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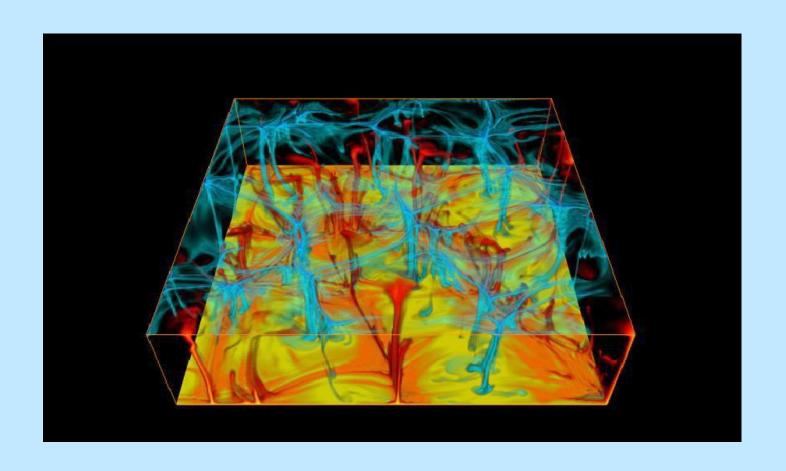
Advanced School on Scaling Laws in Geophysics: Mechanical and Thermal Processes in Geodynamics

23 May - 3 June, 2011

Convection - Part II

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France



 $Ra = 10^8$

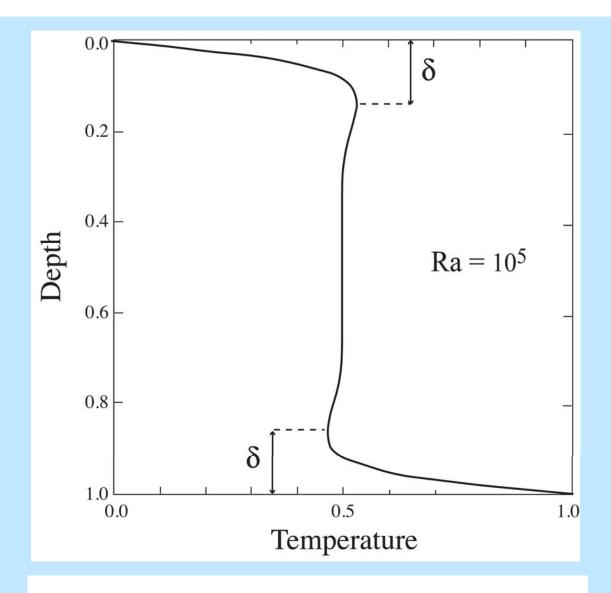
$$T = \overline{T}(z,t) + \theta(x,y,z,t).$$

$$\rho C_p \left[\frac{\partial \overline{T}}{\partial t} + \frac{\partial \overline{w\theta}}{\partial z} \right] = \lambda \frac{\partial^2 \overline{T}}{\partial z^2} \cdot$$

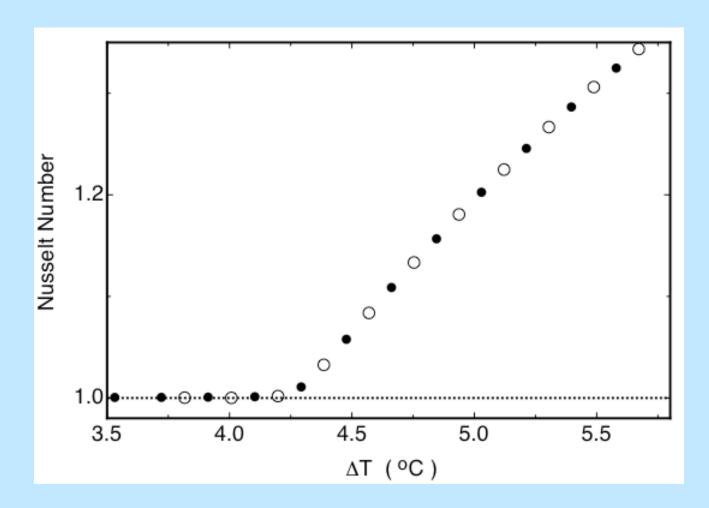
$$\rho C_p \frac{\partial \overline{T}}{\partial t} = -\frac{\partial}{\partial z} \left[-\lambda \frac{\partial \overline{T}}{\partial z} + \rho C_p \overline{w\theta} \right]$$

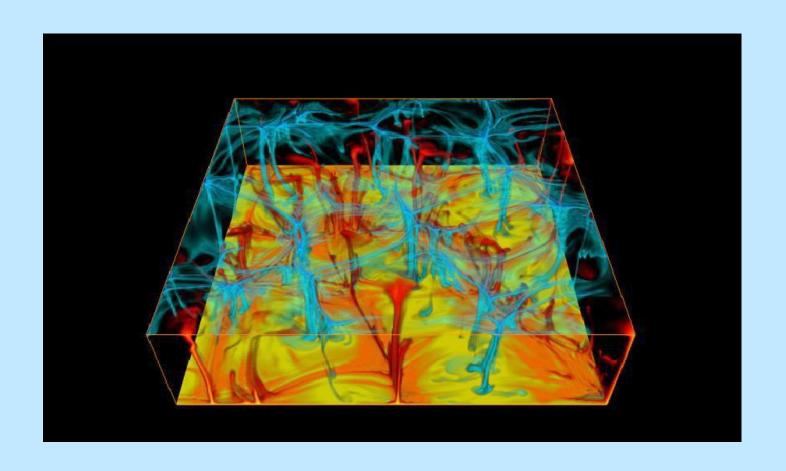
$$\rho C_p \frac{\partial \overline{T}}{\partial t} = -\frac{\partial \overline{q}}{\partial z}$$

$$\overline{q} = -\lambda \frac{\partial \overline{T}}{\partial z} + \rho C_p \overline{w\theta}.$$



$$\overline{q} = -\lambda \frac{\partial \overline{T}}{\partial z} + \rho C_p \overline{w\theta} = \text{constant} = Q,$$





 $Ra = 10^8$

. Physical characteristics of geological convective systems

System	h	ΔT , K	μ, Pa s	Pr	Ra
Upper mantle	660 km	1300 †	5×10^{20}	10 ²³	16
Whole mantle	3000 km	3300 †	5×10^{21}	10^{24}	10^{7}
Basaltic lava lake	50 m	50 ‡	10	10^{3}	10^{12}
Basaltic magma reservoir	1 km	50 ‡	10	10^{3}	10^{16}
Dacitic magma reservoir	1 km	50 ‡	10^{6}	10^{8}	10^{11}

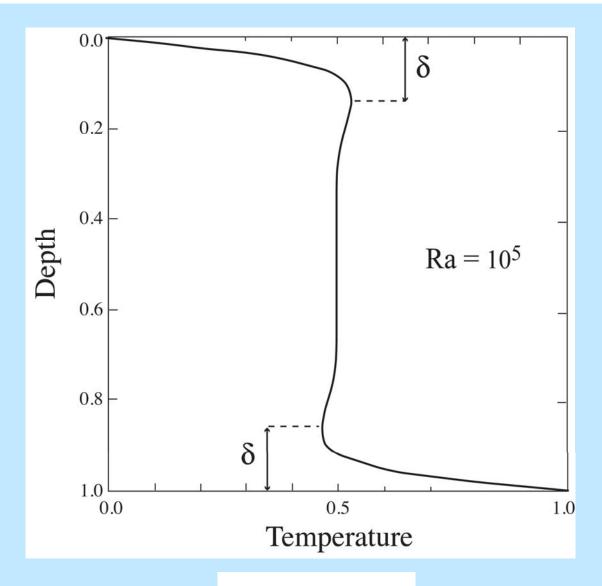
Values have been rounded off for clarity.

[†] True temperature difference deduced from the mantle geotherm of Figure 2.4.

[‡] temperature difference across the actively convecting part of the system.

The "4/3" law for the convective heat flux at high Rayleigh number

$$Nu = C_N(Pr)f_N(Ra)$$
,



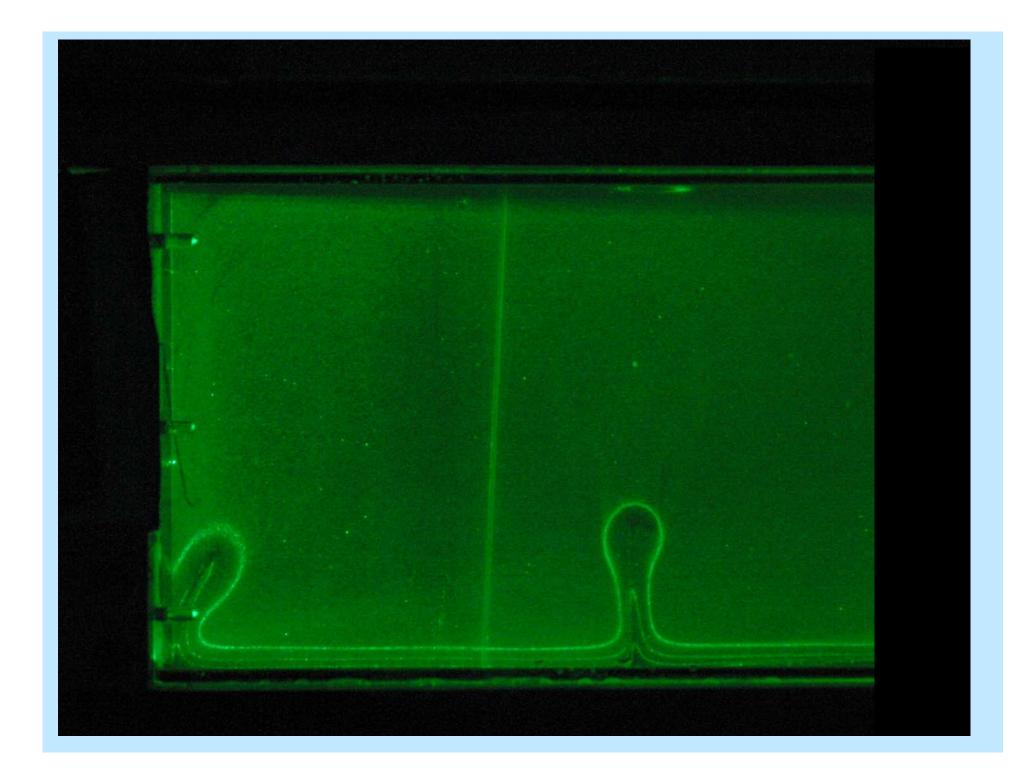
$$Q = \kappa \frac{\Delta T}{2\delta},$$

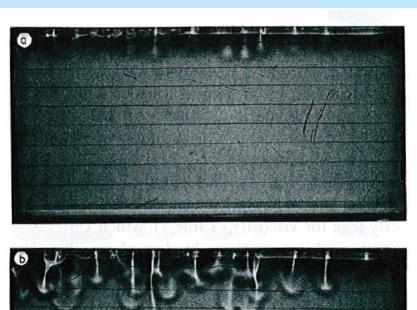
The "4/3" law for the convective heat flux at high Rayleigh number

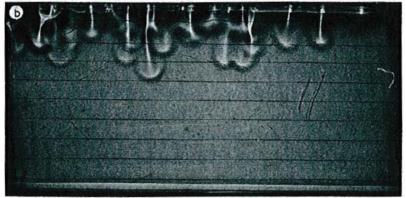
$$Nu = C_N(Pr)f_N(Ra)$$
,

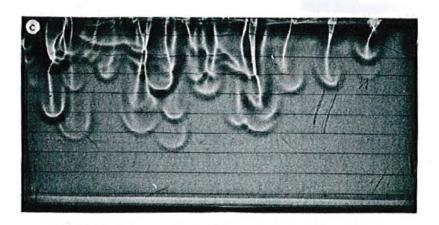
$$Q: k \lambda \frac{\Delta T}{2\delta},$$

$$Nu = \frac{h}{2\delta}.$$









$$Q = \operatorname{Nu.k} \frac{\Delta T}{h} = C_N(\operatorname{Pr}) \, k \frac{\Delta T}{h} f_N \left(\frac{\rho_o g \alpha \, \Delta T h^3}{\kappa \, \mu} \right),$$

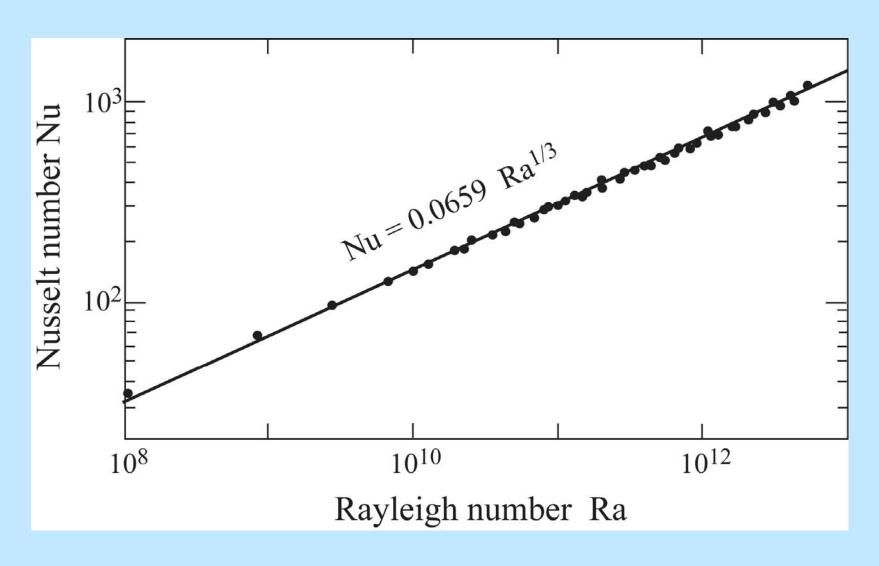
$$f_N(\text{Ra}) \propto \text{Ra}^{1/3}$$

$$Nu = C_N Ra^{1/3}$$
.

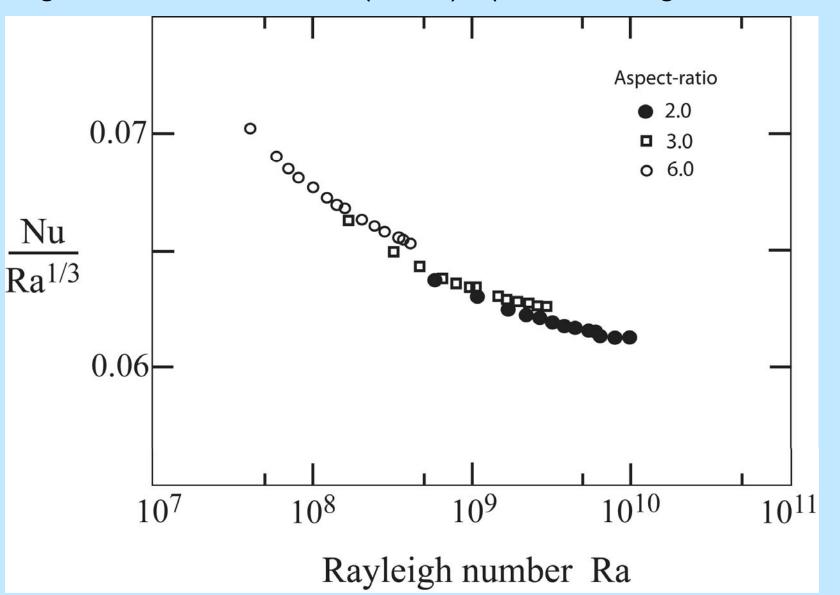
$$Q = C_Q k \left(\frac{g\alpha}{\kappa \nu}\right)^{1/3} \Delta T_{\delta}^{4/3},$$

$$C_Q = 2^{4/3} C_N$$

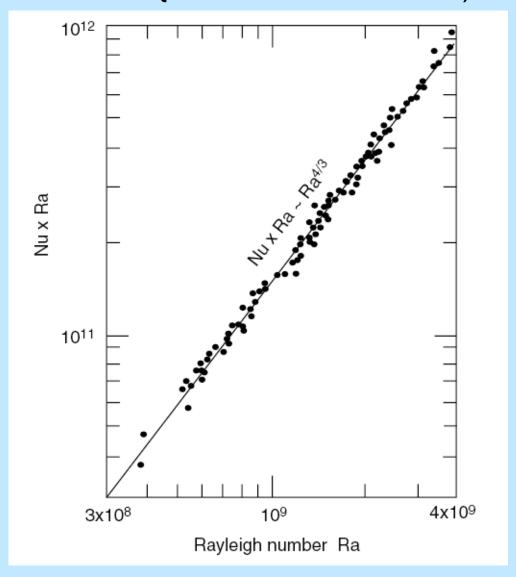
Rigid boundaries, Pr = 2750, L/h >1 (Goldstein et al., 1990)



Rigid boundaries, Pr ≈ 5 (water) (Funfschilling et al., 2005)



Free upper boundary (cooling from top only), Pr ≈ 5 (water) L/h = 1 {Katsaros et al., 1977)



Data on the convective heat flux in Rayleigh-Benard convection

Pr	Ra		Aspect ratio	C_N +	C_Q ++	Reference
4–6	$5 \times 10^{10} - 10^{11}$	Rigid	0.98	0.060	0.15	(Funfschilling et al., 2005)
4–6	10^{10}	Rigid	2	0.062	0.16	(Funfschilling et al., 2005)
4–6	$3 \times 10^{8} - 4 \times 10^{9}$	Free	1	§	0.16†	(Katsaros et al., 1977)
2750	$10^{8} - 10^{13}$	Rigid	> 1	0.0659	0.17	(Goldstein et al., 1990)
∞	$10^{6} - 10^{9} \ddagger$	Free	1.5	0.150¶	0.378¶	(Hansen et al., 1992)

⁺ Constant in the Nu versus Ra relationship (5.81).

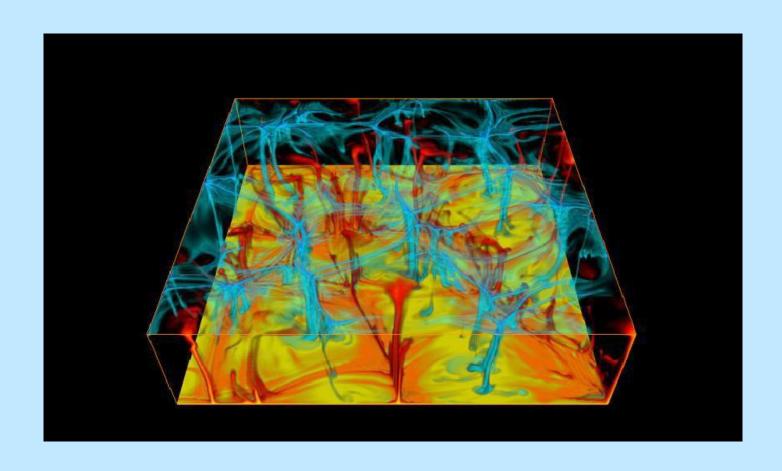
⁺⁺ Constant in the local heat flux scaling law (5.82).

[§] Only the boundary layer scaling can be determined in this transient cooling experiment.

[†] Value re-calculated for a 1/3 scaling exponent (instead of 0.33).

[¶] Value re-calculated for a 1/3 scaling exponent at $Ra = 10^9$.

[‡] Numerical calculations in 2D.



 $Ra = 10^8$

$$0 = -\nabla P_h + \rho_o \left[1 - \alpha \left(\overline{T} - T_o \right) \right] \mathbf{g},$$

Irreversible kinetic dissipation

$$\psi = \mathbf{v} \cdot (\nabla \cdot \mathbf{o} \, \mathbf{\tau} - \nabla \cdot (\mathbf{o} \, \mathbf{\tau} \, \mathbf{v}).$$

$$\int_{V} \rho_{o} \frac{\partial e_{c}}{\partial t} dV + \int_{S} \rho_{o} e_{c} \mathbf{v} \cdot dS = -\int_{S} p \mathbf{v} \cdot dS + \int_{V} p \nabla \cdot \mathbf{v} dV$$
$$-\int_{V} \psi dV - \int_{S} (\boldsymbol{\tau} \cdot \mathbf{v}) \cdot dS + \int_{V} \alpha \rho_{o} w \theta g dV.$$

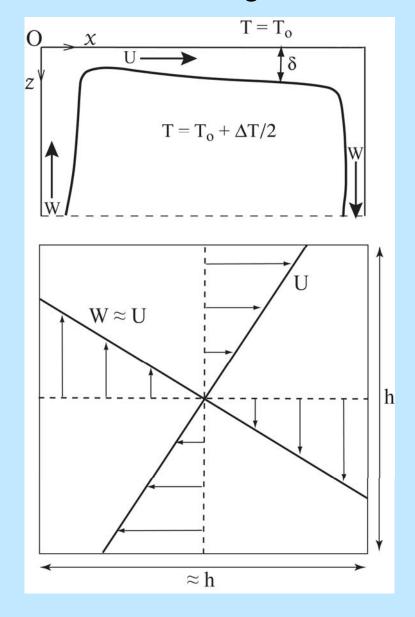
$$+ \int_{V} \rho \alpha g w \theta \, dV - \int_{V} \psi \, dV = 0.$$

$$+ \int_{0}^{h} \rho \alpha g \overline{w \theta} \, dz - \int_{0}^{h} \overline{\psi} \, dz = 0.$$

$$\int_{0}^{h} \rho C_{p} \overline{w\theta} dz = \int_{0}^{h} \left(Q + \kappa \frac{k d \overline{T}}{dz} \right) dz$$
$$= Qh + \kappa [T(h) - T(0)] = Qh - \kappa \Delta T.$$

$$\epsilon = \int_0^{h} \overline{\psi} \, dz = \mu \frac{v^2}{h^3} (\text{Nu} - 1) \, \text{RaPr}^{-2}.$$

Free boundaries, large Prandtl number



$$\int_0^h \psi \, dz \sim \mu \frac{U^2}{h^2} h \sim \mu \frac{v^2}{h^3} \mathrm{Re}^2.$$

$$\mu \frac{v^2}{h^3} (\text{Nu} - 1) \, \text{RaPr}^{-2} \sim \mu \frac{v^2}{h^3} \text{Re}^2,$$

Remember that $Nu \sim h/\delta$.

Add balance between horizontal advection and vertical diffusion (remember scalings for laminar plumes)

$$\delta \sim \sqrt{\kappa h/U}$$

$$Re^{1/2}Pr^{1/2} \sim Nu$$
.

 $Nu \sim Ra^{1/3}$, $Re \sim Ra^{2/3}Pr^{-1}$,

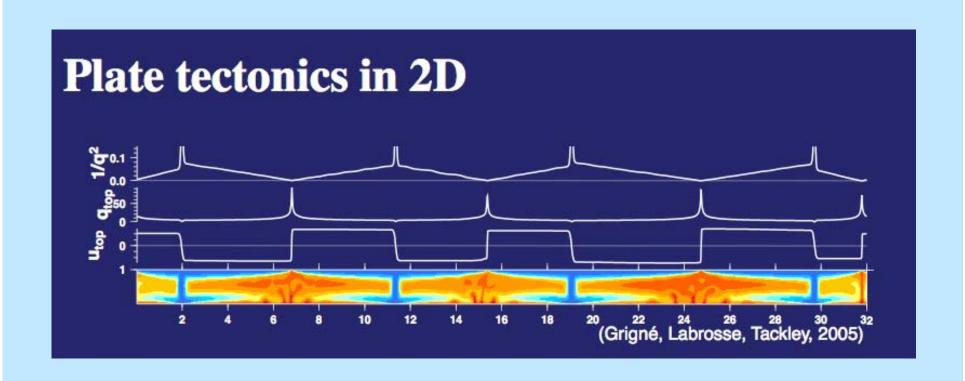
 $\delta \sim h \mathrm{Ra}^{-1/3}$, $U \sim \frac{\kappa}{h} \mathrm{Ra}^{2/3}$.

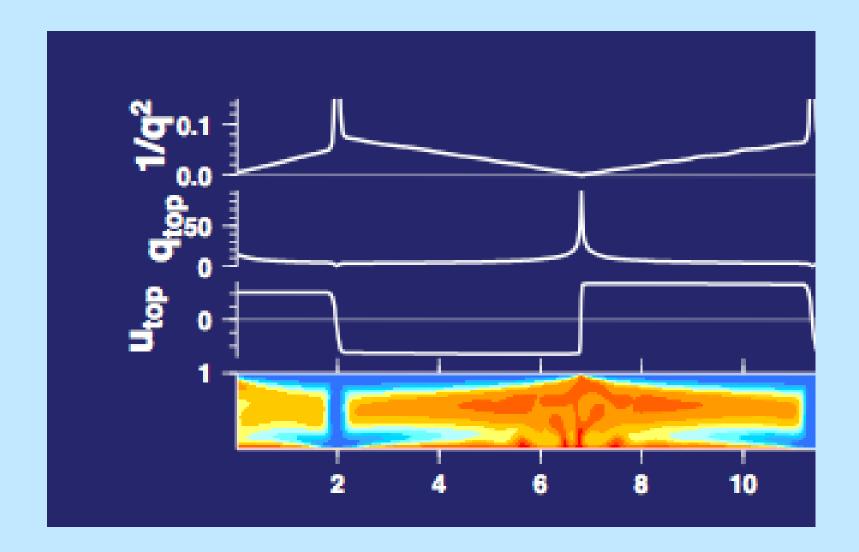
$$\delta \sim \sqrt{\kappa h/U}$$

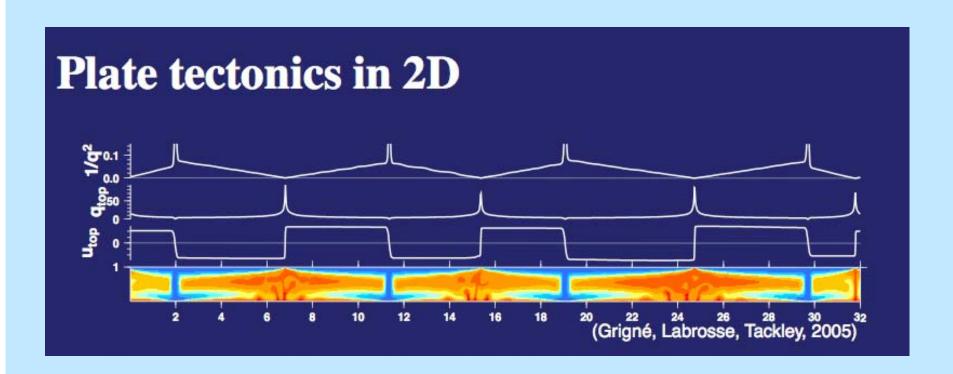
This is the average boundary layer thickness.

The local thickness at distance **x** from upwelling is

$$\delta \sim \sqrt{\kappa \; {\it x}/U}$$



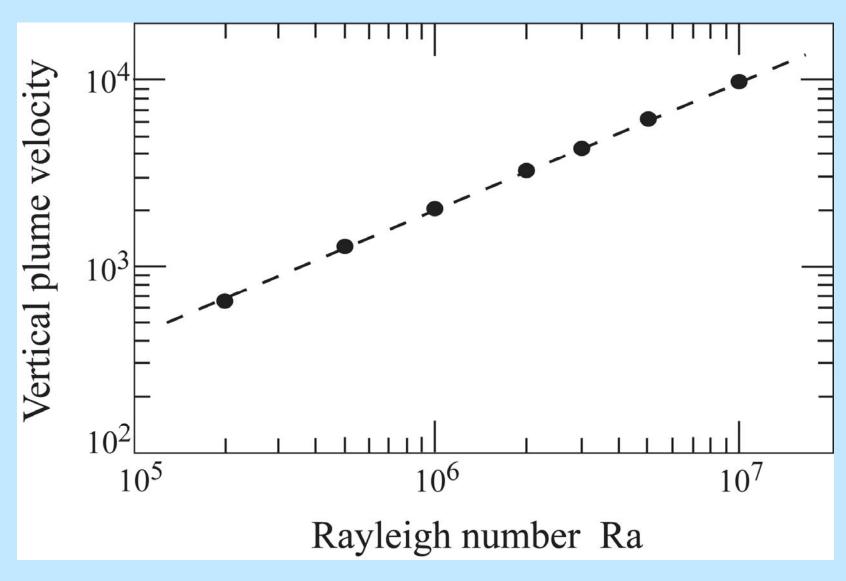




Heat flux \sim (distance)^{-1/2}

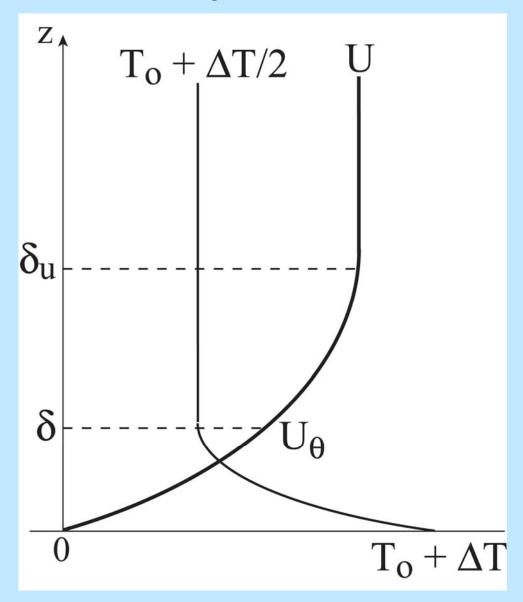
 $\text{Nu} \sim \text{Ra}^{1/3}$, $\text{Re} \sim \text{Ra}^{2/3} \text{Pr}^{-1}$,

 $\delta \sim h \mathrm{Ra}^{-1/3}$, $U \sim \frac{\kappa}{h} \mathrm{Ra}^{2/3}$.



(Galsa & Lenkey, Phys. Fluids 2007)

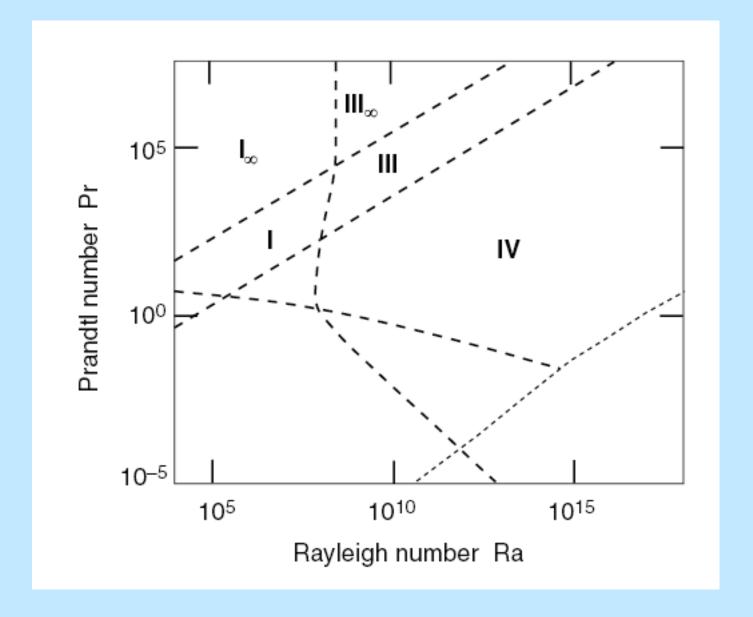
With rigid boundaries



The regimes of Rayleigh-Bénard convection in rigid enclosures (Grossmann & Lohse, J. Fluid Mech. 2000, Phys. Fluids. 2001)

Regime	Dominant dissipation §	Nu	Re
I $I_{\infty} (Pr \gg 1)$ III $III_{\infty} (Pr \gg 1)$ IV	$(u,B) - (\theta,B)$	0.31 Ra ^{1/4} Pr ^{-1/12}	0.073 Ra ^{1/3} Pr ^{-5/6}
	$(u,B) - (\theta,B)$	0.35 Ra ^{1/5}	0.054 Ra ^{3/5} Pr ⁻¹
	$(u,B) - (\theta,I)$	0.018 Ra ^{3/7} Pr ^{-1/7}	0.023 Ra ^{4/7} Pr ^{-6/7}
	$(u,B) - (\theta,I)$	0.027 Ra ^{1/3}	0.015 Ra ^{2/3} Pr ⁻¹
	$(u,I) - (\theta,I)$	0.060 Ra ^{1/3}	0.088 Ra ^{4/9} Pr ^{-2/3}

§Dominant contributions to kinetic and thermal dissipation (see text). u and θ stand for the kinetic and thermal dissipation, respectively, and symbols I and B indicate interior and boundary-layer contributions, respectively.



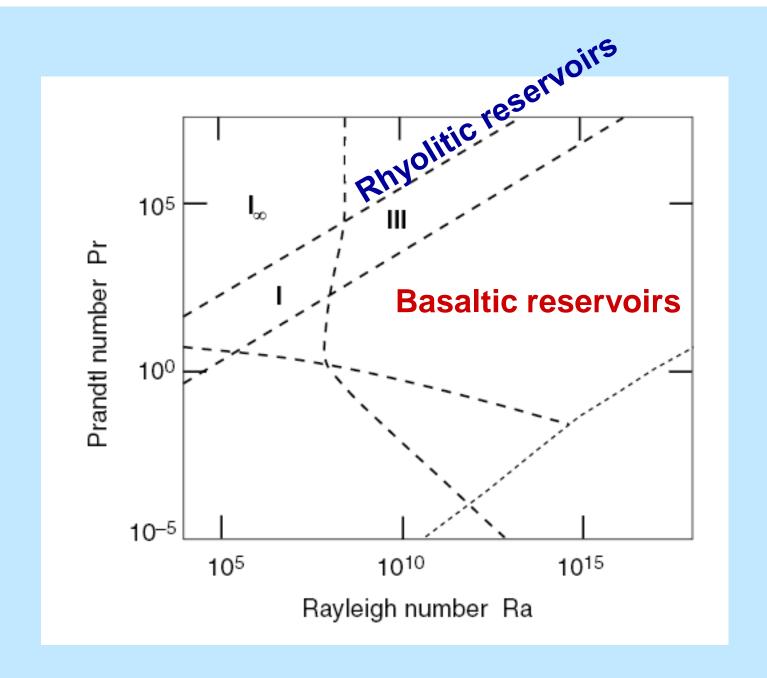
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$ III_{\infty} (Pr \gg 1) $ $IV $	$(u,B) - (\theta,I)$ $(u,I) - (\theta,I)$	$0.027~{ m Ra}^{1/3} \ 0.060~{ m Ra}^{1/3}$	$0.015 \text{ Ra}^{2/3} \text{Pr}^{-1}$ $0.088 \text{ Ra}^{4/9} \text{Pr}^{-2/3}$

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