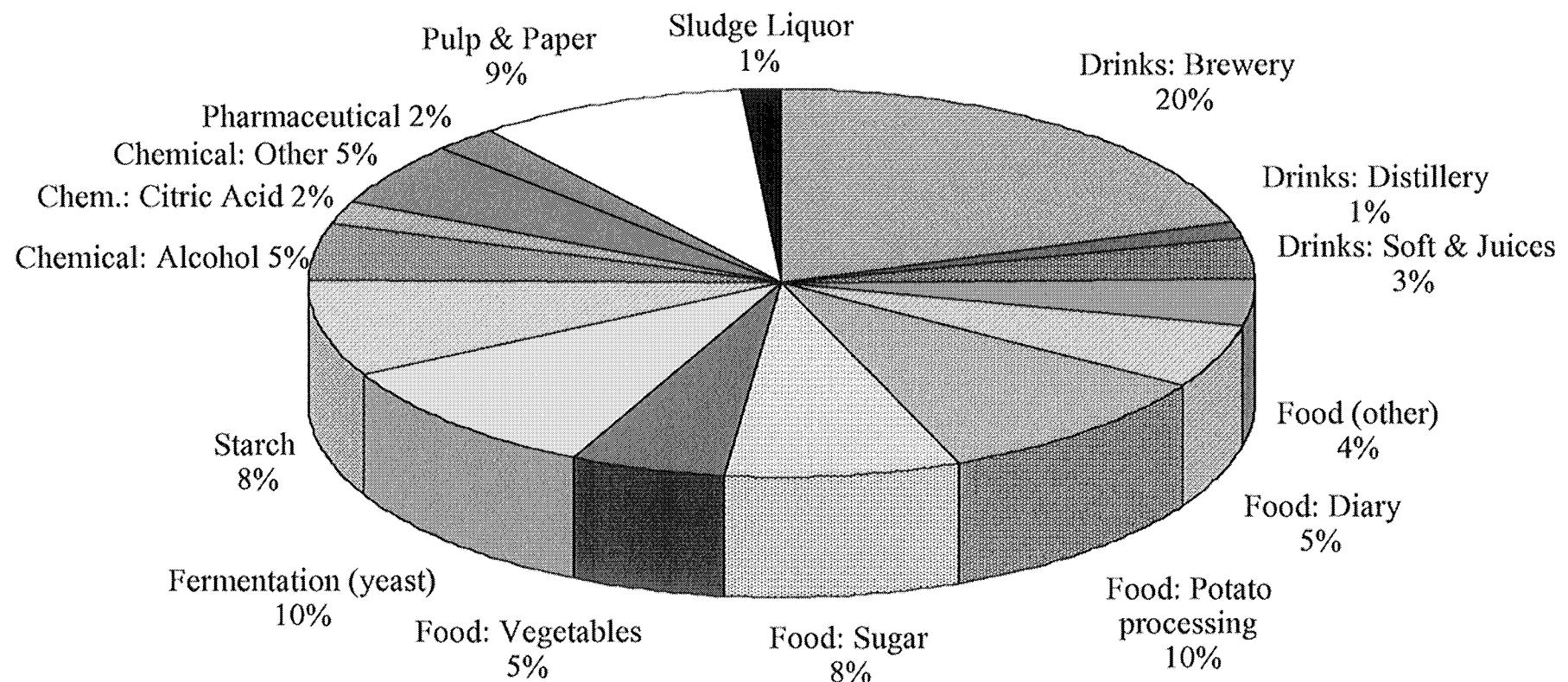
## ↳ Drawbacks

- ✓ Considered as a pretreatment
- ✓ Not really suitable for diluted effluent
- ✓ Slow growth of microorganism
- ✓ Sensitivity to organic overloads (biological system / size)

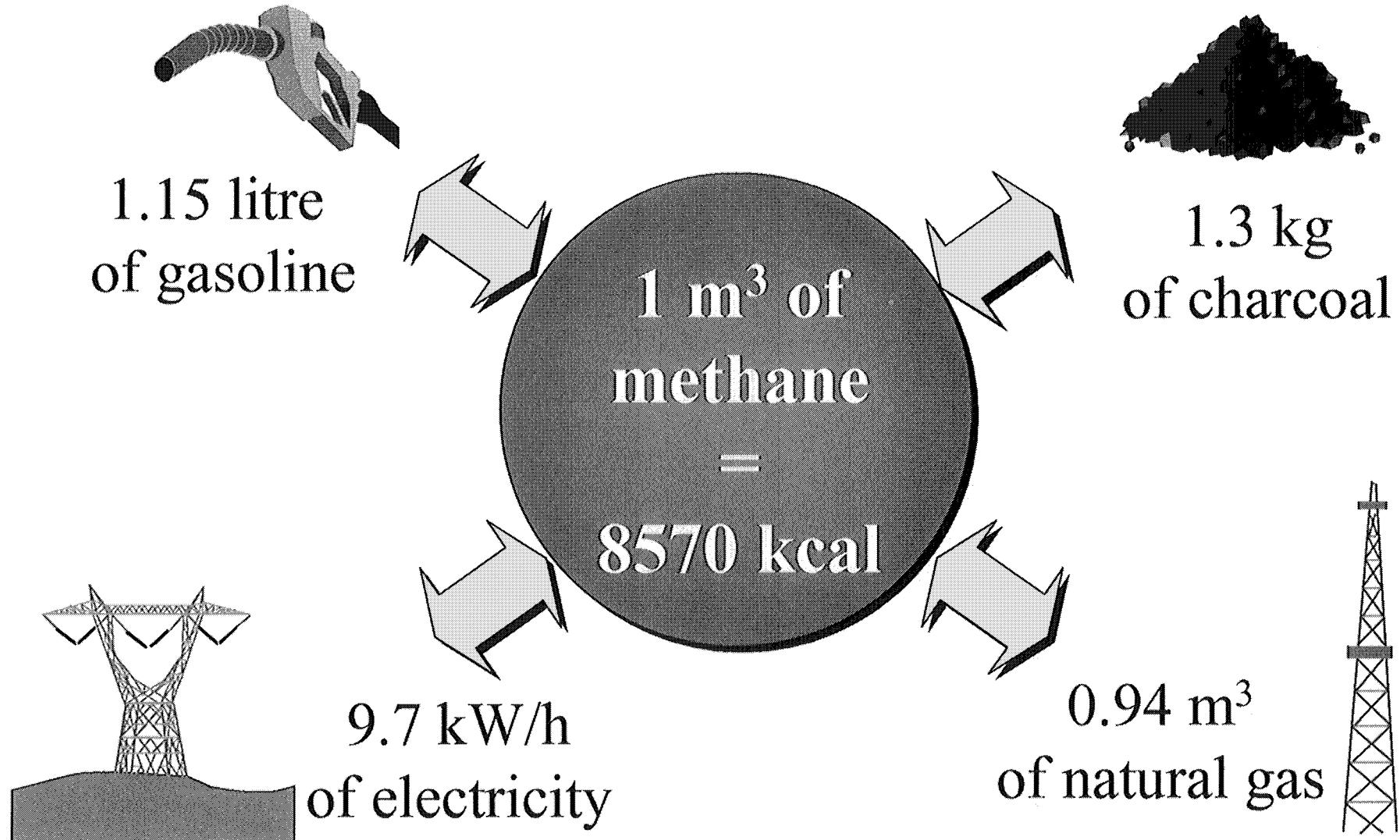
# *Number of Industrial Applications worldwide*



# *Types of Industries using AD Processes*



## *Biogas is valorizable*



# *Contents of the Presentation*

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*1) The anaerobic digestion process*



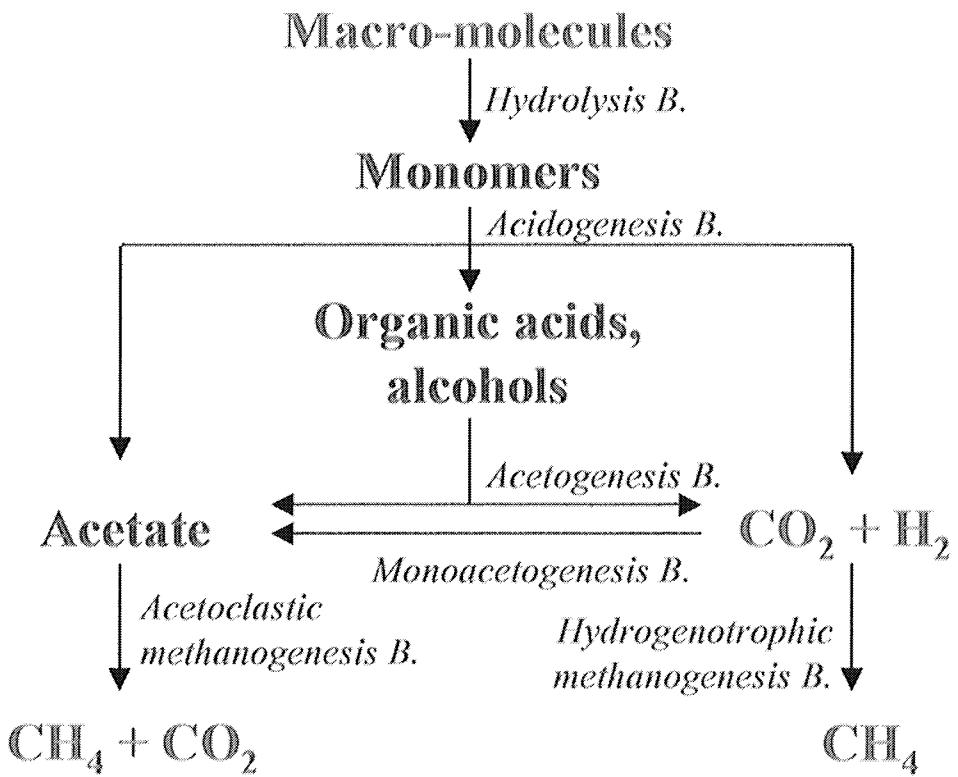
*2) Some examples of (off-line) sensors*

*3) Practical illustration of on-line sensors*

*4) Benefits from on-line instrumentation*

# The Anaerobic Digestion Reaction Scheme

Objective : Get closer to the microorganisms

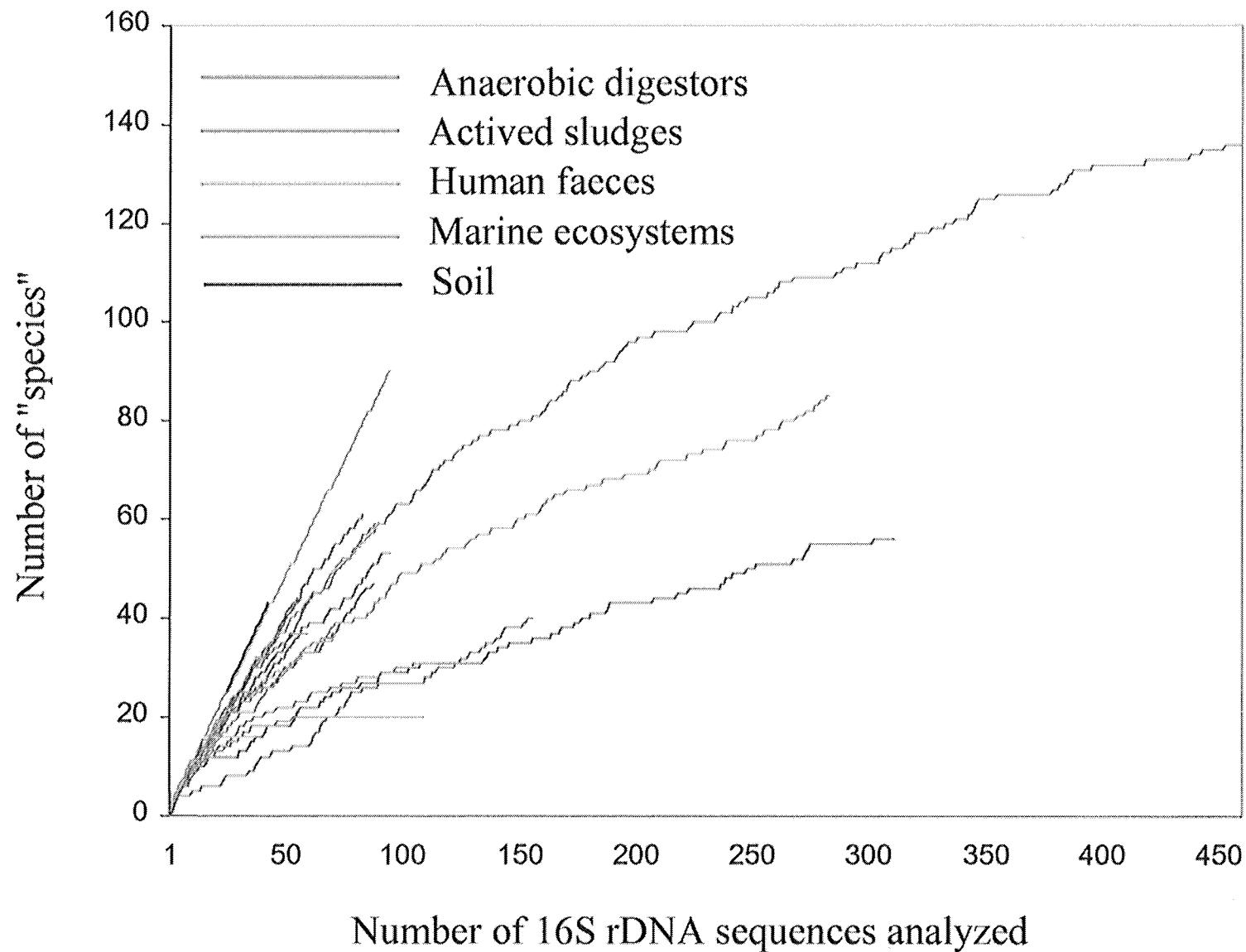


In the solid phase :  
**Difficult**  
 (samples taking)

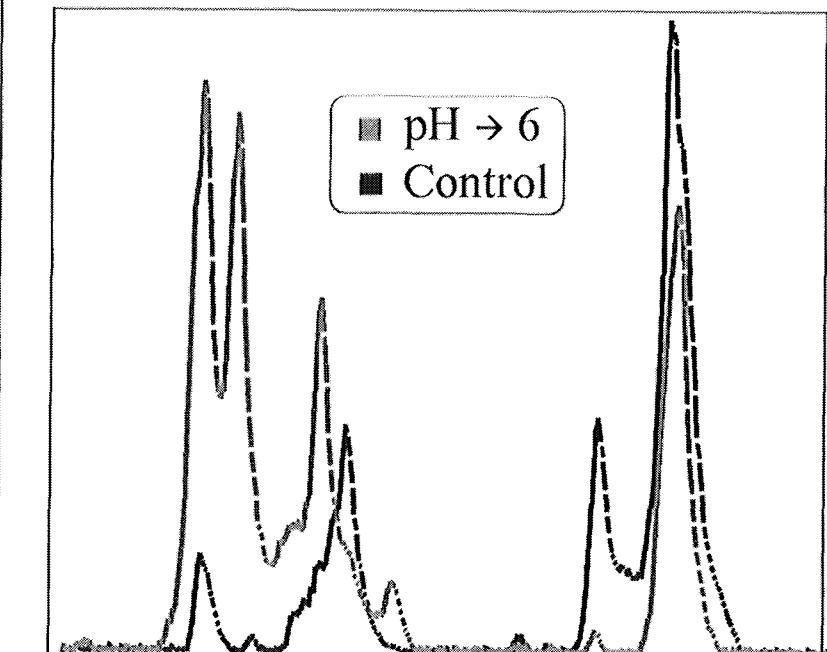
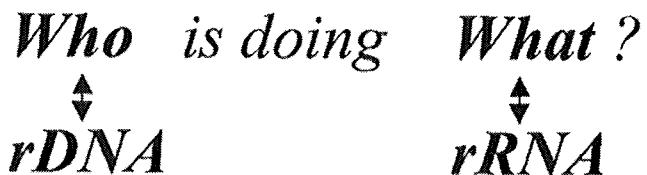
In the liquid phase :  
**Difficult**  
 (suspended solids and  
 global measurement of  
 biomass)

In the gas phase :  
**Easy but end products**  
 (aggregated measurements  
 and delay)

# *Anaerobic Digestion is a Complex Ecosystem*



*Molecular approach to answer the question :*



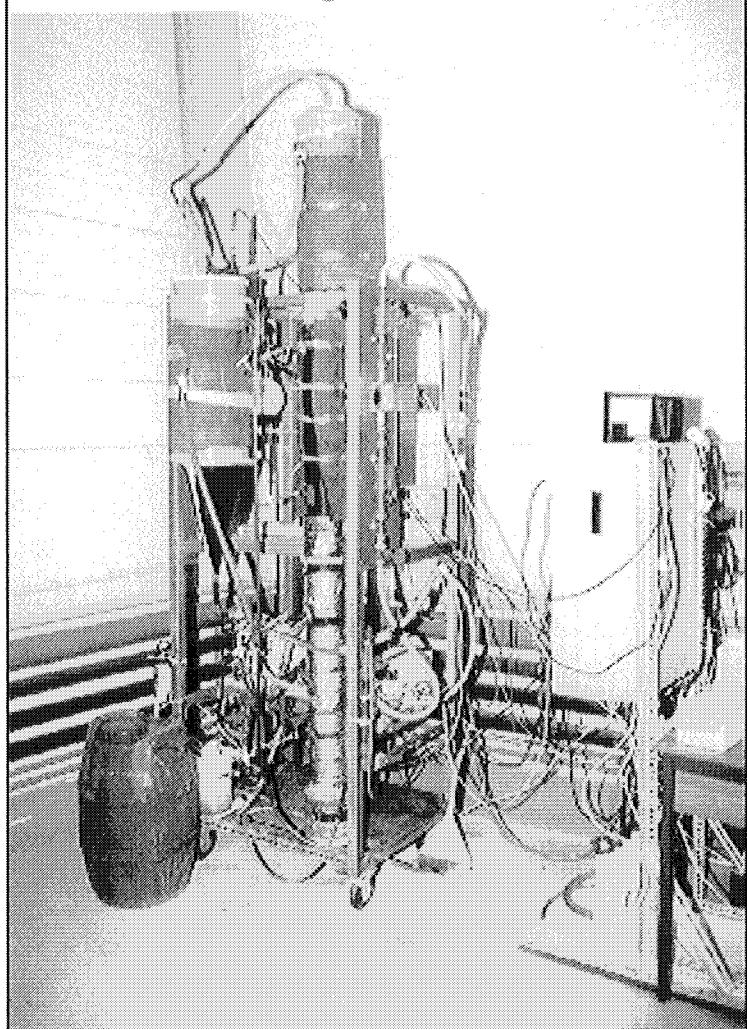
*Effect of an acidic shock (pH : 7 → 6)  
on the activity of the different species*

- ✓ Species can be identified by cloning and sequencing the 16S rDNA genes
- ✓ A peak = one species
- ✓ Area of a peak ≈ activity of the corresponding species

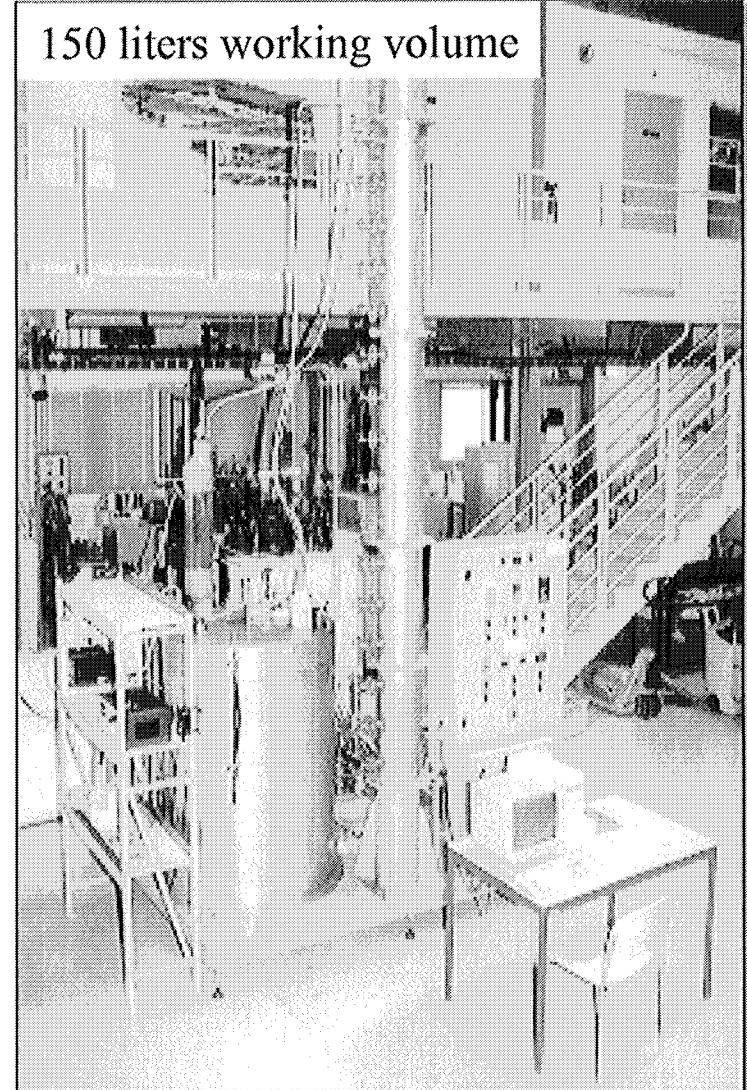
## *Examples of AD Processes in Narbonne*

- Fluidized Bed Reactors
- Effluent : Industrial distillery vinasses

15 liters working volume



150 liters working volume

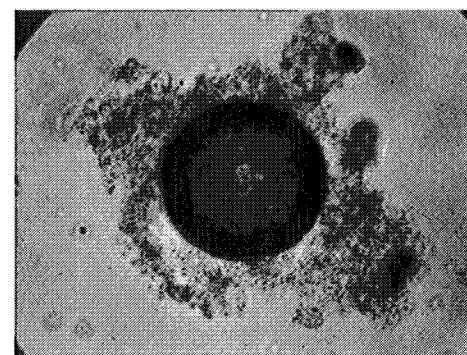


# *Analysis of Biofilms*

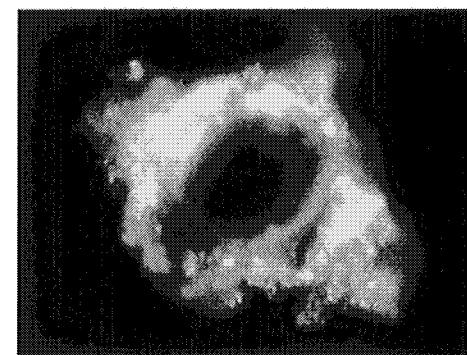
**General objective :** To study and to improve the kinetics  
of biofilm development on granular carriers

*One way : Image Analysis*

*Example of qualitative analysis using DAPI coloration  
for fluidized bed reactor*



Normal light



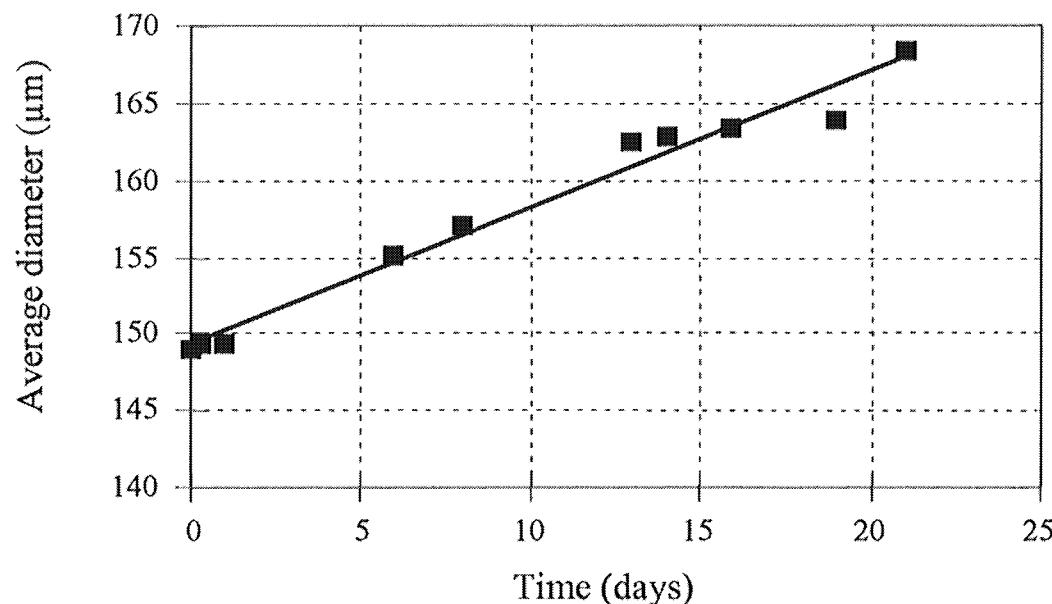
UV fluorescence

# *Analysis of Biofilms*

*Based on the previous results,  
quantitative measurement of biofilm growth*

↳ For example, estimation of  
*equivalent diameters and shape factors*

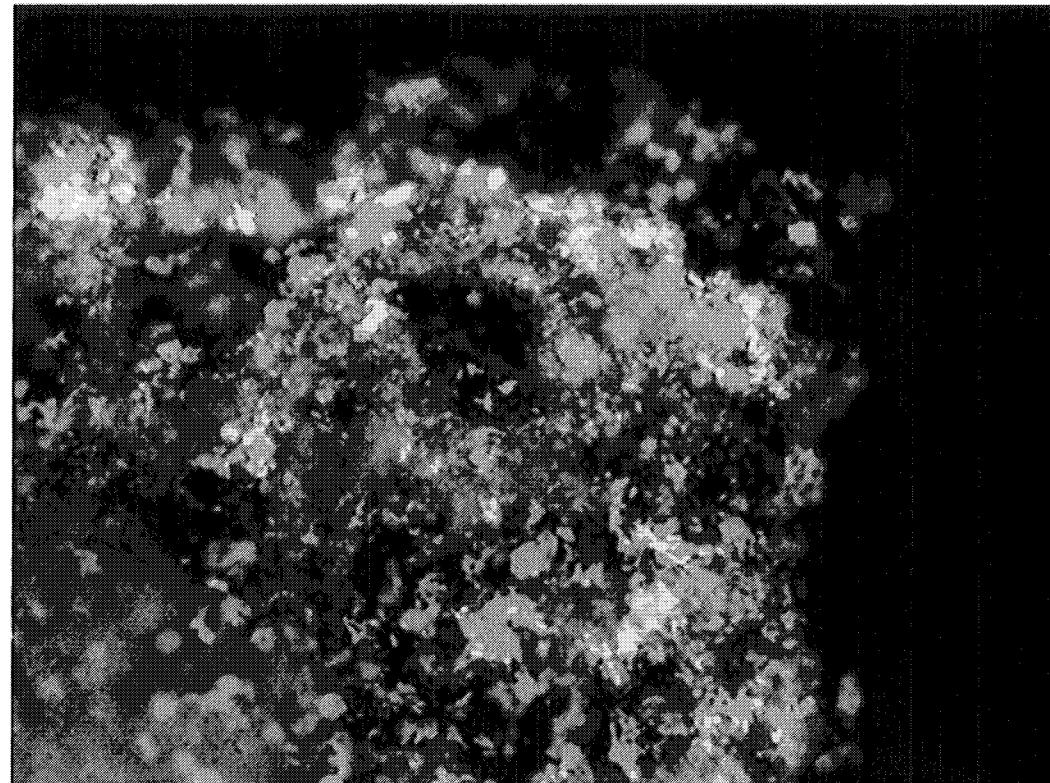
Example: biofilm growth in an anaerobic biofilm reactor : evolution of particle size



*If you get closer ...*

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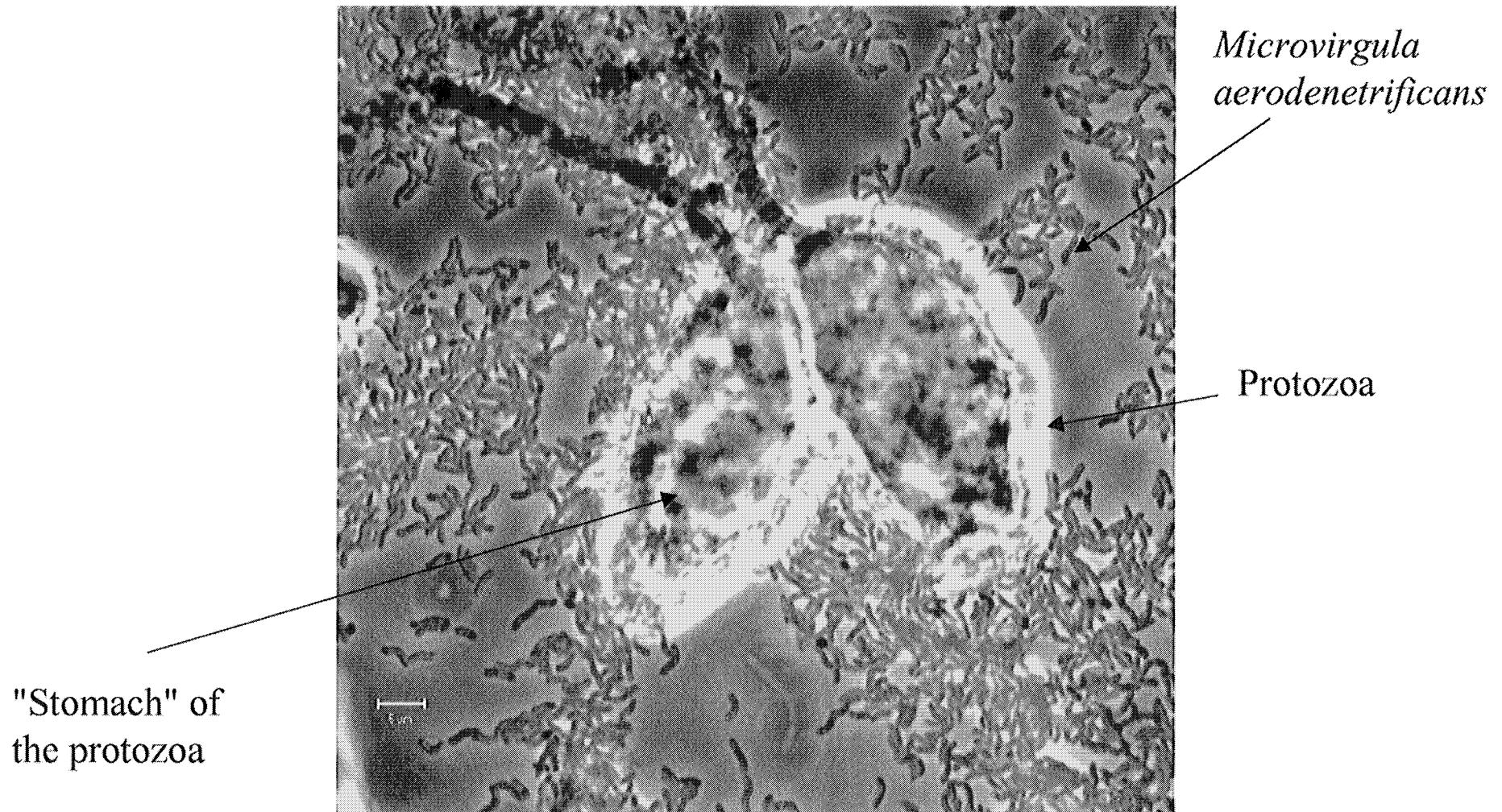
## Fluorescent In Situ Hybridization (FISH)

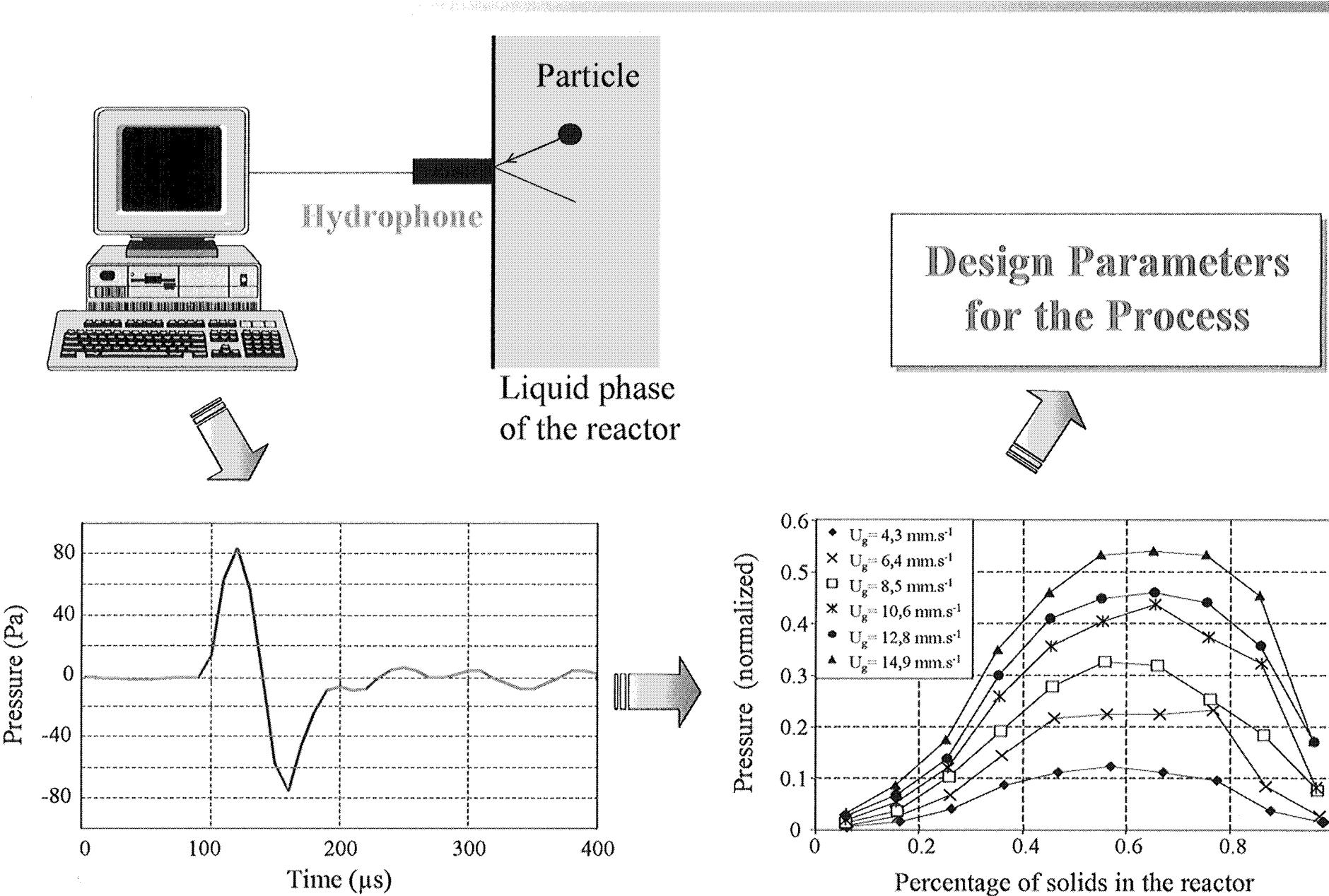


Blue : All species

Red : One specific bacteria

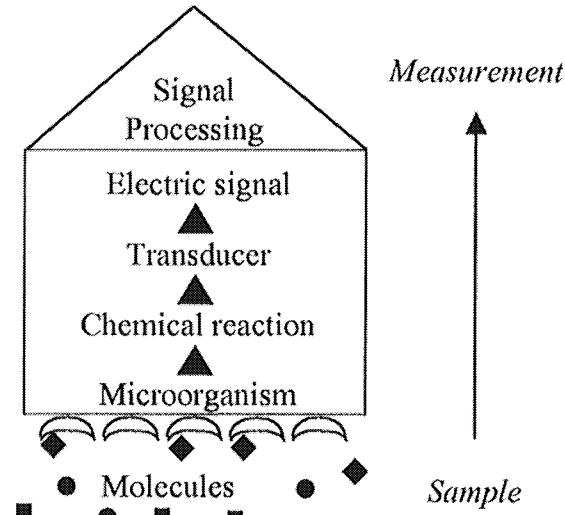
# *Life is sometimes difficult for bacteria ...*



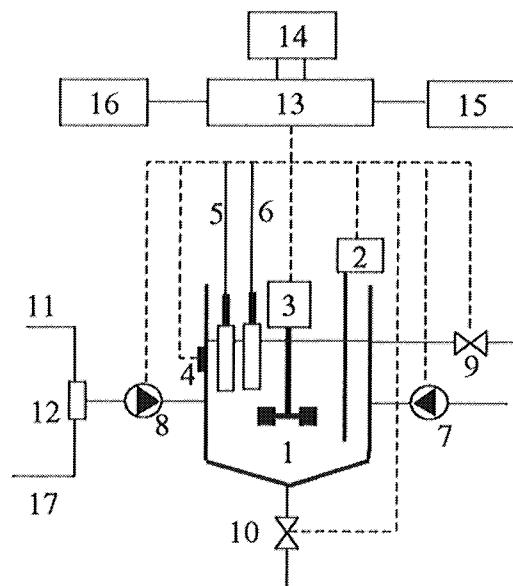


# *Examples of advanced sensors*

*1) Biosensor  
(e.g., biological reaction directly in a probe)*



*2) In-situ sensor  
(e.g., respirometric sensor)*



1. Reactor (10 cm<sup>3</sup> sludge)
2. Aerator
3. Stirrer
4. Temperature sensor
5. DO electrode
6. pH electrode
7. Calibration pump
8. Sample pump
9. Decantation valve
10. Sludge outlet valve
11. Bypass
12. Filter system (0.5 mm)
13. Microprocessor
14. Display/keyboard
15. Computer (PC)
16. Printer
17. Wastewater

# *Contents of the Presentation*

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CONTENTS

INTRODUCTION

ANALYSIS

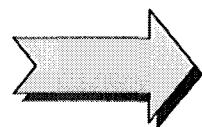
MONITORING

PREDICTION

OPTIMIZATION

CONCLUSION

REFERENCES



*1) The anaerobic digestion process*

*2) Some examples of (off-line) sensors*

*3) Practical illustration of on-line sensors*

*4) Benefits from on-line instrumentation*

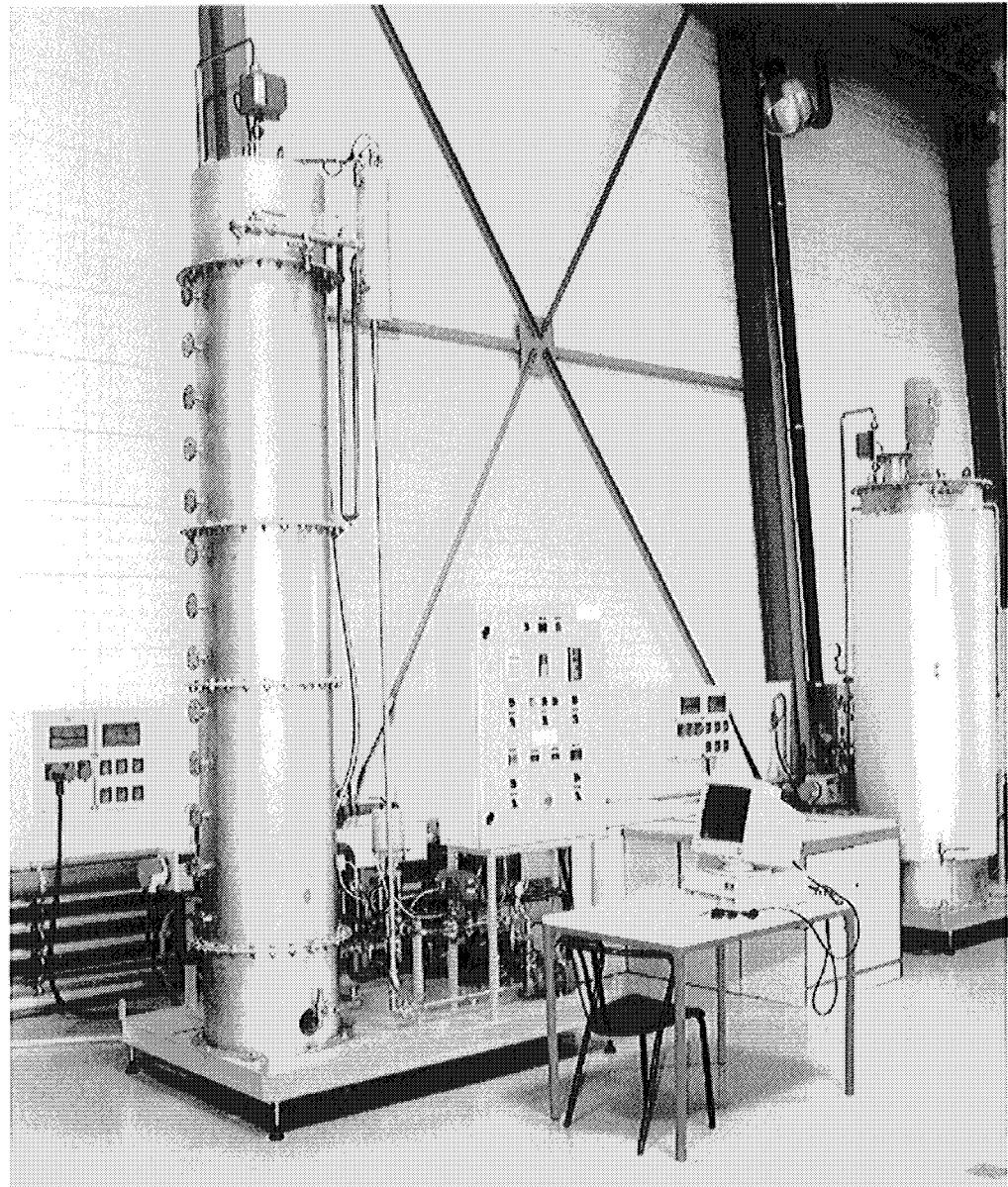
## *The process used*

Influent : Raw industrial  
distillery vinasses

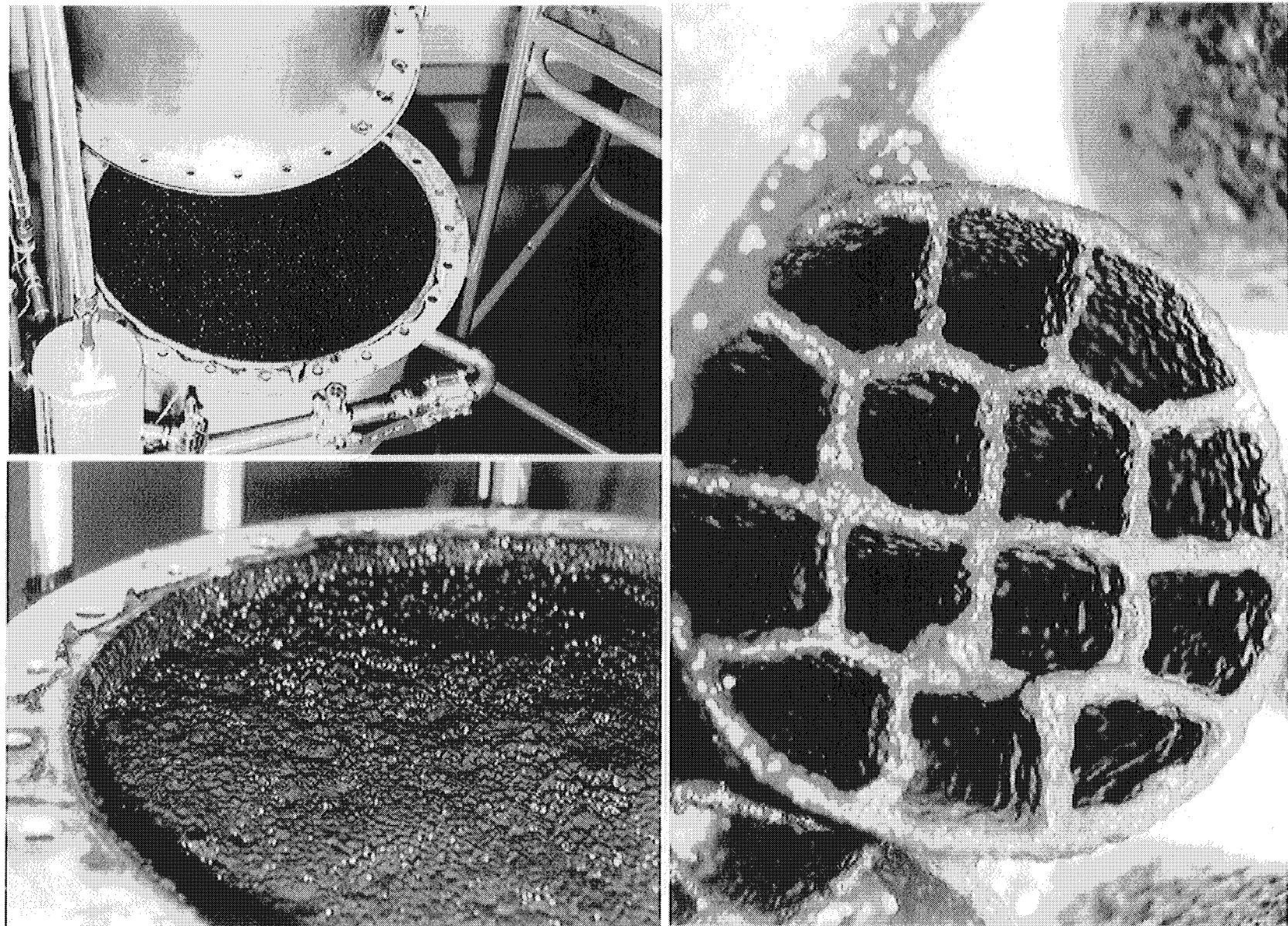
Reactor : Circular column  
Up-flow fixed bed reactor  
- 3.5 m height,  
- 0.6 m diameter,  
- 982 liters of total volume.

Media : Cloisonyl  
- Specific surf. :  $180 \text{ m}^2/\text{m}^3$   
- Volume : 33.7 liters

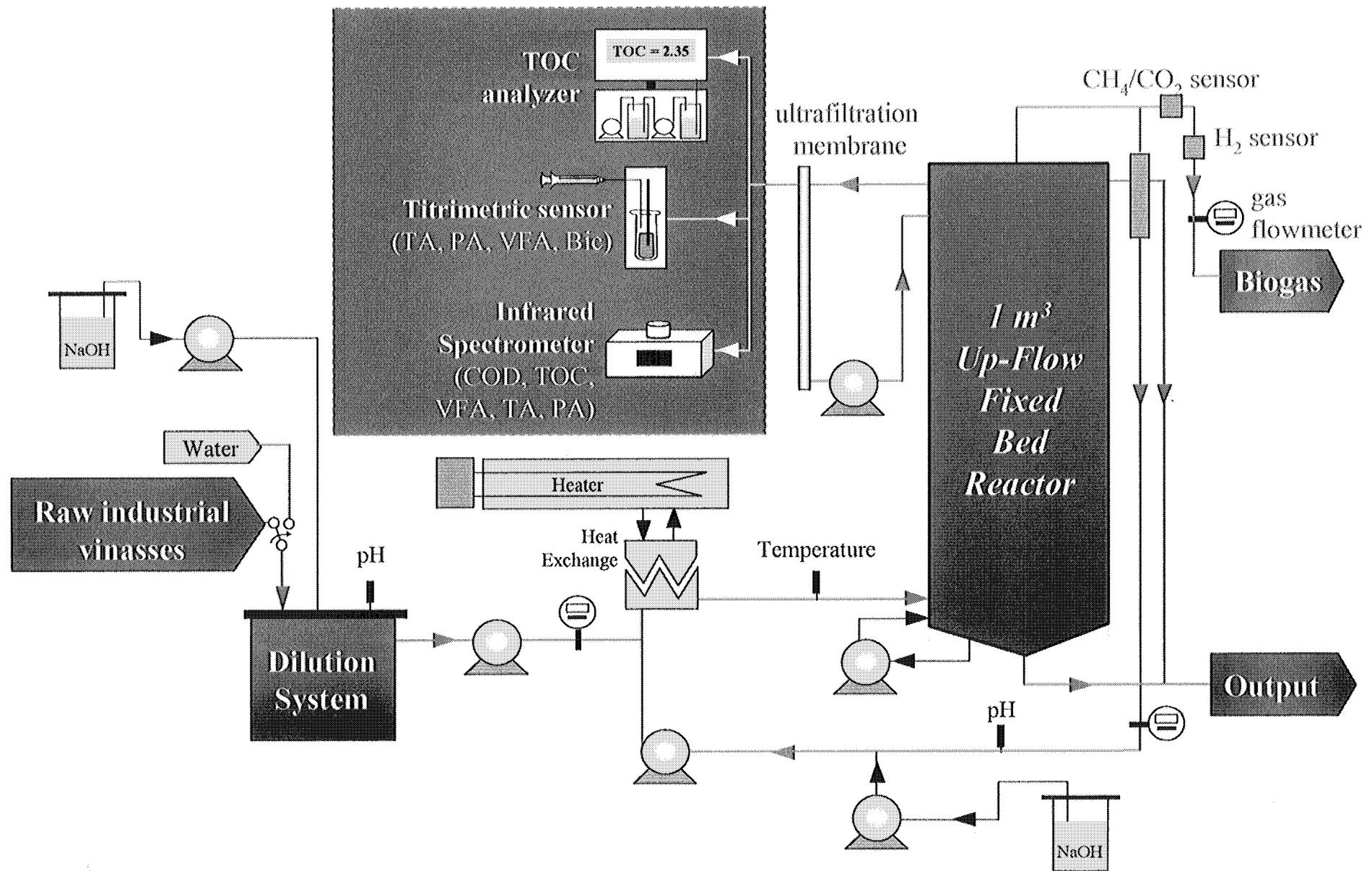
Total effective volume : 948 liters



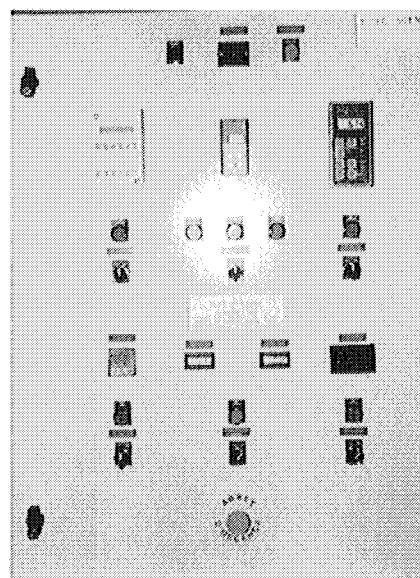
# *Media for Microorganisms (Cloisonyl)*



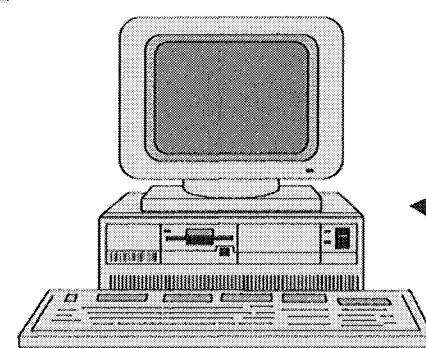
# *Schematic layout of the plant*



# *The Input/Output Device*

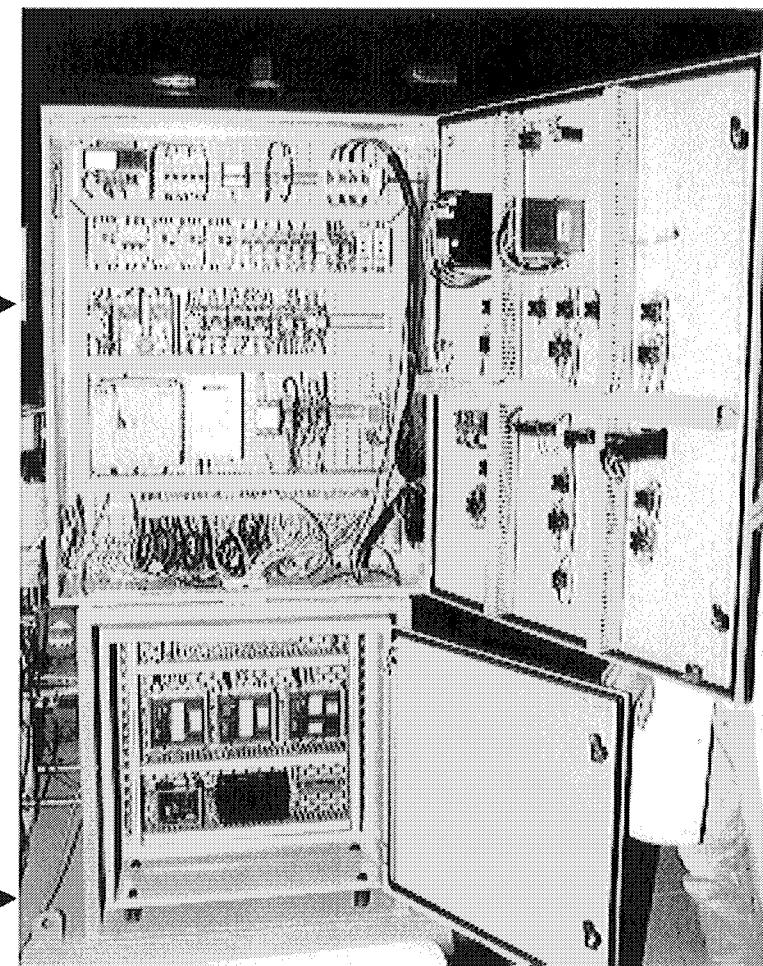


*View from outside*



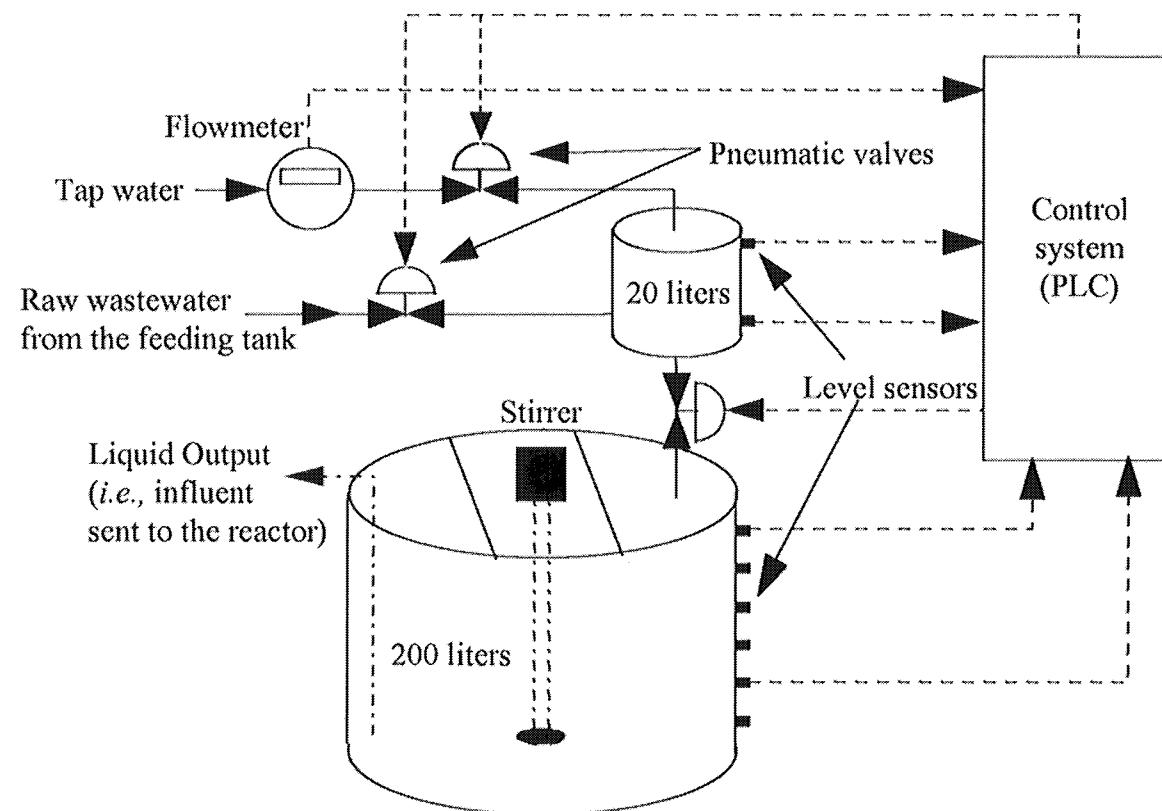
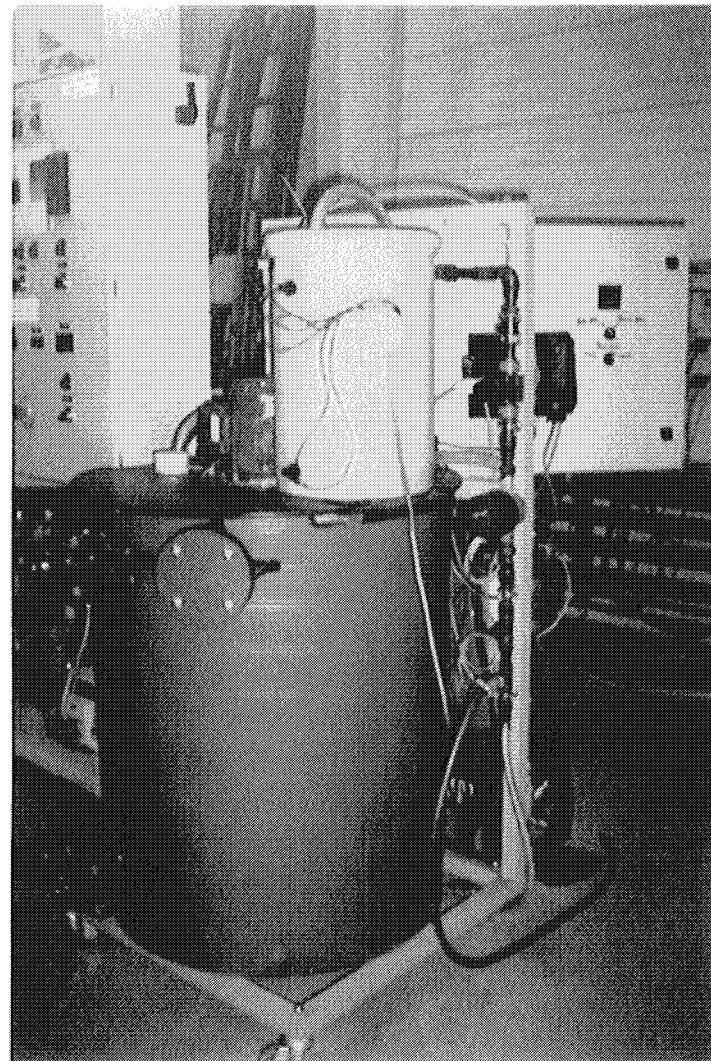
Analogic/Digital Conversion

Link with a PC

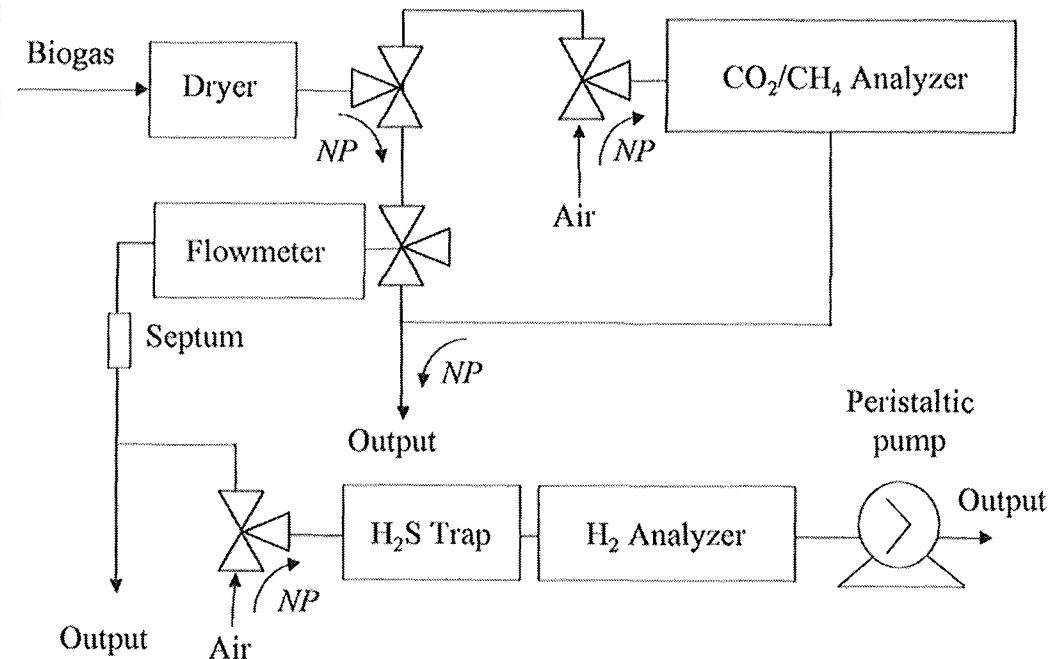
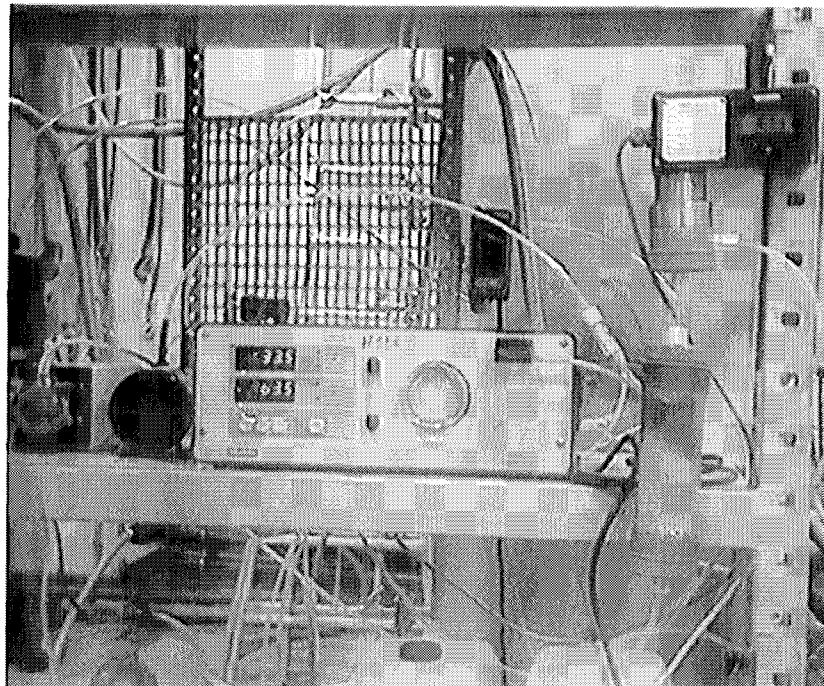


*View from inside*

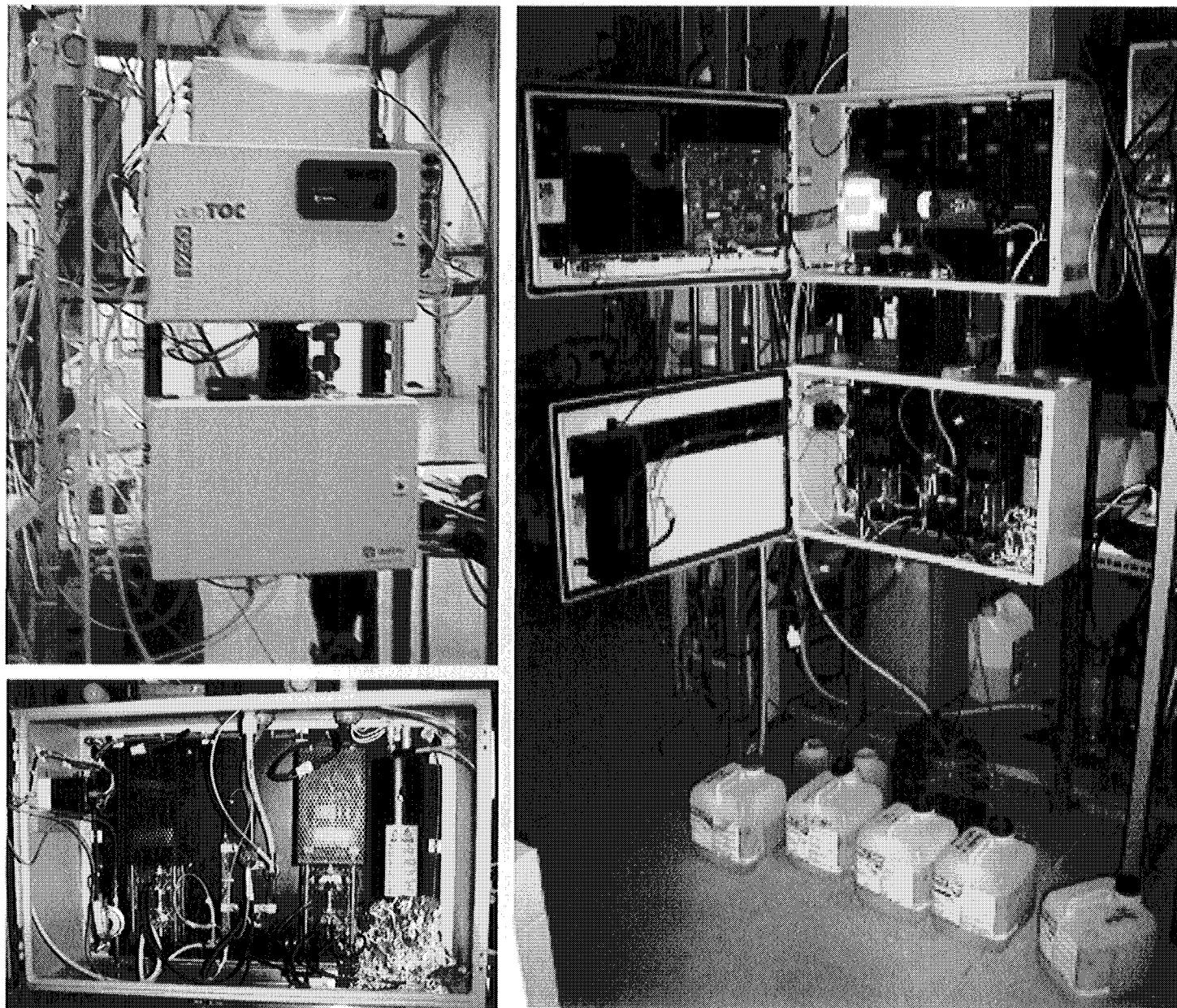
# The Dilution System



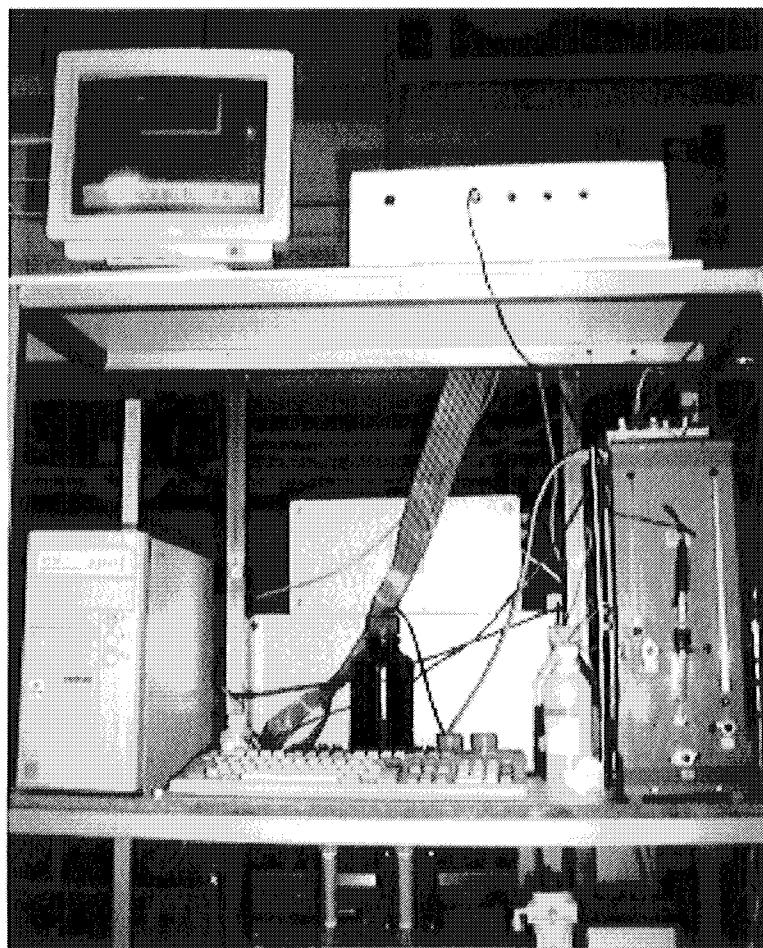
# The Gaz Analyzing Loop



# *The TOCmeter*

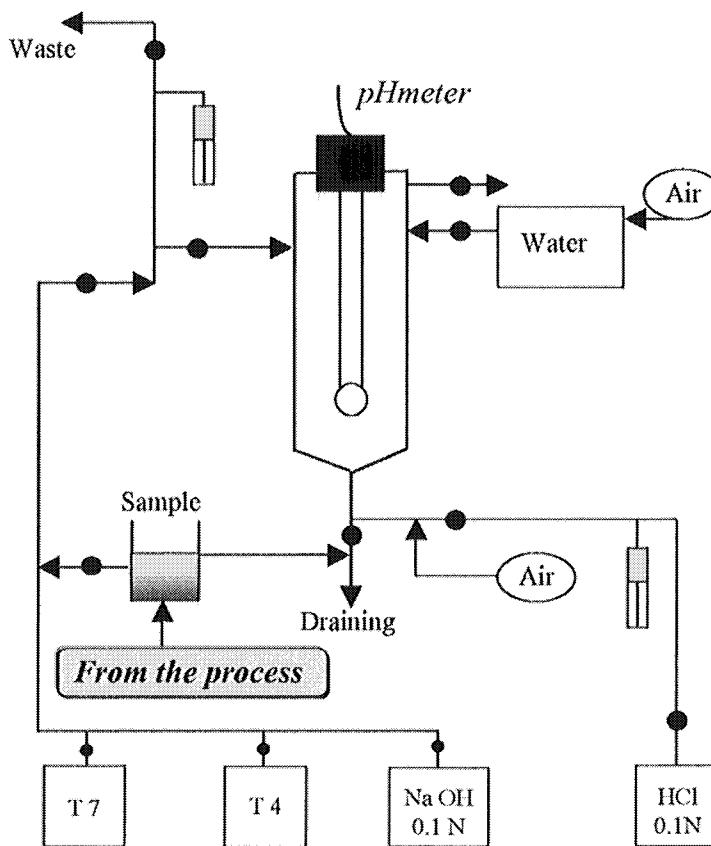


# *The Titrimetric Sensor*



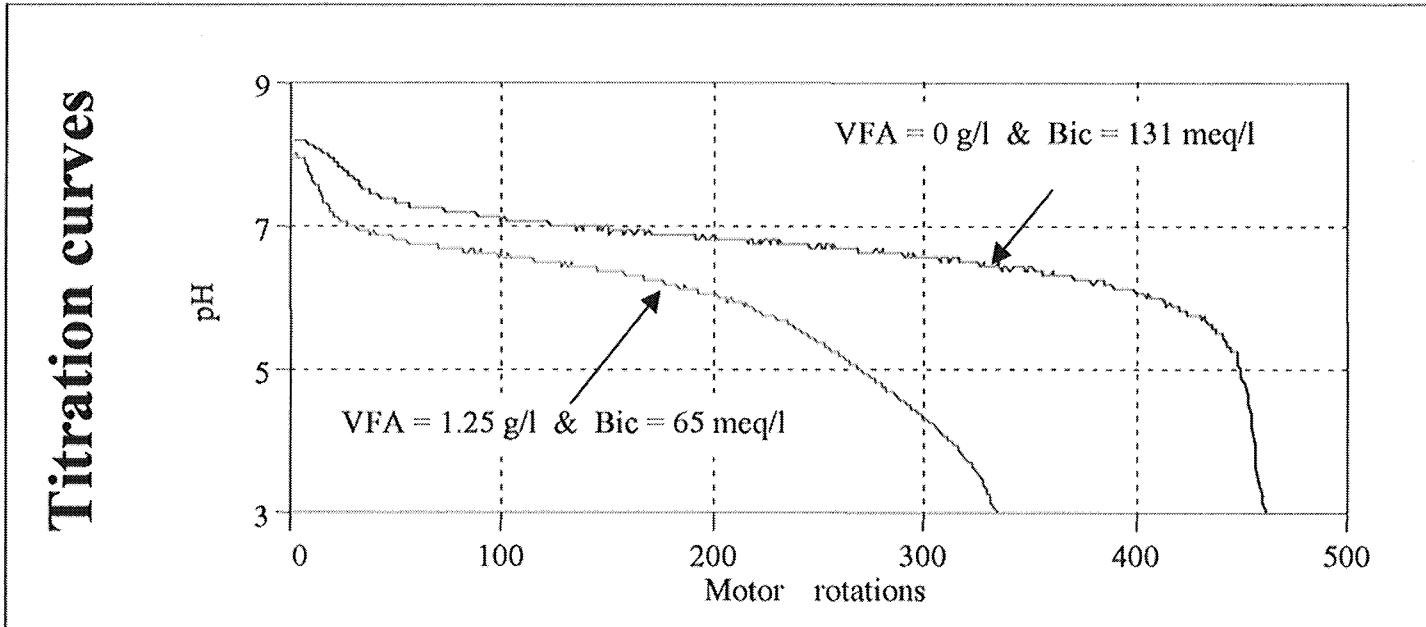
## Sensor for On-Line Automated Titration

- ✓ Measurements of Partial and Total Alkalinity,
- ✓ Estimations of Bic and VFA concentrations

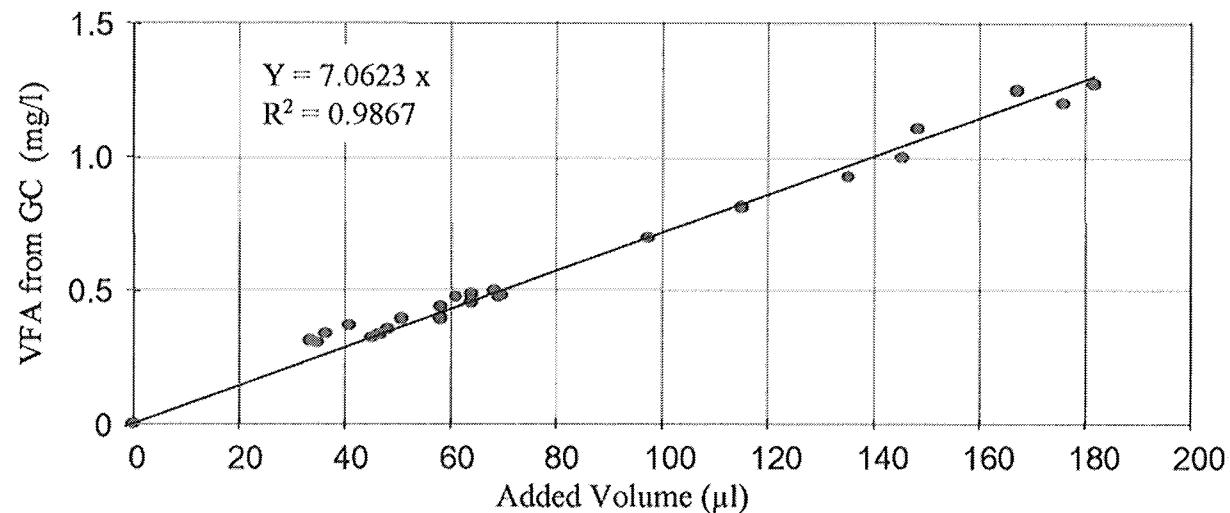


# *The Titrimetric Sensor*

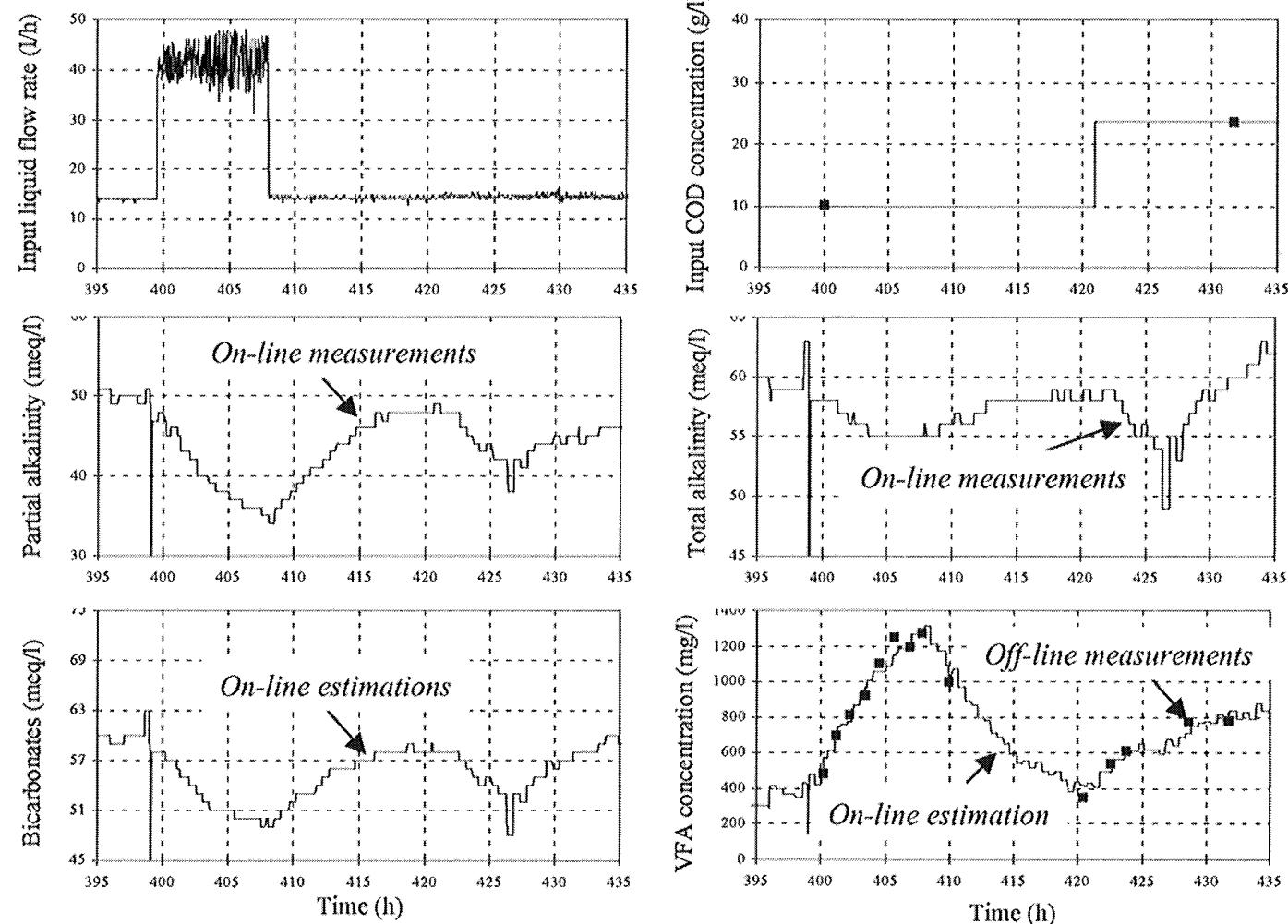
## Titration curves



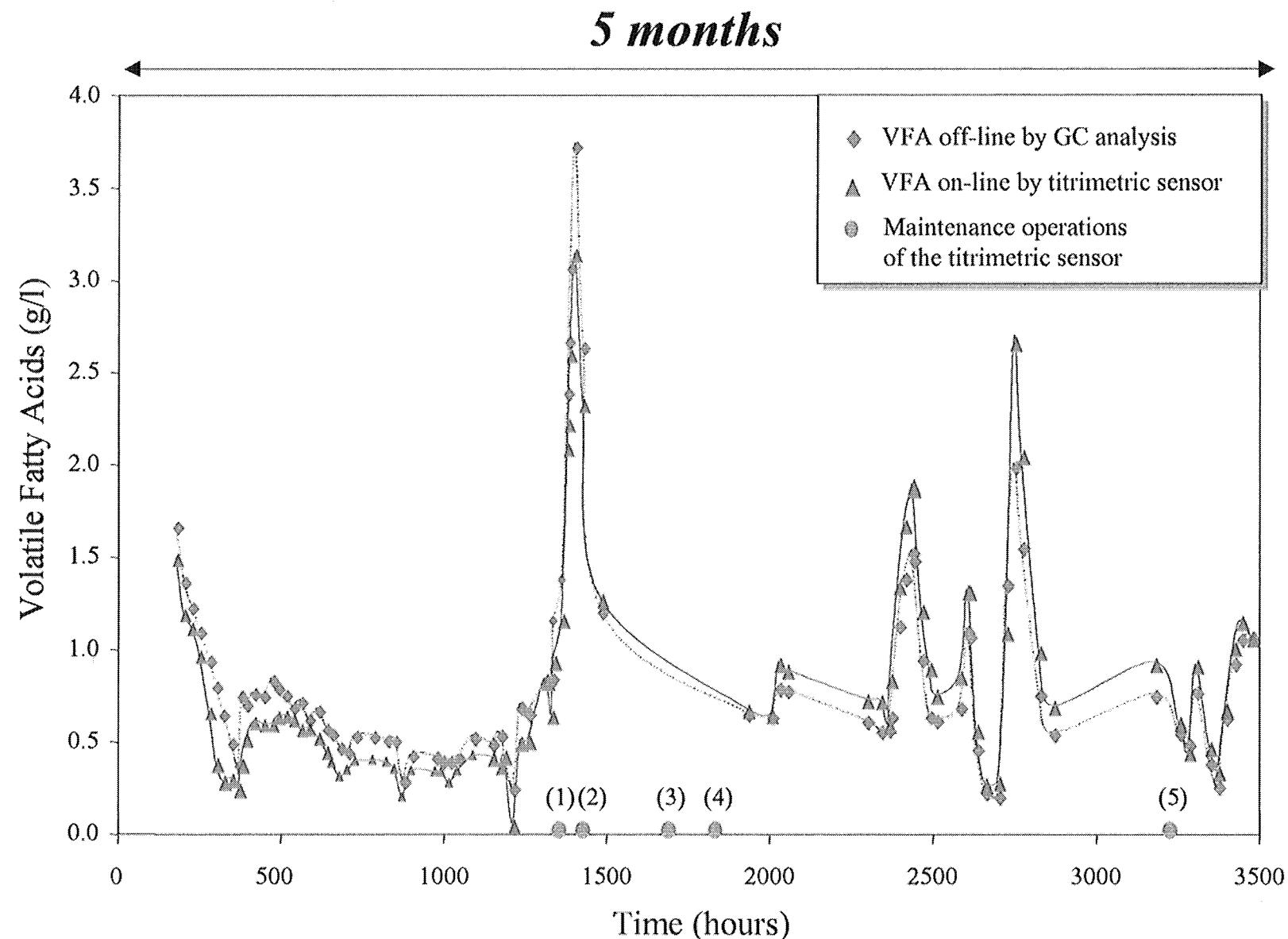
## Sensor Validation



# *Titrimetric Sensor : On-line Results*

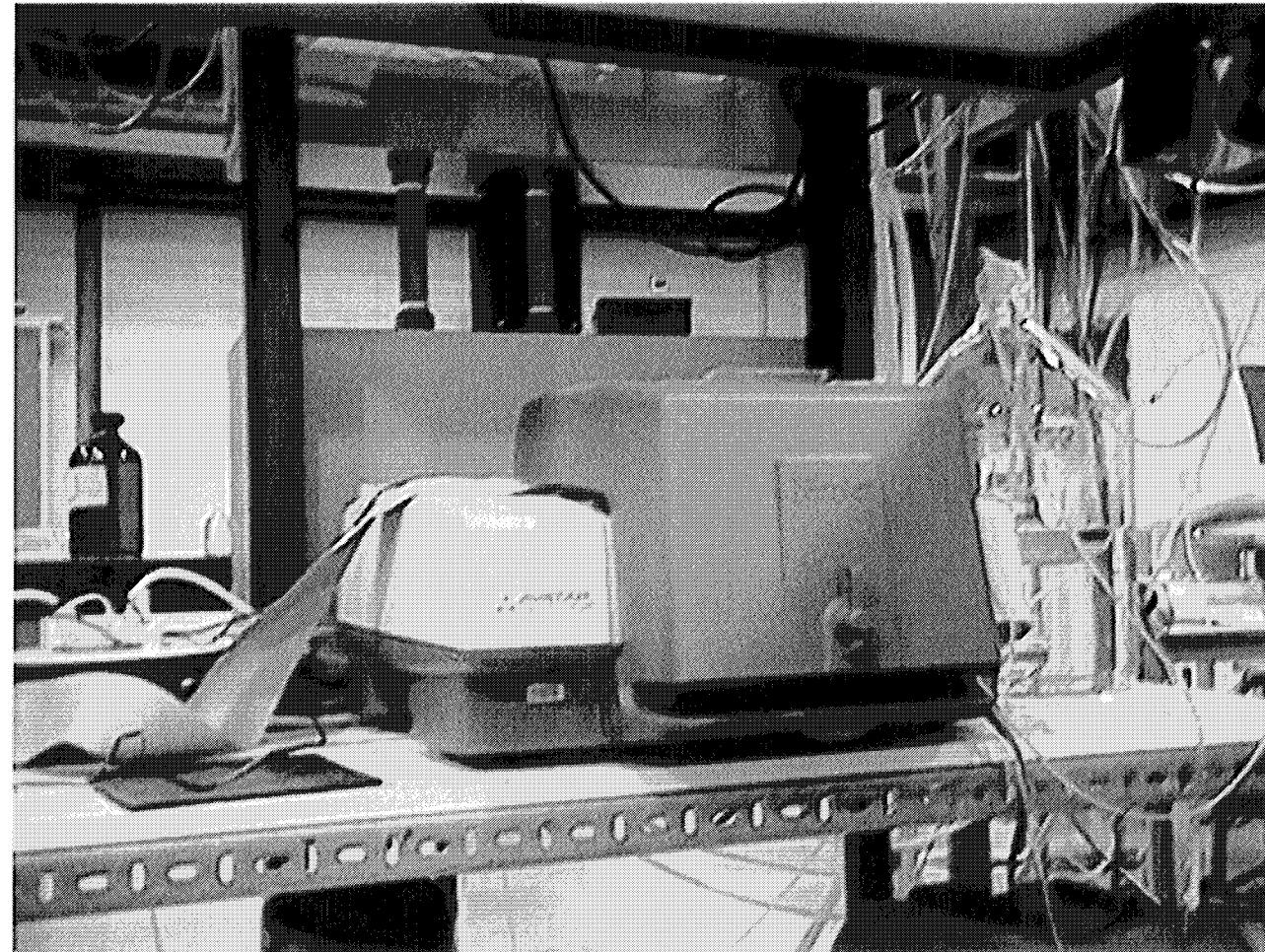


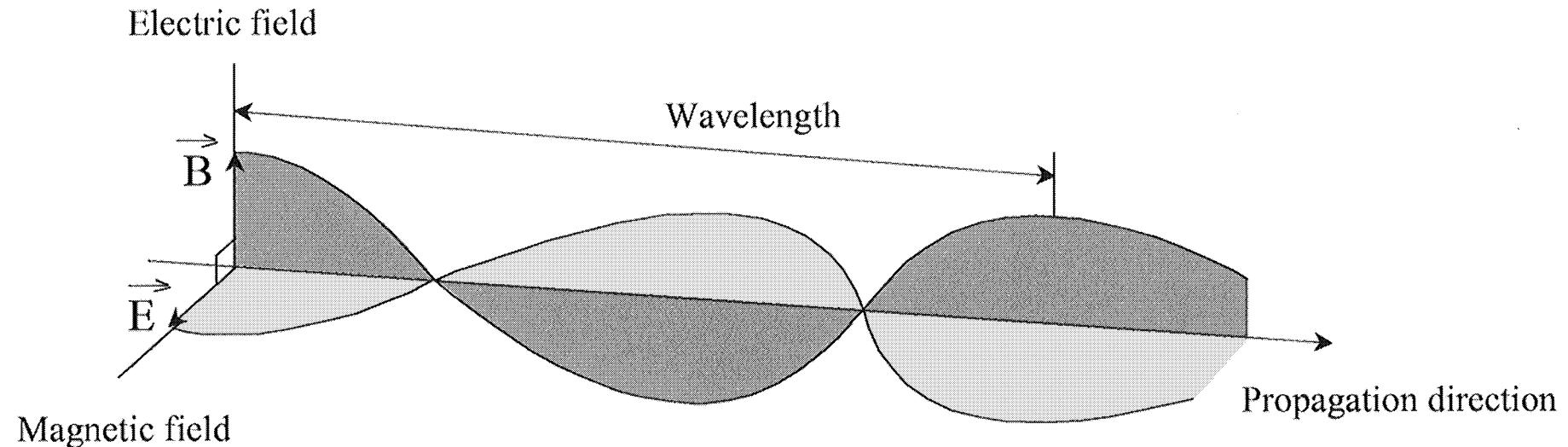
# Titrimetric Sensor : On-line Results



# *The Mid InfraRed Spectrometer*

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Wavelength :  $\lambda$  ( $\mu\text{m} = 10^{-6} \text{ m}$ ,  $\text{nm} = 10^{-9} \text{ m}$ )

Wavenumber :  $v = 1/\lambda$  ( $\text{cm}^{-1}$ )

Frequency :  $f = C/\lambda$  ( $\text{s}^{-1}$ )

Propagation speed in vacuum :  $C = 3 \cdot 10^8$  ( $\text{m.s}^{-1}$ )

*Each electromagnetic wave conveys energy*

If the wave has a frequency  $f$ ,  
it is associated to an energy quantum  $E$

$$E = h \cdot f = h \cdot C / \lambda$$

With  $h$  : Planck constant ( $6.62 \cdot 10^{-34}$  J.s)

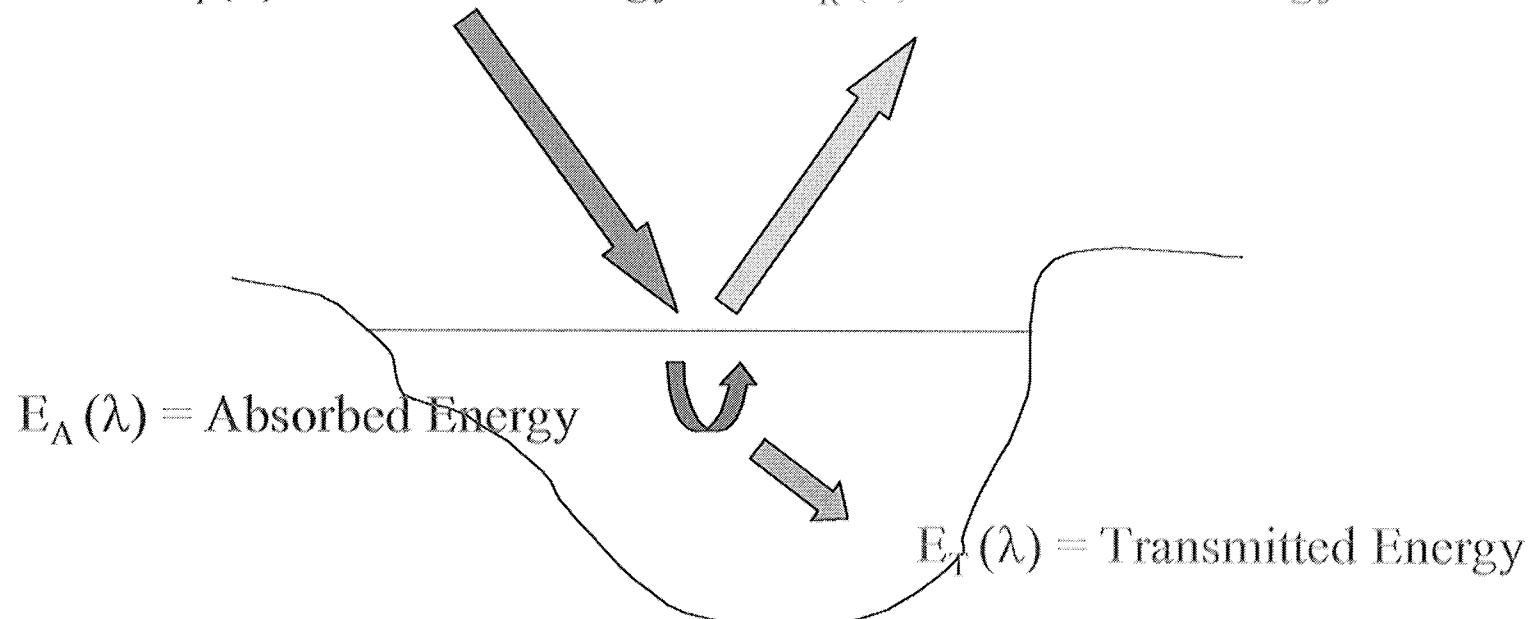
$E$  : energy quantum in J

$f$  : frequency in Hz

## Energy conservation principle

$E_I(\lambda)$  = Incident Energy

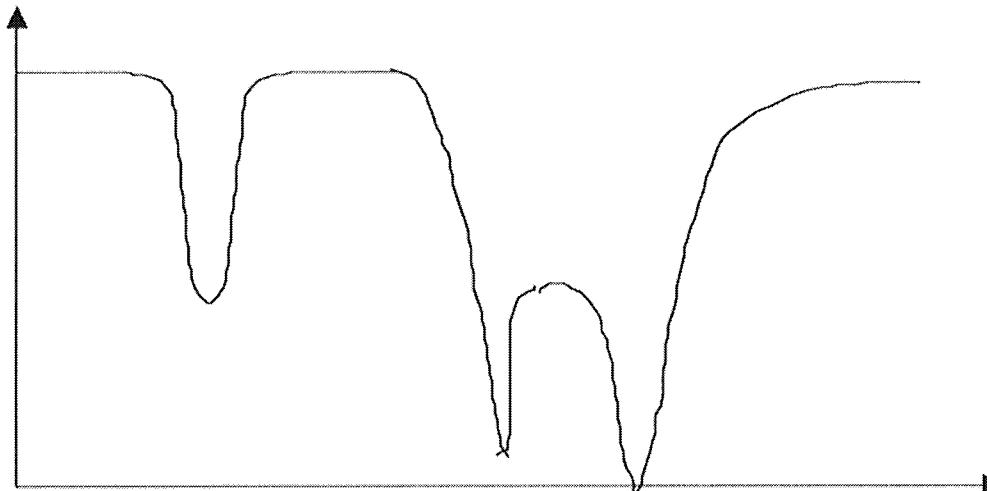
$E_R(\lambda)$  = Reflected Energy



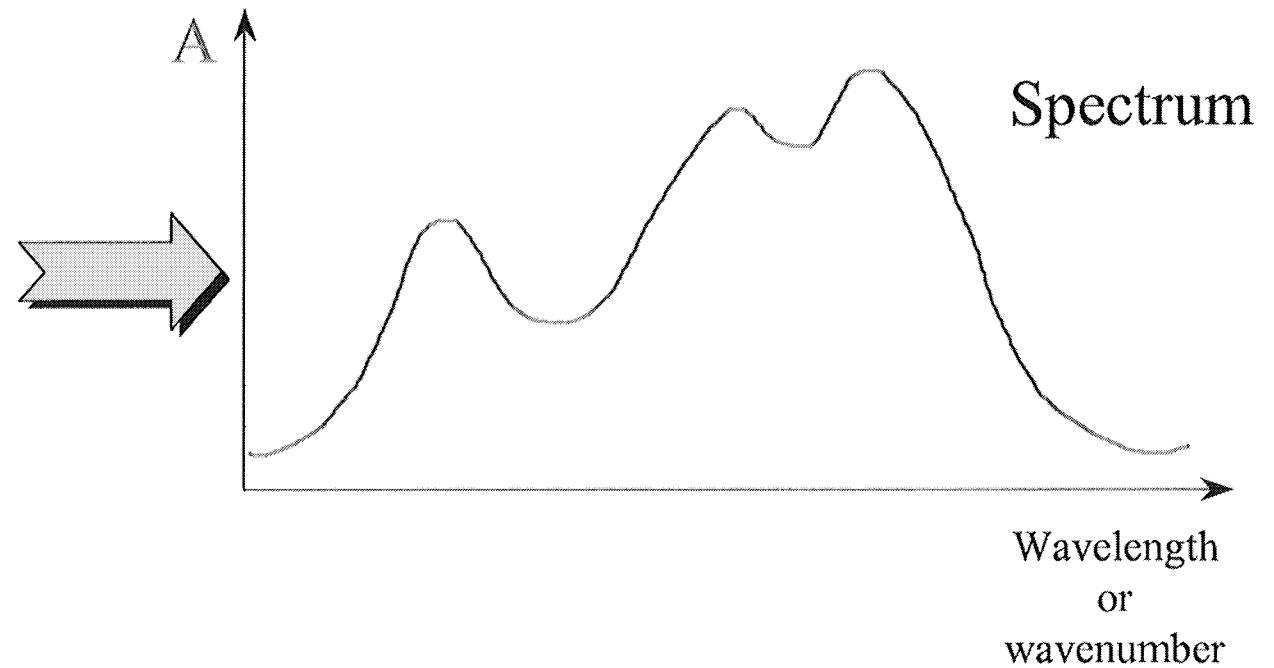
Incident Energy = Reflected Energy + Absorbed Energy + Transmitted Energy

$$E_I(\lambda) = E_R(\lambda) + E_A(\lambda) + E_T(\lambda)$$

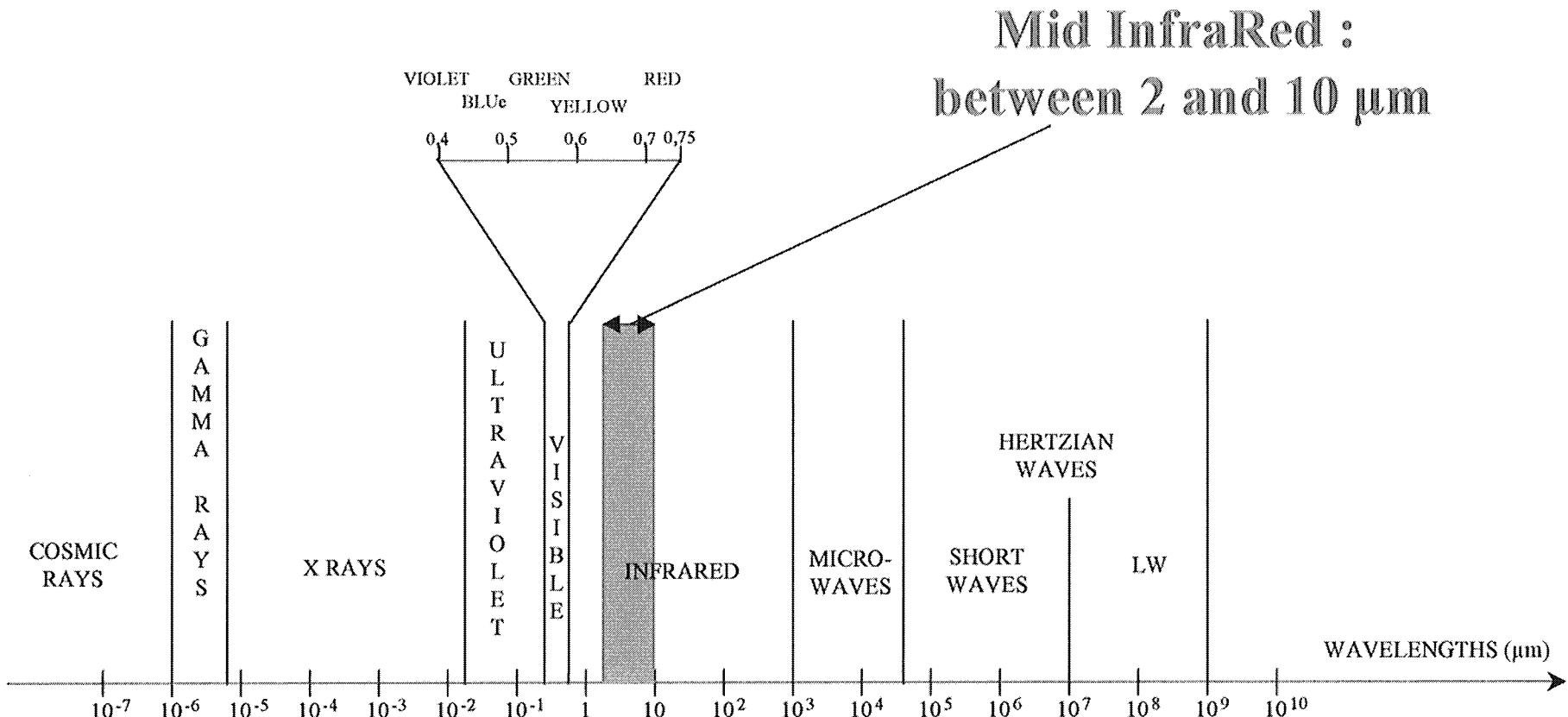
Er (reflected)  
or  
Et (transmitted)



Transmission  
 $A = \log(E_T/E_0)$

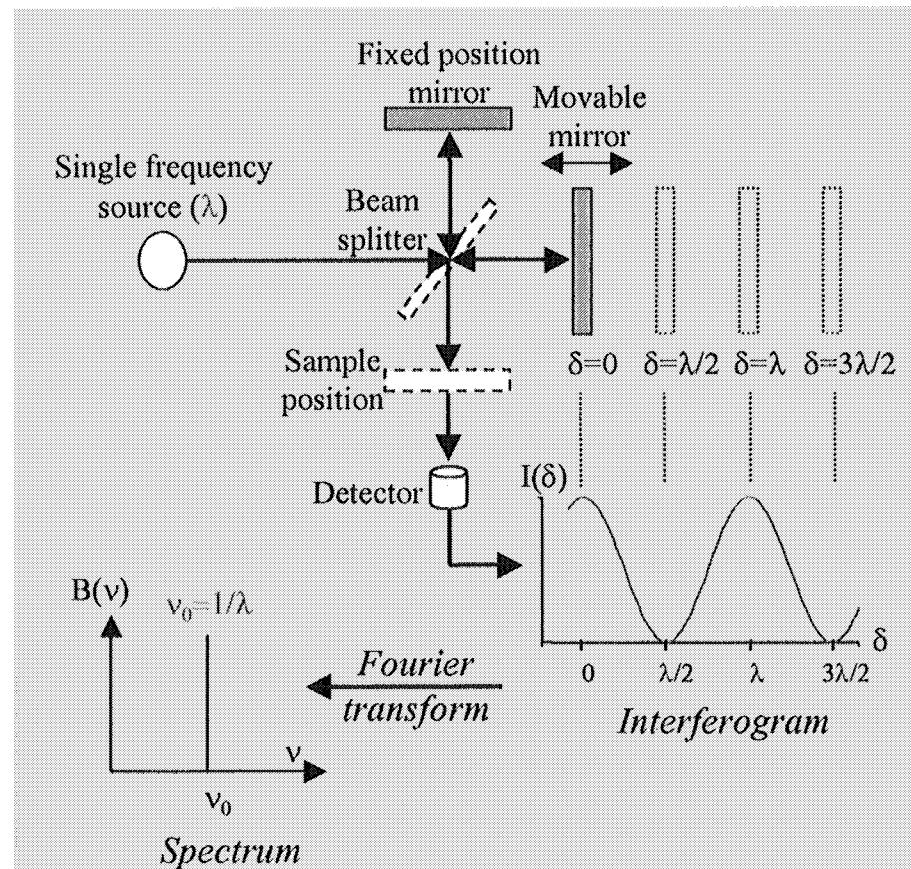
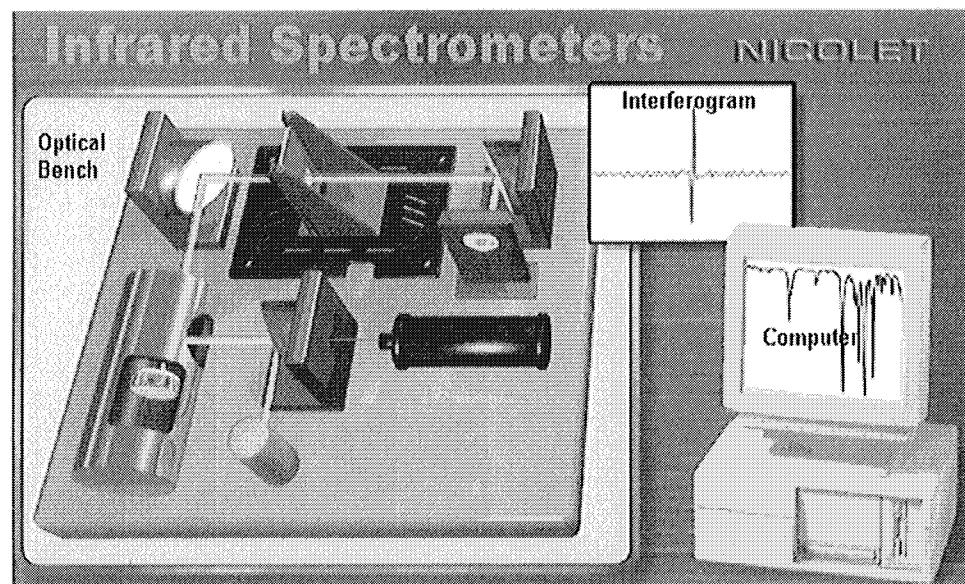


# *Wavelength in the Mid InfraRed*



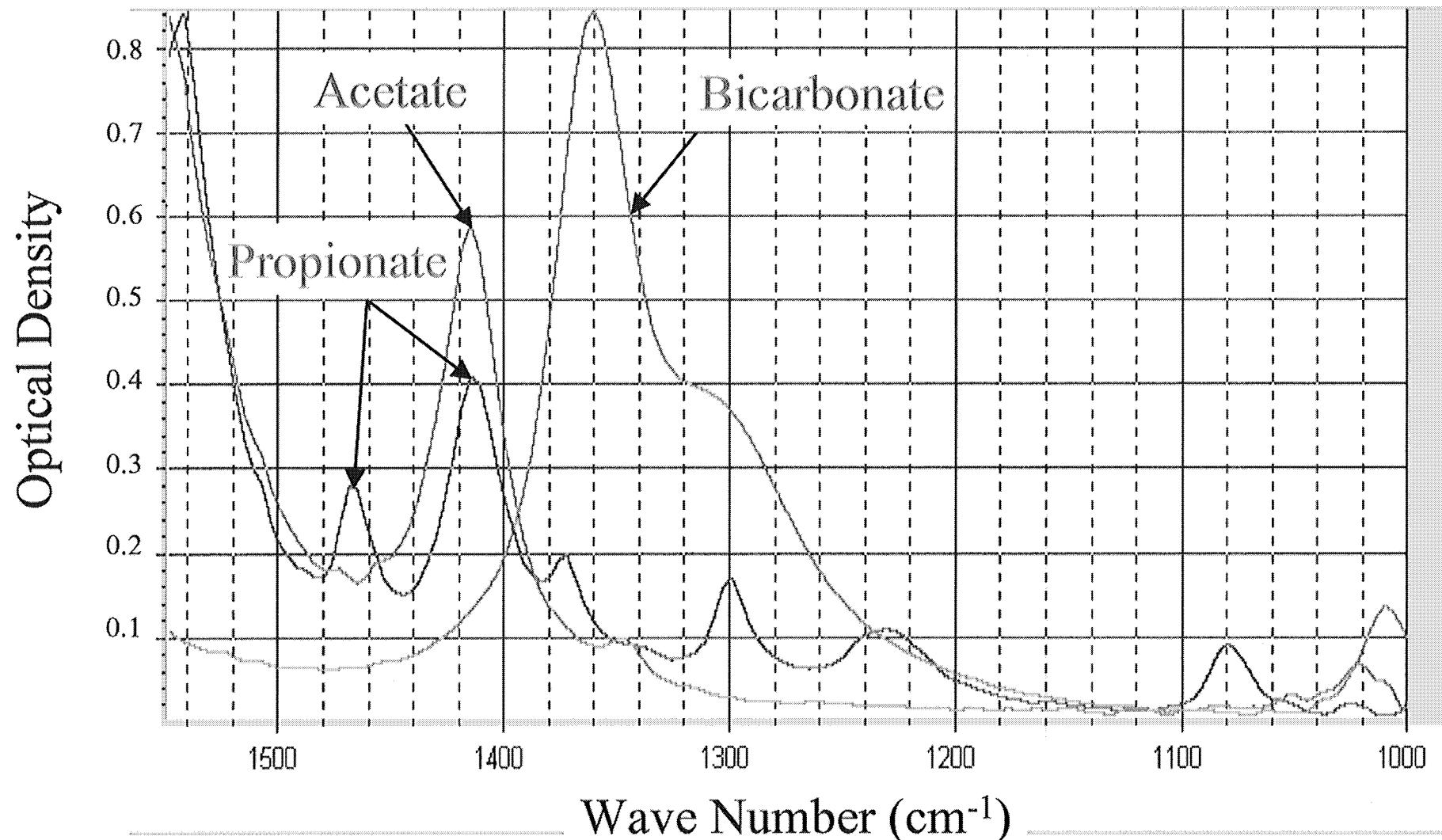
# *Principle of FT-IR Spectrometry*

*First interferometer :*  
*Michelson (1891)*

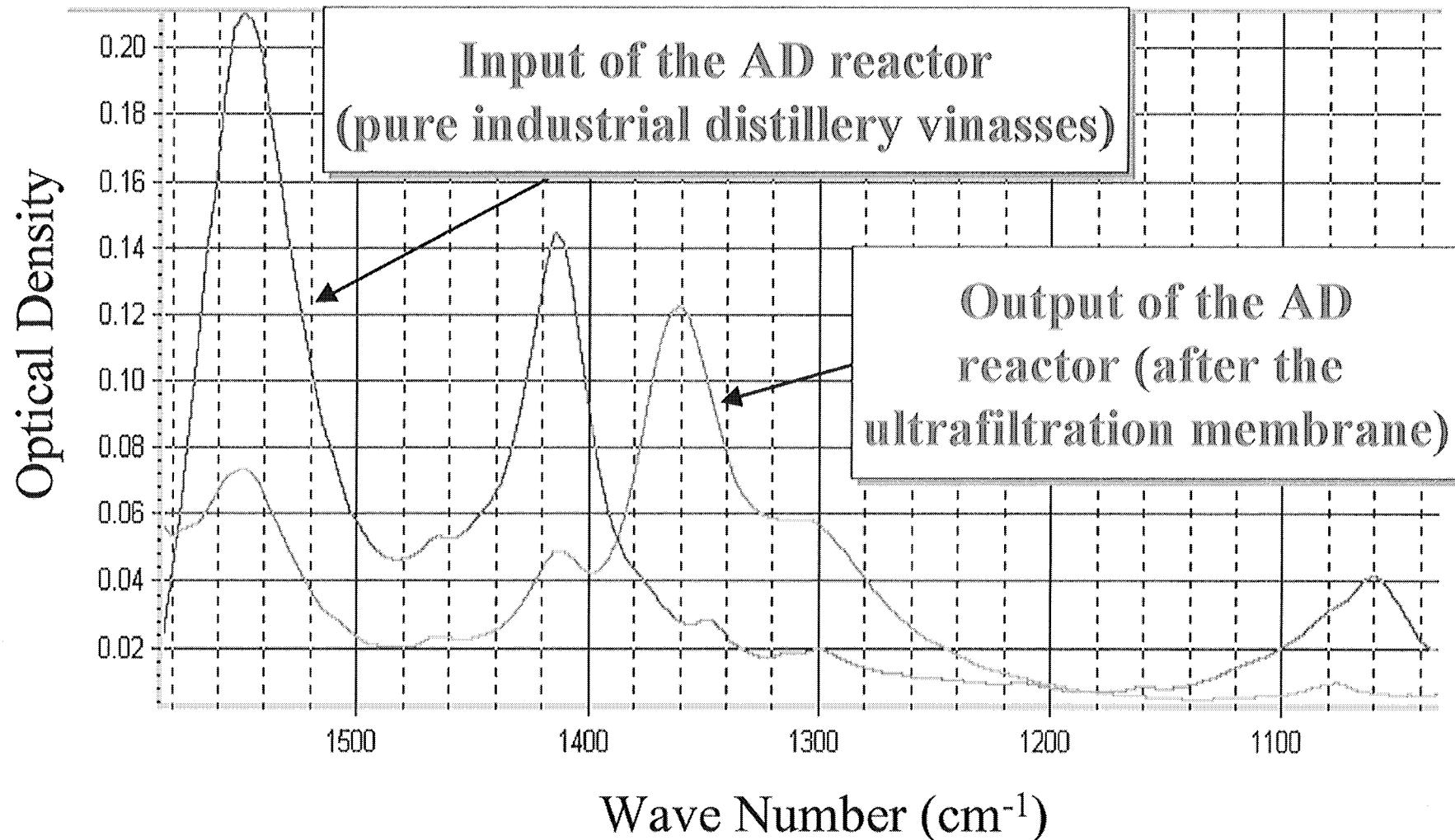


*FT-IR :*  
*Fourier Transform*  
*Infra Red*

# Spectra of Pure Samples

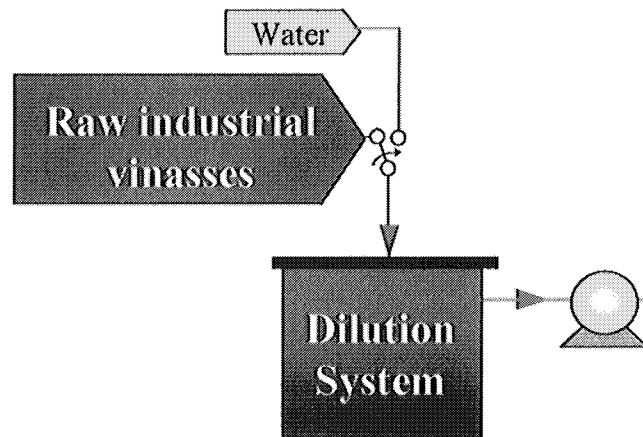


# Spectra of Complex Samples

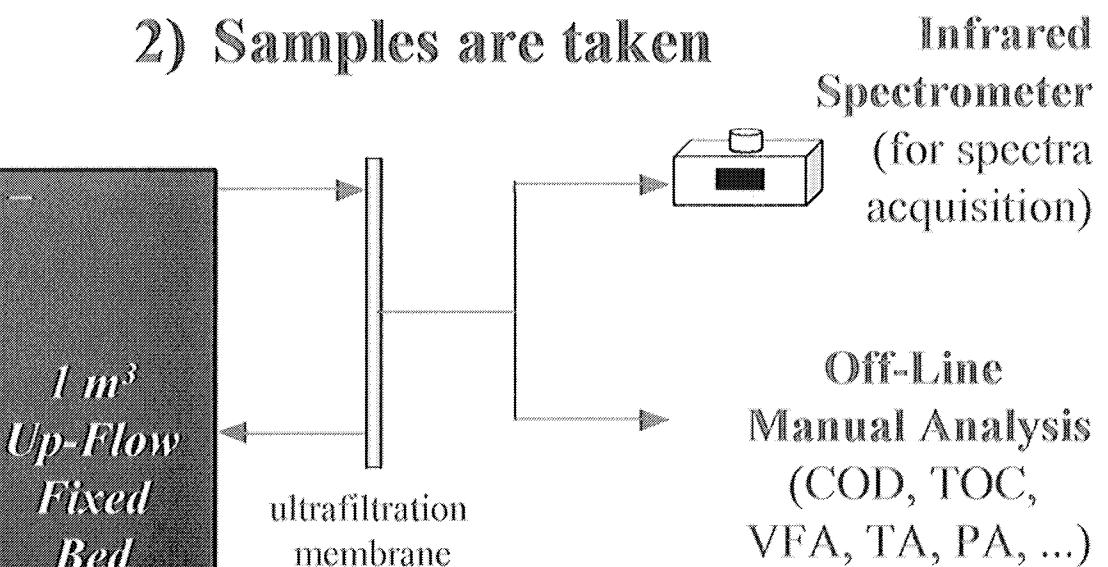


# *Calibration Principle*

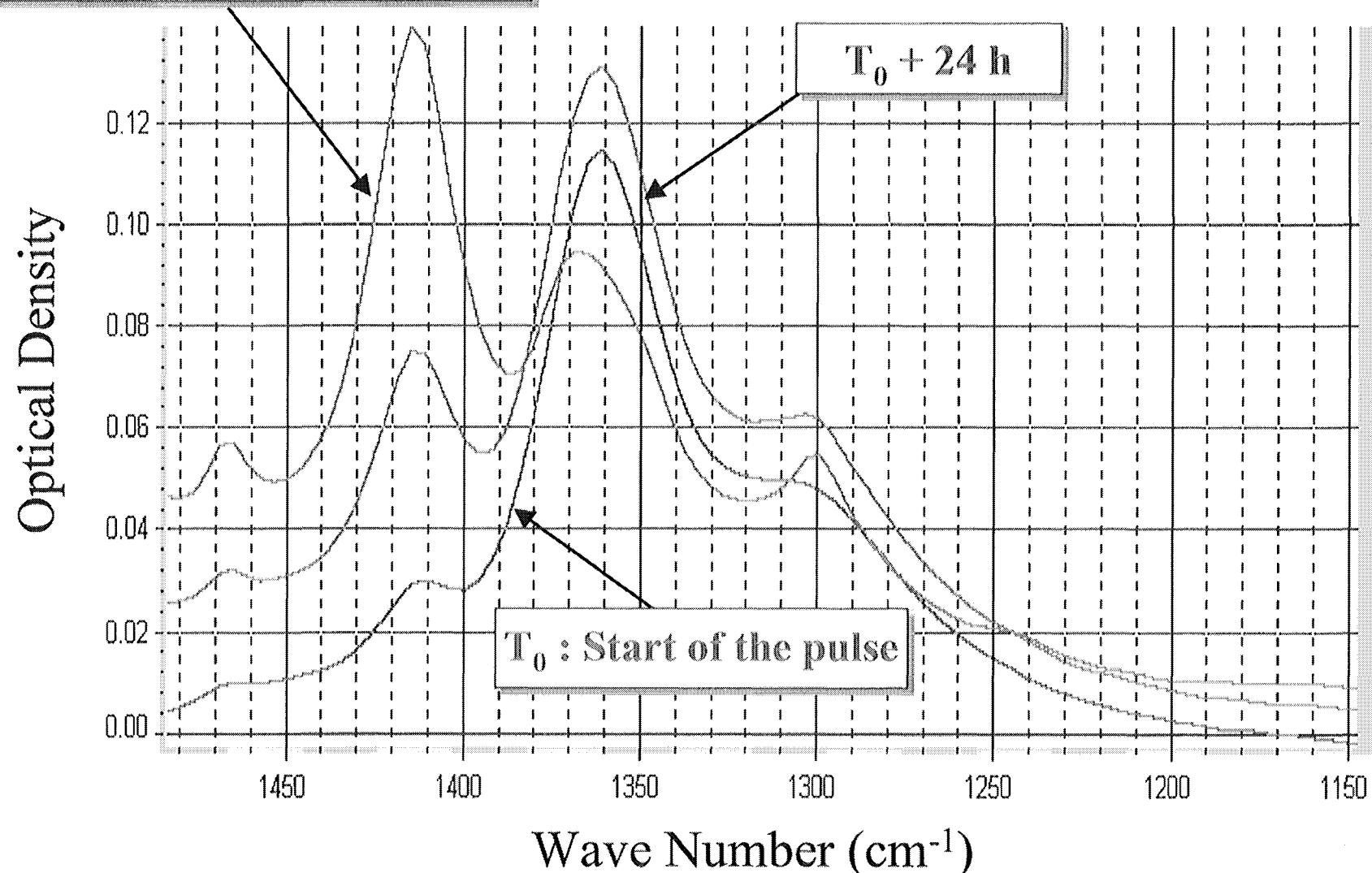
1) Change of the  
organic loading rate  
(*i.e.*, input flow rate or  
input concentration)



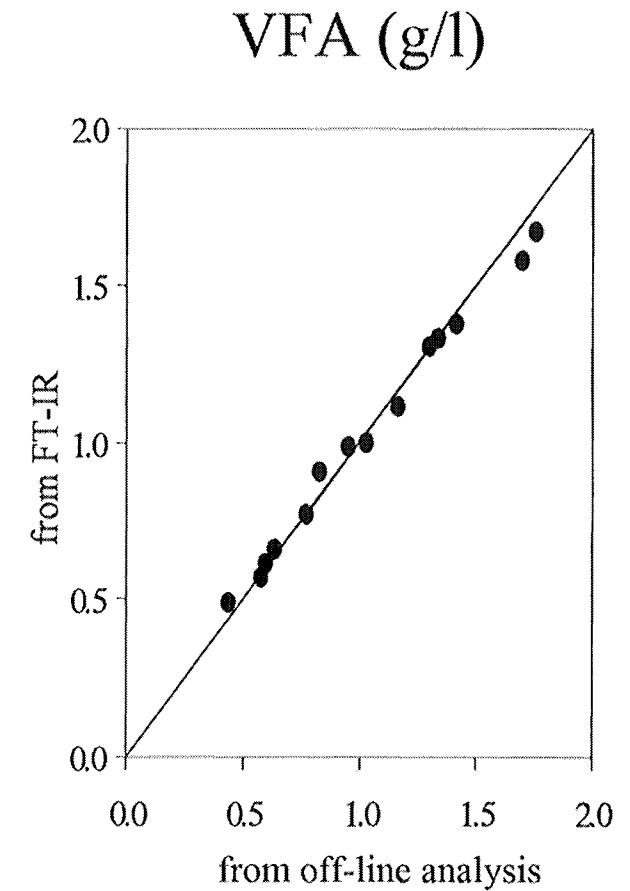
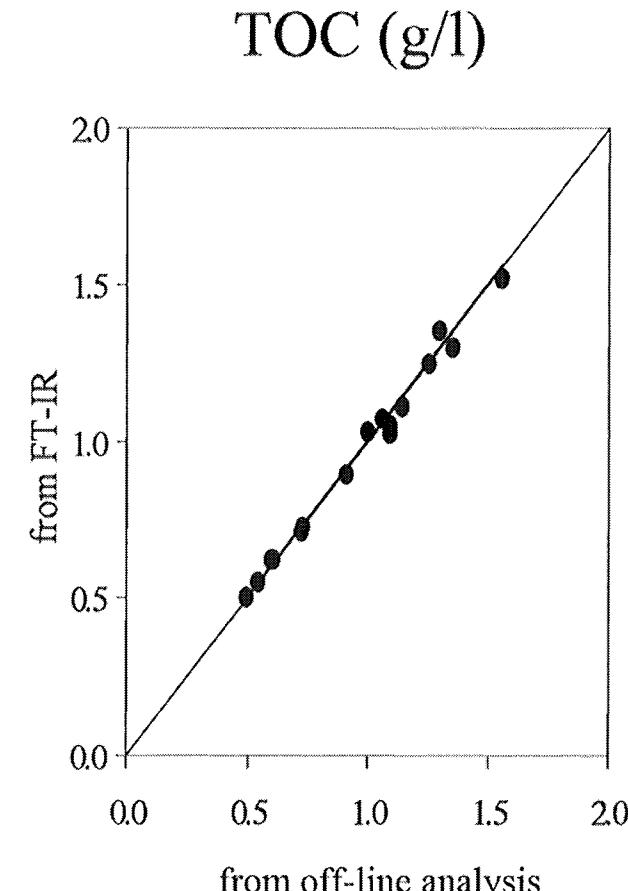
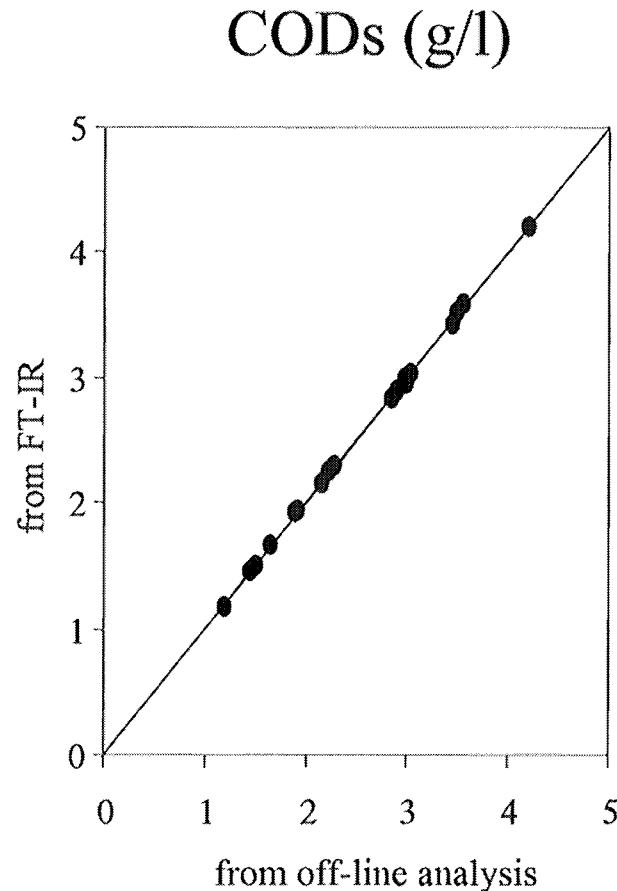
2) Samples are taken



3) Calibration by statistical analysis (PLS) of the results

*Spectra Evolution during a Pulse* $T_0 + 36\text{ h}$  : End of the Pulse

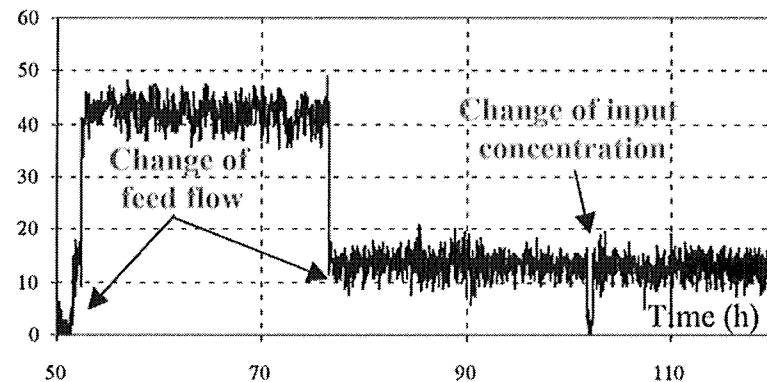
# Calibration Results



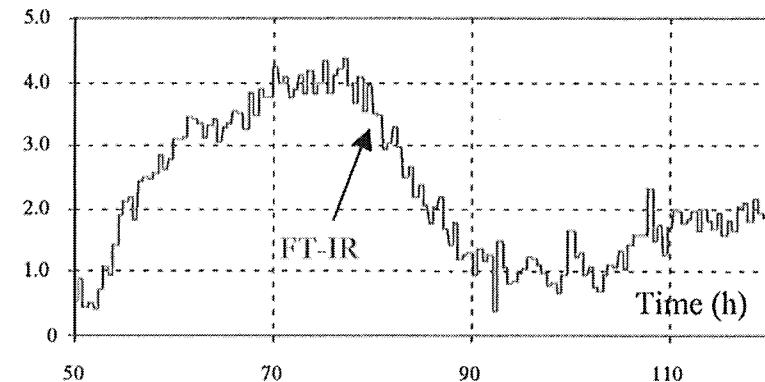
*Similar results on partial and total alkalinity*

# *On-Line Results*

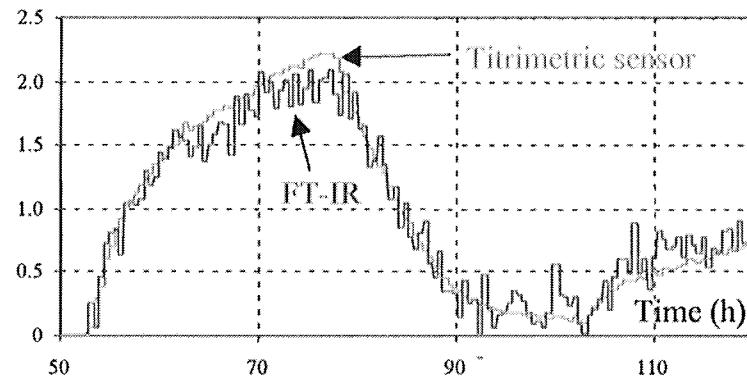
*Influent flow rate (l/h)*



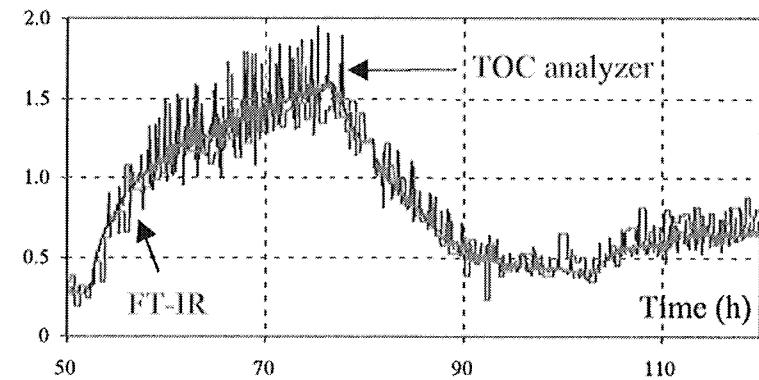
*Soluble Chemical Oxygen Demand (g/l)*



*Volatile Fatty Acids (g/l)*

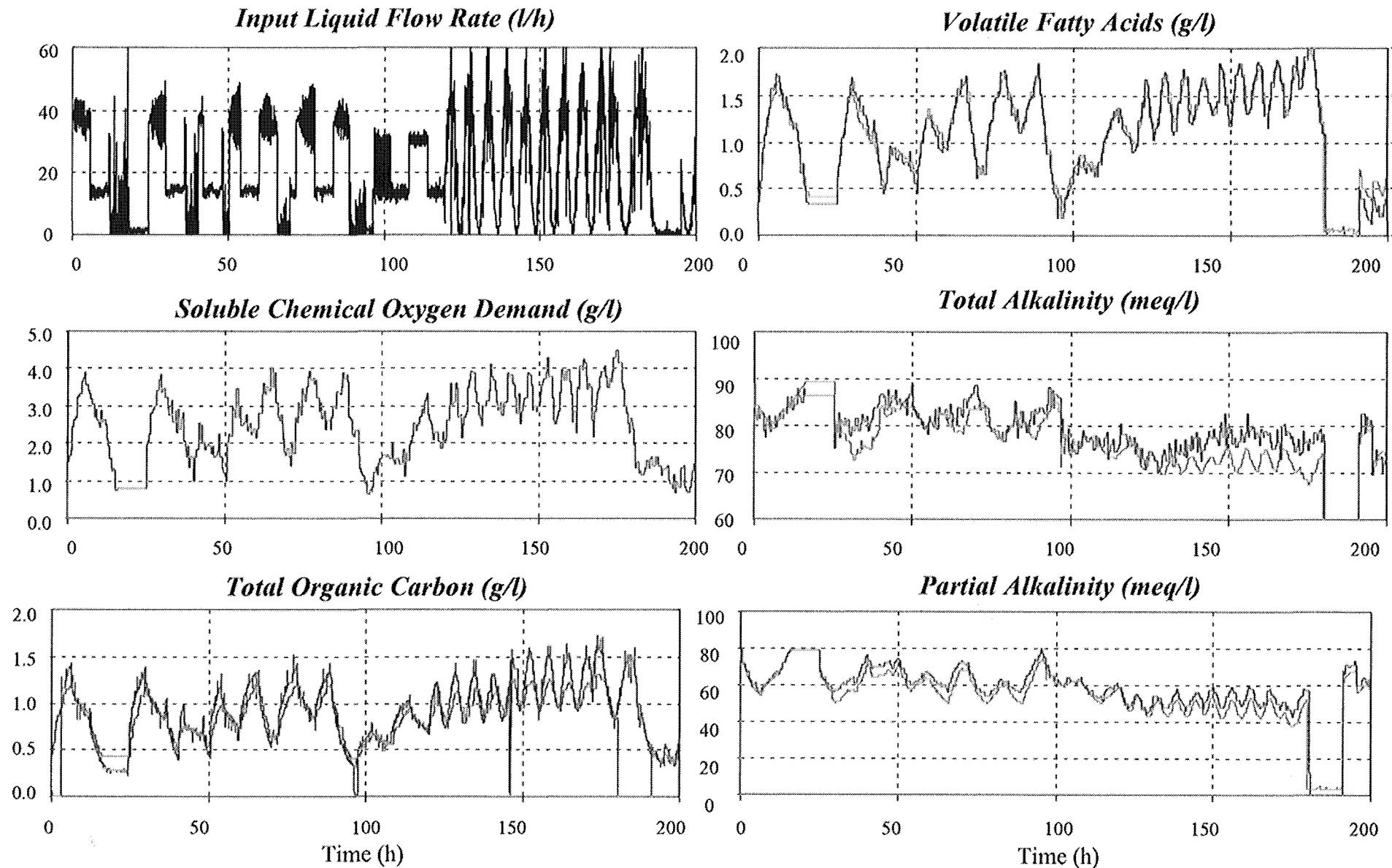


*Total Organic Carbon (g/l)*



*Similar results on partial and total alkalinity*

# *One Year Later (i.e., after many changes of vinasses)*



# *Contents of the Presentation*

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*1) The anaerobic digestion process*

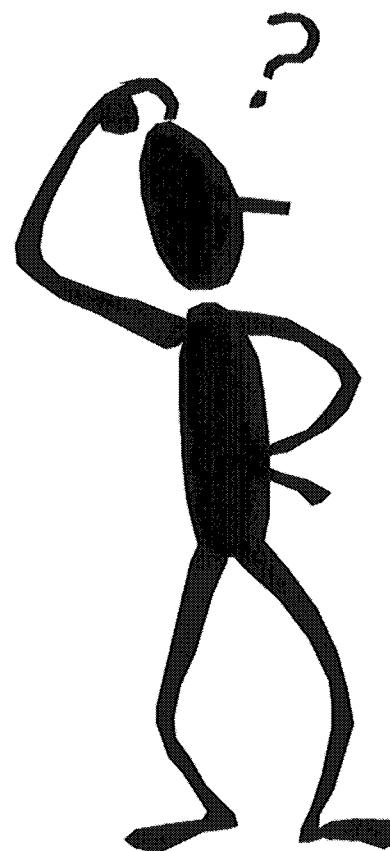
*2) Some examples of (off-line) sensors*

*3) Practical illustration of on-line sensors*

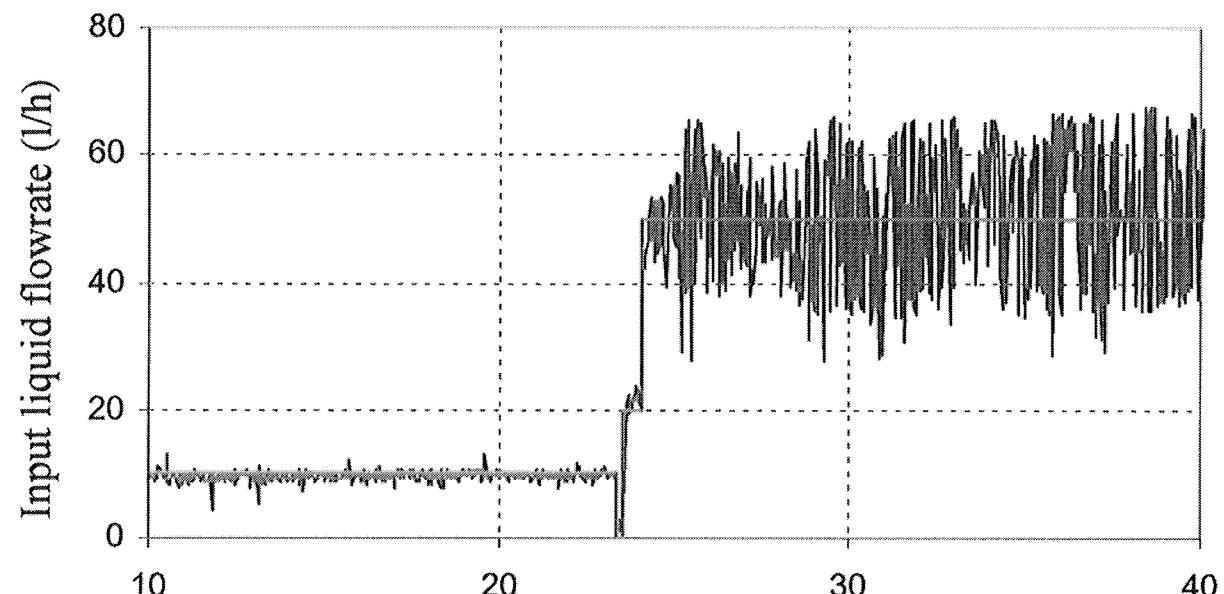


*4) Benefits from on-line instrumentation*

# *Benefits from fully instrumented process*

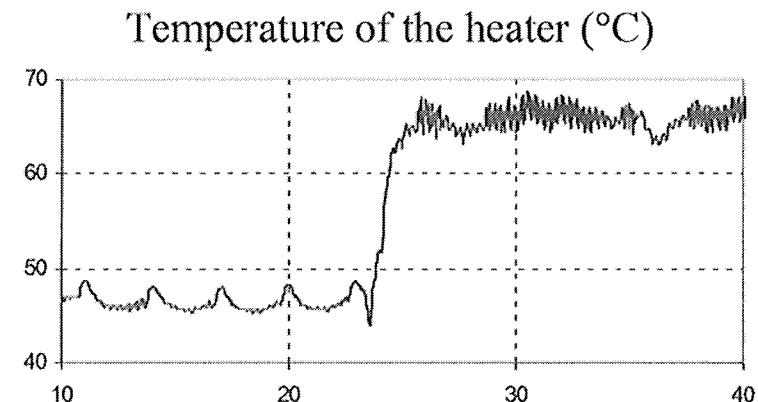
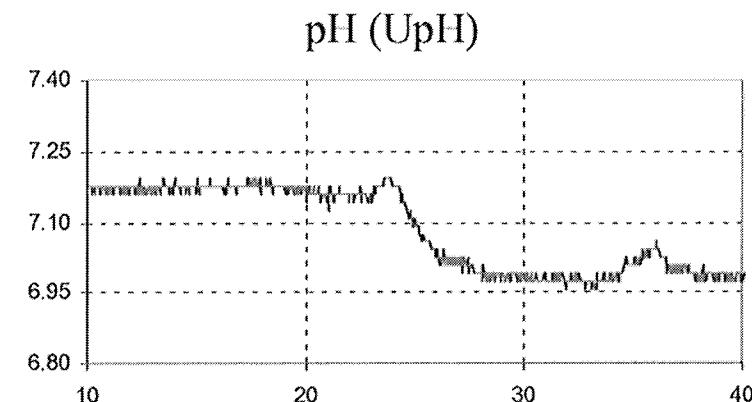
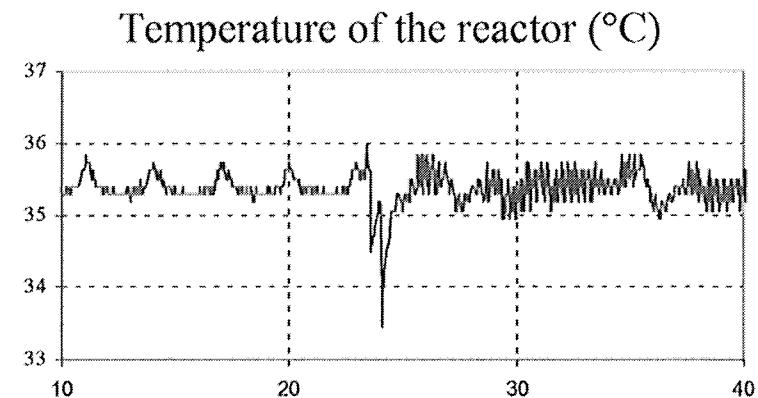
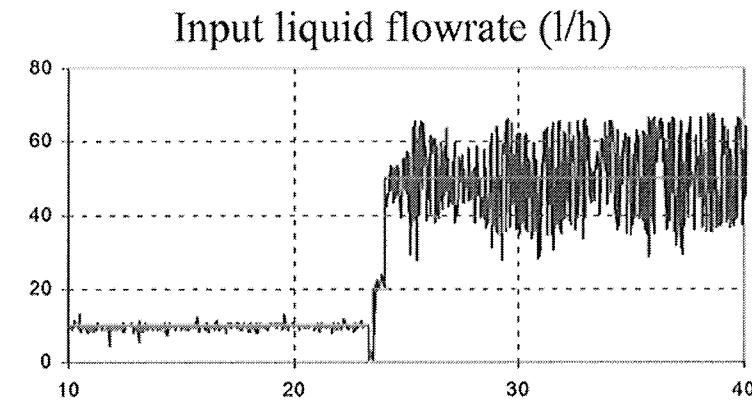
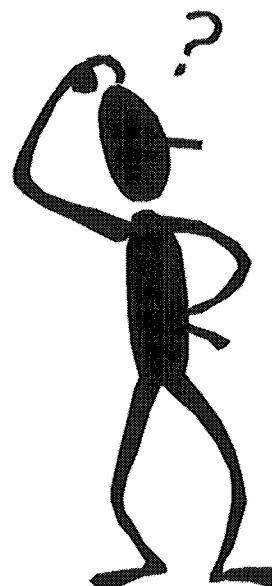


*What happens if the organic loading rate changes ?*



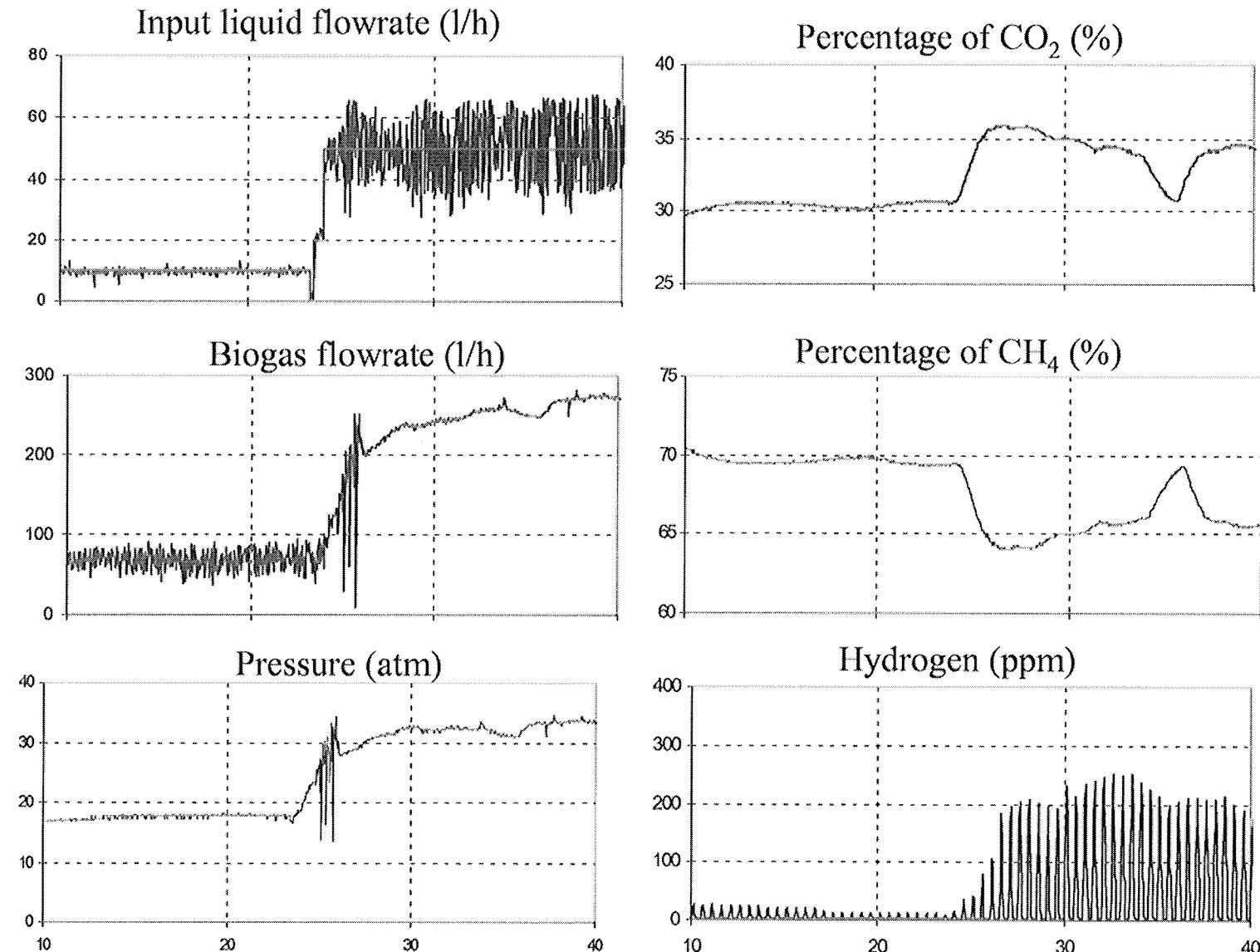
# *Benefits from fully instrumented process*

*From the classical measurements in the liquid phase*



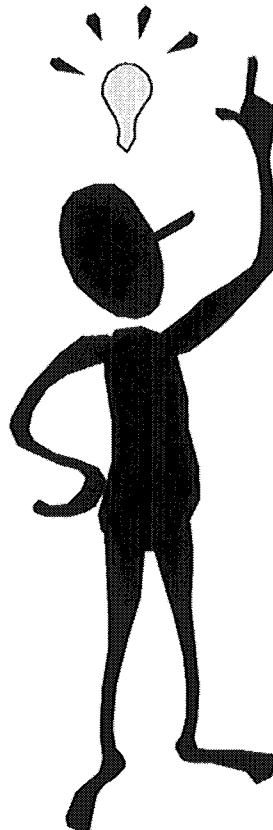
# *Benefits from fully instrumented process*

*From the more or less classical measurements in the gas phase*

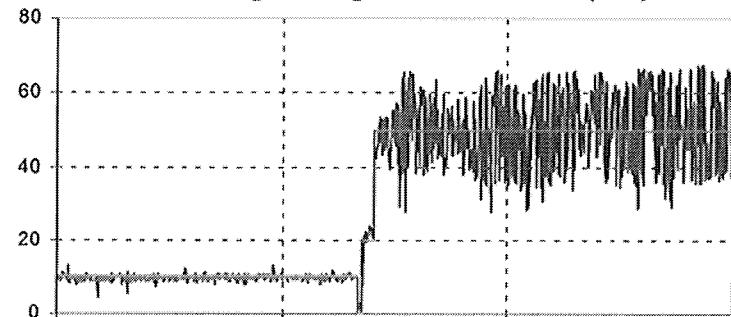


# *Benefits from fully instrumented process*

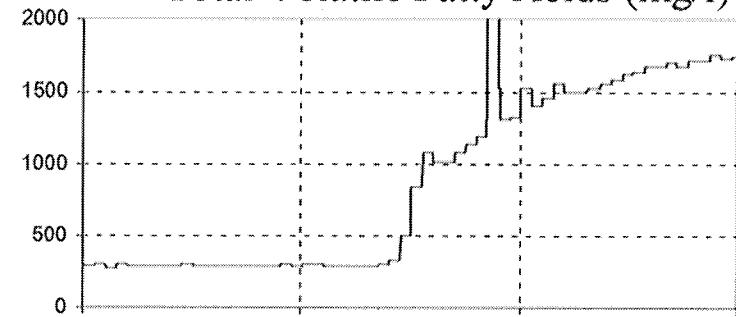
*From the non classical measurements in the liquid phase*



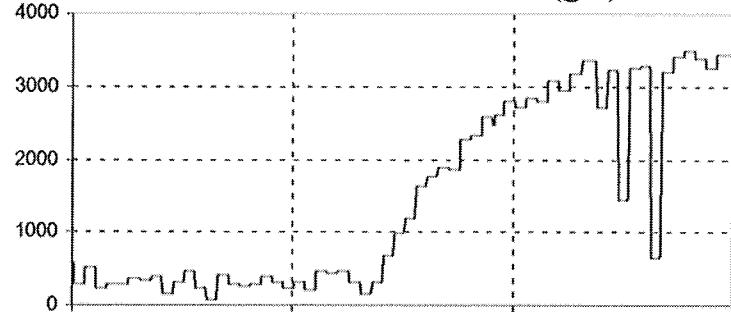
Input liquid flowrate (l/h)



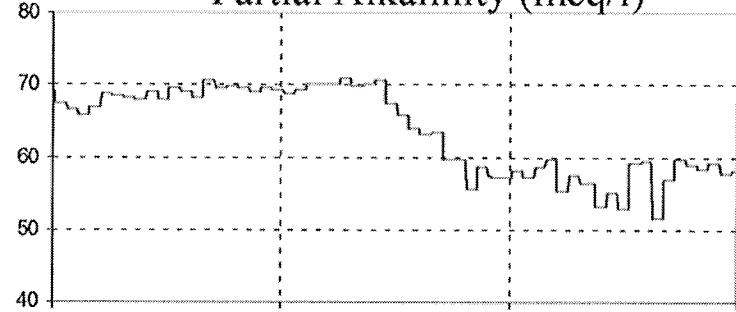
Total Volatile Fatty Acids (mg/l)



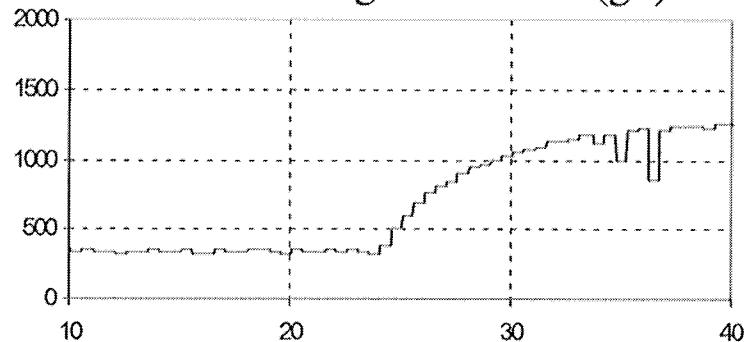
Soluble COD (g/l)



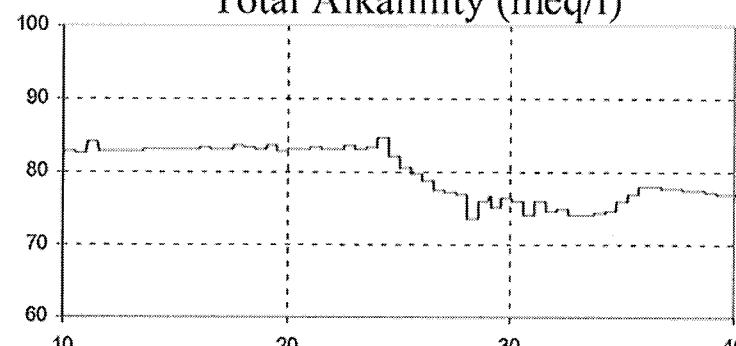
Partial Alkalinity (meq/l)



Total Organic Carbon (g/l)

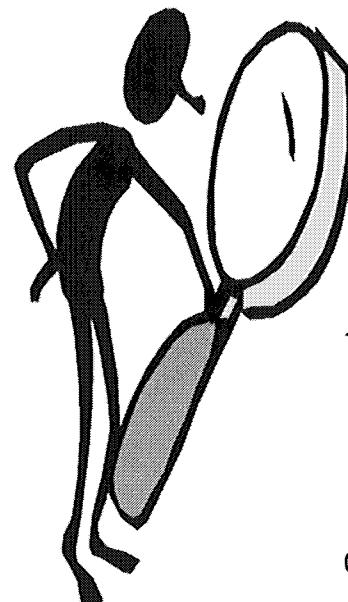


Total Alkalinity (meq/l)

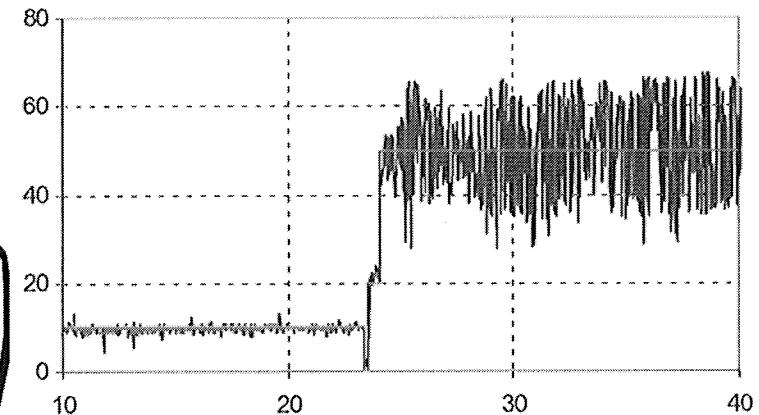


# *Benefits from fully instrumented process*

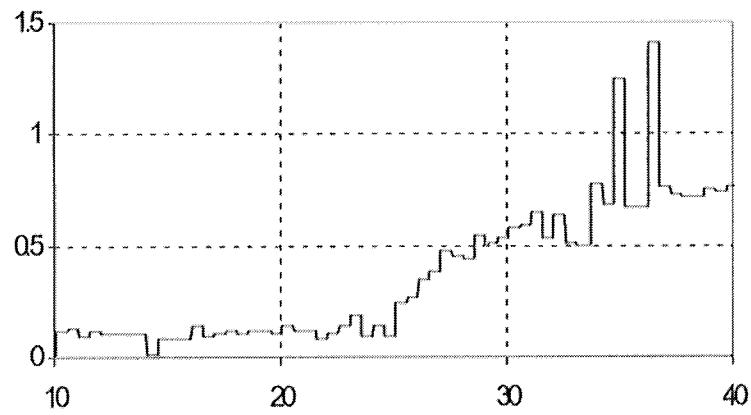
*We can even get closer !...*



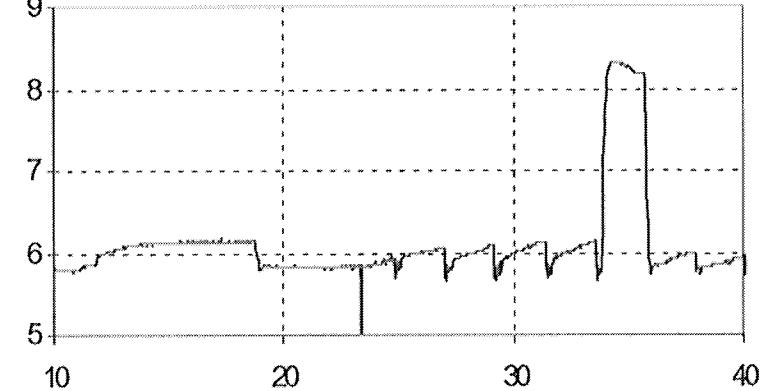
Input liquid flowrate (l/h)



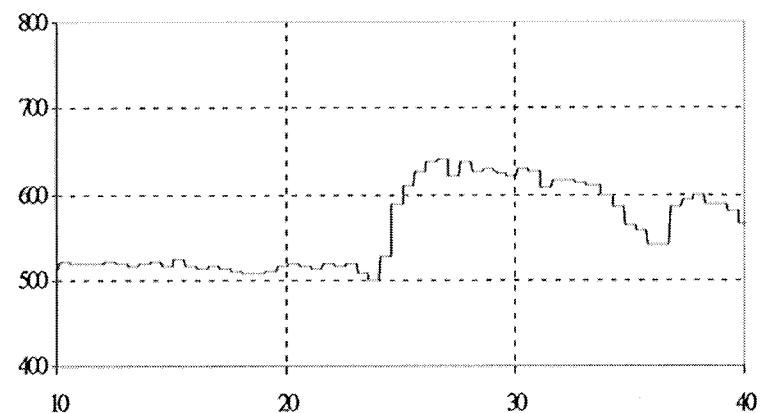
Specific Volatile Fatty Acids (g/l)



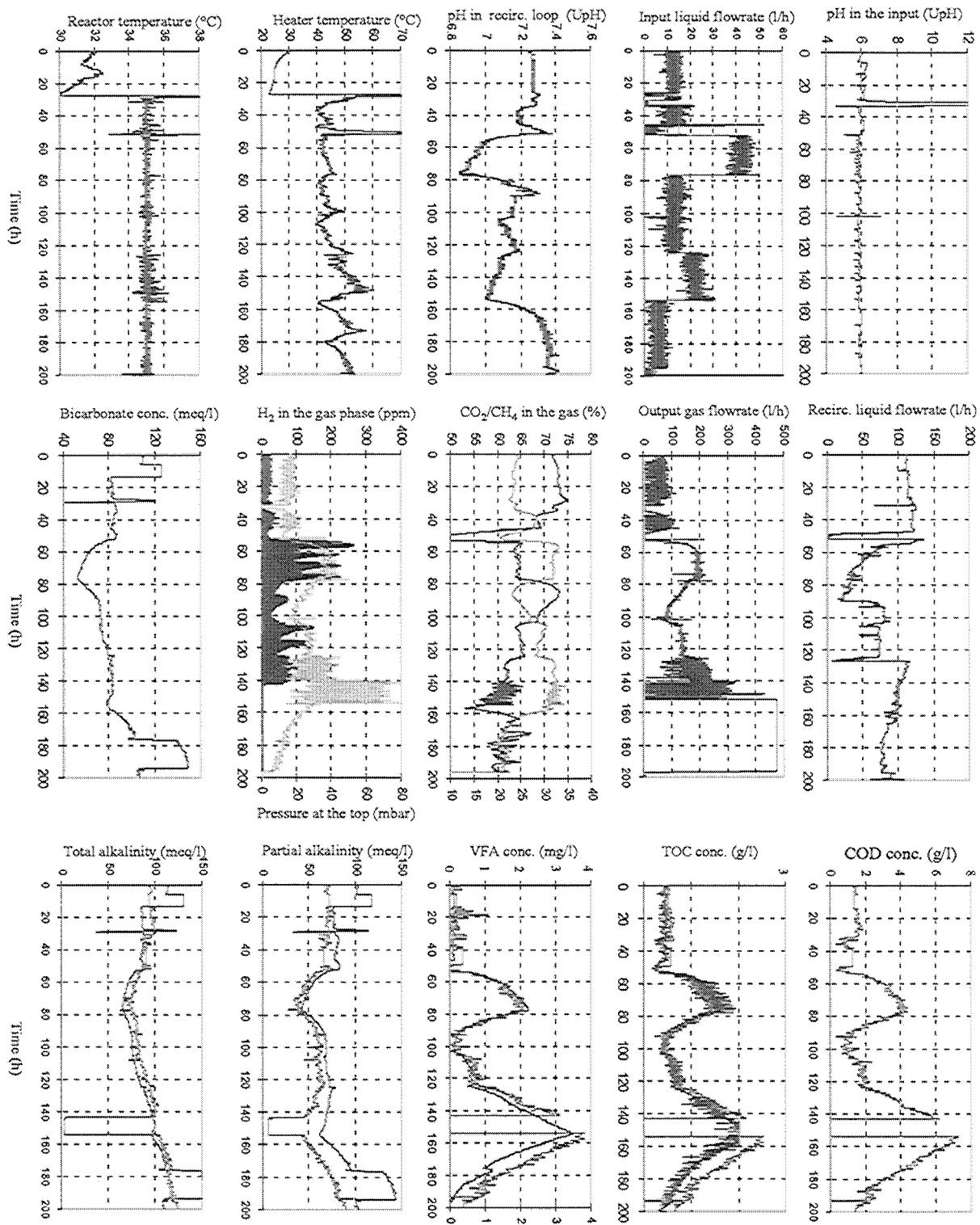
pH in the input (UpH)



Dissolved CO<sub>2</sub>



# *Benefits from fully instrumented process*



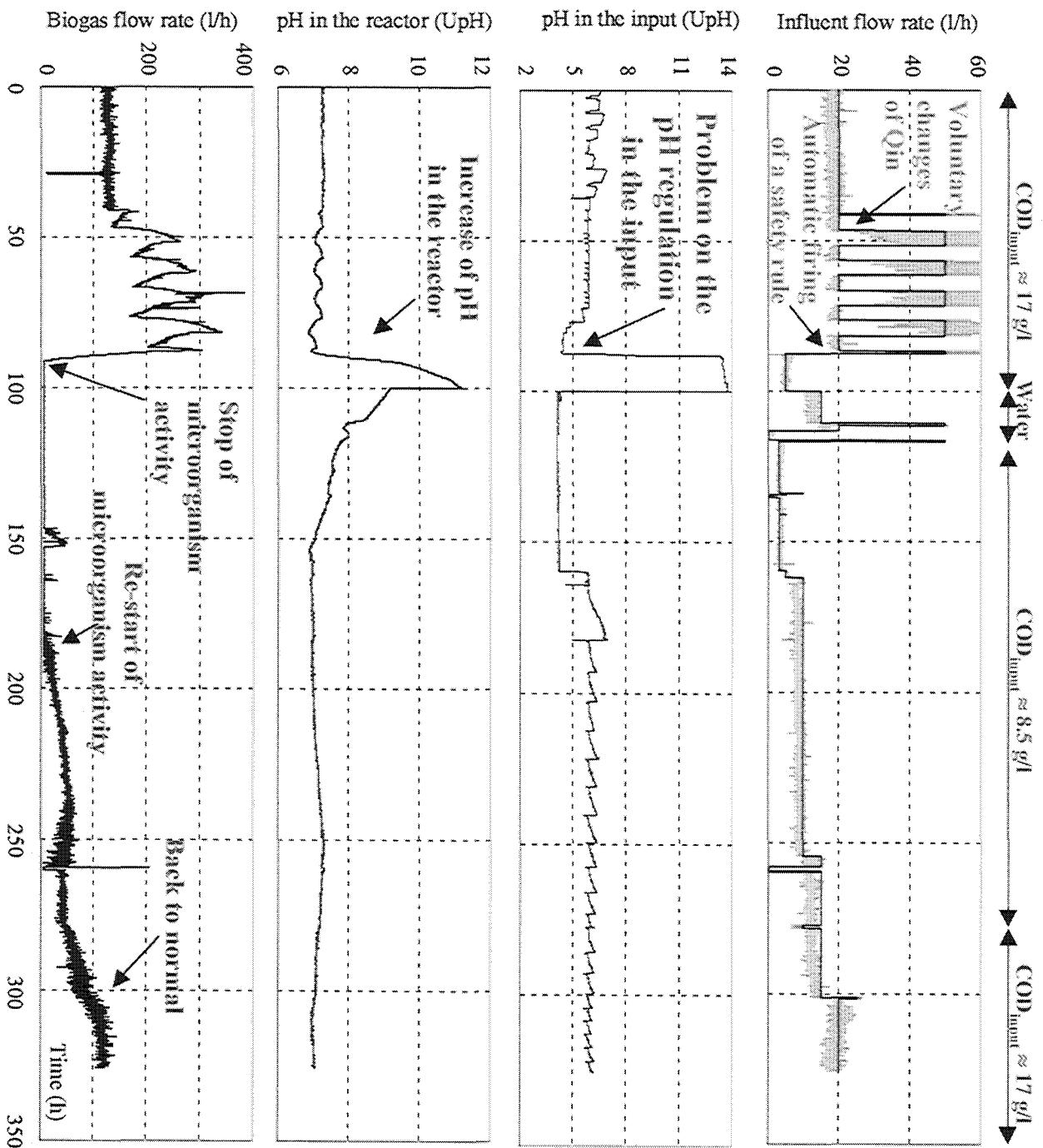
## Advantages :

- ☺ Dynamic (vs. static) and global view of the process
- ☺ Deep understanding of the phenomena
- ☺ Door open to optimal management of WWTPs

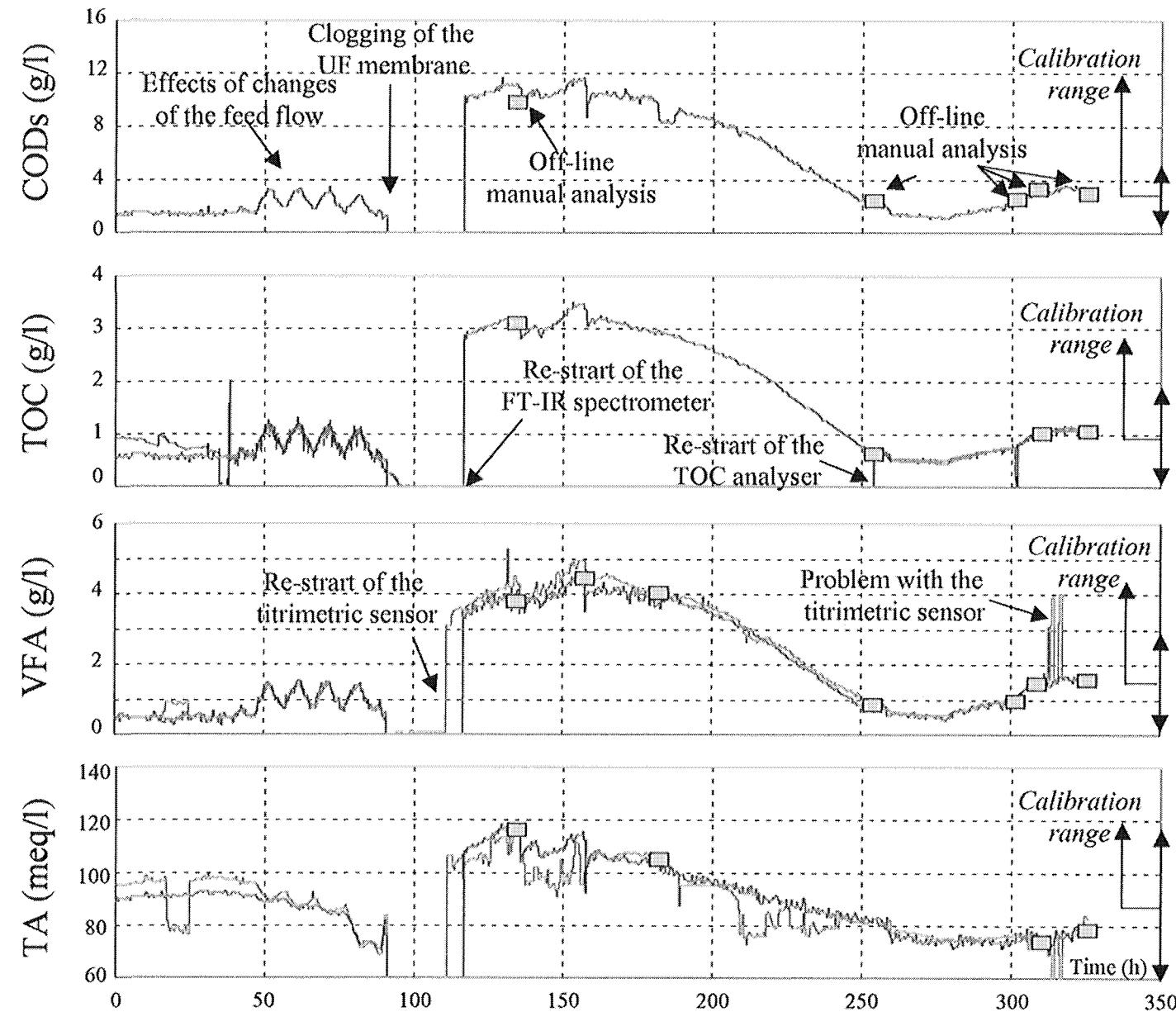
## Drawbacks :

- ☹ Expensive (money *and* maintenance)

# *Application (1) : Monitoring of AD processes*

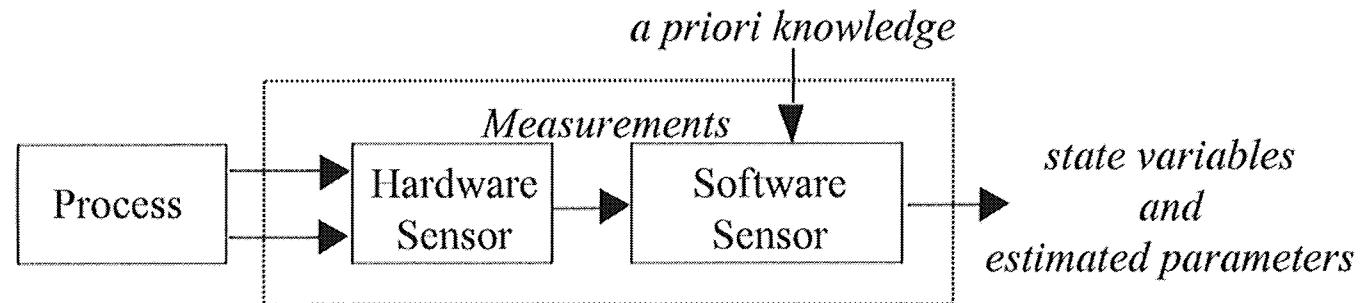


# *Application (1) : Monitoring of AD processes*

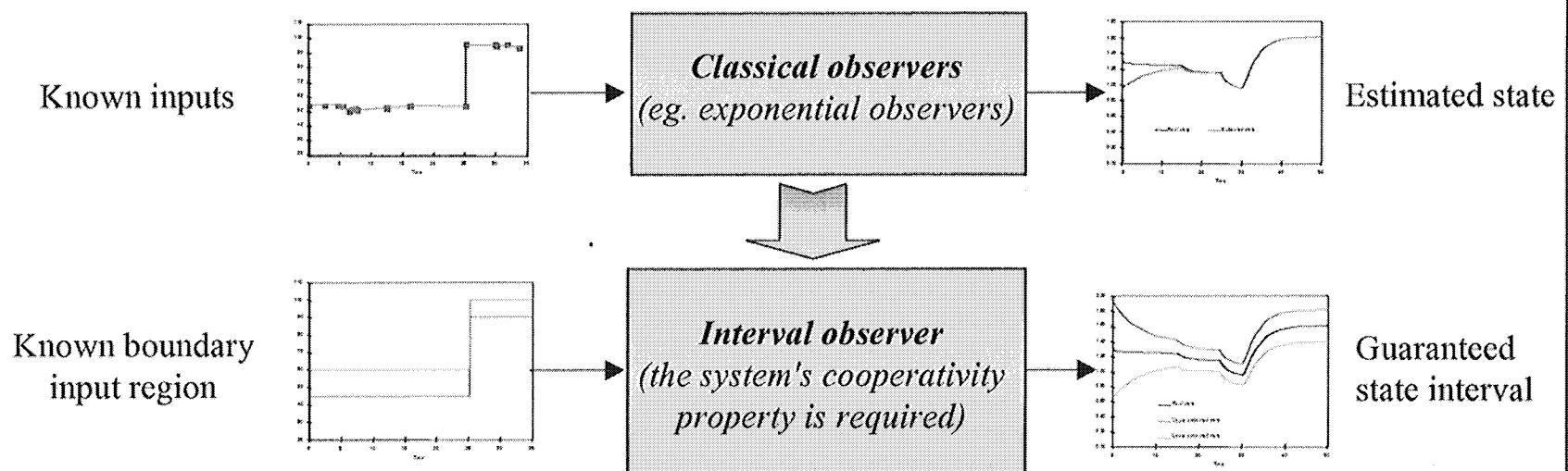


# *Application (2) : Software sensors*

*When technical solutions are not available, it can be useful to combine sensor signals within a mathematical framework in order to estimate unknown parameters.*



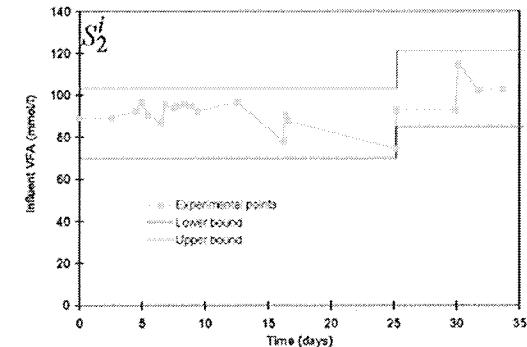
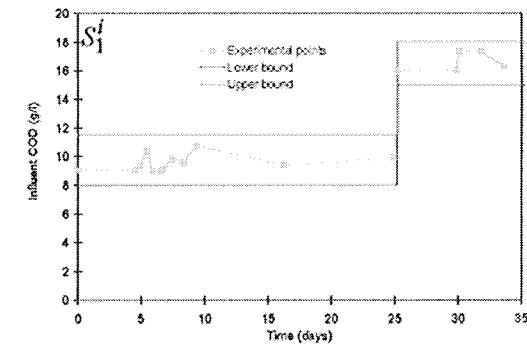
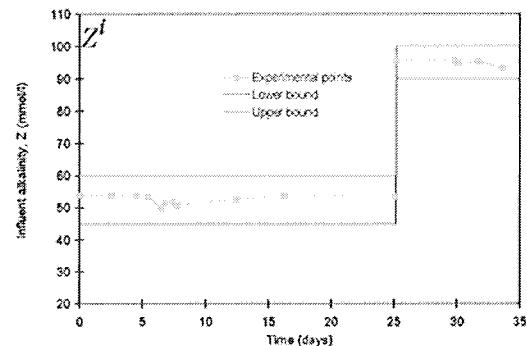
## *Software sensors in WWTPs : Internal observers*



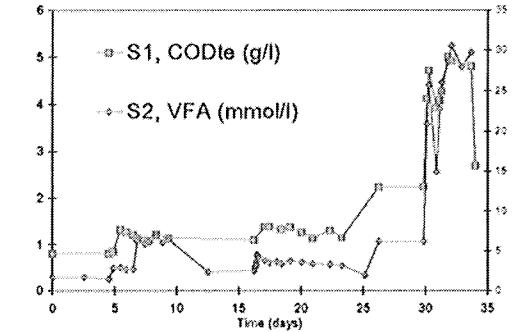
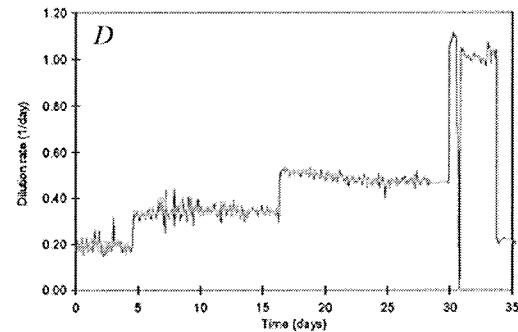
If the observer is cooperative, the estimated state are guaranteed to live within the estimated bounds

# *Application (2) : Software sensors*

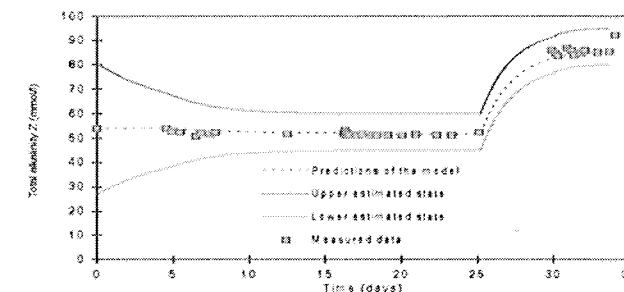
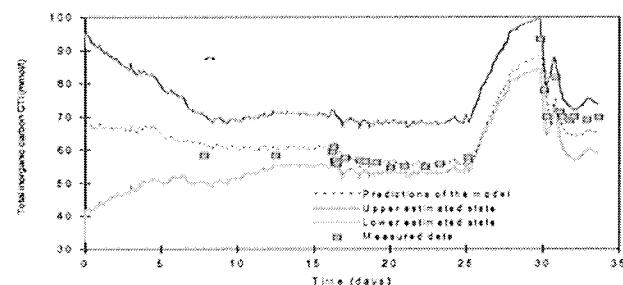
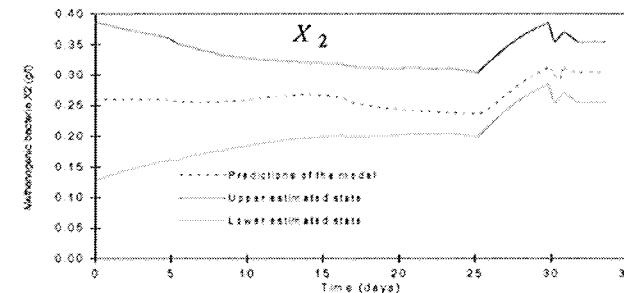
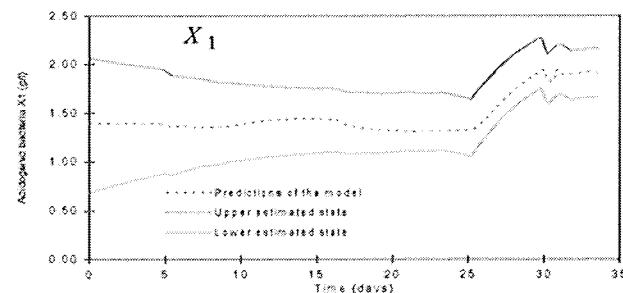
## Hypothesis about the inputs of the process (knowledge of the bounds)



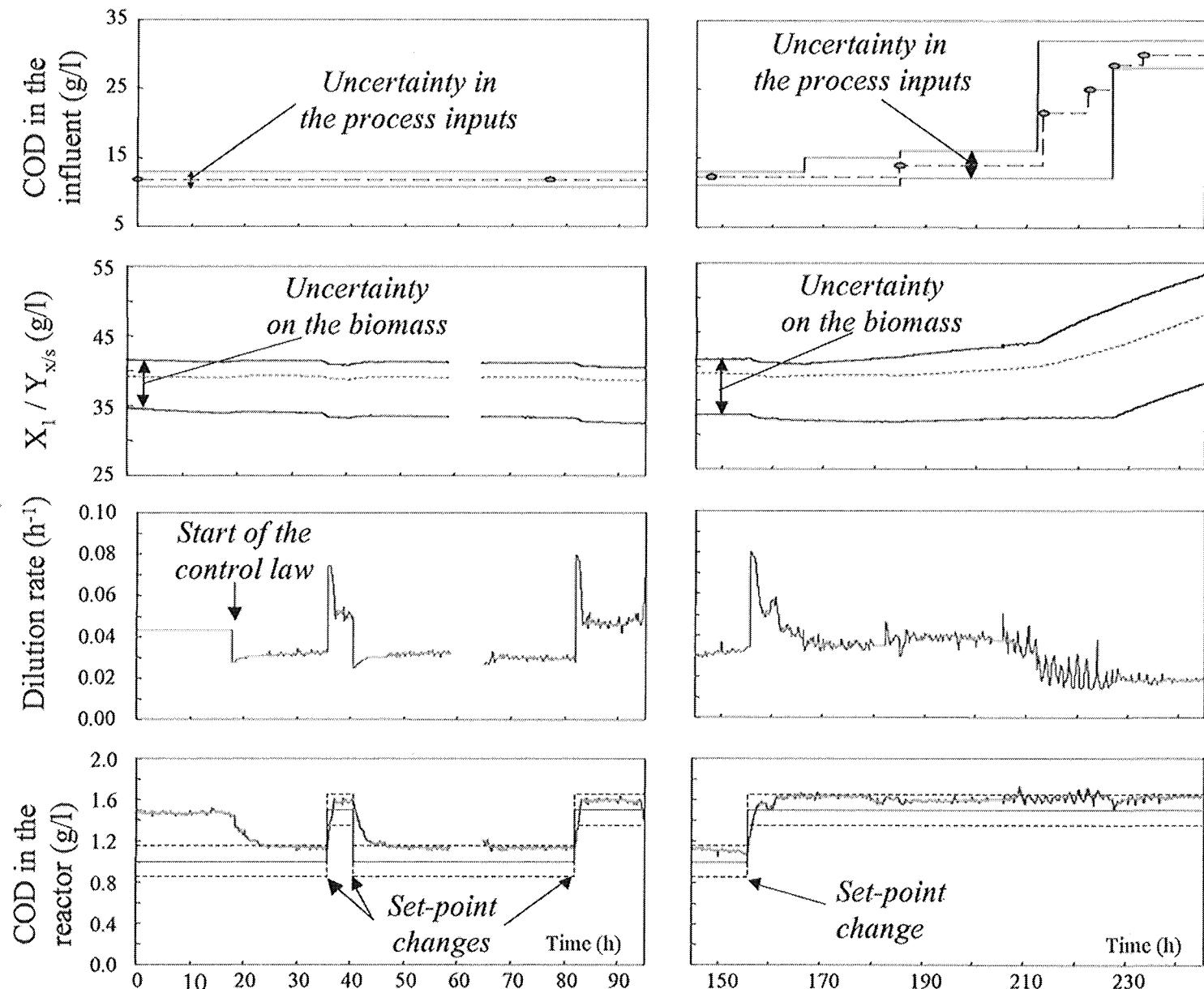
## On-line measurements on the process



## Estimations of the intervals : Comparison with experimental off-line data



# Robust Interval Based Regulation of COD in the reactor

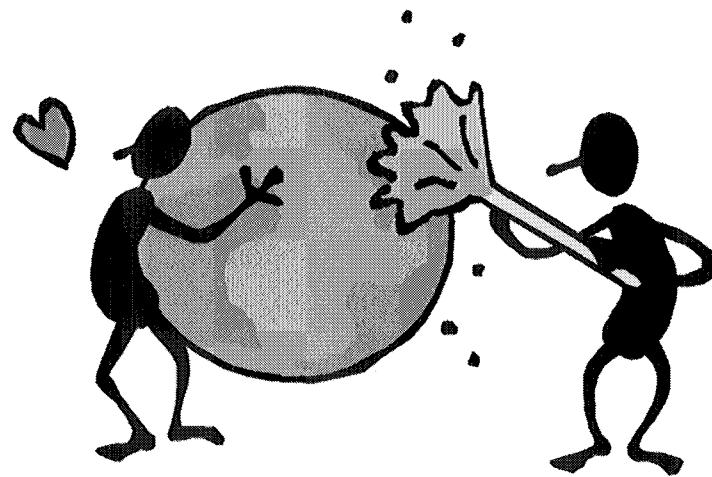


## *Conclusion*

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- ↳ *On-line instrumentation is mandatory*
- ↳ *It allows large benefits*
- ↳ *Reliability is coming*
- ↳ *In the near future : spectral measurements*
- ↳ *In the long future : molecular tools*

Thank you very much for your attention !



I will be very happy to answer your questions