



2269-14

Workshop on New Materials for Renewable Energy

17 - 21 October 2011

First-principles modeling of electrochemical reactions for solar-tofuel energy storage

> Simone PICCININ CNR-IOM Istituto Officina dei Materiali Trieste Italy





First-principles modeling of electrochemical reactions for solar-to-fuel energy storage

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Artificial photosynthesis: using light to make fuels

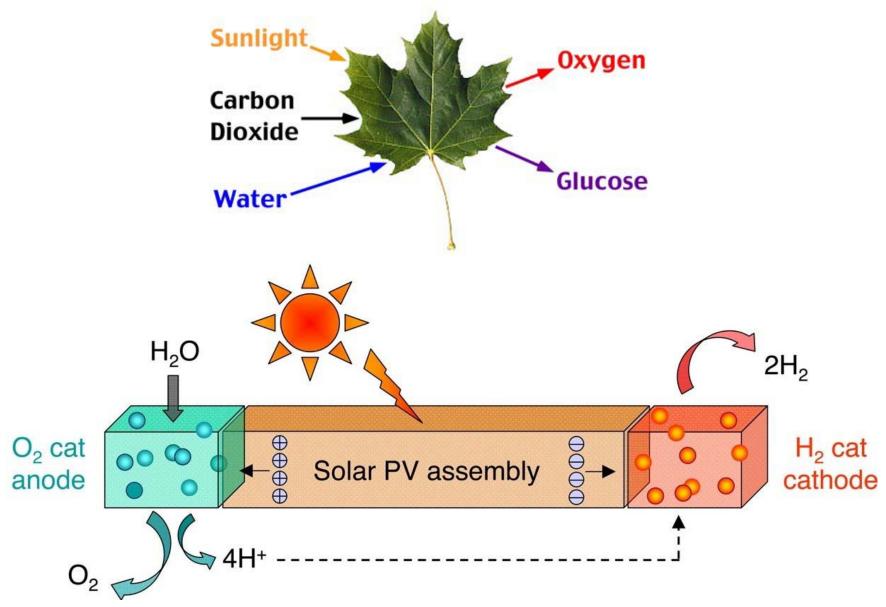
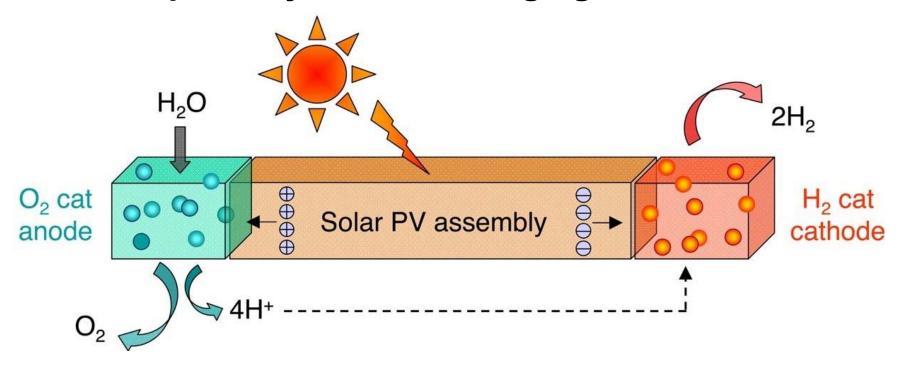


Figure from: Lewis and Nocera, PNAS 103, 15729 (2006)

Artificial photosynthesis: using light to make fuels



Overall reaction: $2H_2O \rightarrow O_2 + 2H_2$ $(\Delta G^0 = 4.92 \text{ eV}, E^0 = -1.23 \text{ V})$

Oxidation: $2H_2O \to O_2 + 4H^+ + 4e^- (E^0 = 1.23 \text{ V})$

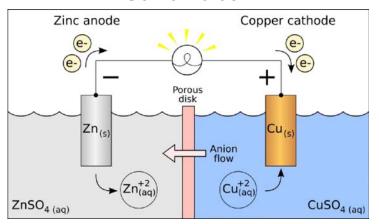
Reduction: $2H^+ + 2e^- \rightarrow H_2$ (E⁰ = 0.00 V)

Outline

- Reduction potentials, free energies, reference electrodes ...: a quick overview of electrochemistry
- Lessons from the oxygen evolving complex in PSII
- Theoretical approaches for modeling electrochemical reactions:
 - (a) Nørskov's approach
 - (b) Applications to OER on metal and metal-oxide surfaces

Electrochemistry: a quick overview

Galvanic cell



$$Cu^{2+}(aq) + Zn(s) \rightarrow Cu(s) + Zn^{2+}(aq)$$

Cathode (Red): $Cu^{2+}(aq) + 2e^{-} \rightarrow Cu(s)$

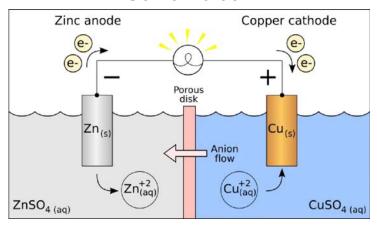
Anode (Ox): $Zn(s) \rightarrow Zn^{2+}(aq) + 2e^{-}$

Zn is oxidized (e⁻removed from Zn)

Cu is reduced (e⁻ donated to Cu)

Electrochemistry: a quick overview

Galvanic cell



$$Cu^{2+}(aq) + Zn(s) \rightarrow Cu(s) + Zn^{2+}(aq)$$

Cathode (Red): $Cu^{2+}(aq) + 2e^{-} \rightarrow Cu(s)$ Anode (Ox): $Zn(s) \rightarrow Zn^{2+}(aq) + 2e^{-}$

E⁰: standard reduction potential

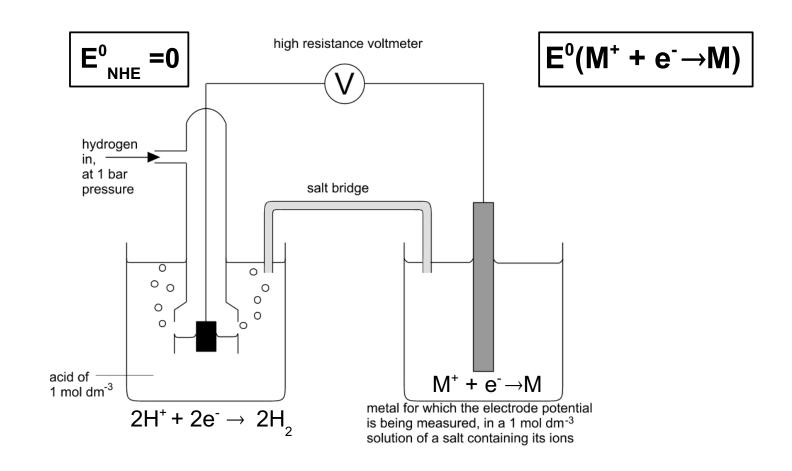
Cu²⁺(aq) + 2e⁻
$$\rightarrow$$
 Cu(s) E⁰ = 0.34 V
Zn²⁺(aq) + 2e⁻ \rightarrow Zn(s) E⁰ = -0.76 V
E⁰ = 0.34 - (-0.76) = 1.10 V

$$-nFE^0 = \Delta G^0$$

Higher E⁰: reduction

Lower E⁰: oxidation

Normal (Standard) Hydrogen Electrode (NHE)

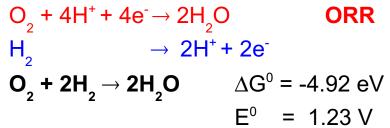


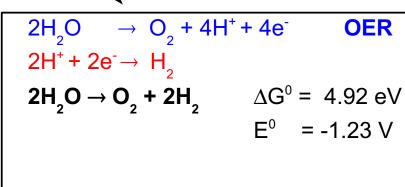
Electrochemistry: a quick overview



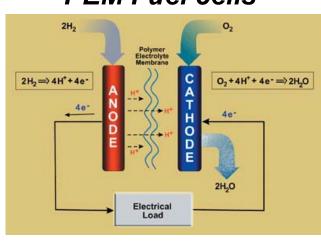
$$O_2 + 4H^+ + 4e^- \rightarrow 2H_2O$$
 $E^0 = 1.23 \text{ V}$
 $2H^+ + 2e^- \rightarrow H_2$ $E^0 = 0.00 \text{ V}$

Higher E^0 : reduction Lower E^0 : oxidation -nFE⁰ = ΔG^0

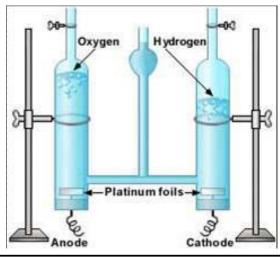




PEM Fuel cells

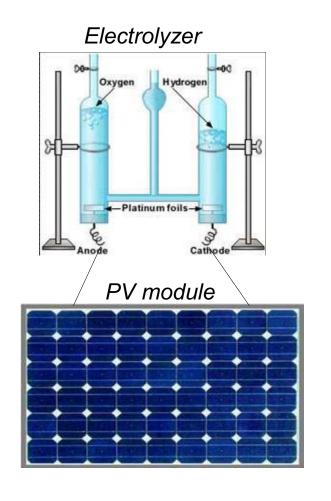


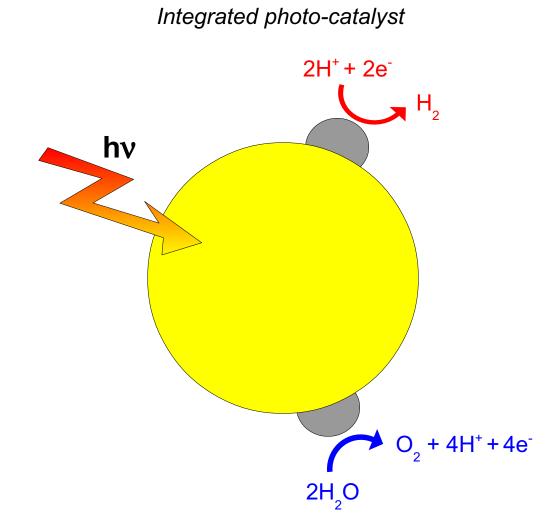
Electrolysis



Artificial photosynthesis: using light to make fuels

Goal: storing solar energy through water splitting

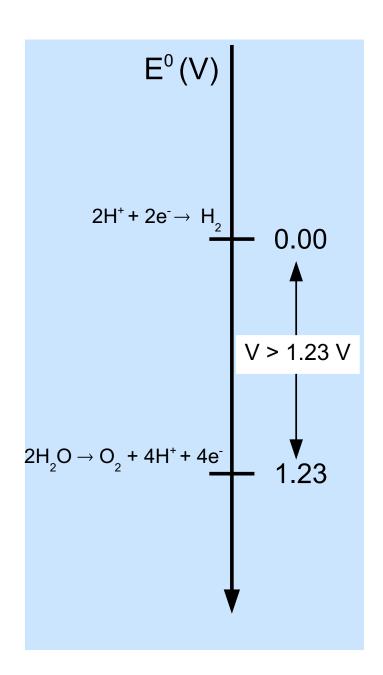




Energy level alignment

Higher E⁰: reduction Lower E⁰: oxidation

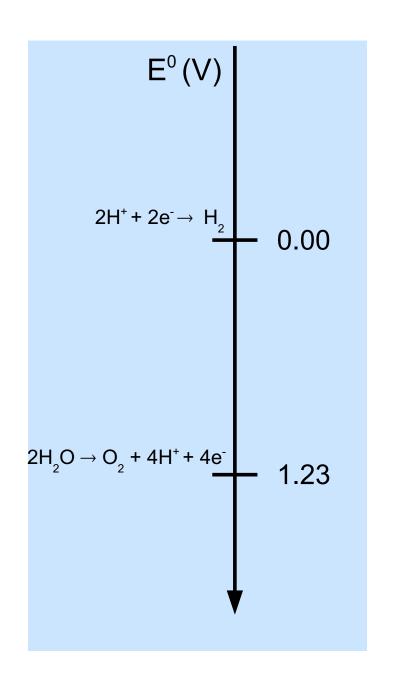
 $-nFE^0 = \Delta G^0$

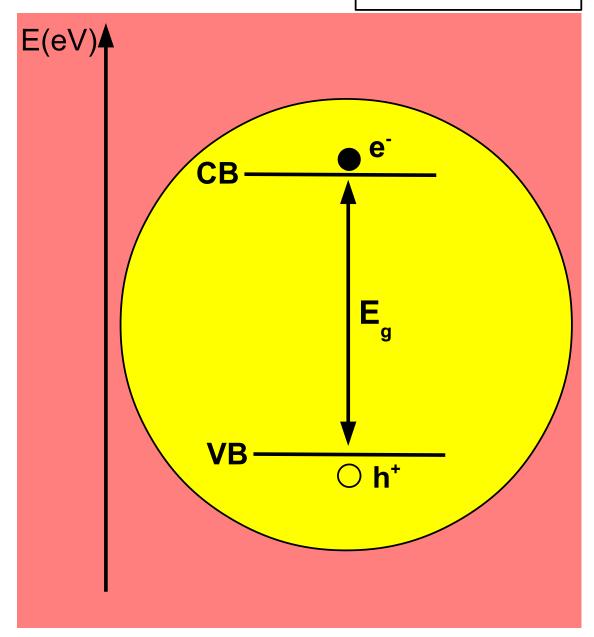


Energy level alignment

Higher E⁰: reduction Lower E⁰: oxidation

 $-nFE^0 = \Delta G^0$

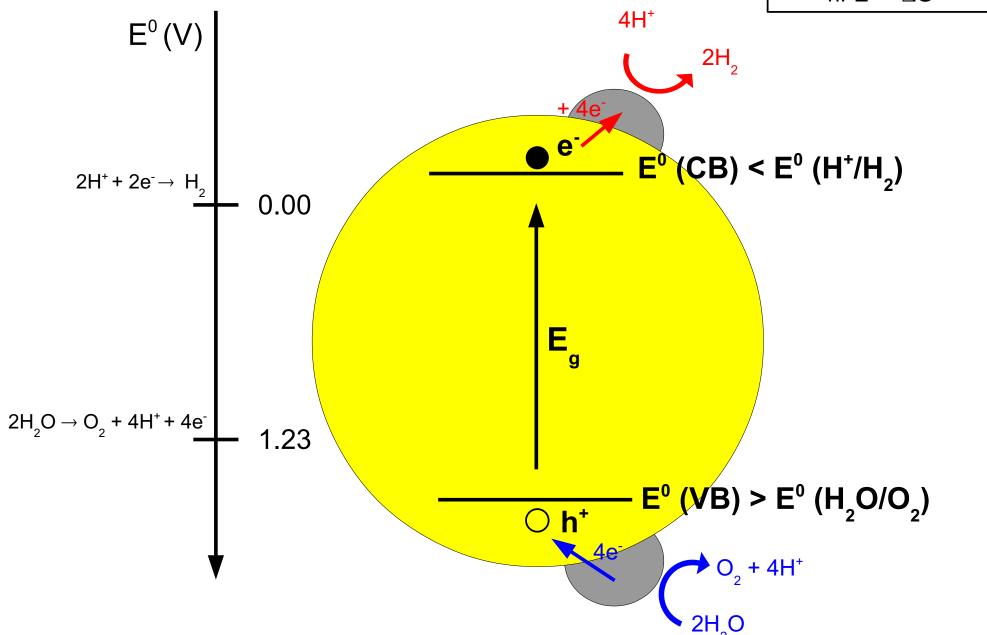




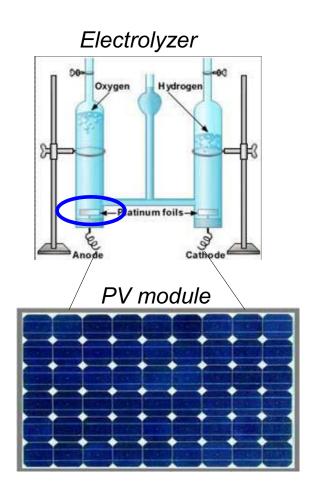
Energy level alignment

Higher E⁰: reduction Lower E⁰: oxidation

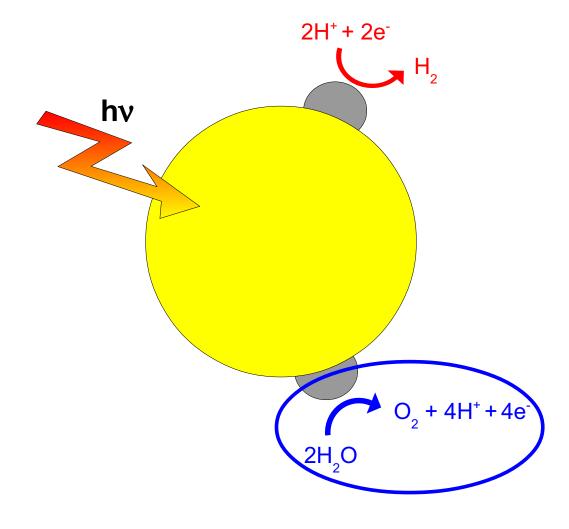
 $-nFE^0 = \Delta G^0$



Artificial photosynthesis: using light to make fuels



Integrated photo-catalyst



Water oxidation: a 4 electron reaction

$$2H_2O \rightarrow O_2 + 4H^+ + 4e^-$$
 (E⁰ = 1.23 V)

- Oxidizing water is thermodynamically demanding
- This reaction involves a 4-electron mechanism: 1- and 2-electron intermediates need to be avoided

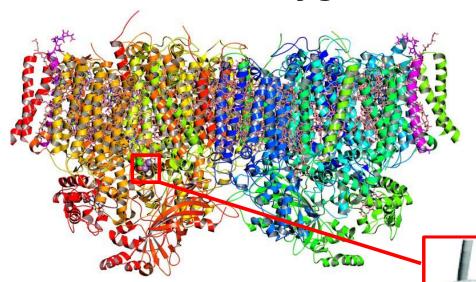
1-electron mechanism:
$$H_{2}O \rightarrow OH^{\bullet} + H^{+} + e^{-}$$
 $(\Delta G^{0} = 2.31 \text{ V})$

2-electron mechanism:
$$2H_2O \rightarrow H_2O_2 + 2H^+ + 2e^- \quad (\Delta G^0 = 1.78 \text{ V})$$

4-electron mechanism:
$$2H_2O \rightarrow O_2 + 4H^+ + 4e^- \qquad (\Delta G^0 = 1.23 \text{ V})$$

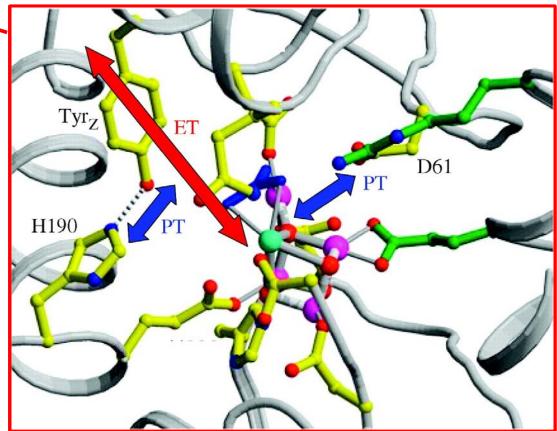
 We need catalysts that efficiently promote the 4-electron mechanism

Oxygen evolving complex in PSII

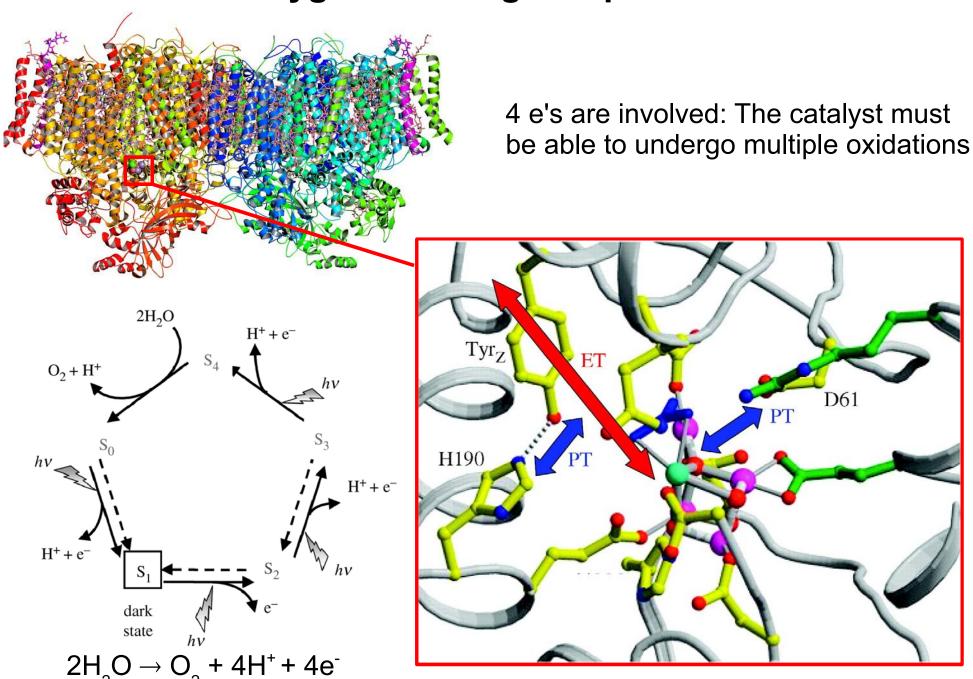


Photosystem II

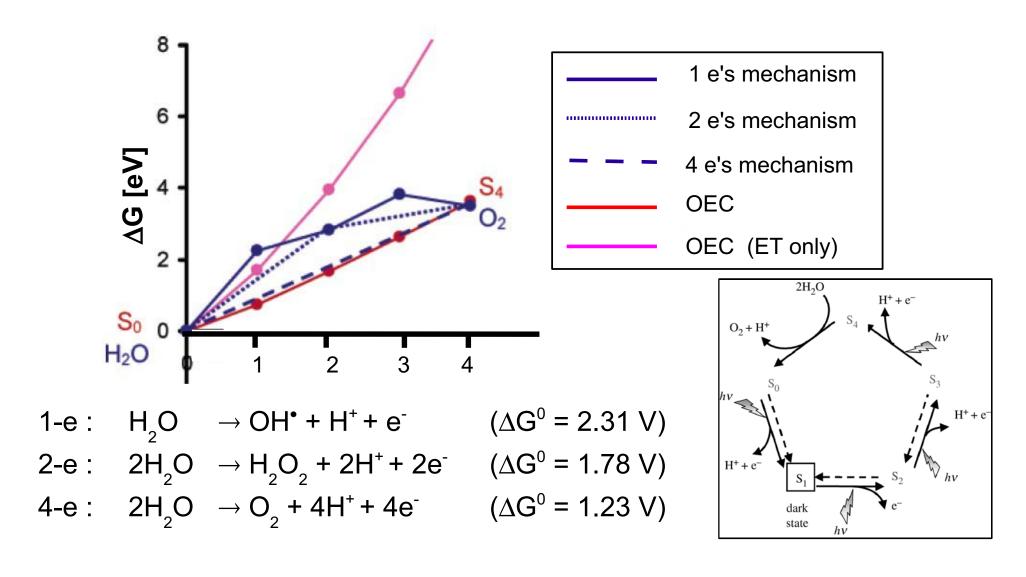
OEC in Photosystem II: Mn₃CaO₄-Mn



Oxygen evolving complex in PSII

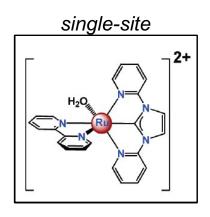


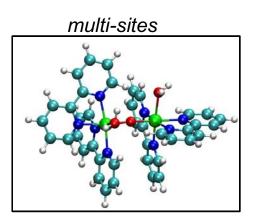
Oxygen evolving complex in PSII

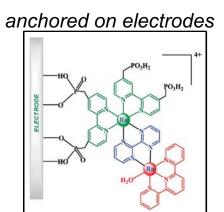


Artificial Catalysts for OER

Homogeneous catalysts for OER



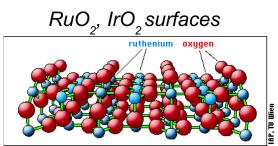


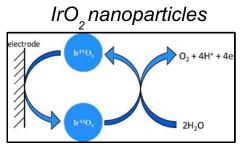


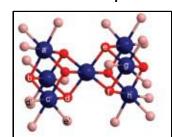
Ru-, Co-POM

Co-Pi amorphous

Heterogeneous catalysts for OER







Artificial Catalysts for OER

- Mechanism of water oxidation?
- What determines the efficiency of a catalyst?

17886

J. Phys. Chem. B 2004, 108, 17886-17892

Origin of the Overpotential for Oxygen Reduction at a Fuel-Cell Cathode

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We present a method for calculating the stability of reaction intermediates of electrochemical processes on the basis of electronic structure calculations. We used that method in combination with detailed density functional calculations to develop a detailed description of the free-energy landscape of the electrochemical oxygen reduction reaction over Pt(111) as a function of applied bias. This allowed us to identify the origin of the overpotential found for this reaction. Adsorbed oxygen and hydroxyl are found to be very stable intermediates at potentials close to equilibrium, and the calculated rate constant for the activated proton/electron transfer to adsorbed oxygen or hydroxyl can account quantitatively for the observed kinetics. On the basis of a database of calculated oxygen and hydroxyl adsorption energies, the trends in the oxygen reduction rate for a large number of different transition and noble metals can be accounted for. Alternative reaction mechanisms involving proton/electron transfer to adsorbed molecular oxygen were also considered, and this peroxide mechanism was found to dominate for the most noble metals. The model suggests ways to improve the electrocatalytic properties of fuel-cell cathodes.

Zero bias: At V=0 relative to the NHE we have:

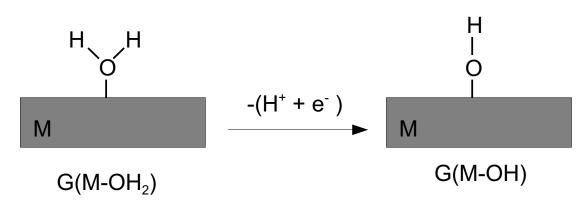
$$E^{0}_{NHE} = \Delta G^{0}_{NHE} = 0 \quad \Rightarrow \quad 2H^{+}(aq) + 2 e^{-} \leftrightarrow H_{2}(g)$$
$$\Rightarrow G^{0}(H^{+} + e^{-}) = G^{0}(1/2 H_{2})$$

Therefore, using NHE as reference, we can compute the chemical potential of the (H⁺ + e⁻) pair from the chemical potential of gas phase H₂

We do need to estimate $\mu(H^+) + \mu(e^-)$ separately

Example: Suppose we want to compute the free energy change ΔG w.r.t. NHE at V=0 for the following half cell reaction:

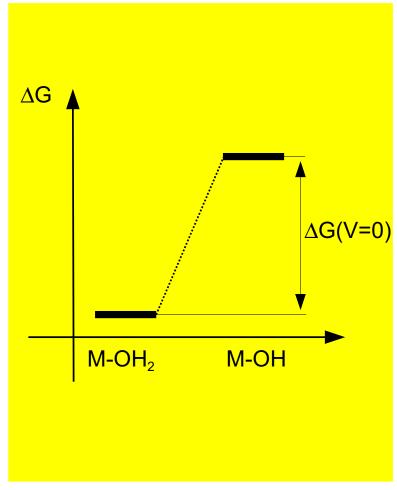
$$M-OH_2 \rightarrow M-OH + H^+ + e^-$$



$$\Delta G = G(M-OH) + \mu(H^{+}) + \mu(e^{-}) - G(M-OH_{2})$$

$$= G(M-OH_{2}) + \frac{1}{2}\mu(H_{2}) - G(M-OH)$$

$$E^{0} = -\Delta G^{0}/F$$



Finite V:

V=0
$$\mu(H^+) + \mu(e^-) = 1/2\mu(H_2)$$

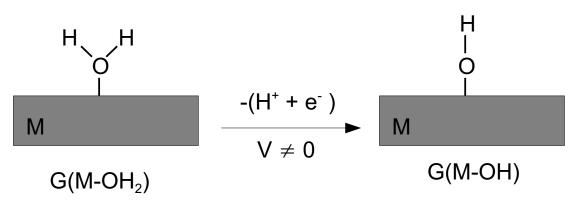
$$V \neq 0 \qquad \mu(e^{-}) \rightarrow \mu(e^{-}) - eV$$

$$\mu(H^{+}) + \mu(e^{-}) = 1/2\mu(H_{2}) - eV$$

All other effects of the bias V are neglected in this approach

Example: $\forall \neq 0$

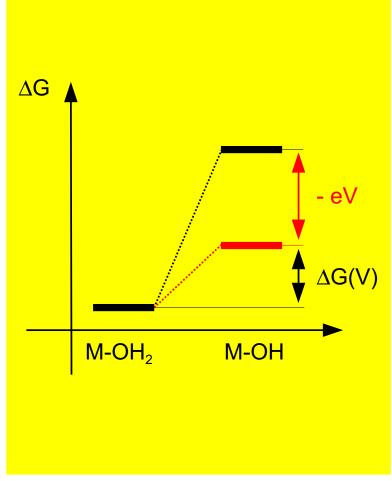
$$M-OH_2 \rightarrow M-OH + H^+ + e^-$$



$$\Delta G(V) = G(M-OH) + \mu(H^{+}) + \mu(e^{-}) - G(M-OH_{2})$$

$$= G(M-OH_{2}) + 1/2\mu(H_{2}) - eV - G(M-OH)$$

$$= \Delta G(V=0) - eV$$



The relative energies of the intermediates depend linearly on the bias V

Finite pH:

pH=0
$$\mu(H^+) + \mu(e^-) = 1/2\mu(H_2)$$

pH
$$\neq$$
 0 $\mu(H^+) \rightarrow \mu(H^+) - 2.303 \text{ kT} \times \text{pH}$
$$\mu(H^+) + \mu(e^-) = 1/2\mu(H_2) - 2.303 \text{ kT} \times \text{pH}$$

Free energies: the free energy changes at V=0 and pH=0 are computed according to:

$$\Delta G \simeq \Delta E + \Delta Z P E - T \Delta S$$

Where:

- ΔE is the reaction energy (*DFT calculation*)
- \triangle ZPE is the change in zero-point-energy (*normal mode analysis*)
- ΔS is the change in entropy (from thermochemical tables)

Solvent: the effect of one monolayer of water has been included (O* interacts negligibly with water while OH* makes hydrogen bonds)

Double layer: the field in the double layer (~1V/3Å) couples weakly to the dipole moments of the adsorbed species (~0.05 eÅ), giving rise to effects of the order of 0.01 eV

Limits: only $(H^+ + e^-)$ pairs (PCET). No ET nor PT steps

Limits: no dynamical (configurational entropy) effects due to the solvent rearrangement upon the formation of new intermediates are neglected. This is probably a good approximation for (H⁺ + e⁻) steps, since the overall charge of the system is constant.

Limits: thermodynamics only. No kinetics.

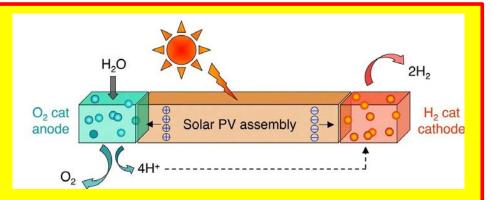
OER and **ORR**

Electrolysis

$$2H_2O \rightarrow O_2 + 2H_2$$
 $\Delta G^0 = 4.92 \text{ eV}$

OER:
$$2H_{2}O \rightarrow O_{2} + 4H^{+} + 4e^{-}$$

 $2H^{+} + 2e^{-} \rightarrow H_{2}$

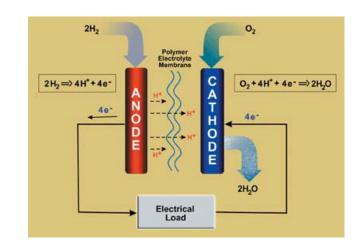


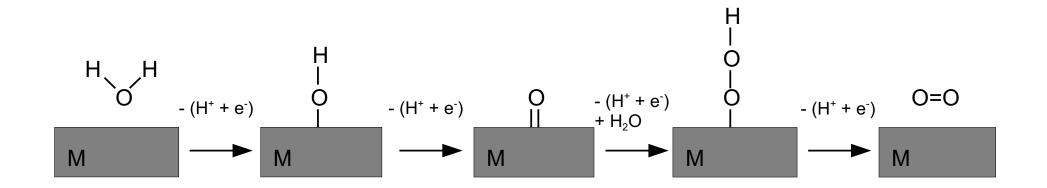
PEM Fuel cells

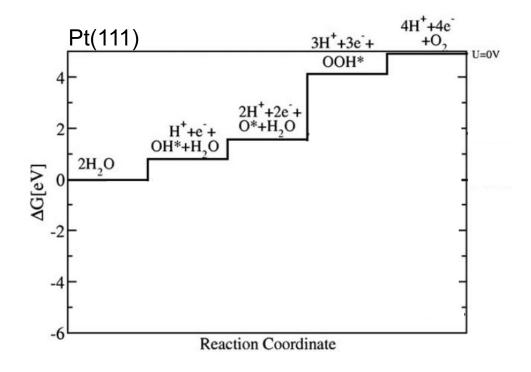
$$O_2 + 2H_2 \rightarrow 2H_2O$$
 $\Delta G^0 = -4.92 \text{ eV}$

ORR:
$$O_2 + 4H^+ + 4e^- \rightarrow 2H_2O$$

 $H_2 \rightarrow 2H^+ + 2e^-$



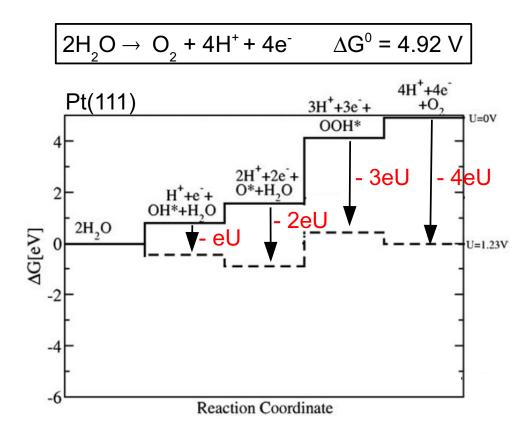




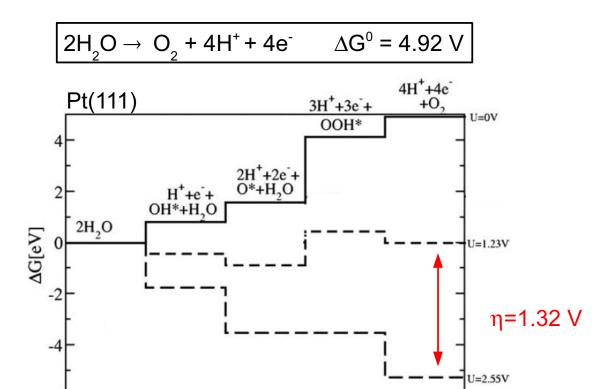
Investigated mechanism (OER) $H_{2}O + * \rightarrow OH^{*} + (H^{+} + e^{-})$ $OH^{*} \rightarrow O^{*} + (H^{+} + e^{-})$ $O^{*} + H_{2}O \rightarrow OOH^{*} + (H^{+} + e^{-})$

$$OOH^* \rightarrow O_2 + (H^+ + e^-)$$

Figures from: Rossmeisl et al. Phys. Chem 319, 178-184 (2005)



 U = 1.23 V is not sufficient to oxidize water on Pt(111): OOH* is too weakly bound compared to O*

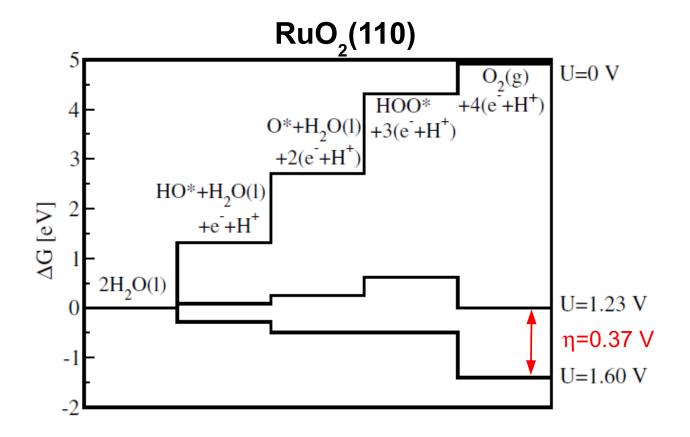


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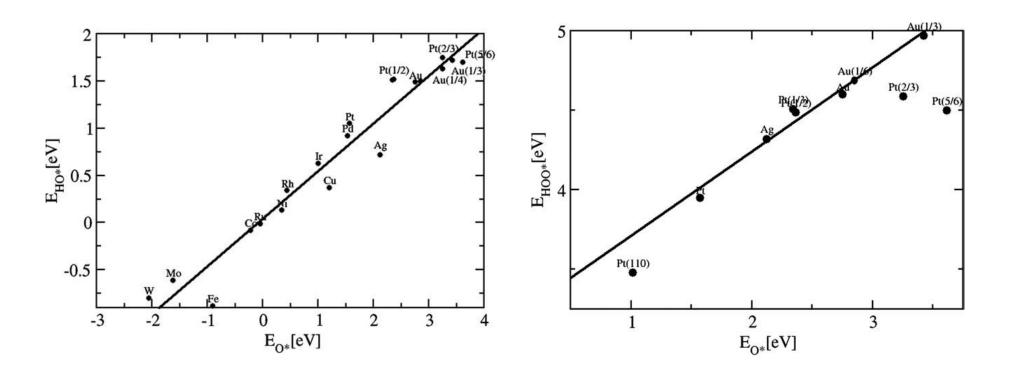
Reaction Coordinate

- At U =2.55 V all steps are downhill in energy
- The overpotential of Pt(111) is 2.55-1.23 = 1.32 V
- The ideal catalyst has 4 identical steps, each with ΔG =1.23 eV (1.23×4=4.92 eV)

Water oxidation on oxide surfaces

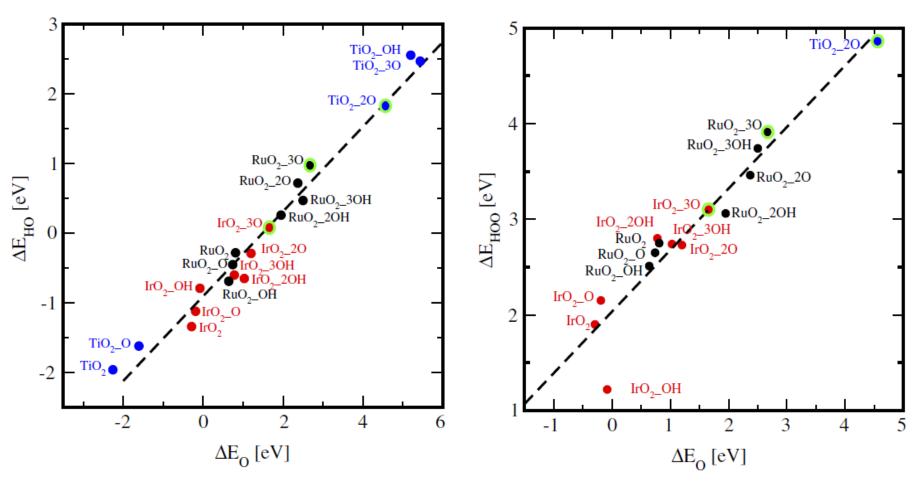


- Also in this case the overpotential-determining step is O* + H₂O → OOH* + (H⁺ + e⁻)
- The overpotential, however, is considerably lower than Pt(111)



 E_{o*} , E_{oh*} and E_{ooh*} are approximately linearly related

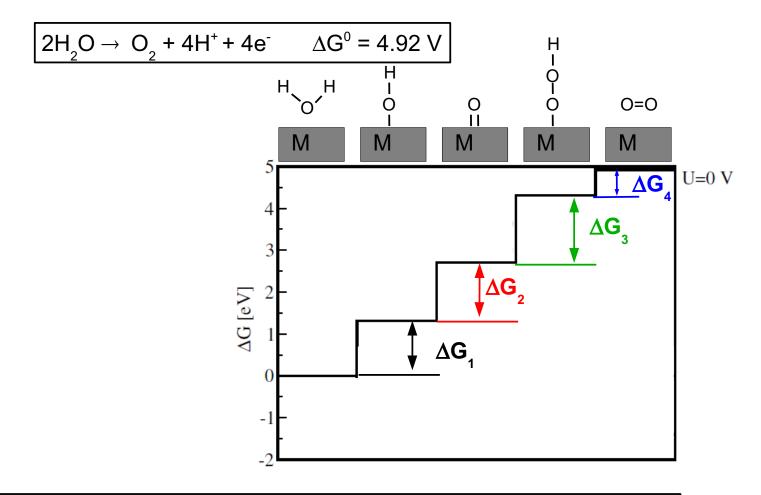
Water oxidation on oxide surfaces



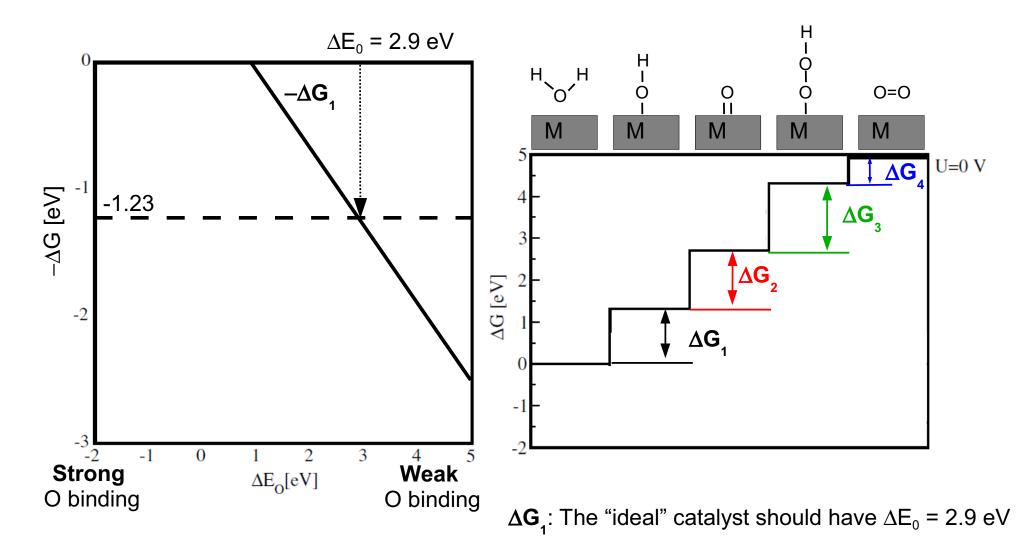
- \bullet Also in this case $\mathsf{E}_{\mathsf{O^*}}\!,\,\mathsf{E}_{\mathsf{OH^*}}$ and $\mathsf{E}_{\mathsf{OOH^*}}\!$ are approximately linearly related
- $\Delta E_O = 0$ eV is defined by the equilibrium: $H_2O \leftrightarrow O^* + H_2$

Figures from: Rossmeisl et al. J. Electr. Chem 607, 83-89 (2007)

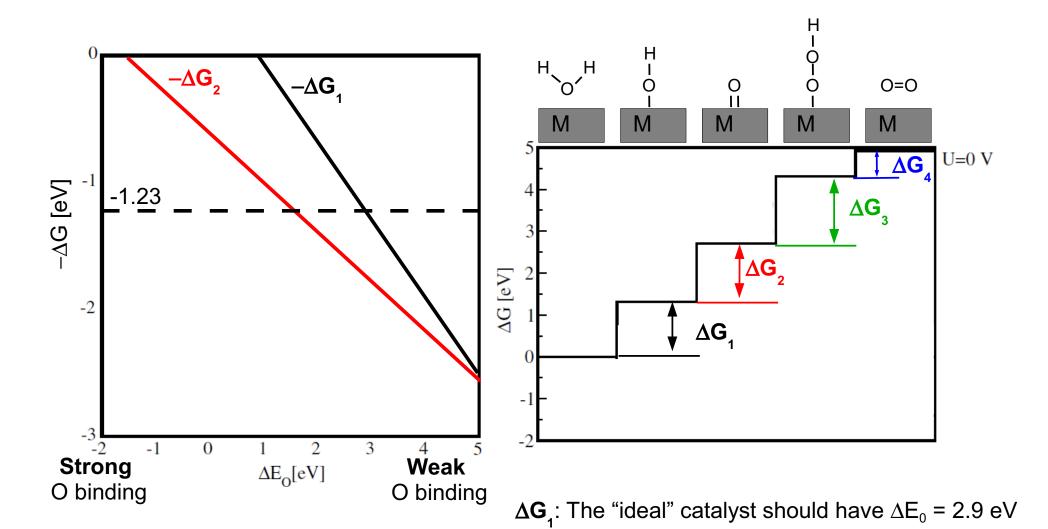
Water oxidation on oxide surfaces



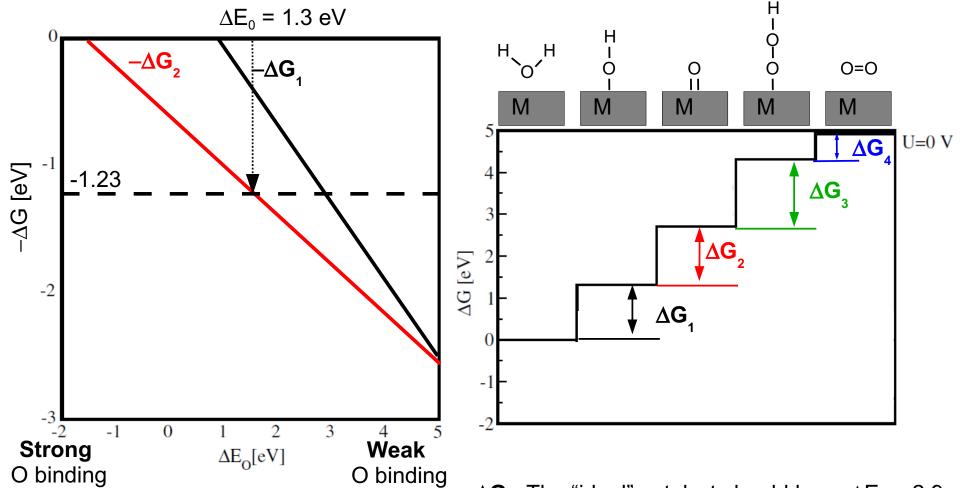
The height of each step ΔG_{1-4} is (approximately) a linear function of ΔE_0 (which is a material-dependent property)



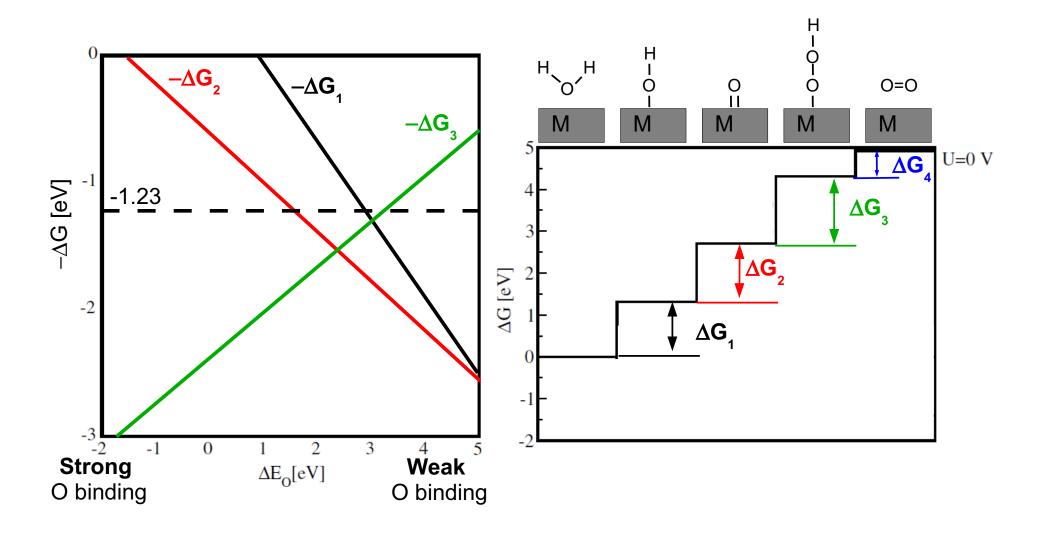
Figures from: Rossmeisl et al. J. Electr. Chem 607, 83-89 (2007)

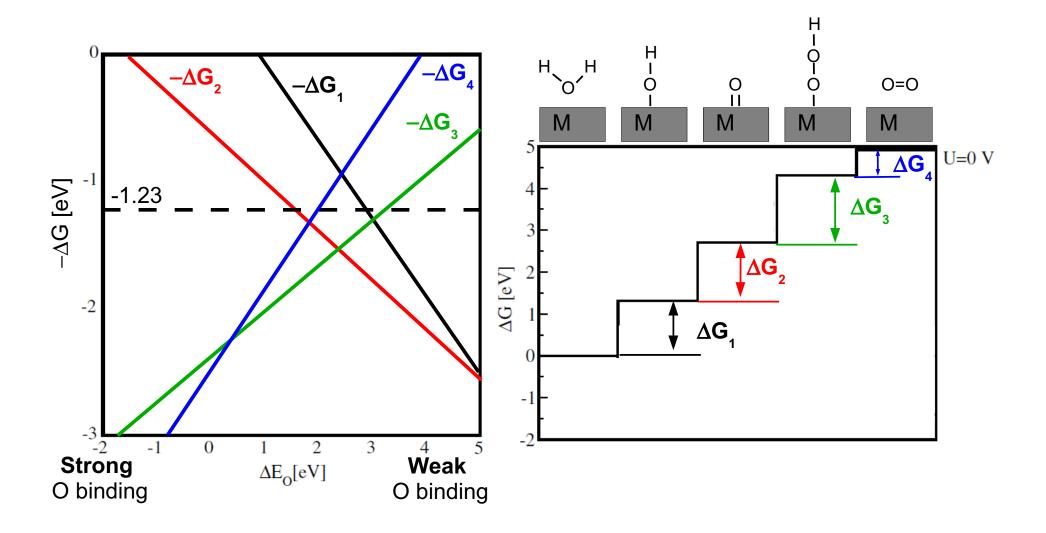


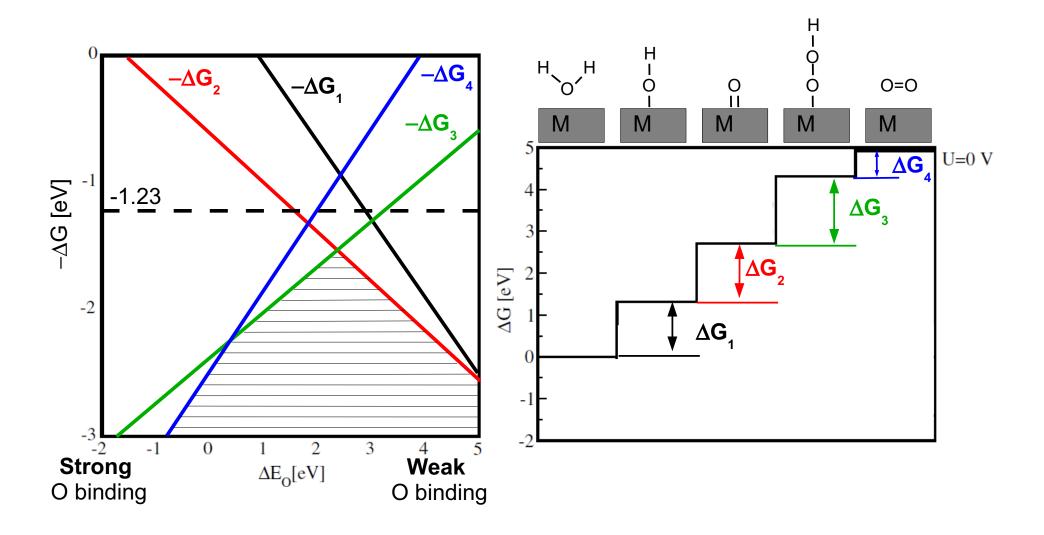
Figures from: Rossmeisl et al. J. Electr. Chem 607, 83-89 (2007)

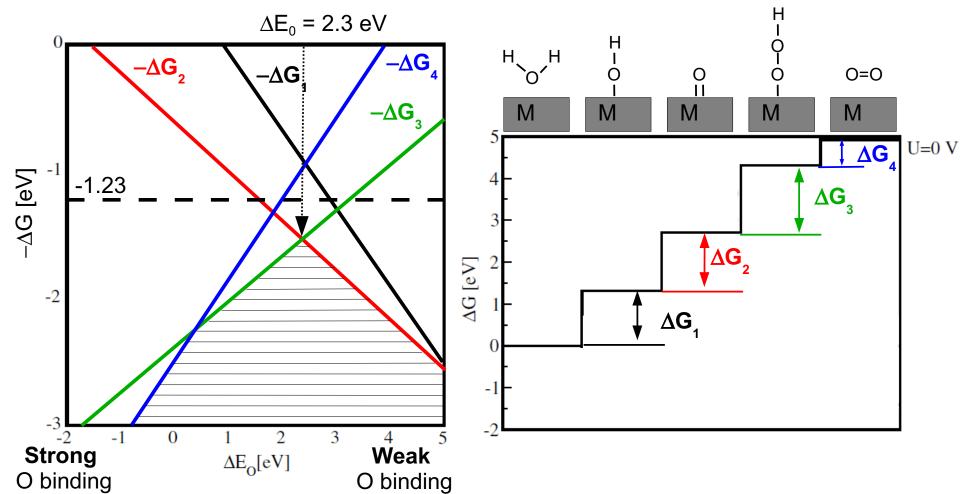


 $\Delta \mathbf{G_1}$: The "ideal" catalyst should have $\Delta E_0 = 2.9 \text{ eV}$ $\Delta \mathbf{G_2}$: The "ideal" catalyst should have $\Delta E_0 = 1.3 \text{ eV}$

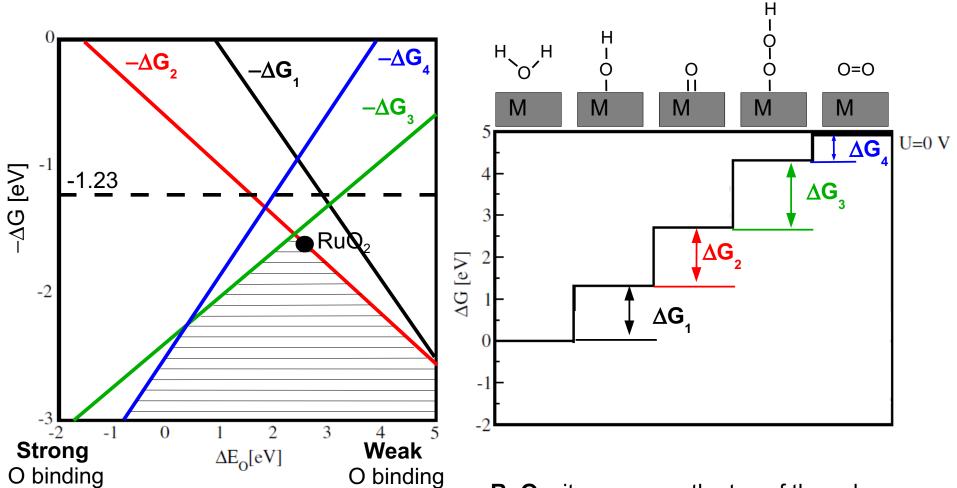




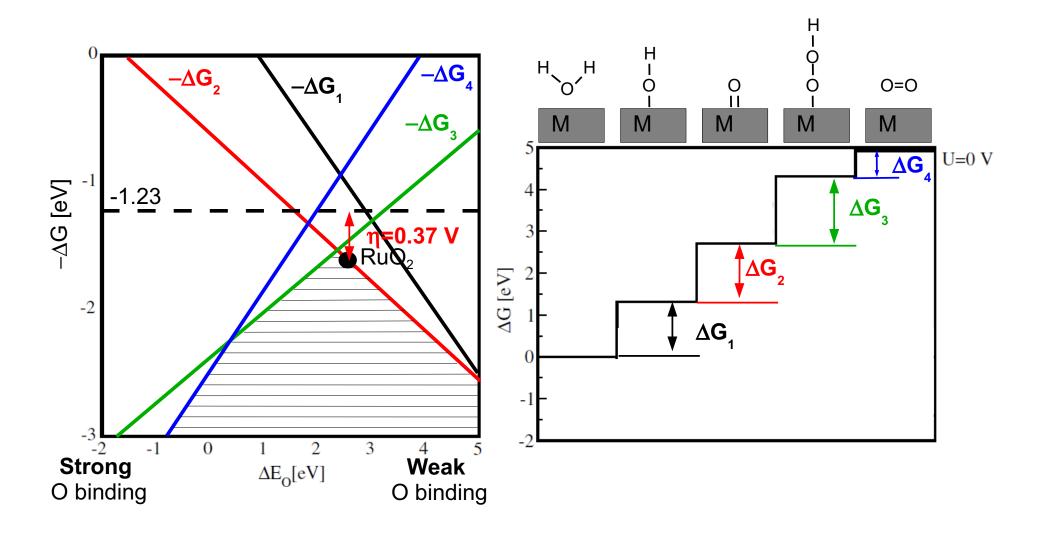


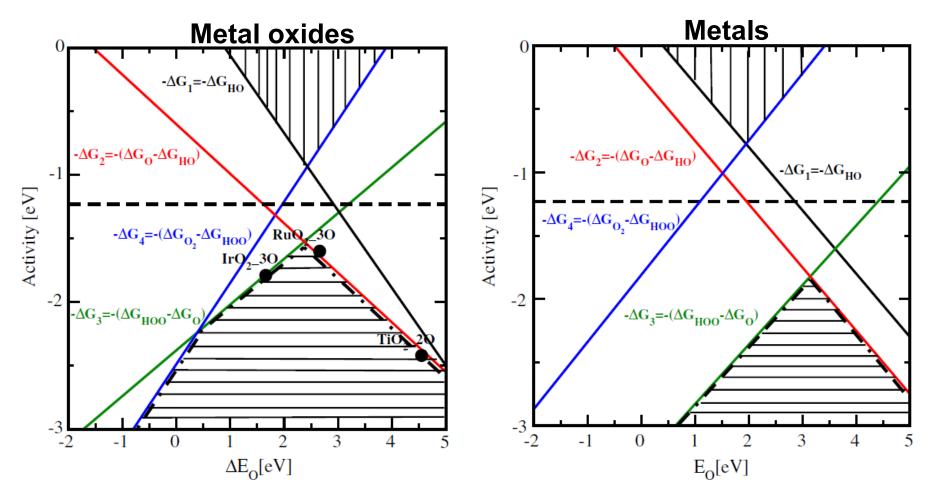


The "best" catalyst should have $\Delta E_0 = 2.3 \text{ eV}$

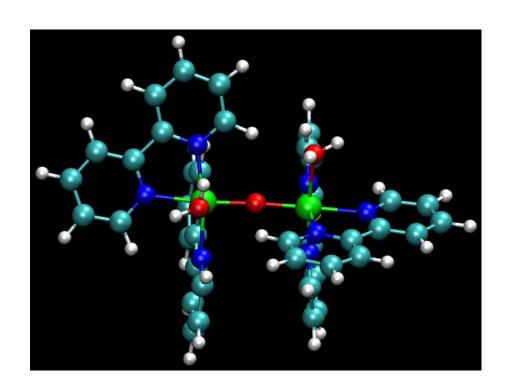


RuO₂ sits very near the top of the volcano There's not much room for improvement.





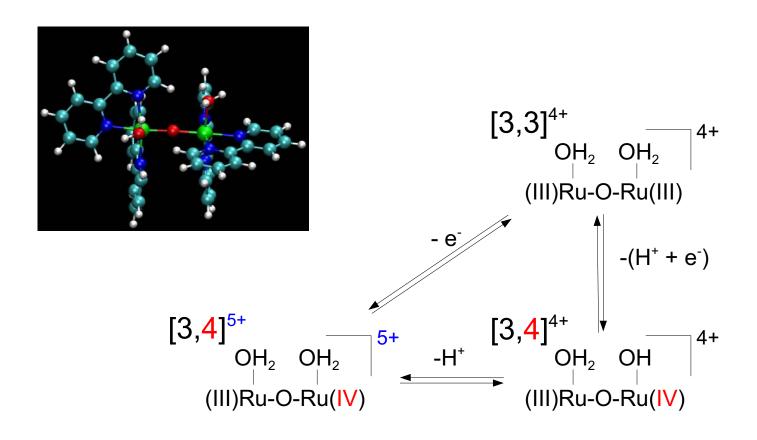
- Using the linear relationships of the the binding energies of the intermediates vs. O*, the activity of different catalysts for OER and ORR can be established
- The "activity" is defined as the overpotential.
- RuO₂ and Pt sit very near the top of the volcanoes. There's not much room for improvement.

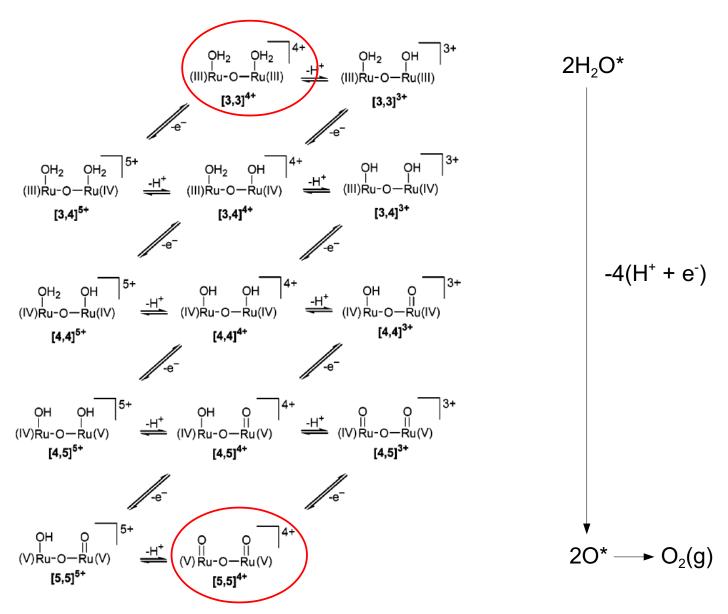


"Blue dimer"

Gersten et al. JACS 104, 4029-4030 (1982)

- Well characterized molecular catalyst
- Ru(III)-H₂O / Ru(V)=O cycle, followed by nucleophilic attack
- Small TN (13) due to deactivation of organic ligands





OER: $2H_2O \rightarrow O_2(g) + 4(H^+ + e^-)$

ET reactions: $[A]^n + e^- \rightarrow [A]^{n-1}$

$$\Delta G(sol) = \Delta G(g) + \Delta G^{solv}$$
 using a continuum solvation model (SCRF, PCM, ...) $\Delta G(g) = \Delta H(g) - T\Delta S(g)$ from normal mode analysis $\Delta H(g) = \Delta H^{SCF} + \Delta ZPE(g) + \Delta H^{T}$ from normal mode analysis $\Delta G(sol) = -FE^{0}$

- E⁰ needs to be referenced to some standard electrode (NHE)
- The absolute potential of the standard hydrogen electrode is difficult to determine precisely: ϕ = 4.43 V 4.85 V

PT reactions:
$$[AH]^n \rightarrow [A]^{n-1} + H^+(sol)$$

In this case we need the free energy of a proton in solution:

$$G(H^{+}) = H^{g}(H^{+}) - TS + 3/2RT + G^{solv}(H^{+})$$

In this approach the chemical potentials $\mu(H^+)+\mu(e^-)$ need to be estimated separately, and each of them is determined only approximately.

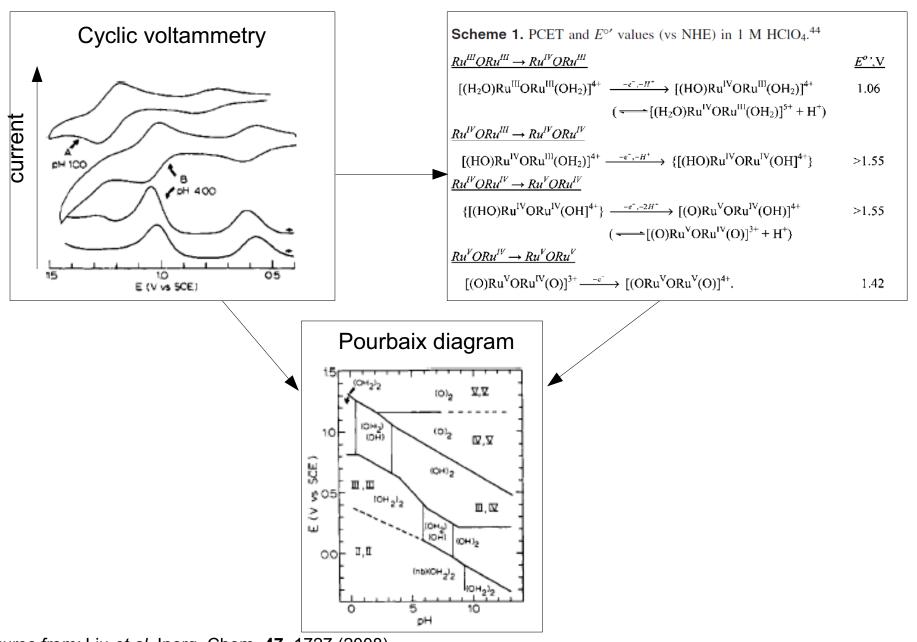
Tuesday, 18 October 2011 (Room:Leonardo da Vinci Building Main Lecture Hall)

18 October 2011

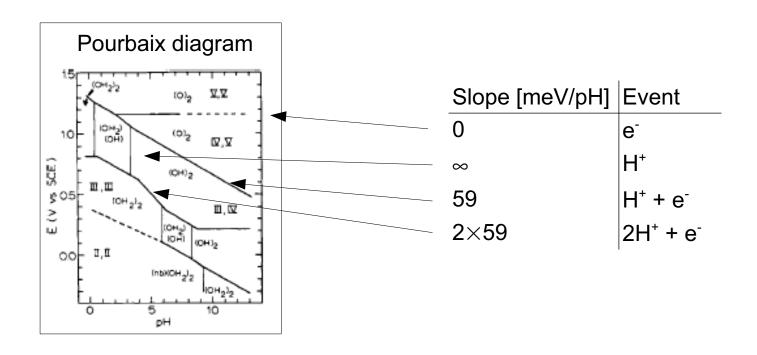
08:30 - 09:30	Christopher CRAMER / Dept. of Chemistry & Supercomputer Inst., Univ. Minnesota, Minneapolis, U.S.A. Practicalities of molecular computational modeling relevant to renewable energy technologies
09:30 - 10:30	Robert SCHLOGL / Dept. of Inorganic Chemistry, FHI der MPG, Berlin, Germany Material challenges in electro catalysis
10:30 - 11:00	Coffee break
11:00 - 12:00	Sossina M. HAILE / Steele Laboratories, Materials Science, Pasadena, CA, U.S.A. Advancing electrocatalysis in intermediate temperature fuel cells
12:00 - 14:00	Lunch break
14:00 - 15:00	Michiel SPRIK / Dept. of Chemistry, Univ. Cambridge, U.K. The thermochemistry of oxidative dehydrogenation of a water molecule at a TiO2/water interface
15:00 - 16:00	Nicola MARZARI / Dept. of Materials, University of Oxford, U.K. What can I do for first-principles simulations?
16:00 - 16:30	Coffee break
16:30 - 17:30	Alexander SOUDACKOV / Dept. of Chemistry, The Pennsylvania State Univ., University Park, PA, U.S.A. Theoretical modeling of proton-coupled electron transfer reactions in energy related materials
17:30 - 18:30	CONTRIBUTED TALKS

Summary

- Splitting water into O₂ and H₂ to store (solar) energy involves electrochemical processes
- The anodic reaction (water oxidation) is a complex 4-electron reaction that require suitable (efficient, stable, cheap) catalysts
- The overpotential is determined by the most endergonic electrochemical step (highest ΔG)
- If electrons and protons are removed at the same time (PCET) the approach proposed by Nørskov *et al.* is particularly convenient
- For a vast class of metals and metal oxides there exist linear relationships between the energies of the intermediates: ΔE_0 is a good descriptor, optimal catalysts can be identified



Figures from: Liu et al. Inorg. Chem. 47, 1727 (2008)



J. Phys. Chem. A 2002, 106, 7407-7412

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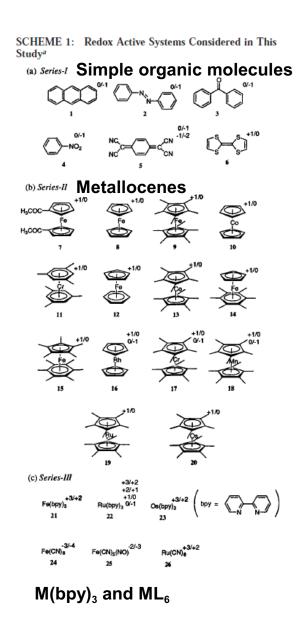
Computing Redox Potentials in Solution: Density Functional Theory as A Tool for Rational Design of Redox Agents

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High-level density functional theory in combination with a continuum solvation model was employed to compute standard redox potentials in solution phase for three different classes of electrochemically active molecules: small organic molecules, metallocenes, and $M(bpy)_3^x$ (M = Fe, Ru, Os; x = +3, +2, +1, 0, -1). Excellent agreement with experimentally determined redox potentials is found with an average deviation of approximately 150 mV when four different solvents commonly in use for electrochemical measurements were included. To obtain quantitative agreement between theory and experiment, the use of a large basis set is crucial especially when the redox couple includes anionic species. Whereas the addition of diffuse functions improved the results notably, vibrational zero-point-energy corrections and addition of entropy effects are less important. The computational protocol for computing redox potentials in solution, which has been benchmarked, is a powerful and novel tool that will allow a molecular-level understanding of the features dictating the properties of redox-active species.



- B3LYP functional
- Basis set(s):
- (a) 6-31G** and LACV3P** for TM
- (b) cc-pVTZ(-f)++ and LACV3P**++ for TM
- SCRF continuum model for the solvents, using gas-phase geometries
- Different solvents (water, acetonitrile, dimethylformamide, dichloromethane)

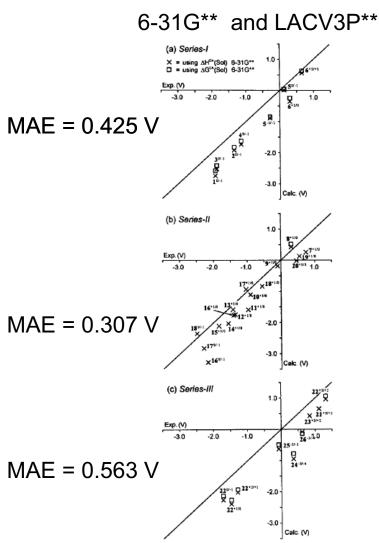


Figure 1. Correlation diagram of the experimental vs calculated redox potentials on the B3LYP/6-31G** level of theory with and without ZPE/entropy corrections.

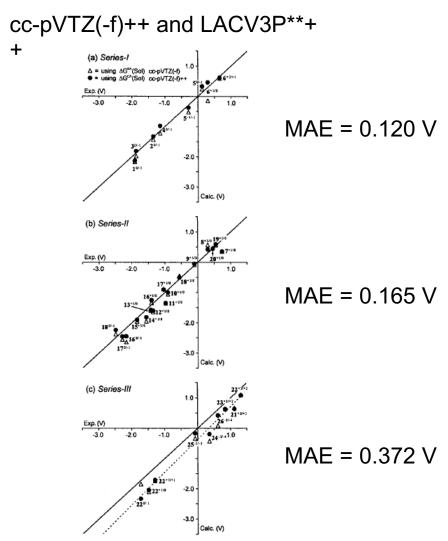
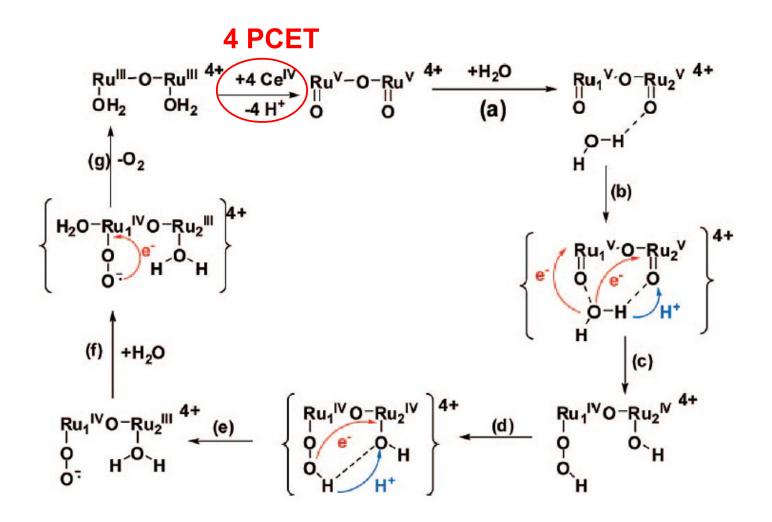
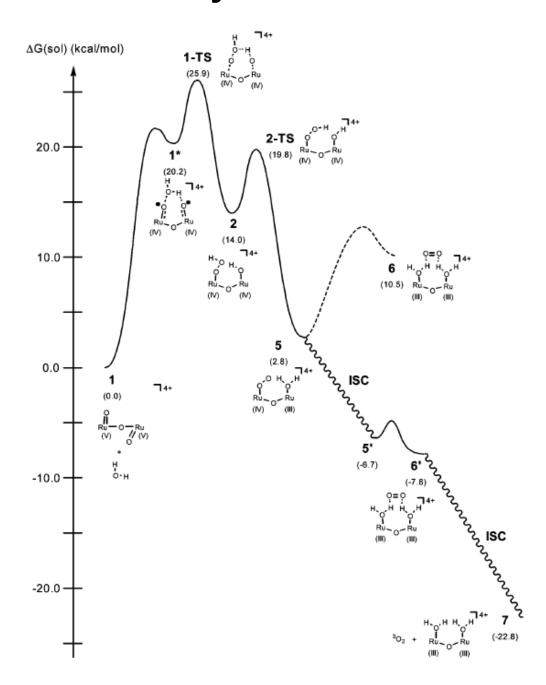


Figure 2. Correlation diagram of the experimental vs calculated redox potentials on the B3LYP/cc-pVTZ(-f) and B3LYP/cc-pVTZ(-f)++ levels of theory (ZPE/entropy-corrected).

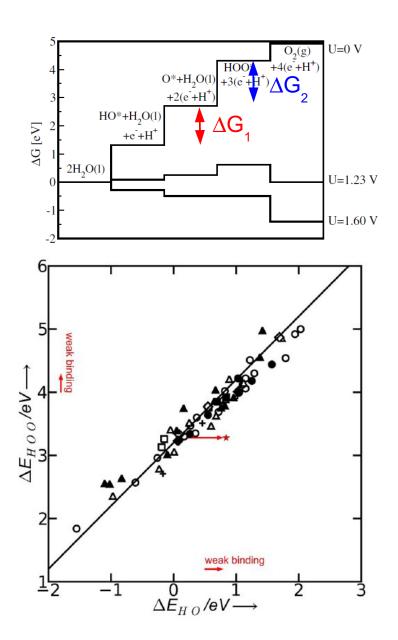
Table 2. Calculated and Experimental Redox Potentials in V^a

	E _{1/2} (calcd)	E _{1/2} (exp)	difference		
$[5,5]^{4+} + 3e^- + 3H^+ \rightarrow [3,4]^{4+}$	AF: 1.323	1.22^{6}	0.103	PCET	
F = 5141	S: 1.845	1 100	0.625		
$[5,5]^{4+} + 4e^- + 4H^+ \rightarrow [3,3]^{4+}$	AF: 1.179	1.12^{6}	0.059	PCET	√
$[3,4]^{4+} + e^- + H^+ \rightarrow [3,3]^{4+}$	S: 1.424 AF: 0.747	0.79^{6}	0.304	PCET	√
[0,1] C H [0,0]	S: 0.162	0.10	-0.628	. 02.	•
$[4,4]^{4+} + e^- + H^+ \rightarrow [3,4]^{4+}$	1.817	$> 1.45^9$			
$[4,5]^{3+} + e^- + 2H^+ \rightarrow [4,4]^{4+}$	0.989	$< 1.45^9$			
$[4,5]^{3+} + 2e^{-} + 3H^{+} \rightarrow [3,4]^{4+}$	1.403	1.45^9	-0.047		
$[5,5]^{4+} + e^{-} \rightarrow [4,5]^{3+}$	AF: 1.887 S: 3.453	1.40^{9}	0.487 2.053	ET	X
	3. 3.433		2.033		





Electrolysis of water on oxide surfaces



$$\Delta G_1 = G(O^*) - G(OH^*) + 1/2\mu(H_2)$$

 $\Delta G_2 = G(OOH^*) - G(O^*) + 1/2\mu(H_2) - \mu(H_2O)$

Several linear relationships have been established:

- $\bullet \ \mathsf{E}_{\mathsf{OH}^*} \ \mu \ \mathsf{E}_{\mathsf{O}^*}$
- $\bullet \ \mathsf{E}_{\mathsf{OOH}^*} \mu \ \mathsf{E}_{\mathsf{O}^*}$
- $\bullet \ \mathsf{E}_{\mathsf{O}^*} \ \mu \ \mathsf{E}_{\mathsf{OOH}^*}$

$$\Delta G_1 + \Delta G_2 = 3.2 \text{ eV} \pm 0.2 \text{ eV} (68\%) \pm 0.4 \text{ eV} (95\%)$$

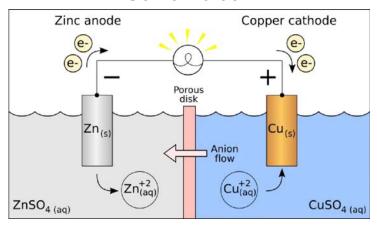
"Ideal" catalyst $\Delta G_1 = \Delta G_2 = 1.6 \text{ eV}$ ($\eta = 0.37 \text{ eV}$)

RuO₂ is therefore as good a catalyst for OER as a metal oxide can be

Figures from: Man et al. ChemCatChem 3, 1159-1165 (2011)

Electrochemistry: a quick overview

Galvanic cell



$$Cu^{2+}(aq) + Zn(s) \rightarrow Cu(s) + Zn^{2+}(aq)$$

Cathode (Red): $Cu^{2+}(aq) + 2e^{-} \rightarrow Cu(s)$

Anode (Ox): $Zn(s) \rightarrow Zn^{2+}(aq) + 2e^{-}$

Electromotive force (efm) E:

$$-nFE = \Delta G$$

F=eN_a Faraday constant

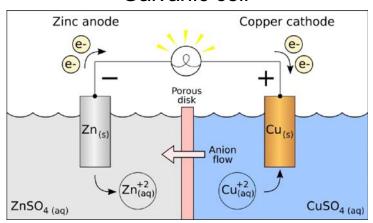
$$\Delta G = \Delta G^0 + RT \ln(K)$$

 $\Delta G = \Delta G^0 + RT \ln(K)$ K: equilibrium constant

$$E = -\Delta G^0 / nF + (RT/nF) ln(K)$$

Electrochemistry: a quick overview

Galvanic cell



$$Cu^{2+}(aq) + Zn(s) \rightarrow Cu(s) + Zn^{2+}(aq)$$

Cathode (Red): $Cu^{2+}(aq) + 2e^{-} \rightarrow Cu(s)$ Anode (Ox): $Zn(s) \rightarrow Zn^{2+}(aq) + 2e^{-}$

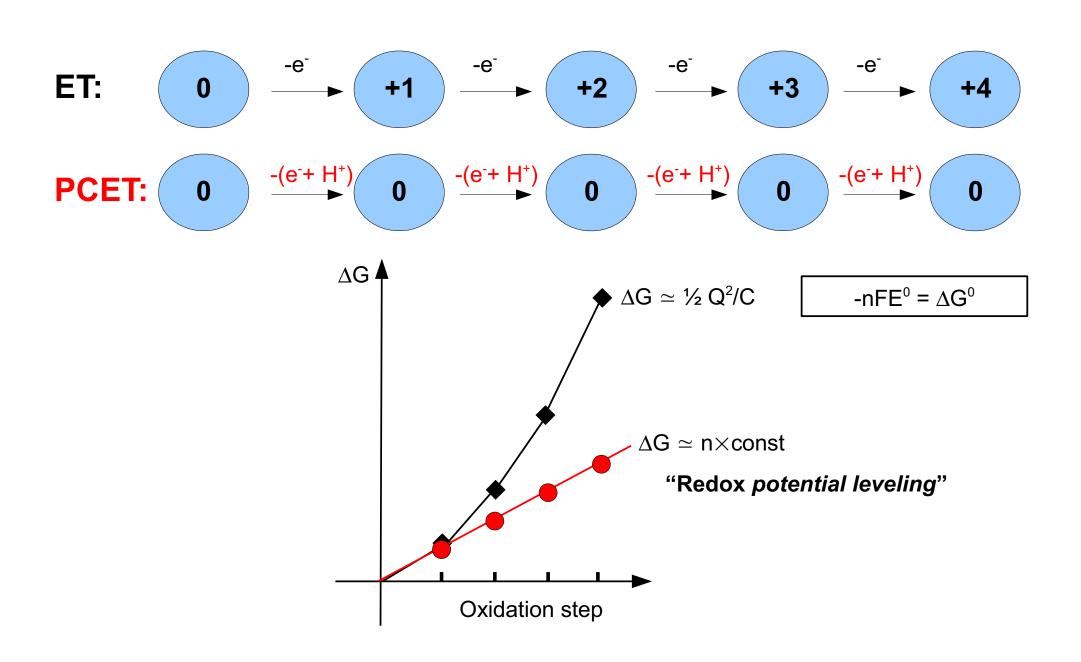
$$E^0 = E^0_2 - E^0_1$$

E_{1,2} of a single electrode: not possible to measure

Reference electrode: NHE (SHE)

We define E^0_{NHE} of the NHE to be zero: $E^0_{NHE} = 0$

PCET in water oxidation



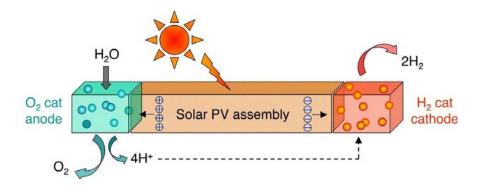
OER and **ORR**

Electrolysis

$$2H_2O \rightarrow O_2 + 2H_2$$
 $\Delta G^0 = 4.92 \text{ eV}$

OER:
$$2H_{2}O \rightarrow O_{2} + 4H^{+} + 4e^{-}$$

 $2H^{+} + 2e^{-} \rightarrow H_{2}$

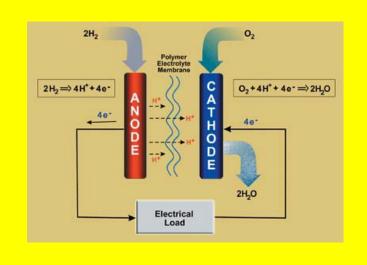


PEM Fuel cells

$$O_2 + 2H_2 \rightarrow 2H_2O$$
 $\Delta G^0 = -4.92 \text{ eV}$

ORR:
$$O_2 + 4H^+ + 4e^- \rightarrow 2H_2O$$

 $H_2 \rightarrow 2H^+ + 2e^-$



Oxygen Reduction Reaction (ORR) in fuel cells

Cathode reaction (Red):
$$O_2 + 4(H^+ + e^-) \rightarrow 2H_2O$$
 $E^0 = 1.23 \text{ V}$

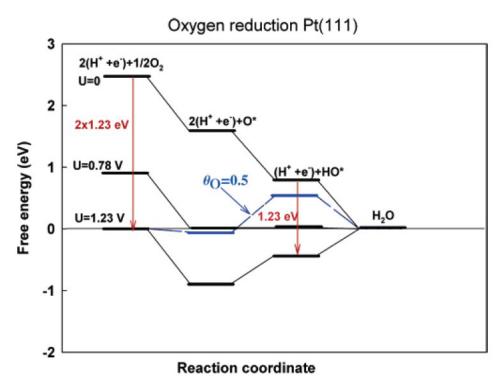
"Dissociative" mechanism

$$O_2^{+*} \rightarrow 2O^*$$

 $O^* + (H^+ + e^-) \rightarrow OH^*$
 $OH^* + (H^+ + e^-) \rightarrow H_2O + *$

"Associative" mechanism

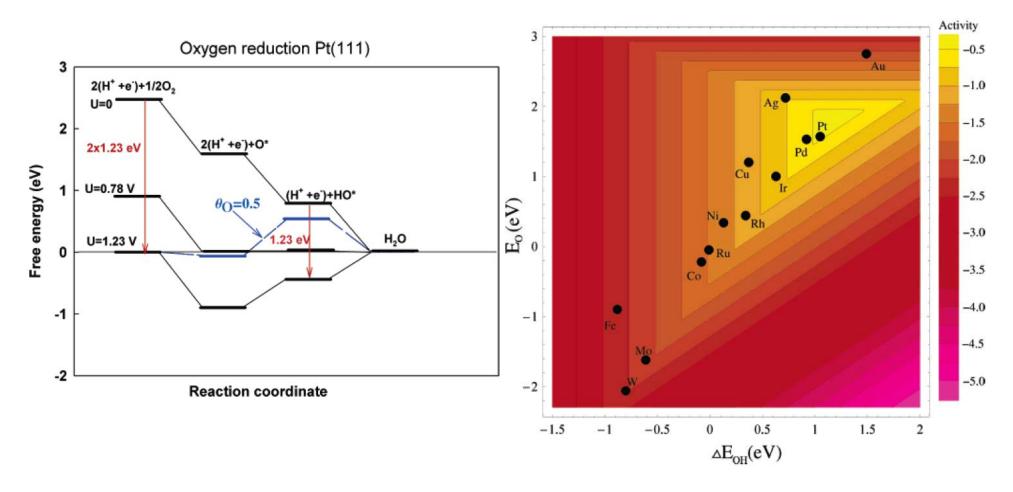
Oxygen Reduction Reaction (ORR)



- Up to U = 0.78 V all steps are downhill
- At the theoretical potential U=1.23 V both (H⁺ + e⁻) steps are uphill.
- Overpotential η = 1.23-0.78 = 0.45 V
- Overpotential due to the stability of O* and OH* on Pt(111)

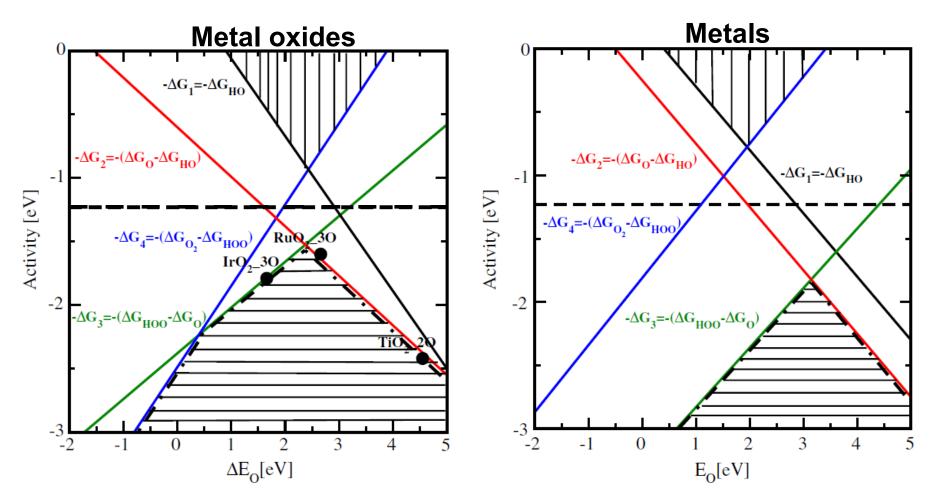
Ideal catalyst: $\Delta G_1(U=0) = \Delta G_2(U=0) = 1.23 \text{ eV}$

Oxygen Reduction Reaction (ORR)



- Pt and Pd are at the top of the volcano
- $E_b(OH^*)$ and $E_b(O^*)$ are approximately linearly related

Electrolysis of water on oxide surfaces



- Using the linear relationships of the the binding energies of the intermediates vs. O*, the activity of different catalysts for OER and ORR can be established
- The "activity" is defined as the overpotential.
- RuO₂ and Pt sit very near the top of the volcanoes. There's not much room for improvement.