



**The Abdus Salam  
International Centre for Theoretical Physics**



**2269-11**

**Workshop on New Materials for Renewable Energy**

*17 - 21 October 2011*

**SOLAR CELLS  
(Solar-driven thermochemical dissociation of Co<sub>2</sub> and H<sub>2</sub>O using ceria)**

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U.S.A.*

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# Solar-Driven Thermochemical Dissociation of CO<sub>2</sub> and H<sub>2</sub>O Using Ceria

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Sossina M. Haile

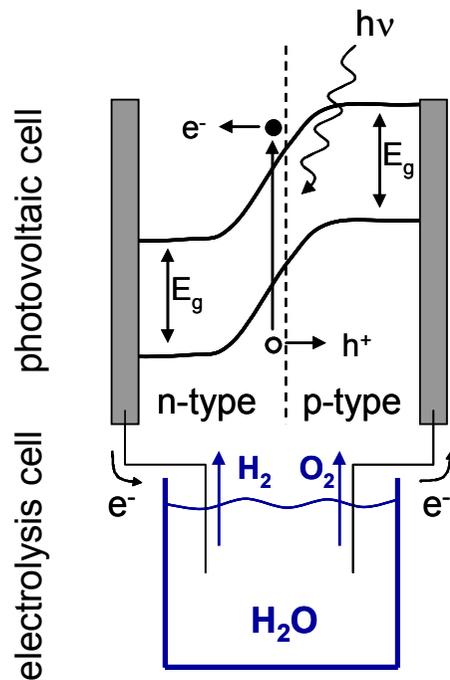
Materials Science / Chemical Engineering  
California Institute of Technology

“Capture and Conversion of CO<sub>2</sub> into Sustainable Fuels”  
April 14-15, 2011; Riso, Denmark



# Using the Sun to Make Fuels

- Solar electricity + electrolysis

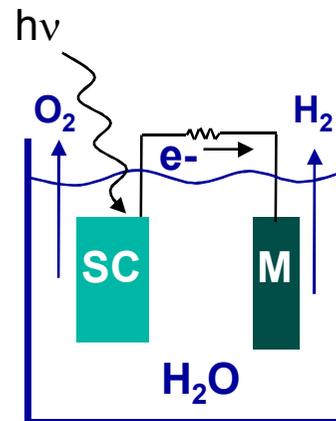


- Separate components

- Precious metal catalysts, poor rates
- Poor use of solar spectrum

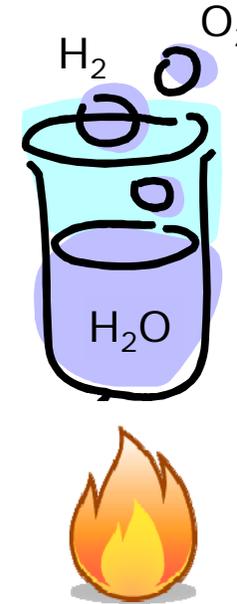


- Photolysis



- Low  $CO_2$  solubility
- Poor product selectivity
- Non-aqueous electrolyte
- Material corrosion

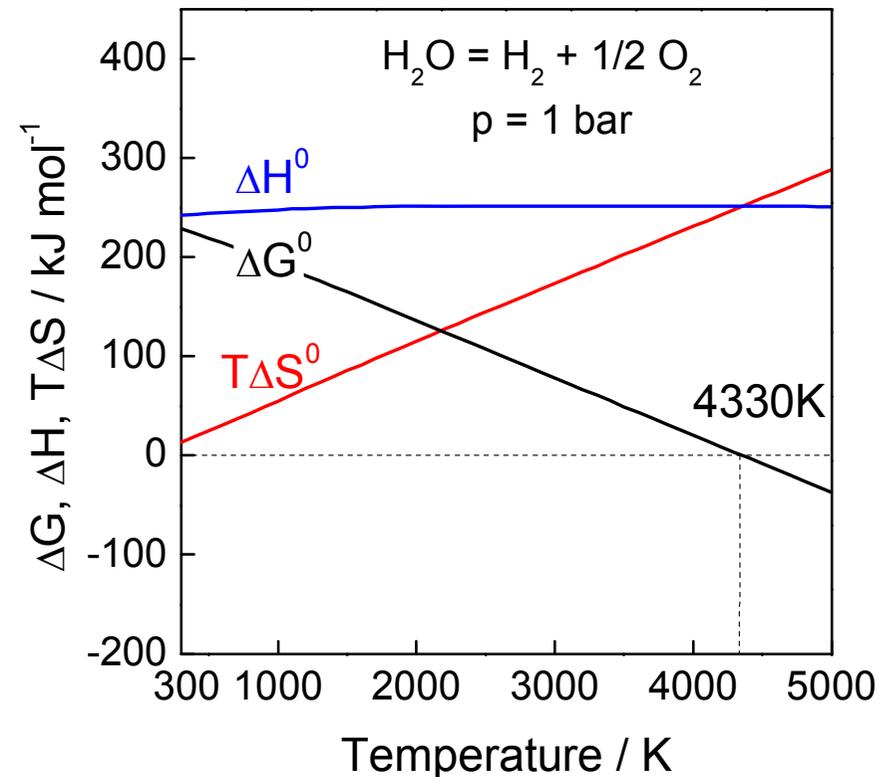
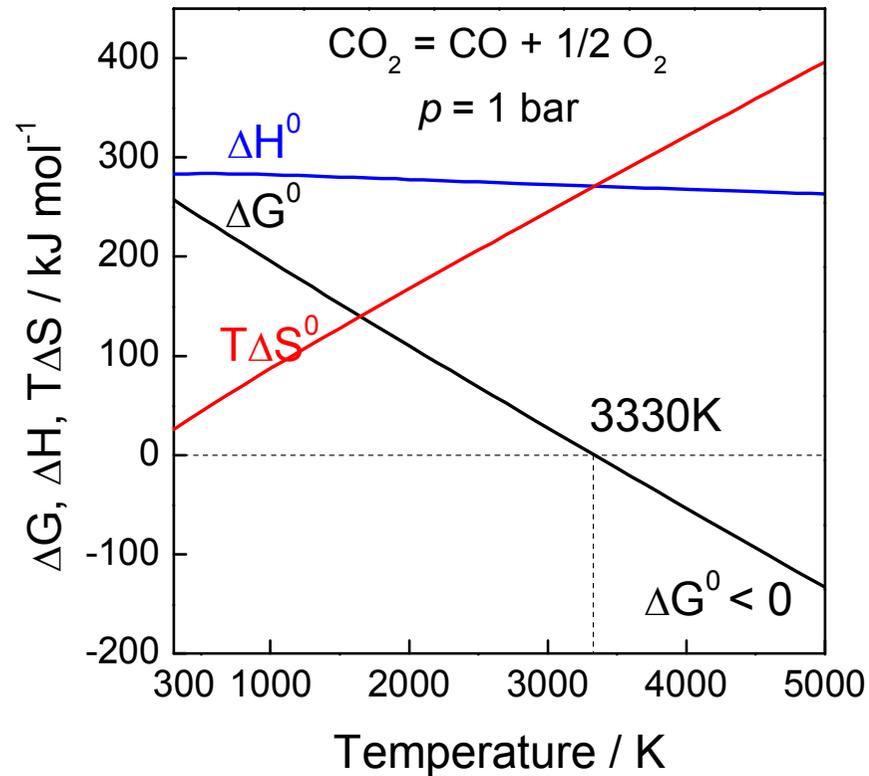
- Thermolysis



- Reaction at  $> 4,000$  °C
- Requires separation



# Direct Thermolysis



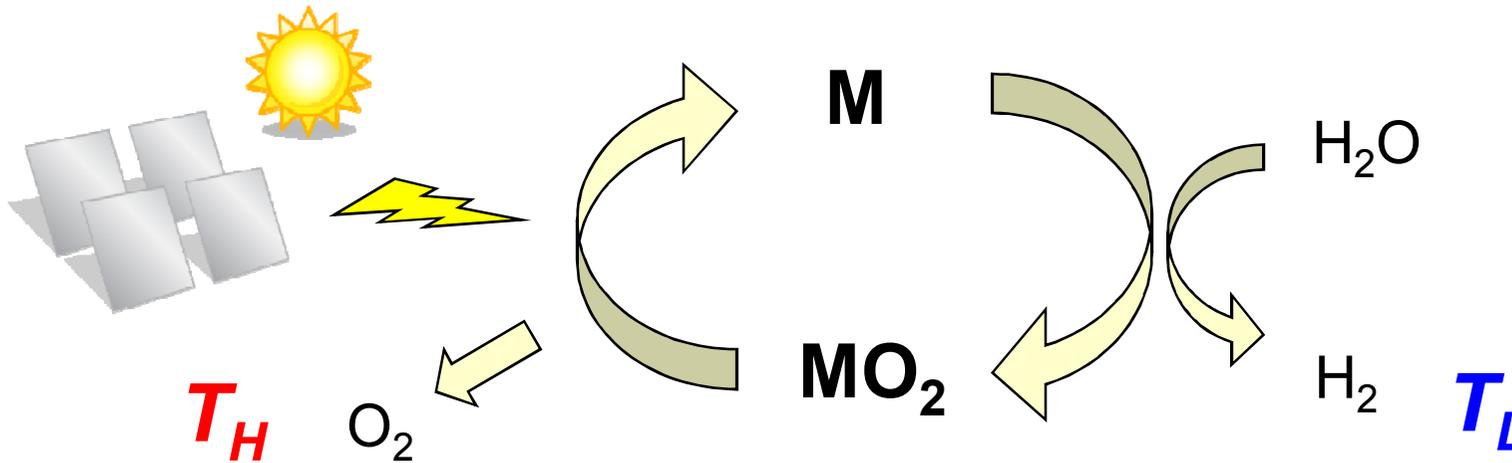
- Slightly easier for  $\text{CO}_2$  dissociation than  $\text{H}_2\text{O}$
- But still extremely challenging  $\rightarrow$  multi-step reaction schemes



# Metal Oxide Solar Thermochemical Cycle

***Thermal Reduction/  
Oxygen Release***

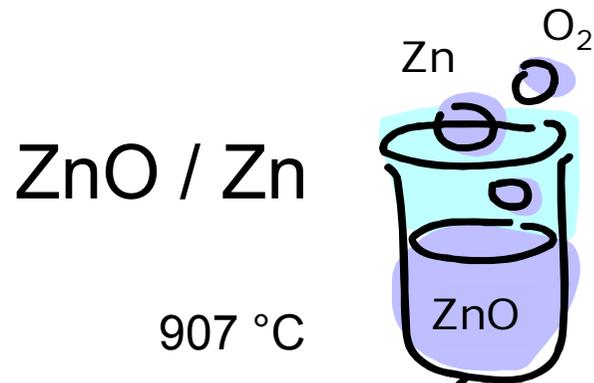
***Oxidation/Fuel Production***



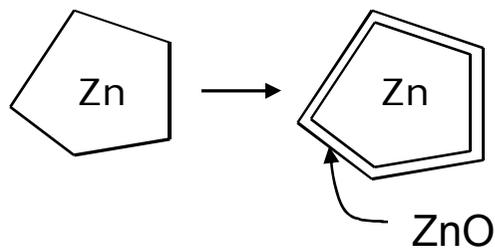
- Integrated solar capture and fuel production
- Oxygen and fuel produced in separate steps
- Challenges due to structural change & volatilization
- Fuel largely limited to hydrogen



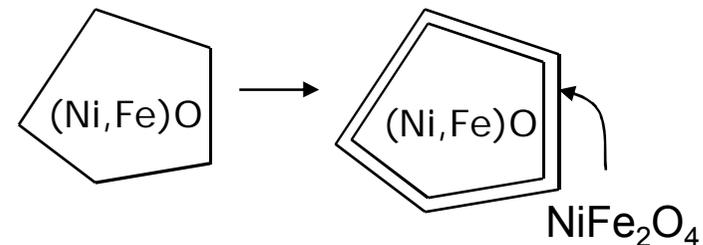
# State-of-the-Art



- Difficult Zn capture
  - Quench step required
- Slow oxidation kinetics



- Solid state transformation
  - T<sub>H</sub> ~ 1400°C
- Two distinct solid phases



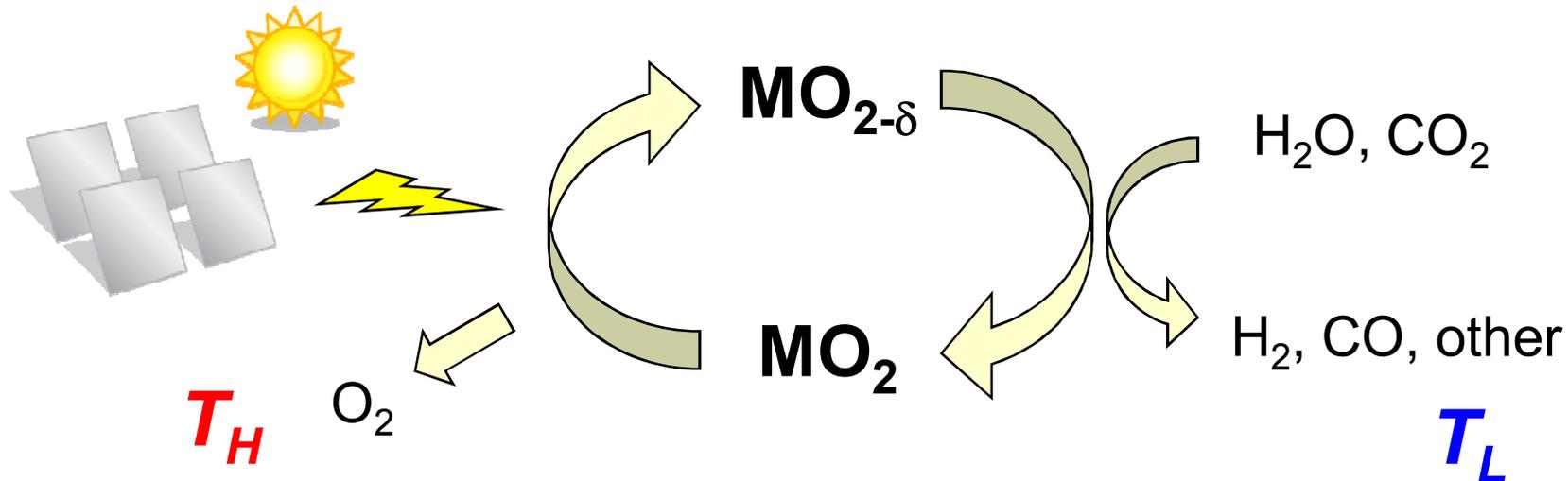
- Slow kinetics
  - Slow oxygen diffusion
  - Slow surface reaction
- Kinetics worsen
  - Loss of porosity (sinter)



# Alternative Thermochemical Cycle

**Thermal Reduction/  
Oxygen Release**

**Oxidation/Fuel Production**



Metal oxide releases/incorporates oxygen

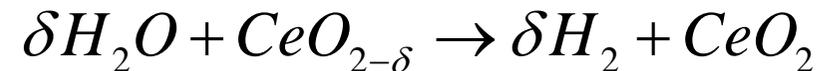
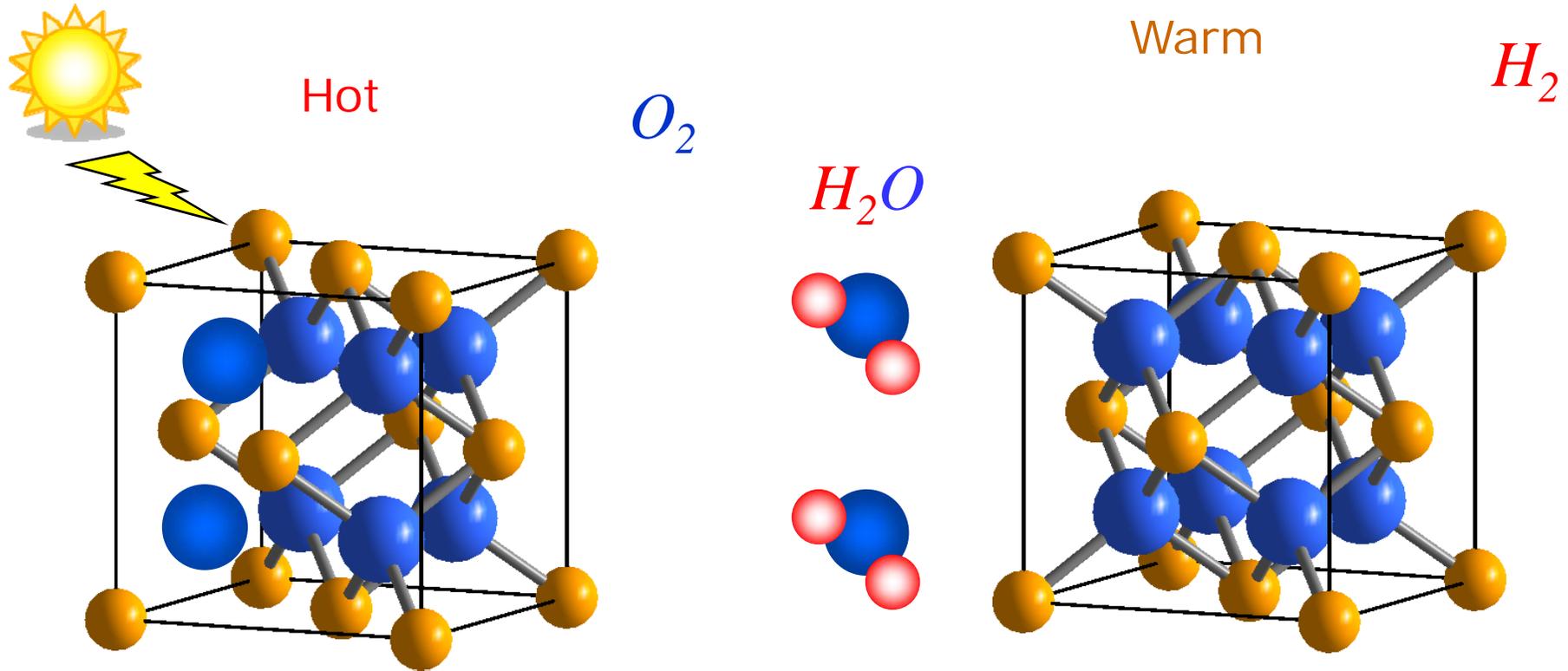
No phase change, large nonstoichiometry range

Rapid kinetics: bulk diffusion, surface reaction

Ideal candidate: *Ceria*,  $CeO_{2-\delta}$



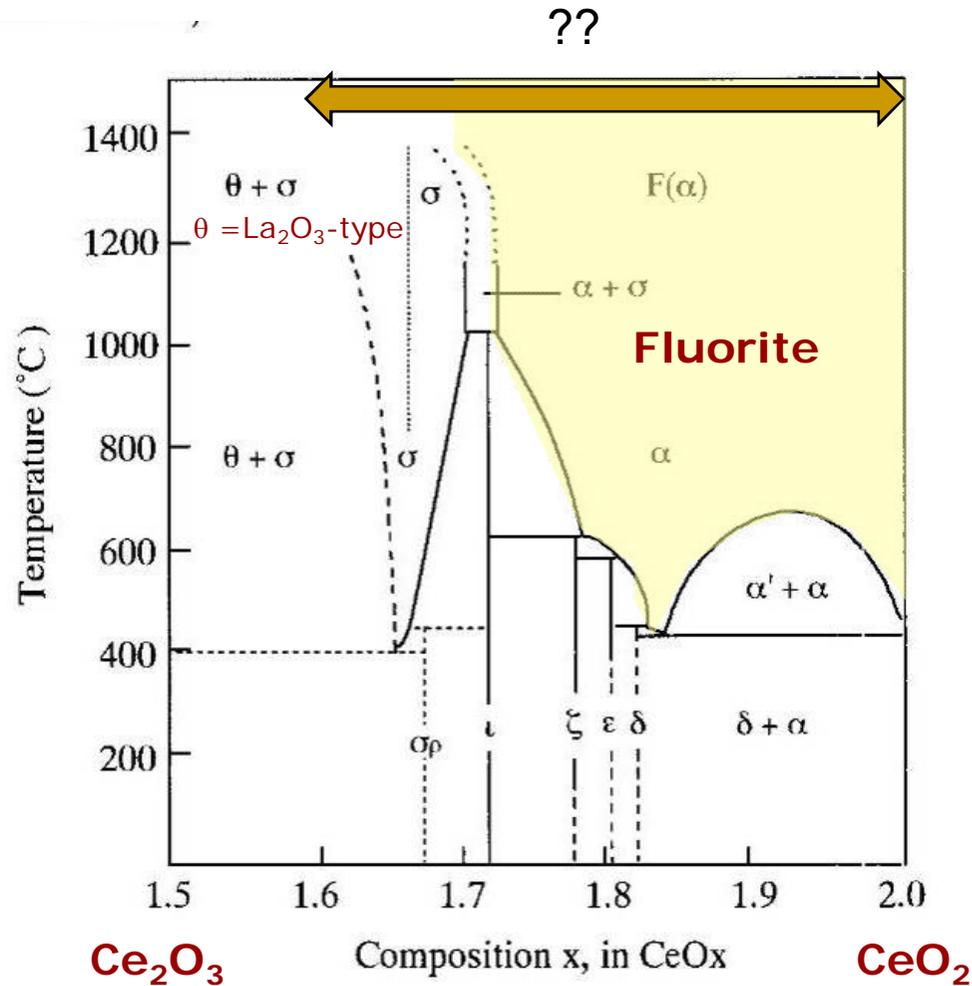
# Ceria thermochemical cycle



- Thermodynamics well-known
- Extremely refractory:  $T_m = 2477 \text{ }^\circ\text{C}$ , non-volatile



# Ce<sub>2</sub>O<sub>3</sub> – CeO<sub>2</sub> Phase Diagram



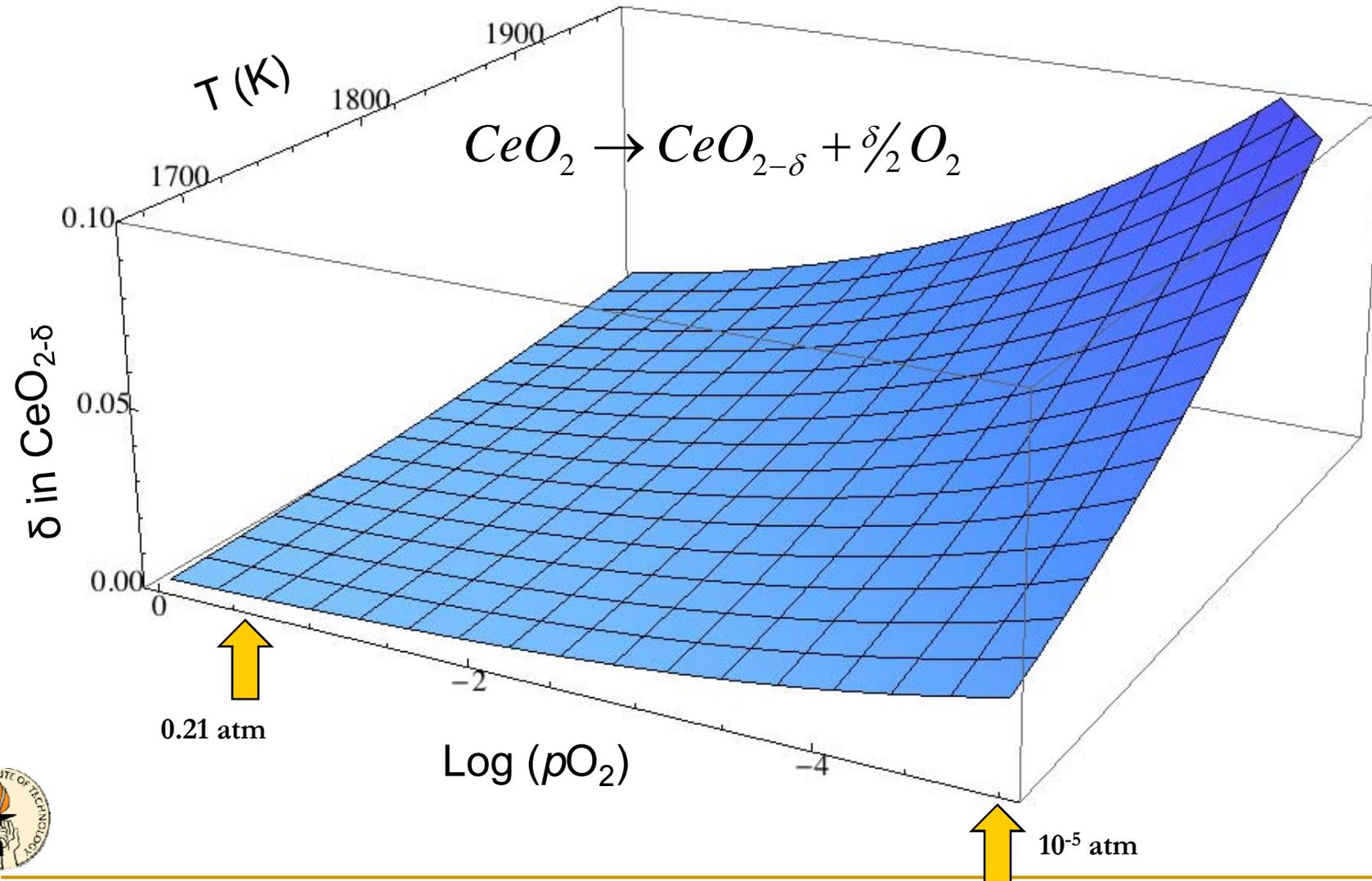
- Phase extent of fluorite unknown
- Favored at high T
- Favored by doping
- Ignore Ce<sub>n</sub>O<sub>2n-m</sub> ordered phases

G. Adachi and N. Imanaka, *Chem. Rev.*, **98**, 1479-1514 (1998).

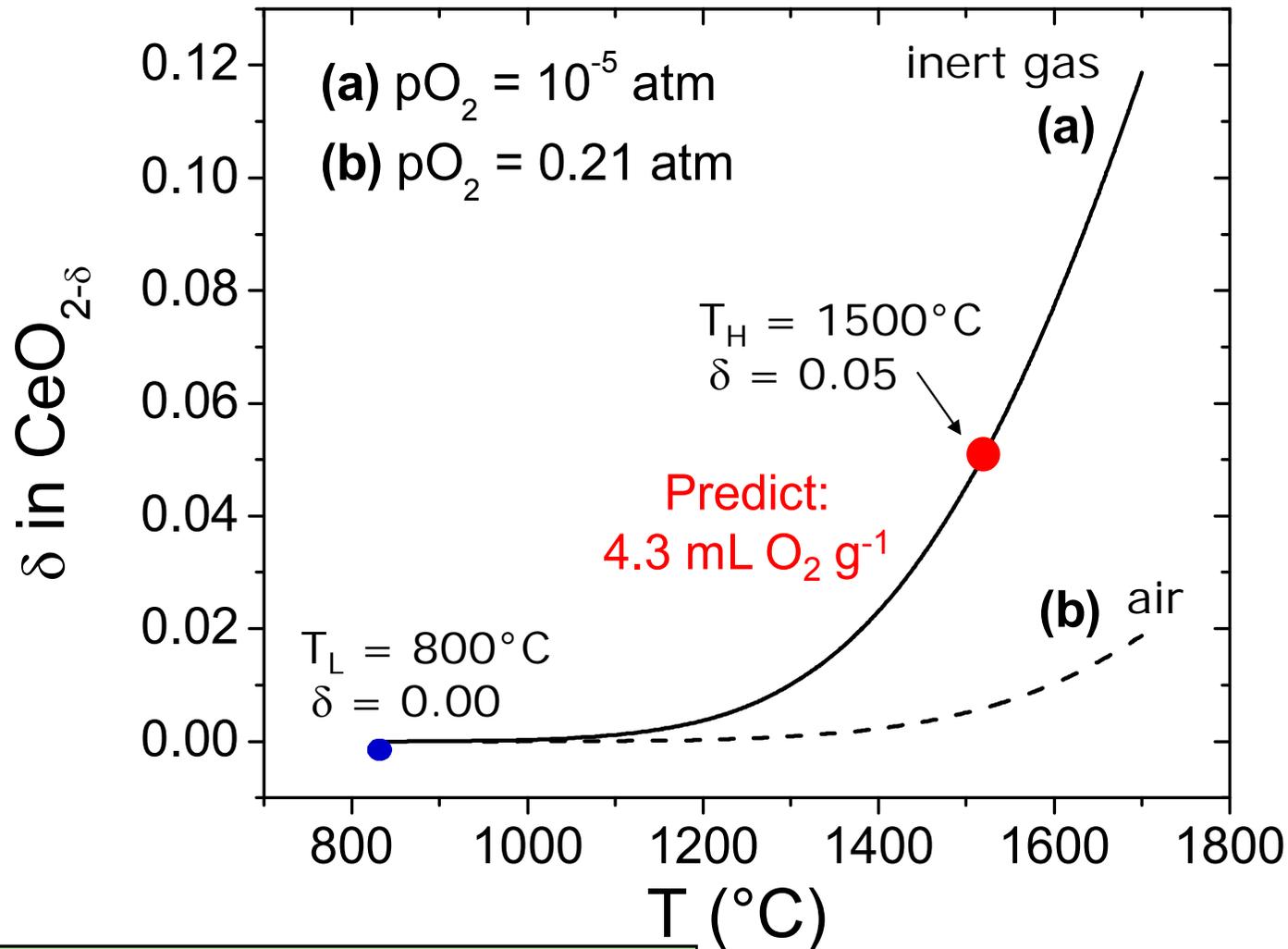


# Thermodynamic Oxidation State

Can compute  $\delta$  ( $T$ ,  $pO_2$ ) from material thermodynamic parameters



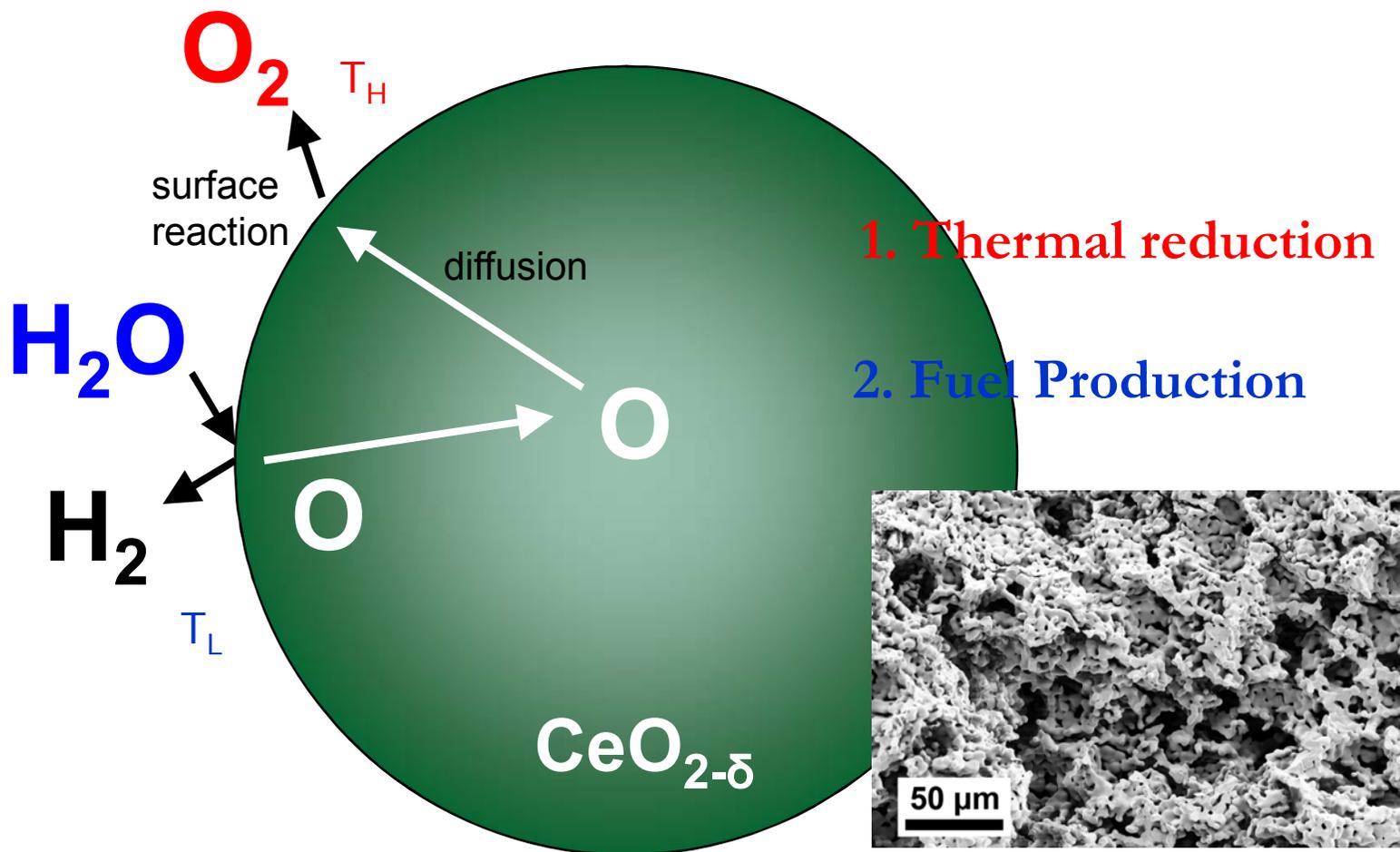
# Predicted Oxygen Release / Fuel Production



**Theoretical fuel production:**  
 8.6 mL  $H_2$  (STP) / gram of ceria / cycle\*

\* 7 g for  $Ce_{0.85}Sm_{0.15}O_{1.925-\delta}$

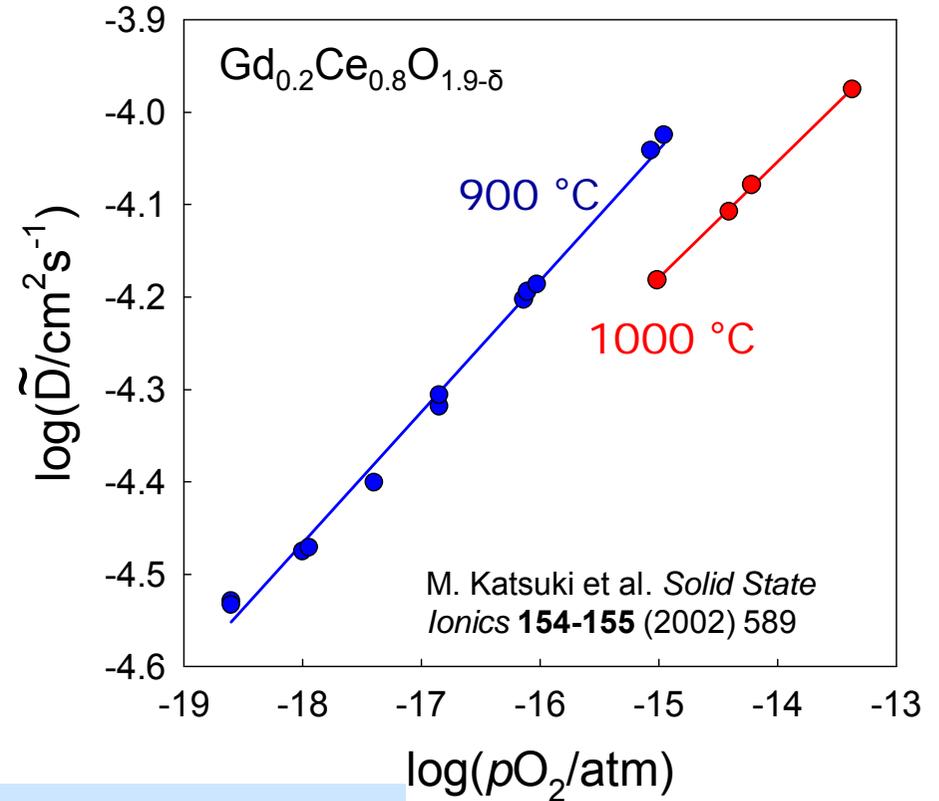
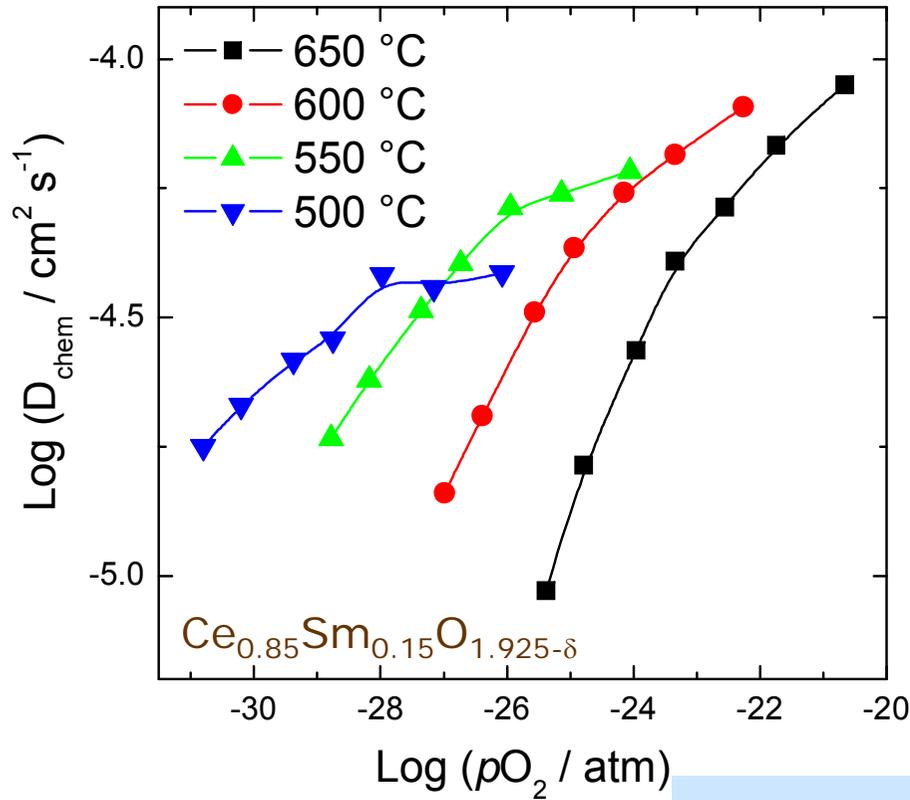
# Kinetics of Reduction and Oxidation



Both bulk and surface kinetics can influence fuel production rate



# Kinetics of Oxygen Release



$T = 1500 \text{ }^\circ\text{C}$ ,  $p\text{O}_2 = 10^{-5} \text{ atm}$   
 extrapolate:  $\tilde{D} \sim 10^{-3} \text{ cm}^2\text{s}^{-1}$

$$t = l^2 / 4\tilde{D}$$

$\sim 2 \text{ } \mu\text{m}$  particles

$t \sim 10^{-5} \text{ s}$  !!!

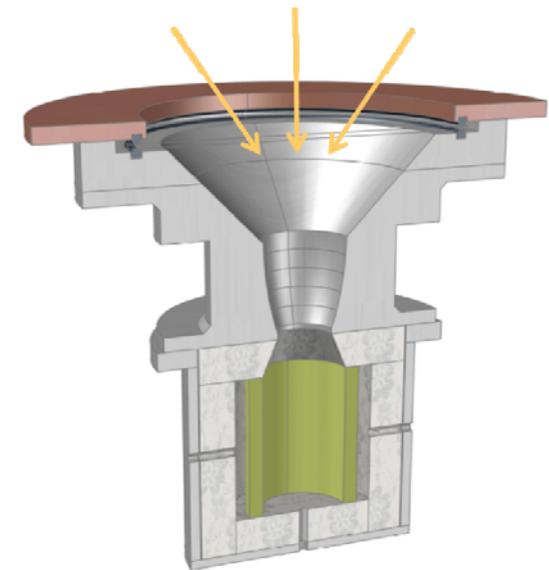
ZnO:  $10^{-15} \text{ cm}^2\text{s}^{-1}$

NiFe<sub>2</sub>O<sub>4</sub>:  $10^{-12} \text{ cm}^2\text{s}^{-1}$

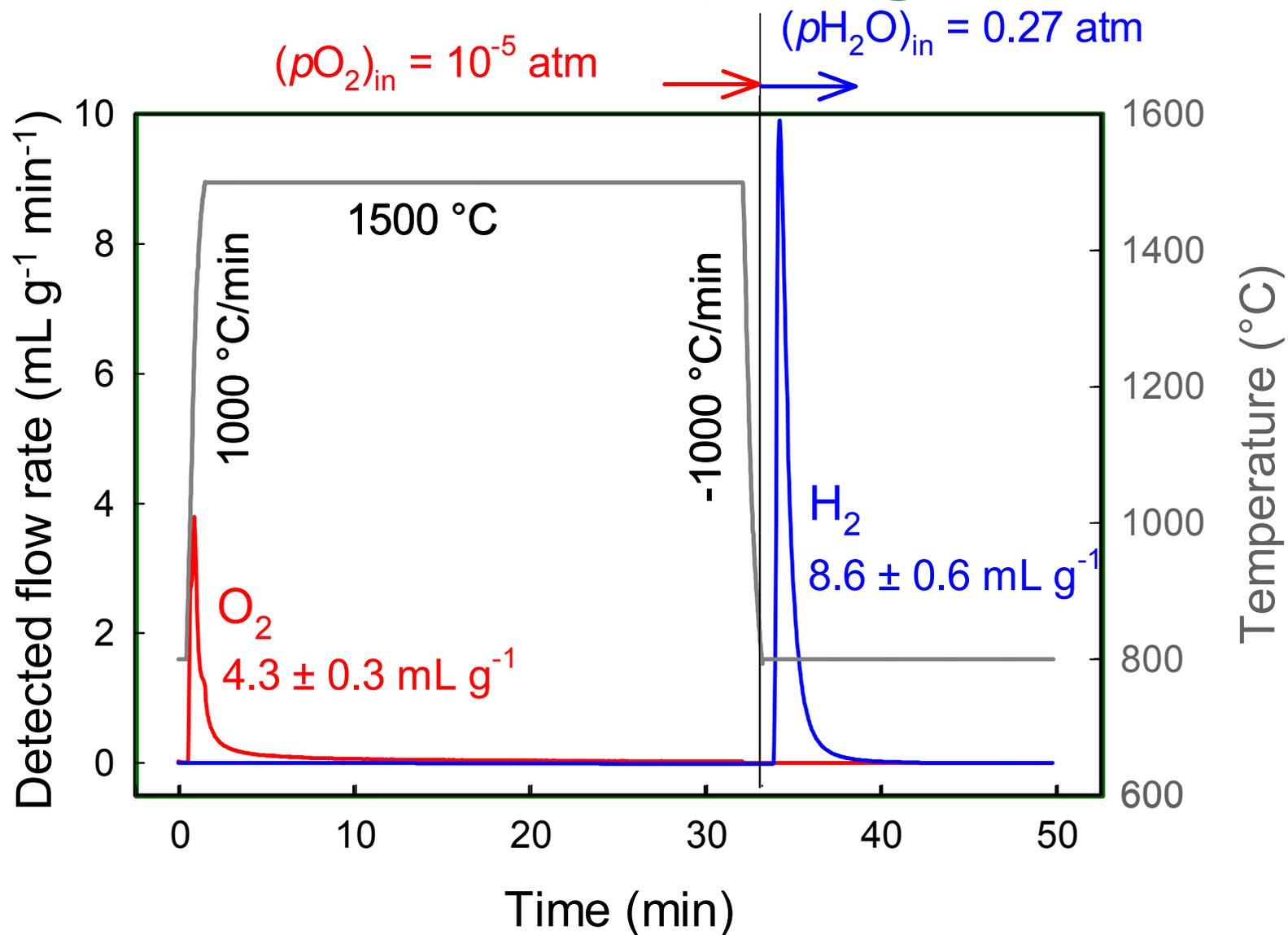


# Progressive Demonstration

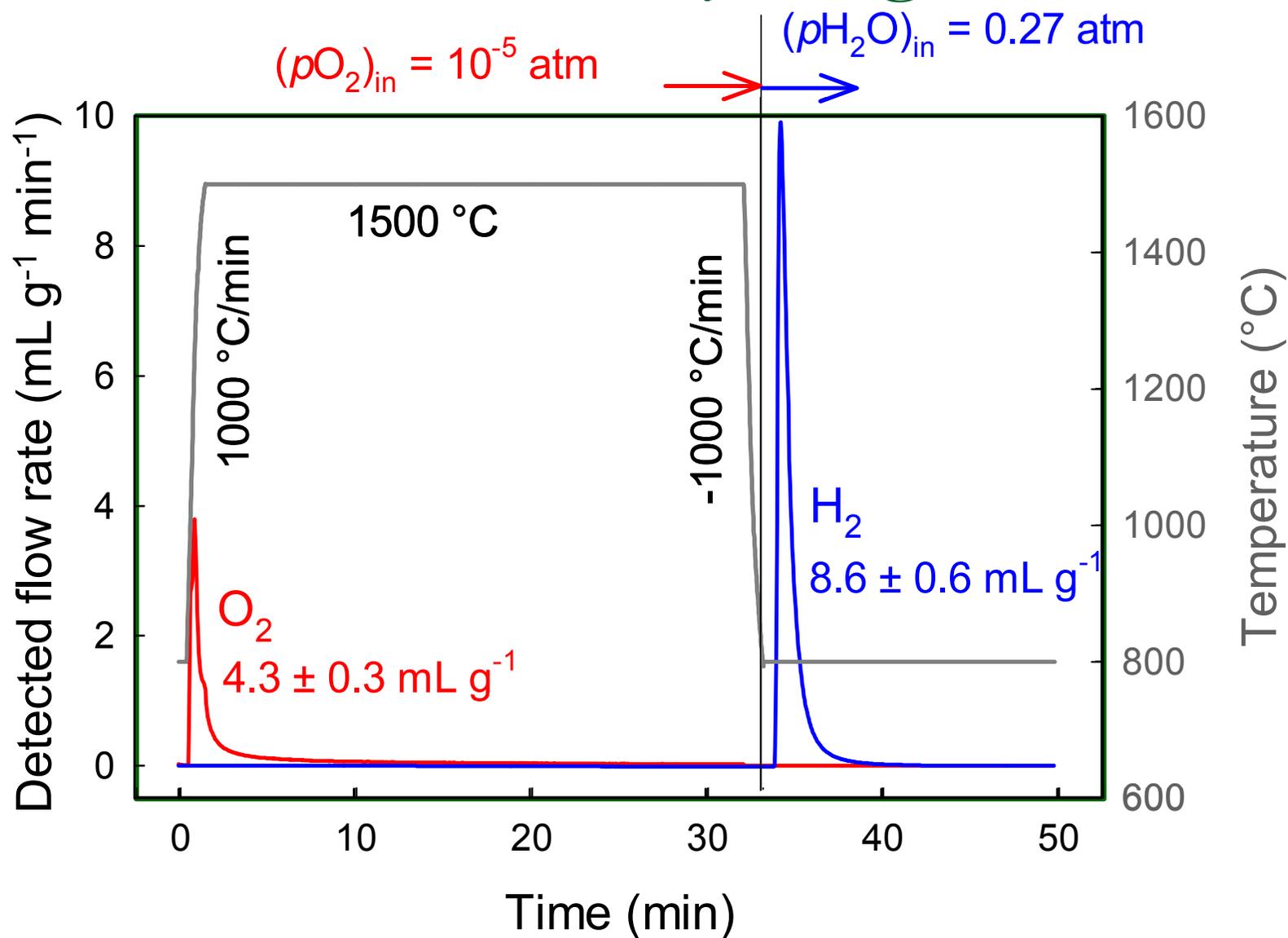
- Conventional Electric Furnace
  - ❑ Analysis by gas chromatography (quantitative)
  - ❑ Moderate temperatures, slow ramp rates
  - ❑ Surrogate reduction step using hydrogen
- IR Imaging Furnace
  - ❑ Analysis by mass spectrometry (rapid)
  - ❑ High temperatures and high ramp rates
  - ❑ Reduce under realistic gas conditions
- Solar Simulator Furnace
  - ❑ Almost direct fuels from sunlight
  - ❑ Exhaust gases to gas chromatograph
  - ❑ Challenging thermal design



# Thermochemical Cycling



# Thermochemical Cycling

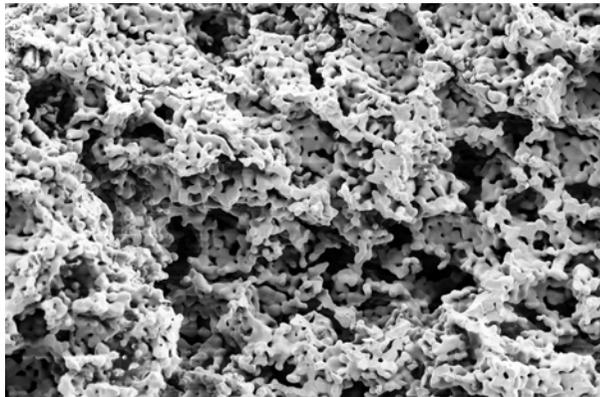
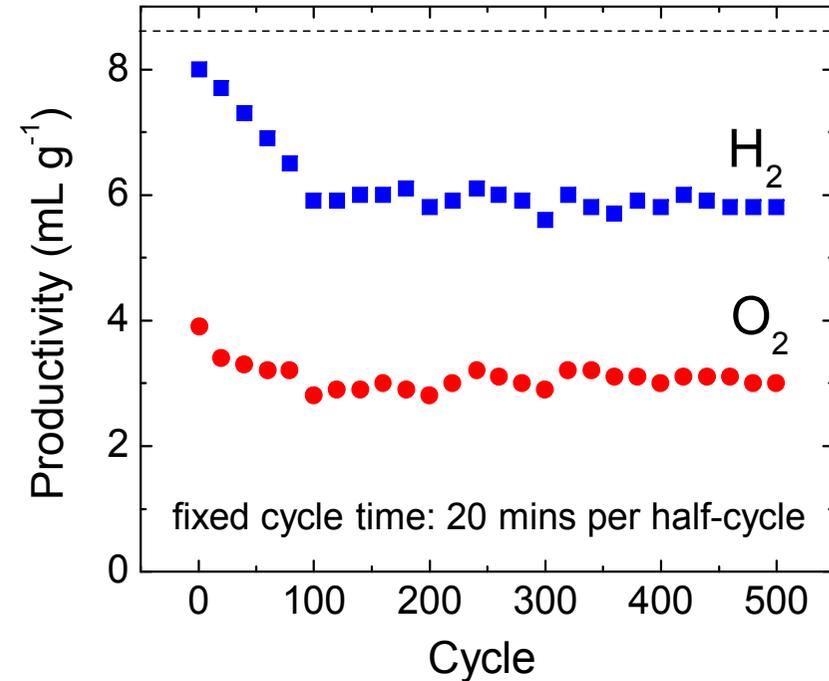
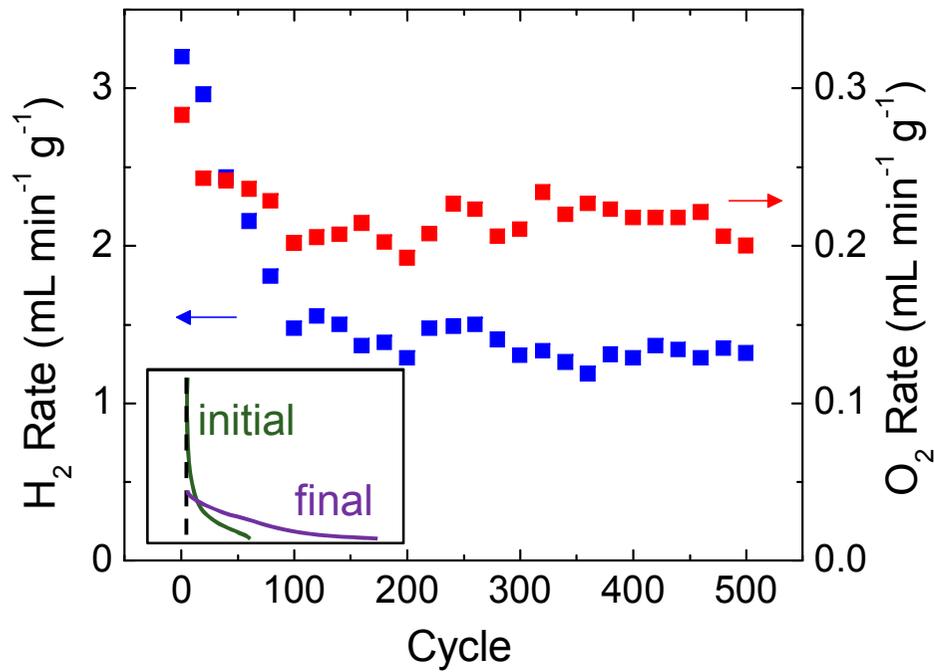


# Thermochemical Cycling

- Yield matches theoretical value of 8 mL H<sub>2</sub> per gram ceria
- Flow H<sub>2</sub>:flow O<sub>2</sub> always 2:1
- $\Rightarrow$  all of the  $\delta_H$  created is utilized in fuel production ( $\delta \rightarrow 0$  at T<sub>L</sub>)

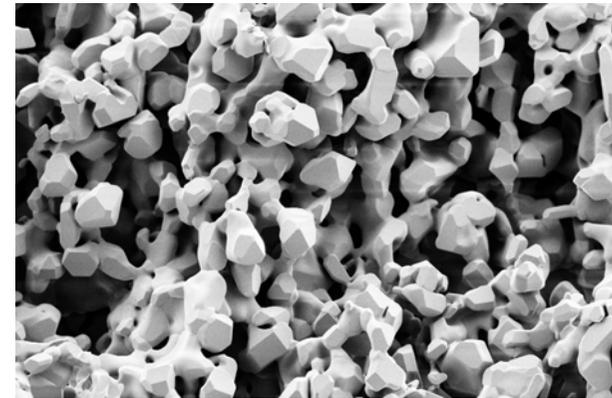


# Stability of Fuel Productivity

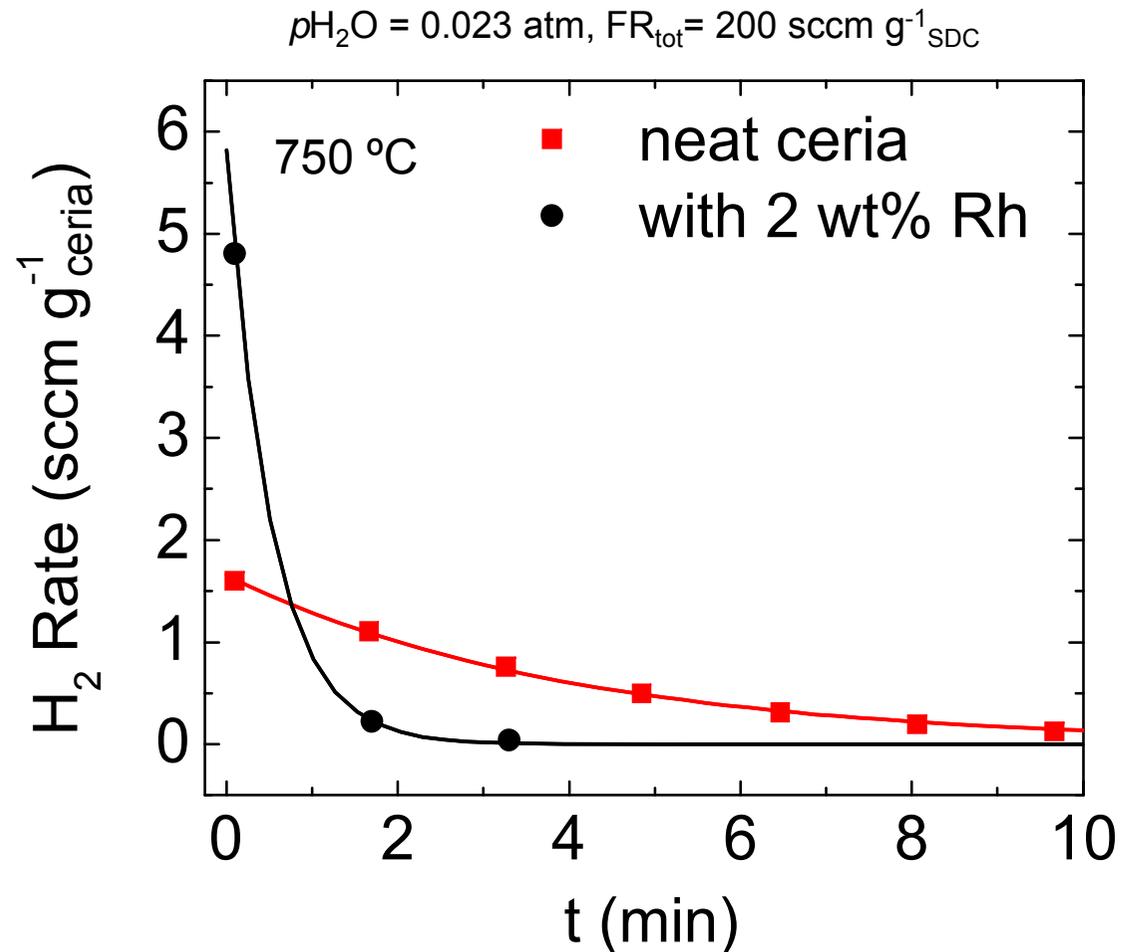
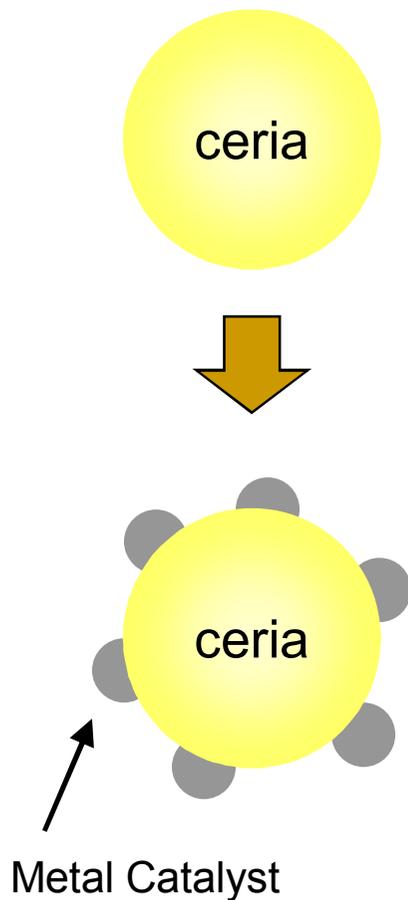


loss of surface area

surface step is rate-limiting



# Rate Limiting Step

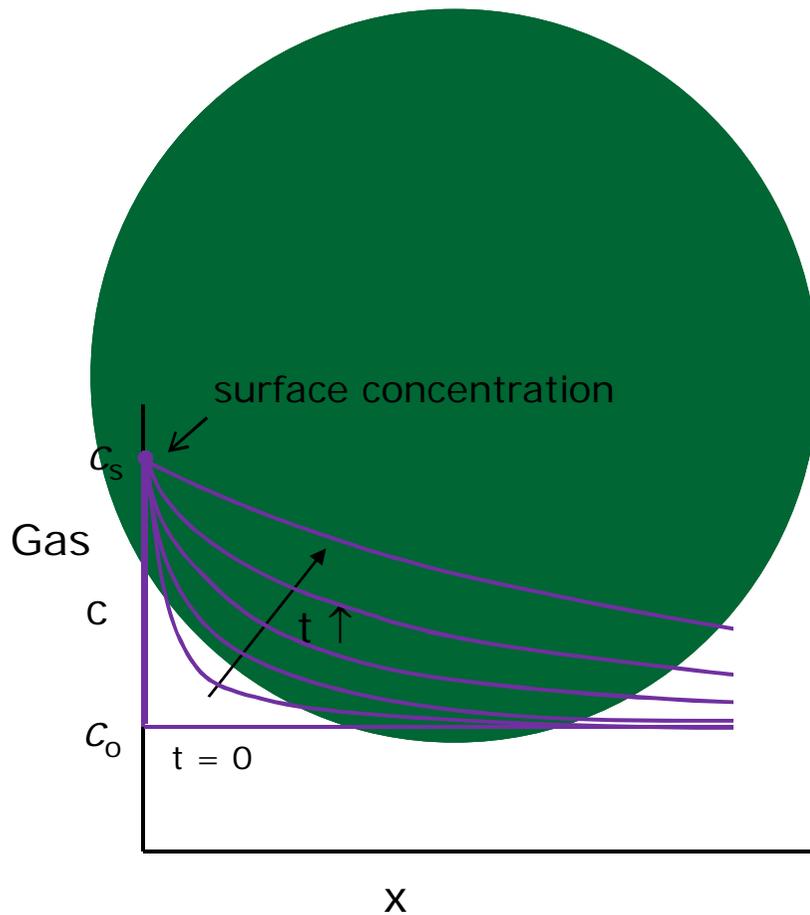


Catalyst improves kinetics → surface limited process

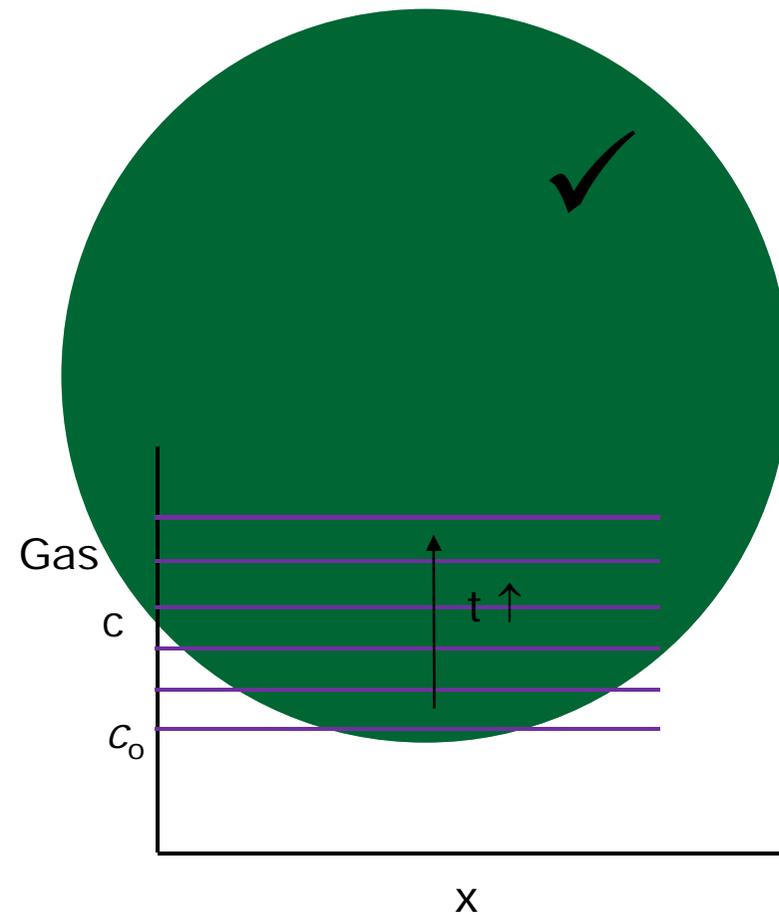


# Kinetics of Reduction and Oxidation

Diffusion controlled



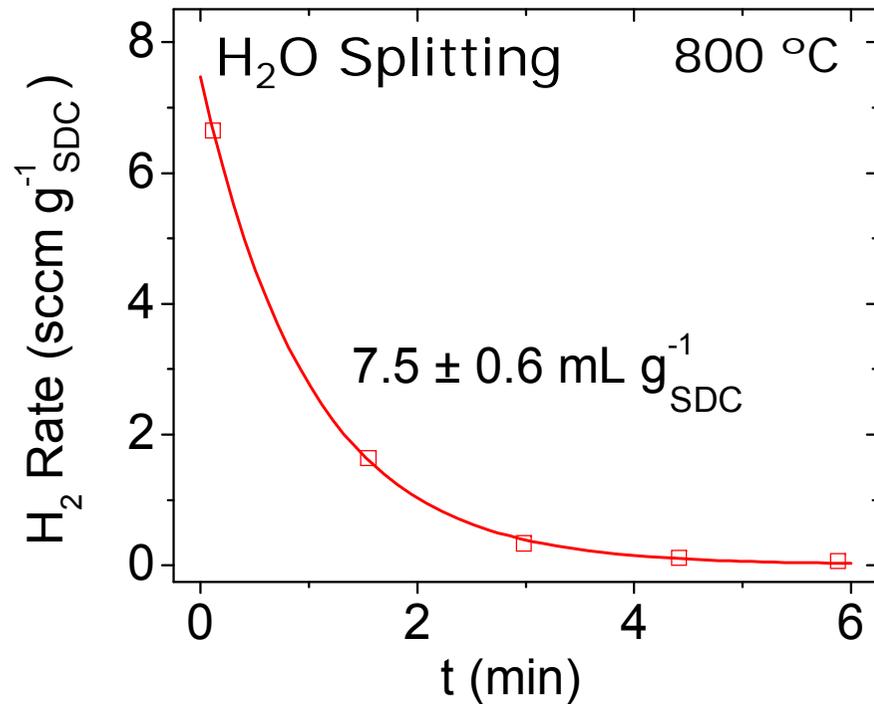
Surface reaction controlled



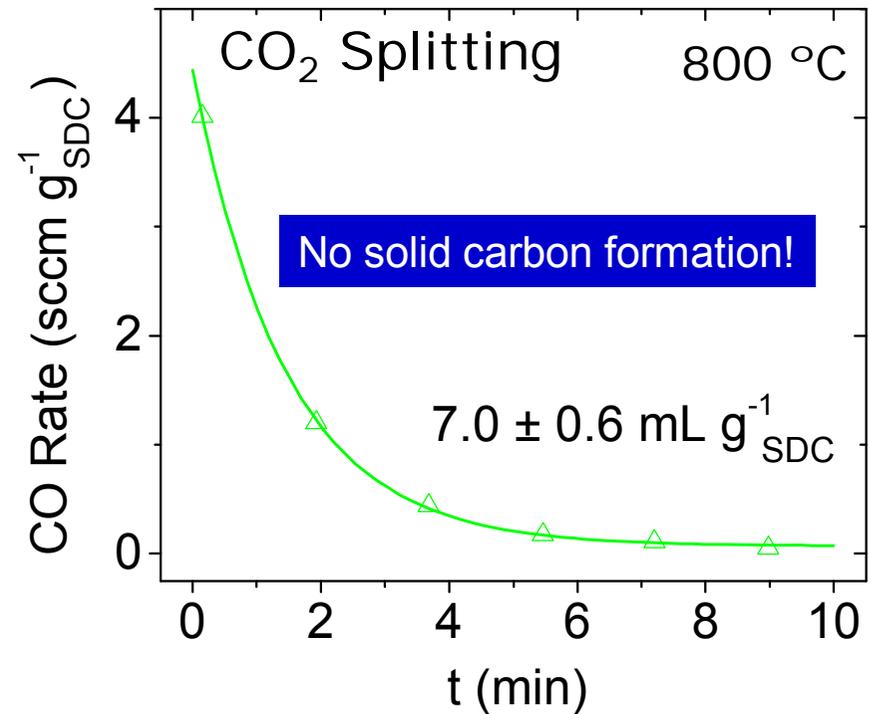
Process is dominated by surface reaction rate



# Making the Fuel of Choice



pH<sub>2</sub>O = 0.064 atm, FR<sub>tot</sub> = 380 sccm g<sup>-1</sup><sub>SDC</sub>



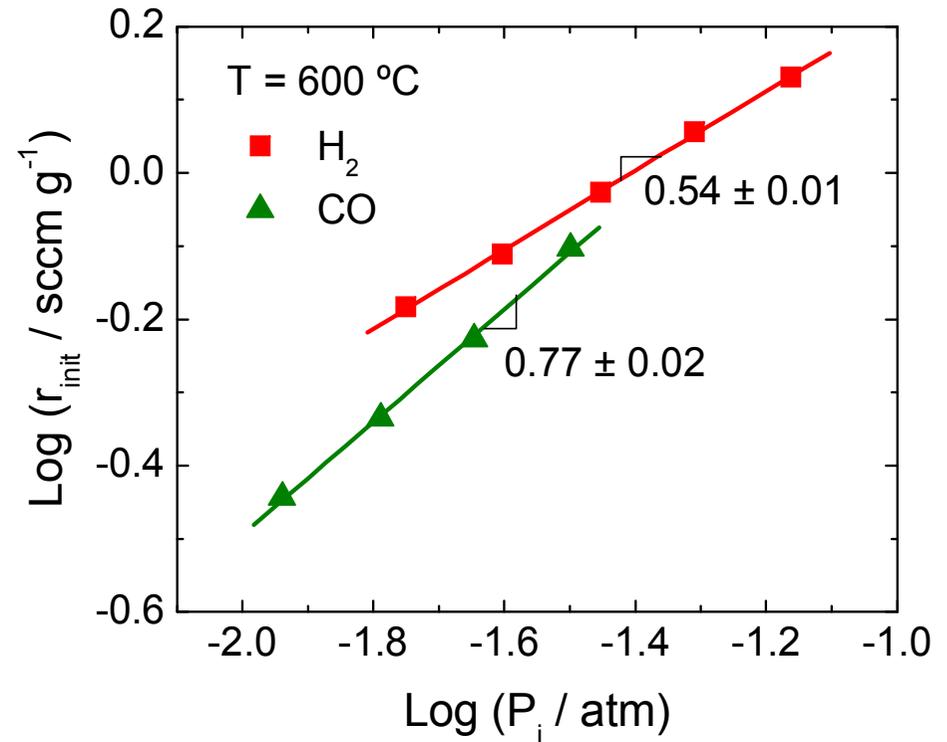
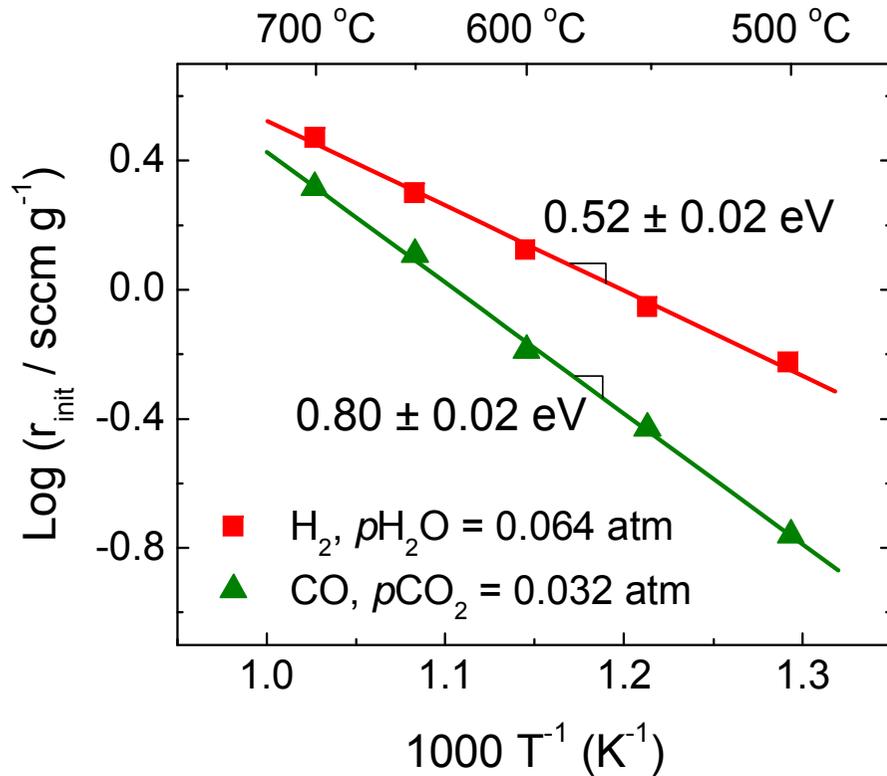
pCO<sub>2</sub> = 0.032 atm, FR<sub>tot</sub> = 300 sccm g<sup>-1</sup><sub>SDC</sub>

Complete utilization of ceria non-stoichiometry for fuel production



*SDC = samaria doped ceria*

# Fuel Production Rates

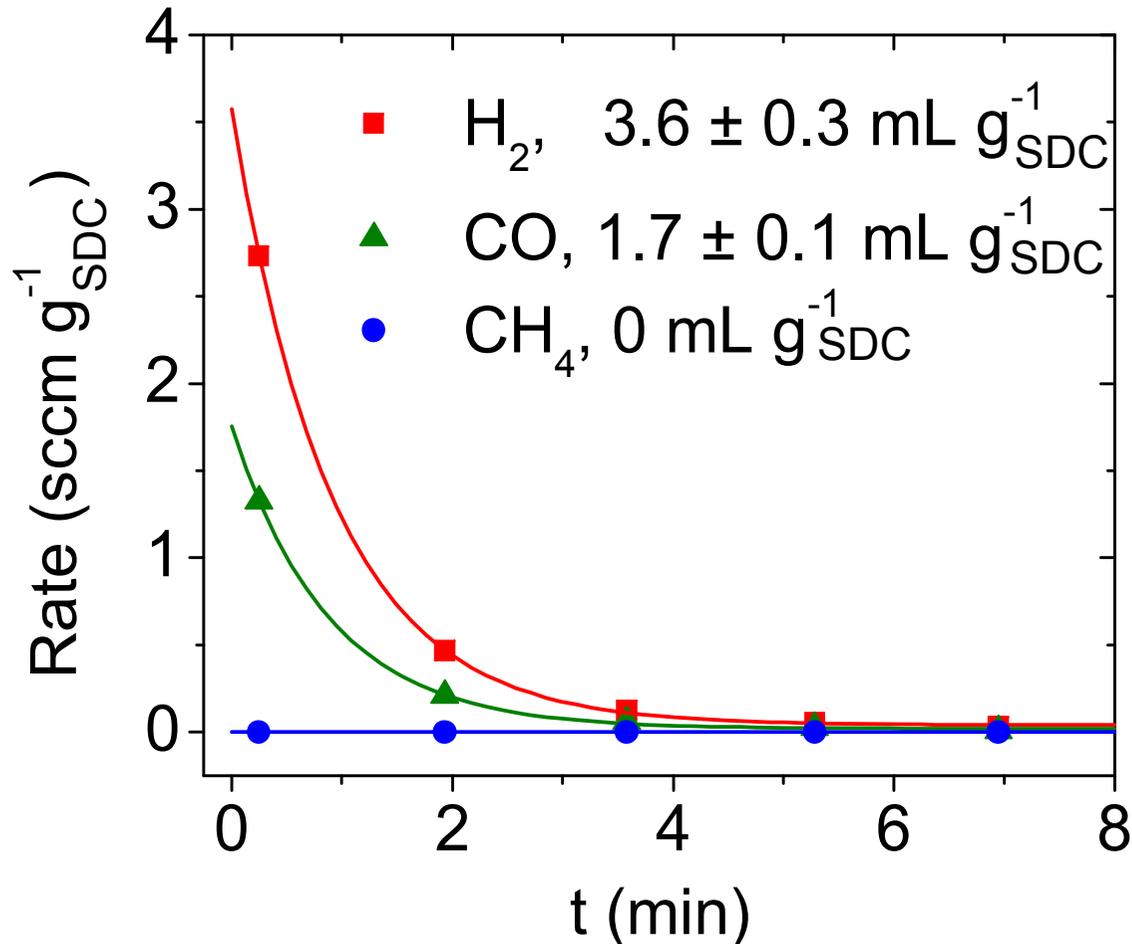


Rate depends on gas species → confirms surface reaction limited



# Making Syngas

$p_{\text{H}_2\text{O}} = 0.132 \text{ atm}$ ,  $p_{\text{CO}_2} = 0.066 \text{ atm}$ ,  $\text{FR}_{\text{tot}} = 40 \text{ sccm g}^{-1}_{\text{SDC}}$ ,  $900 \text{ }^\circ\text{C}$



**$\sim 20,000 \mu\text{L min}^{-1} \text{g}^{-1}$**

$900 \text{ }^\circ\text{C}$ ;  $0.66 \text{ atm } p_{\text{H}_2\text{O}}$ ;  $0.34 \text{ atm } p_{\text{CO}_2}$

**$\sim 2 \mu\text{L min}^{-1} \text{g}^{-1}$**

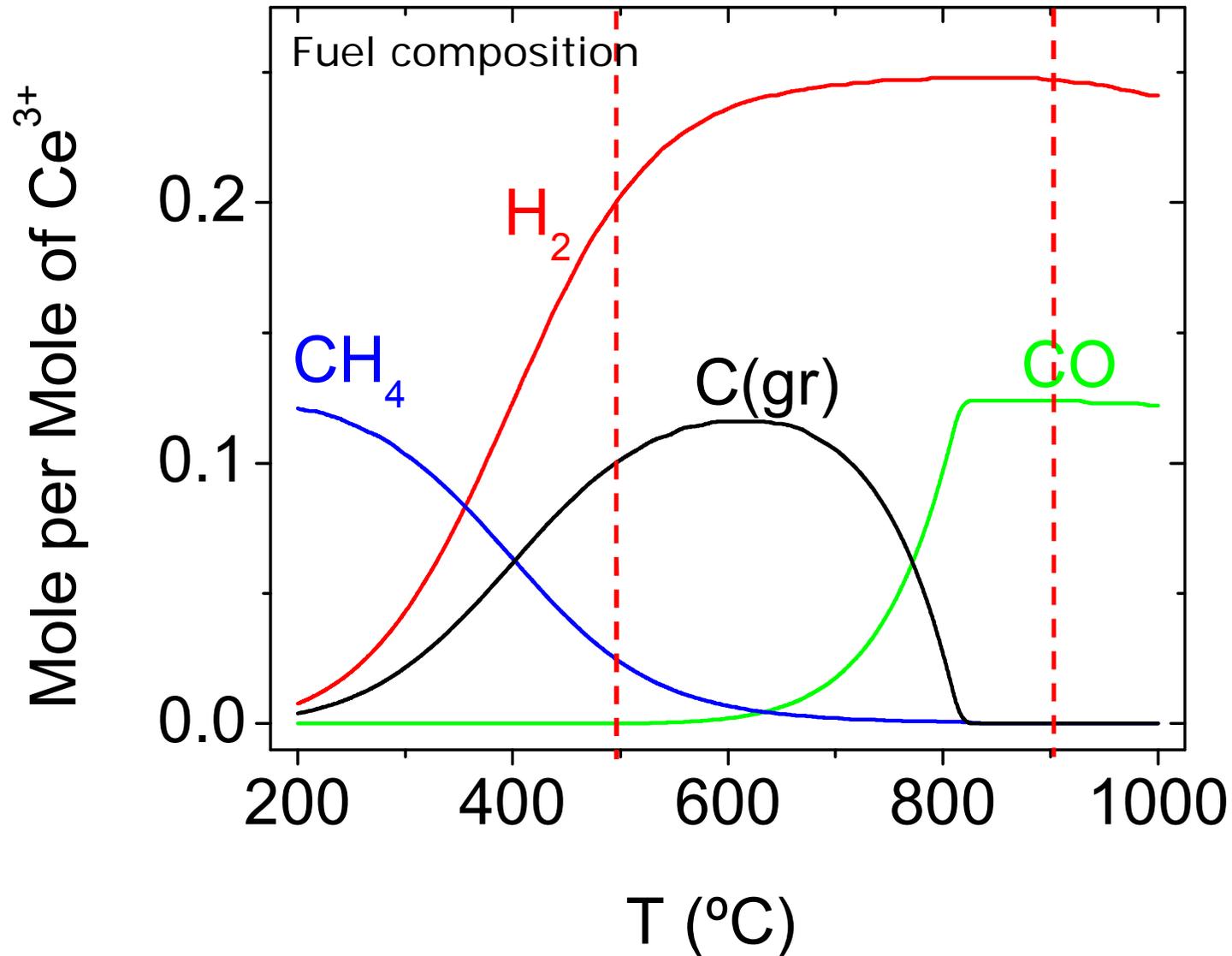
N-doped  $\text{TiO}_2$  nanotubes

Grimes, Nano Lett., 2009, 9 (2), pp 731–737



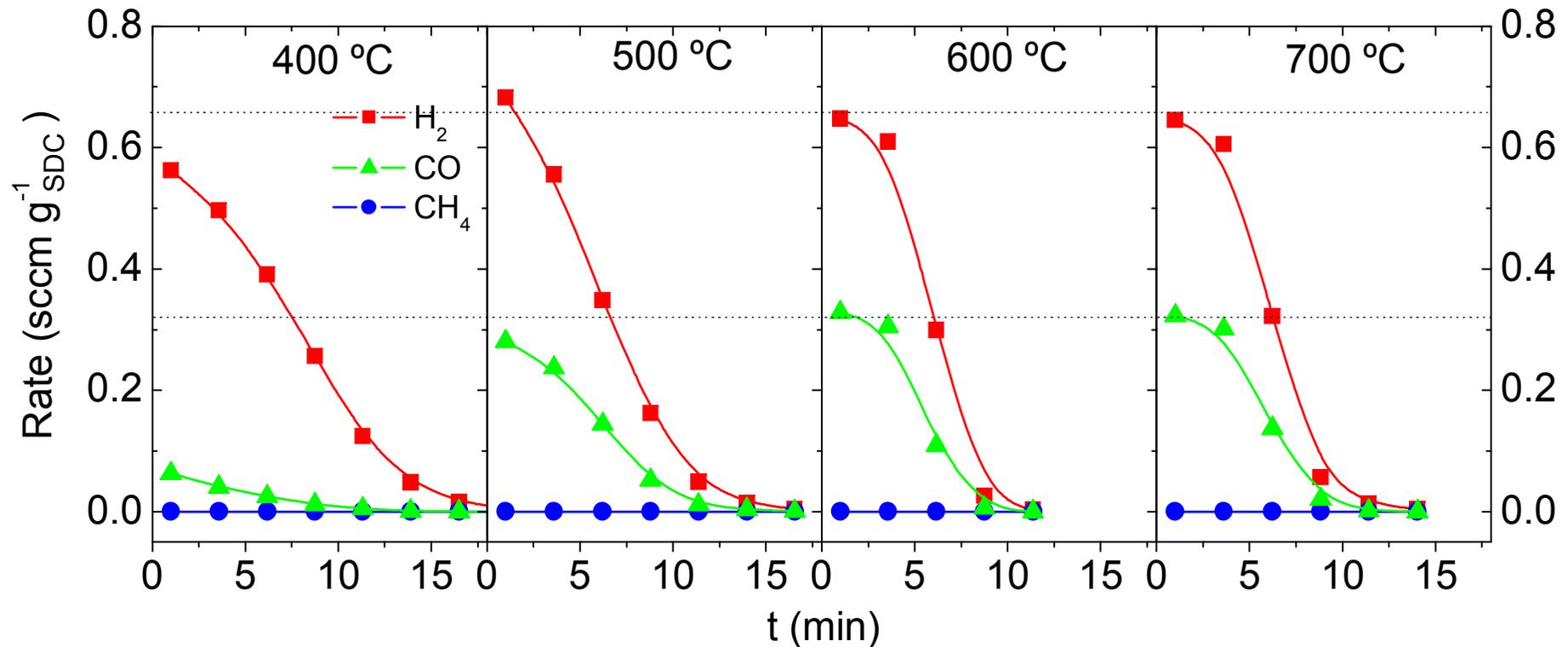
Complete utilization of ceria nonstoichiometry

# Thermodynamic Prediction



# Measured Fuel Composition

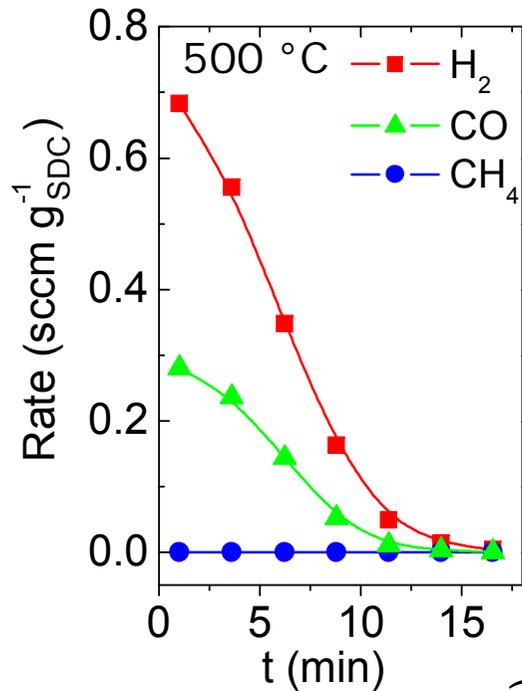
$p_{\text{H}_2\text{O}} = 0.064 \text{ atm}$ ,  $p_{\text{CO}_2} = 0.032 \text{ atm}$ ,  $\text{FR}_{\text{tot}} = 10 \text{ sccm g}_{\text{SDC}}^{-1}$



100% syngas selectivity – no methane produced

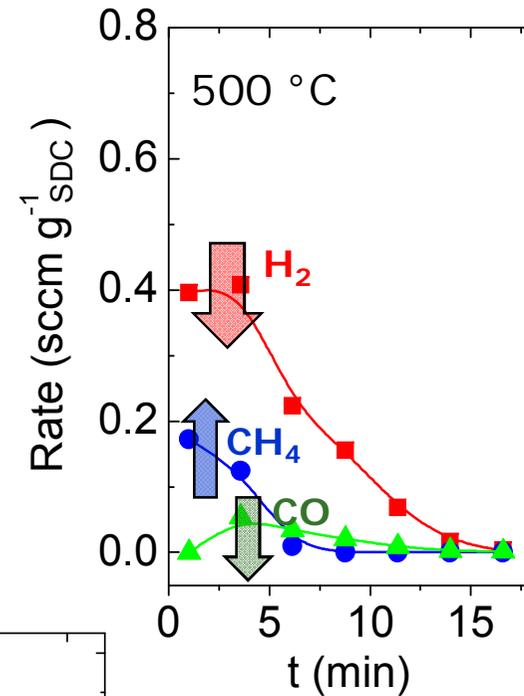


# Producing Methane?

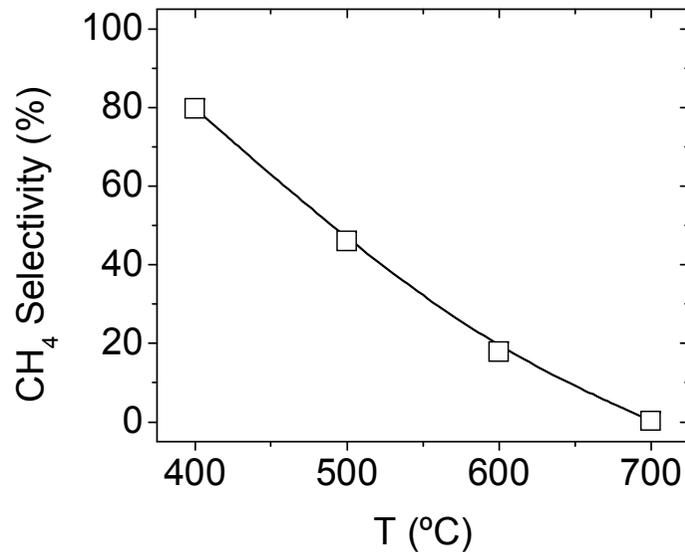


$p_{\text{H}_2\text{O}} = 0.064 \text{ atm}$   
 $p_{\text{CO}_2} = 0.032 \text{ atm}$   
 $\text{FR}_{\text{tot}} = 10 \text{ sccm g}^{-1}_{\text{SDC}}$

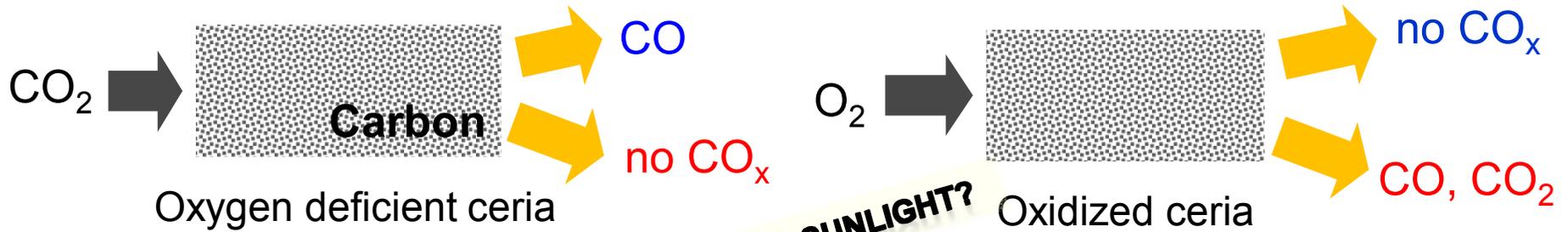
Add Ni catalyst



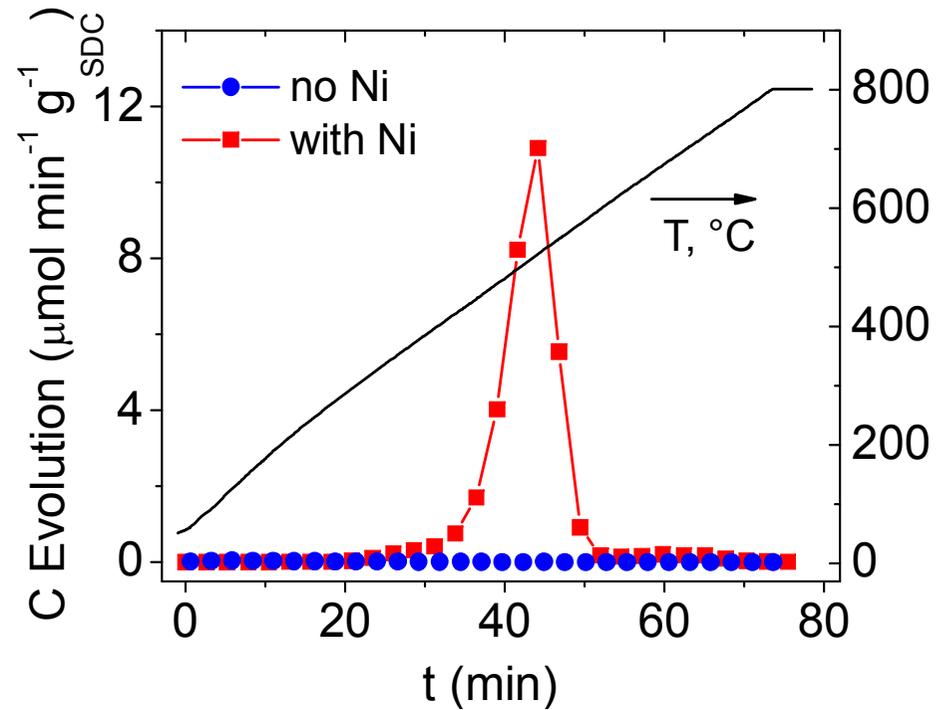
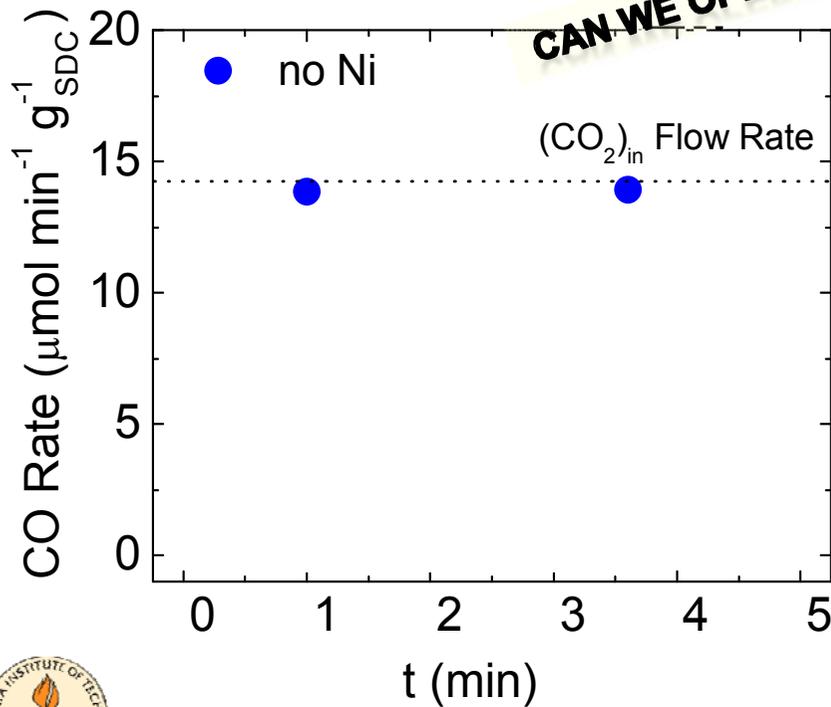
due to "transient" carbon deposition



# Ni induces Carbon Deposition



**CAN WE OPERATE ON SUNLIGHT?**



# Operating on Photons

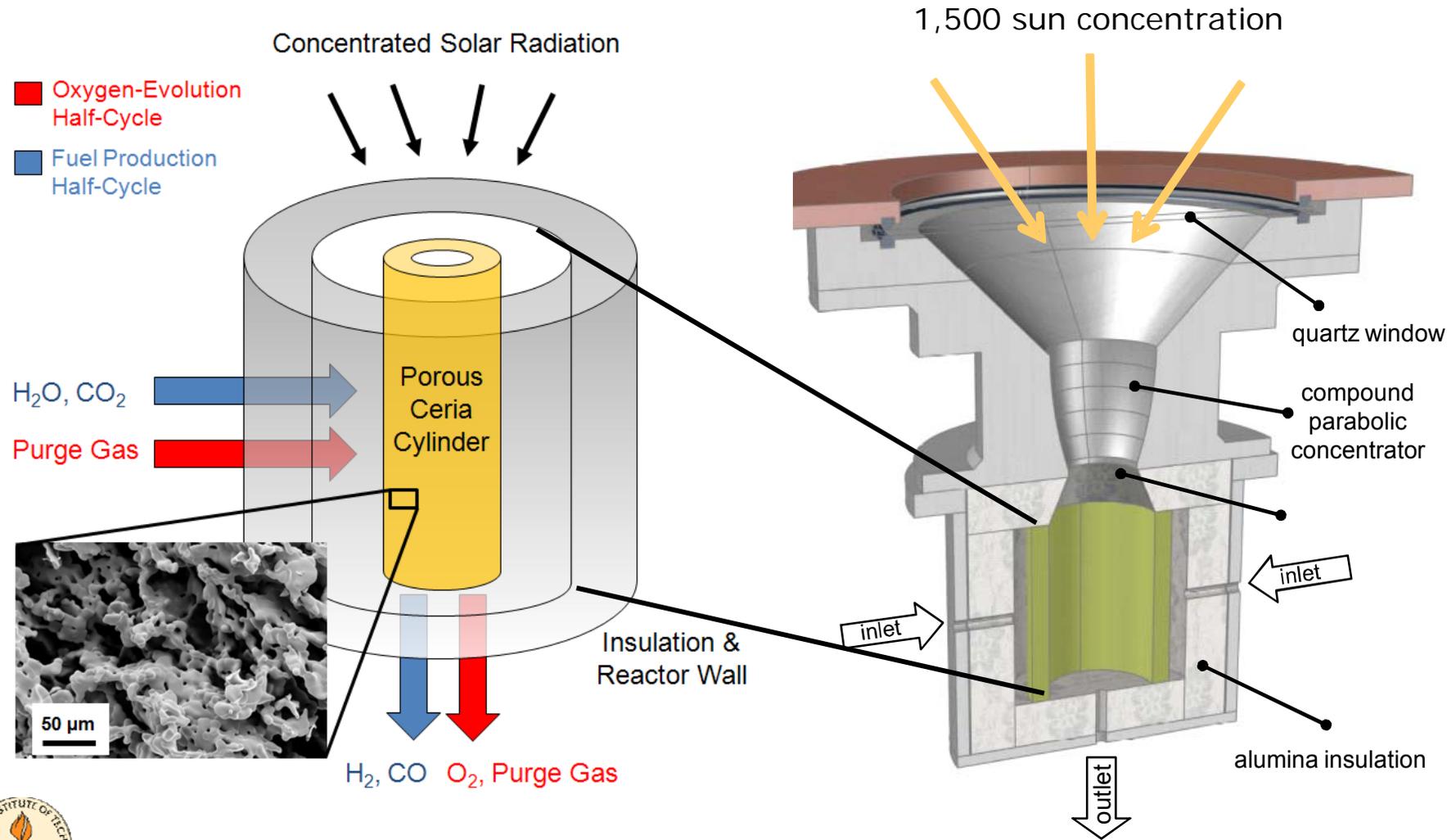
Switzerland in March



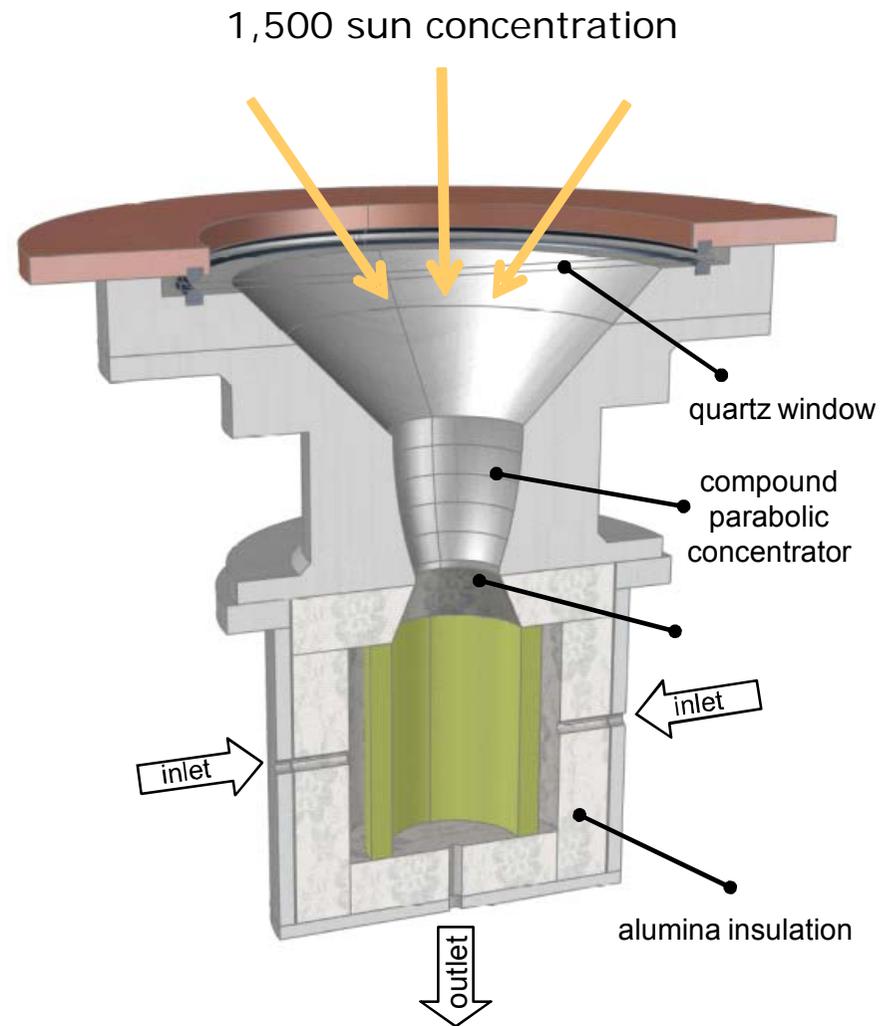
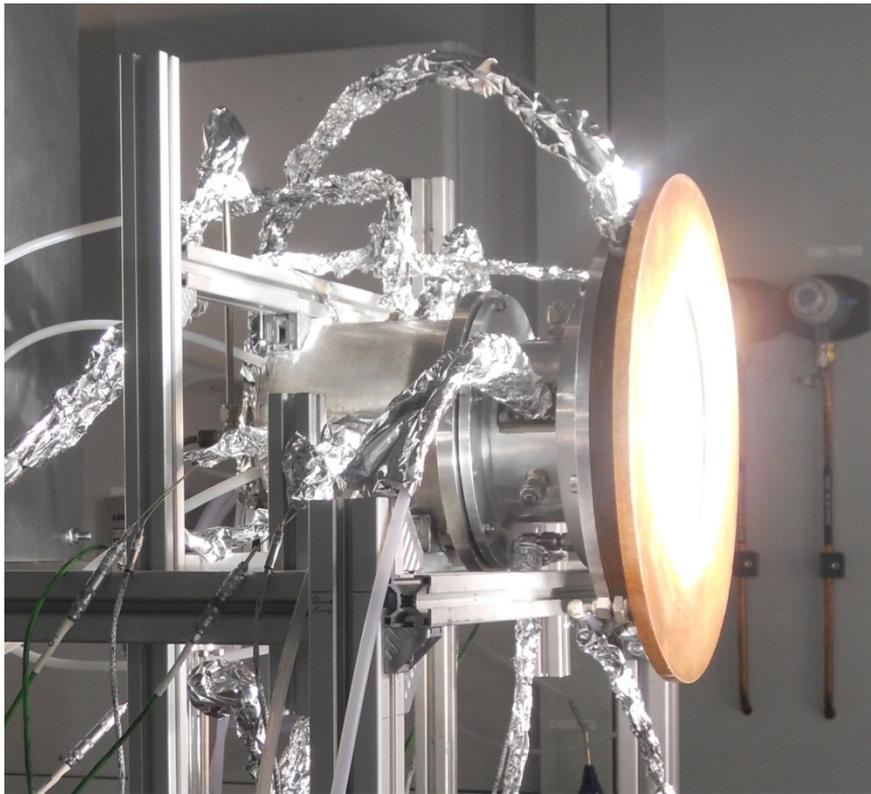
Collaboration with Aldo Steinfeld, ETH Zurich and the Paul Scherer Institute



# Under Simulated Solar Radiation

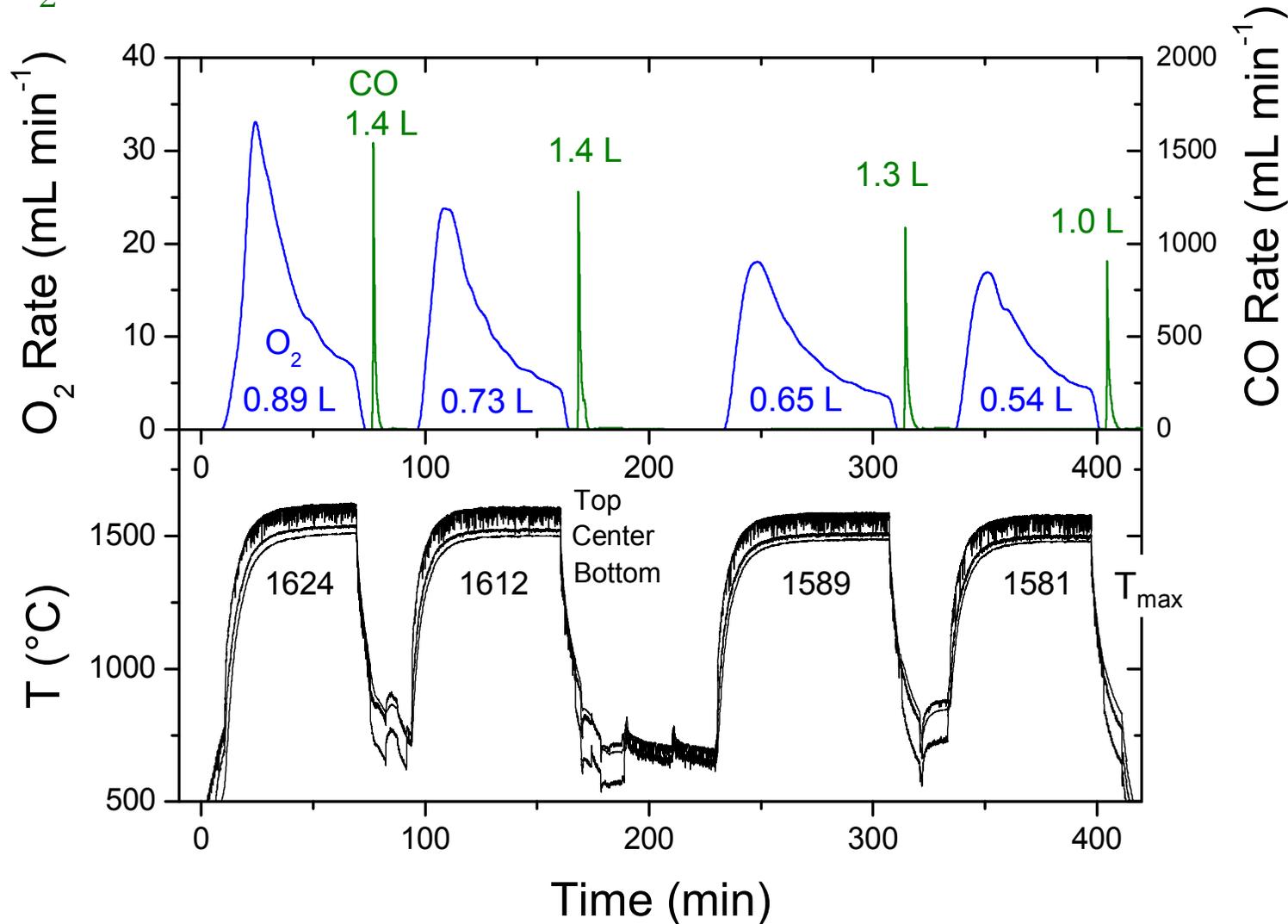


# Under Simulated Solar Radiation



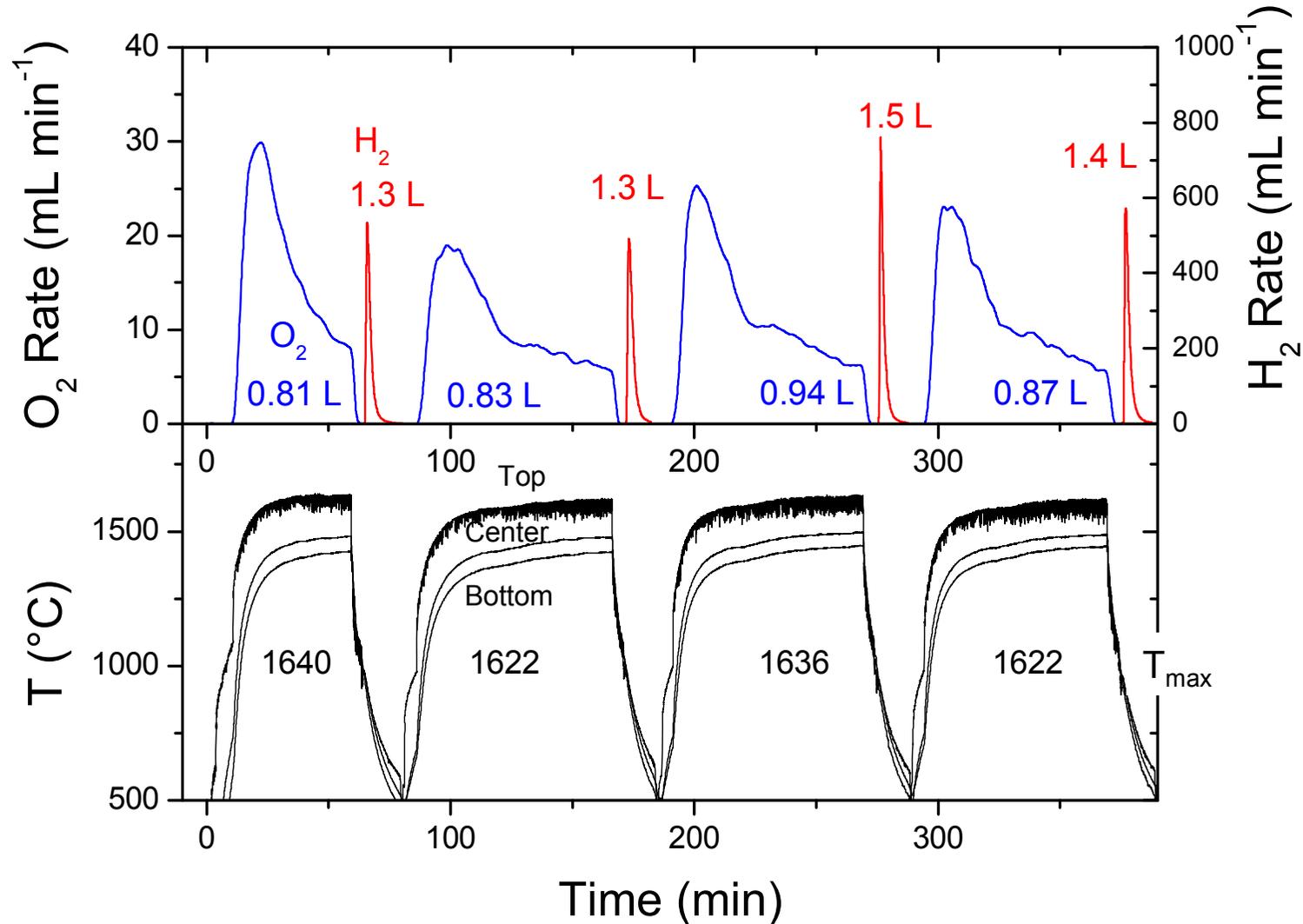
# Under Simulated Solar Radiation

CO<sub>2</sub> dissociation

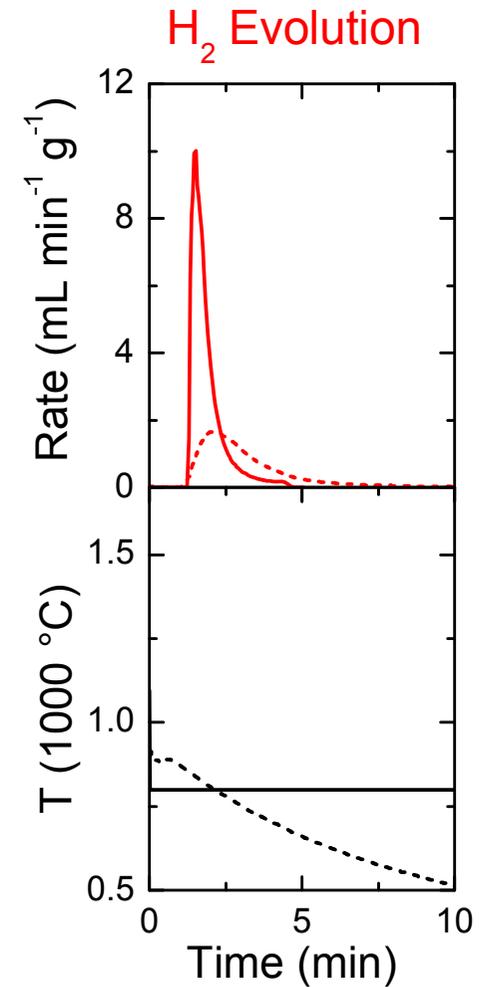
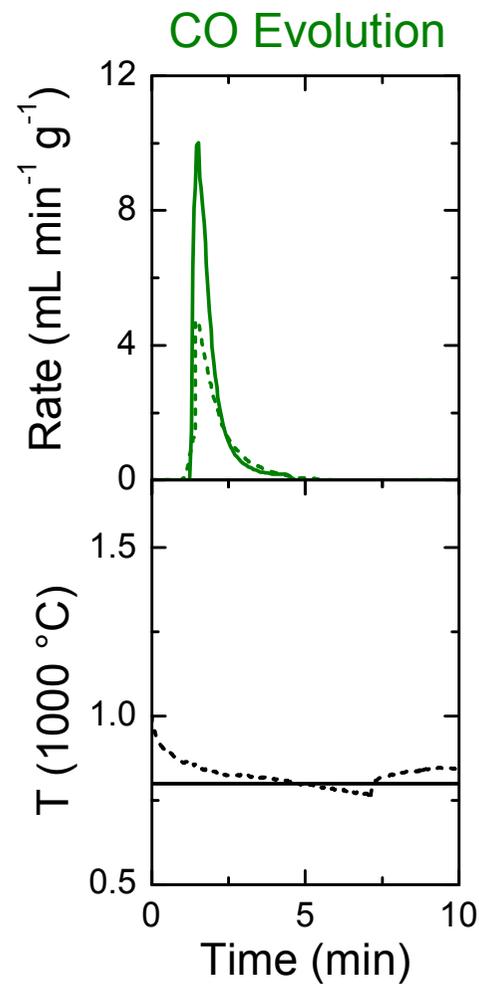
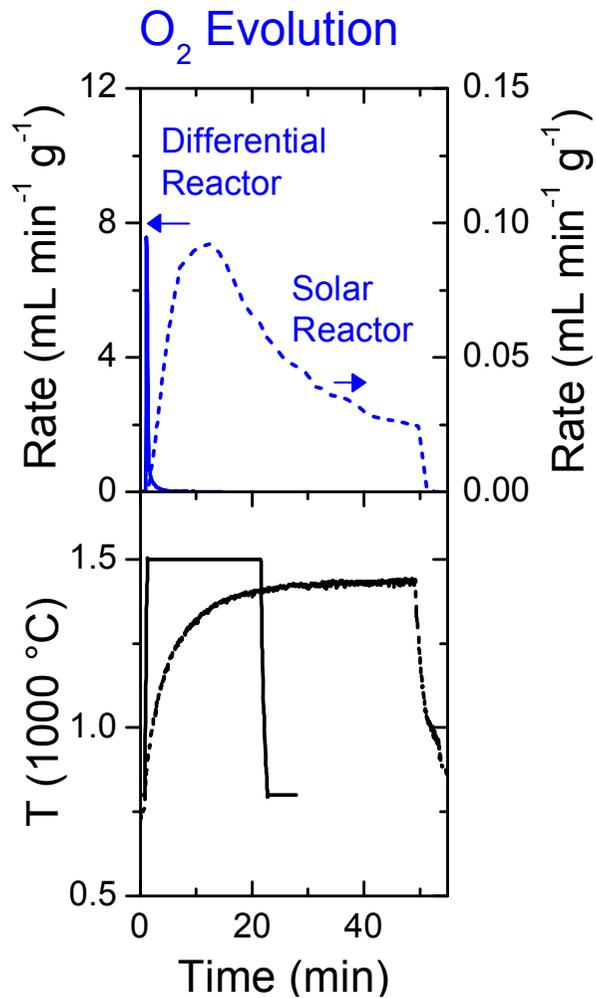


# Under Simulated Solar Radiation

H<sub>2</sub>O dissociation

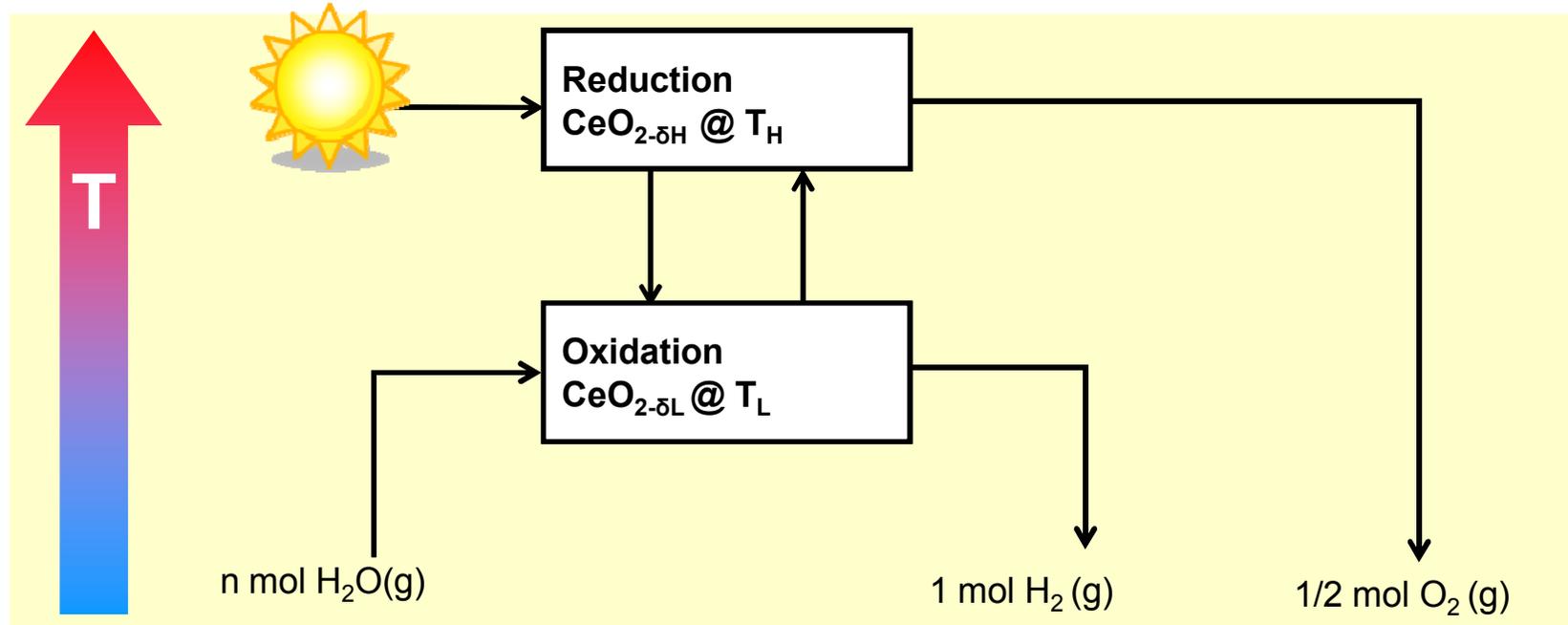


# Impact of Thermal Management



Heat losses in solar reactor have major detrimental impact on efficiency

# Thermodynamic Efficiency



$$\eta = \eta_{solar-thermal} \times \eta_{thermal-fuel} = \eta_{solar-thermal} \times \frac{285.8kJ}{\Delta H_{input}}$$

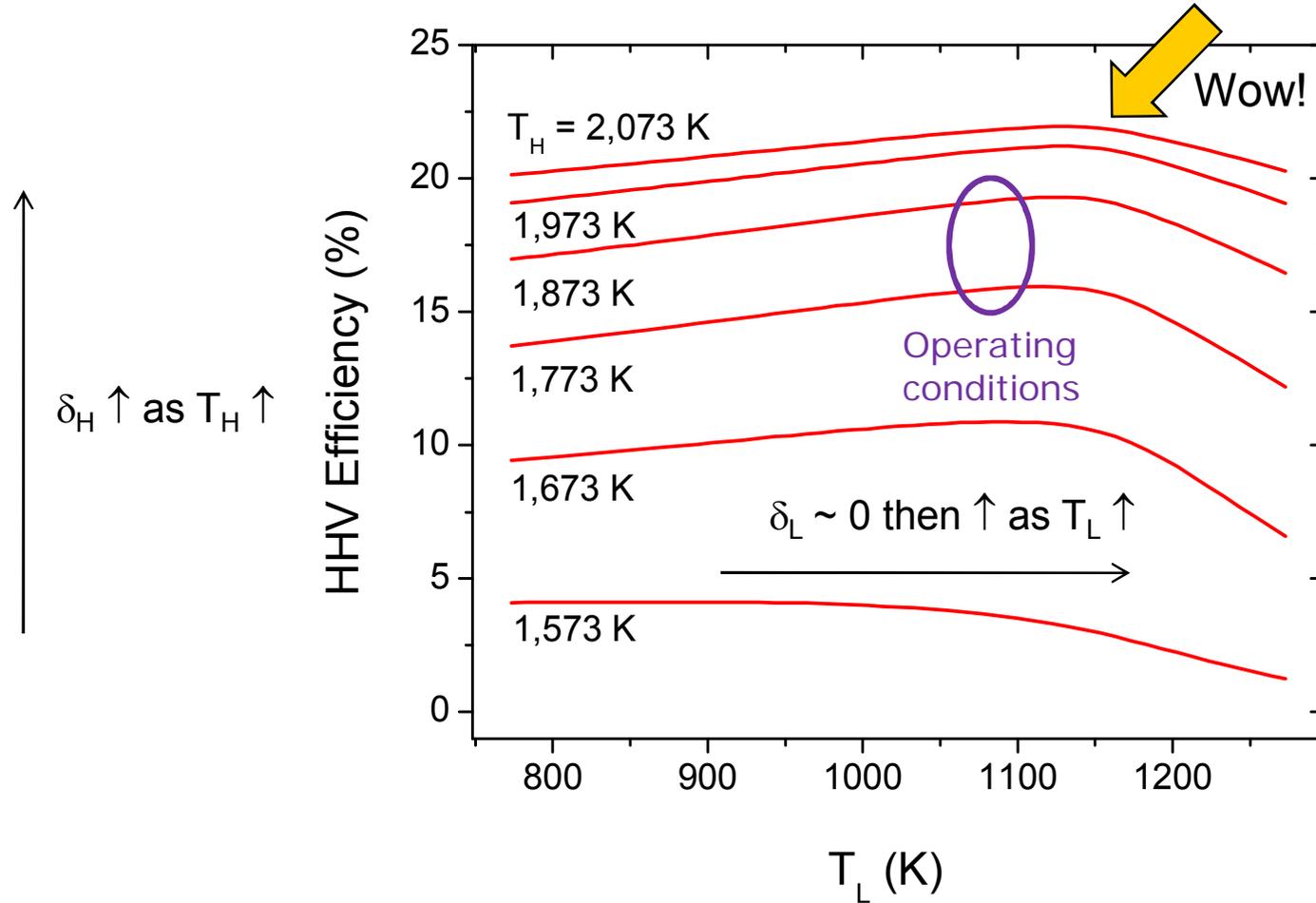
$$\Delta H_{input} = \text{Boil and heat water to } T_L + \text{Heat ceria from } T_L \text{ to } T_H + \text{Reduce ceria}$$



# Influence of Cycling Parameters

decreasing  $\Delta T$  lowers waste heat

too small  $\Delta T$  generates too little fuel



Analysis ignores potential of heat recovery



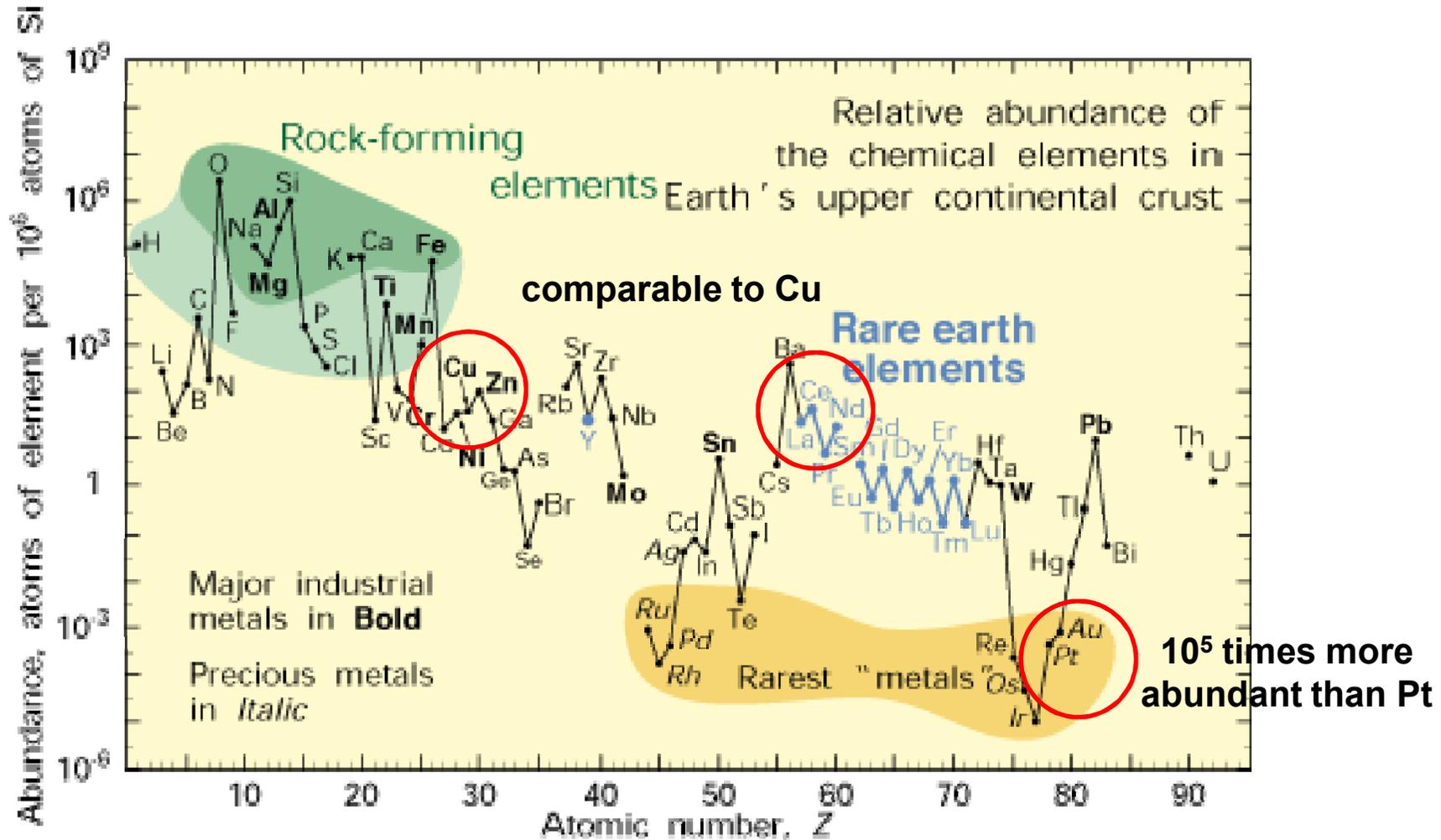
# Actual Reactor Efficiency

$$\eta = \frac{r_{fuel} \Delta H_{fuel}}{P_{solar} + r_{inert} E_{inert}}$$

- Estimate at 0.5 to 1%
  - Reactor heat-up is slow  $\Rightarrow P_{solar}$  is large
    - Heat loss through insulation
    - Re-radiation losses through quartz window
  - Material keeps up with heating rate
    - Immediate efficiency improvements from better reactor design
    - No need to enhance surface reaction rates
  - Material with lower temperature cycling
    - Would ease requirements on reactor design



# Earth Abundance



Source: USGS

~ 40 MT world reserve



# Conclusions & Challenges

**Conclusion:** *Ceria works really, really well!*

## Scientific Challenges

- Thermodynamic measurements at very high temp

## Engineering Challenges

- Thermal management
- How to flush high temperature oxygen?
- Efficiency (cost!) tied to  $\Delta\delta$

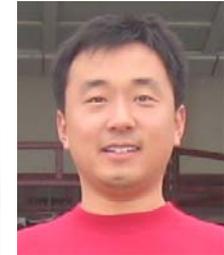
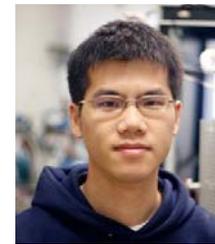
## Grand Challenge

- Design of new materials
  - Wider nonstoichiometry range ( $\text{CeO}_2$ - $\text{ZrO}_2$  solid solutions)
  - Maintain structural stability, non-volatility?



# Acknowledgments

- William, Danien, Yong
- Aldo Steinfeld & students
- National Science Foundation
- Gordon and Betty Moore Foundation
  - Caltech Center for Sustainable Energy Research
- eSolar (Philip Gleckman)



- W.C. Chueh and S. M. Haile, “Cerium as a Thermochemical Reaction Medium for Selectively Generating Syngas or Methane from H<sub>2</sub>O and CO<sub>2</sub>,” *ChemSusChem*, **2**, 735-769 (2009).
- W. C. Chueh and S. M. Haile, “A Thermochemical Study of Cerium: Exploiting an Old Material for New Modes of Energy Conversion and CO<sub>2</sub> Mitigation,” *Phil. Trans. R. Soc.* **368**, 3269-3294 (2010).
- W.C. Chueh, C. Falter, M. Abbott, D. Scipio, P. Furler, S. M. Haile and A. Steinfeld, “High-Flux Solar-Driven Thermochemical Dissociation of H<sub>2</sub>O and CO<sub>2</sub> Using Nonstoichiometric Cerium,” *Science*, **330**, 1797-1801 (2010).

