



International Union of Geodesy and Geophysics



Union Géodésique et Géophysique Internationale

***International School on***

# ***'Geothermal Development'***

**December 7 - 12, 2015**  
*(Miramare, Trieste, Italy)*

## **DIRECT USES/HEAT PUMPS**

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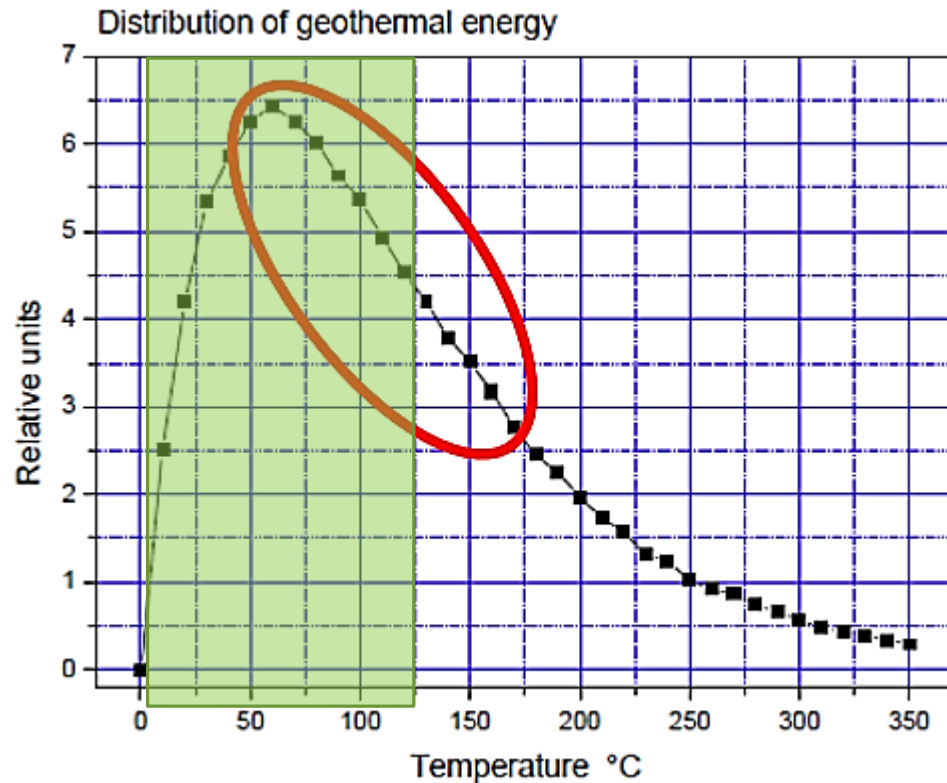
# SUMMARY

1. Direct uses: brief introduction and statistical data
2. Traditional/handbook design approach
3. Advanced/optimized design
4. Examples of optimized design systems
5. Investment assessment of direct uses systems

# MAIN TOPICS

1. Direct uses equipment, layouts, examples
2. Heat exchangers and hydraulic pumps
3. Cost-benefit optimization
4. Performance simulation
5. Economic and main financial indexes

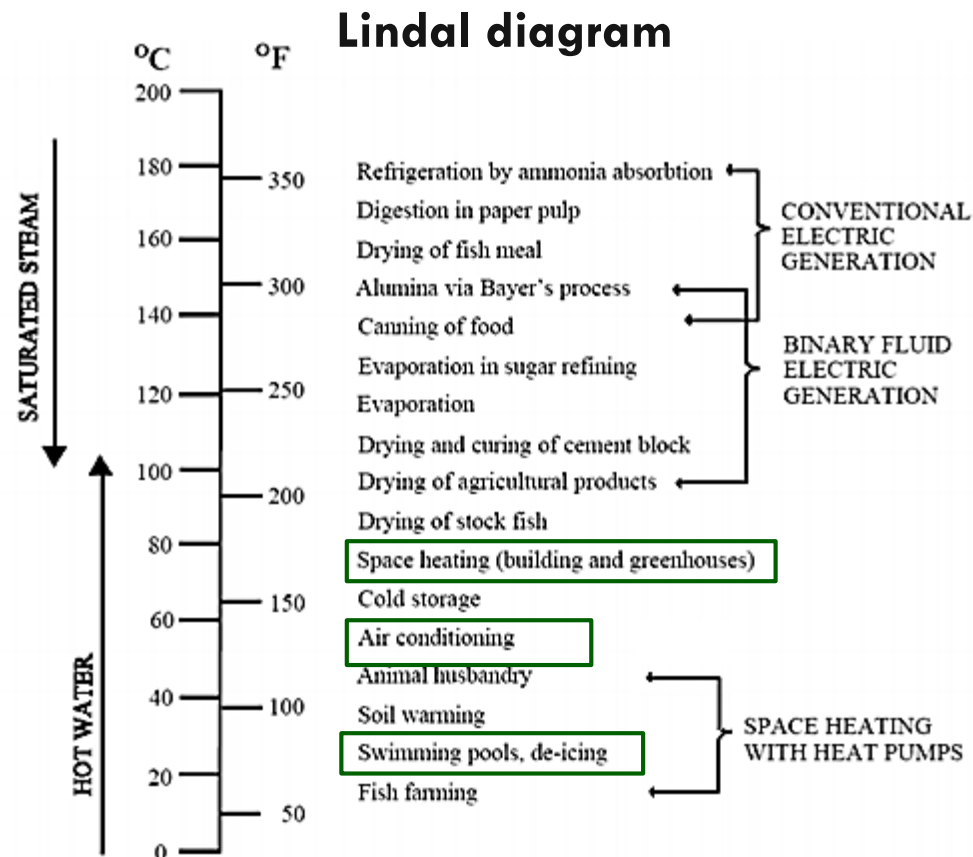
# DIRECT USES OF GEOTHERMAL ENERGY



The figure shows worldwide **distribution of geothermal energy** as function of the resources temperature (Stefansson, 2005)

More than 70 % of the geothermal resources available in the World are estimated to be **water dominated fields** at a temperature **lower than 150 °C**

# DIRECT USES OF GEOTHERMAL ENERGY



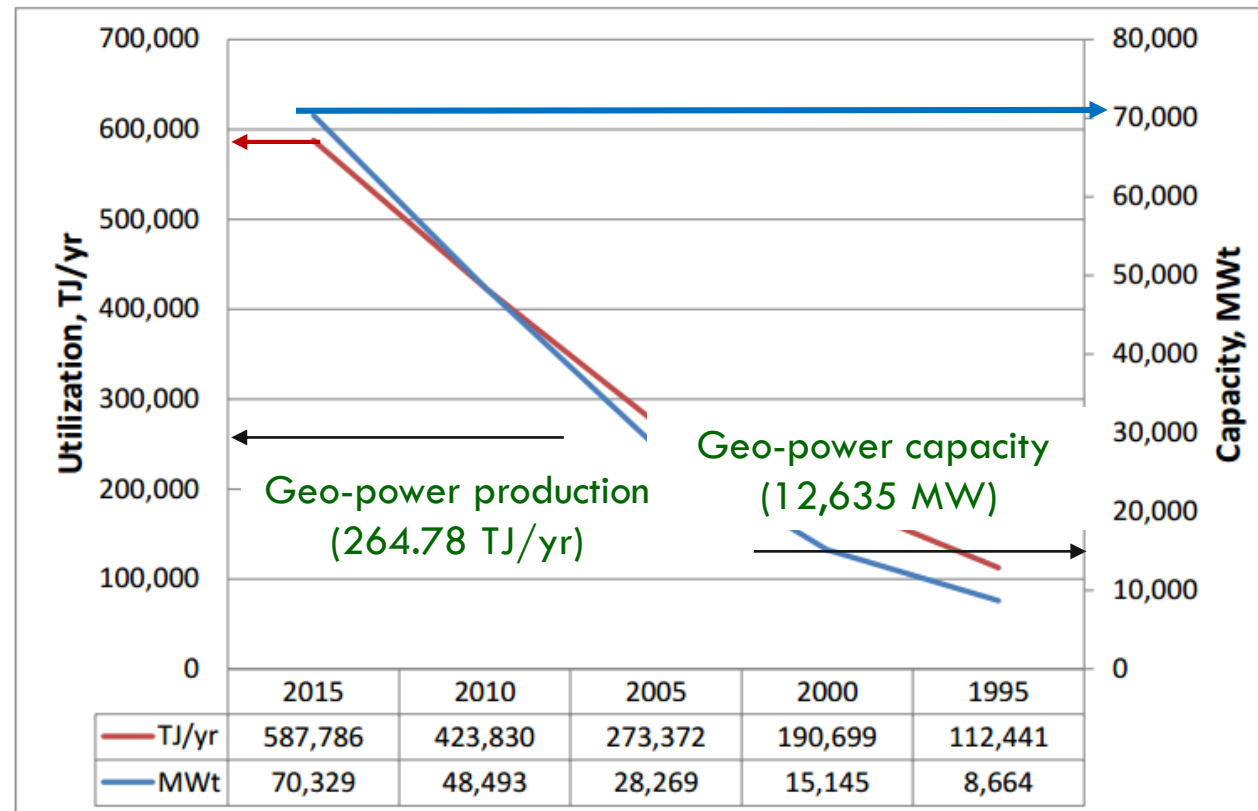
Heating loads correspond to more than 40% of global final energy consumption

Direct uses of geothermal energy have a notable potential in terms of:

- Fields of application (Lindal diagram)
- Worldwide expansion potential
- Energy saving
- Environmental benefit

# DIRECT USES OF GEOTHERMAL ENERGY

## Worldwide geothermal energy statistics



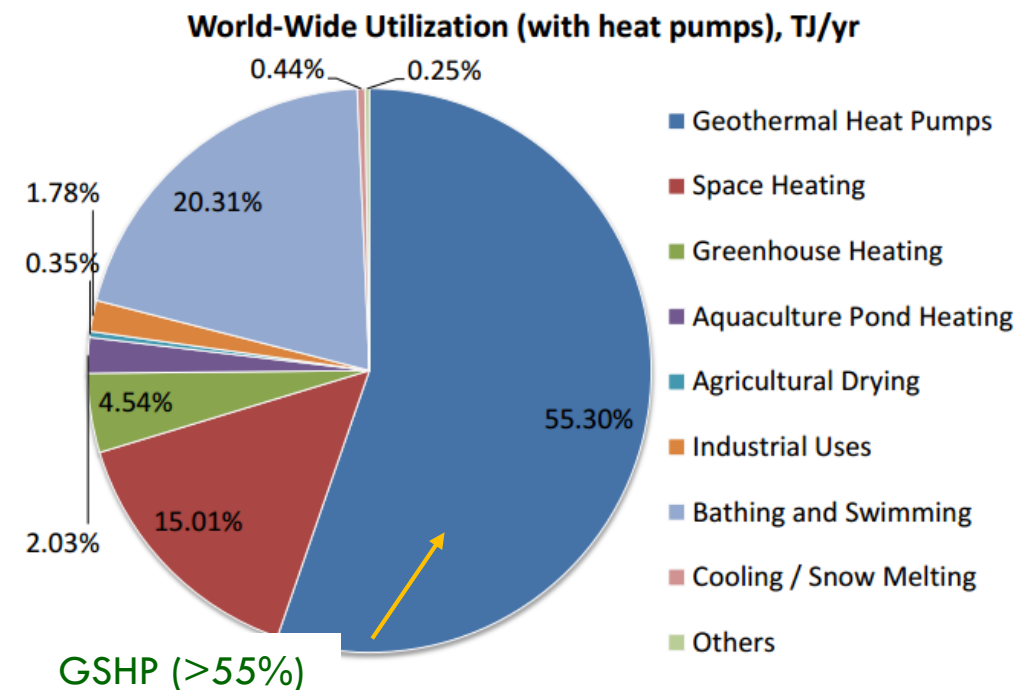
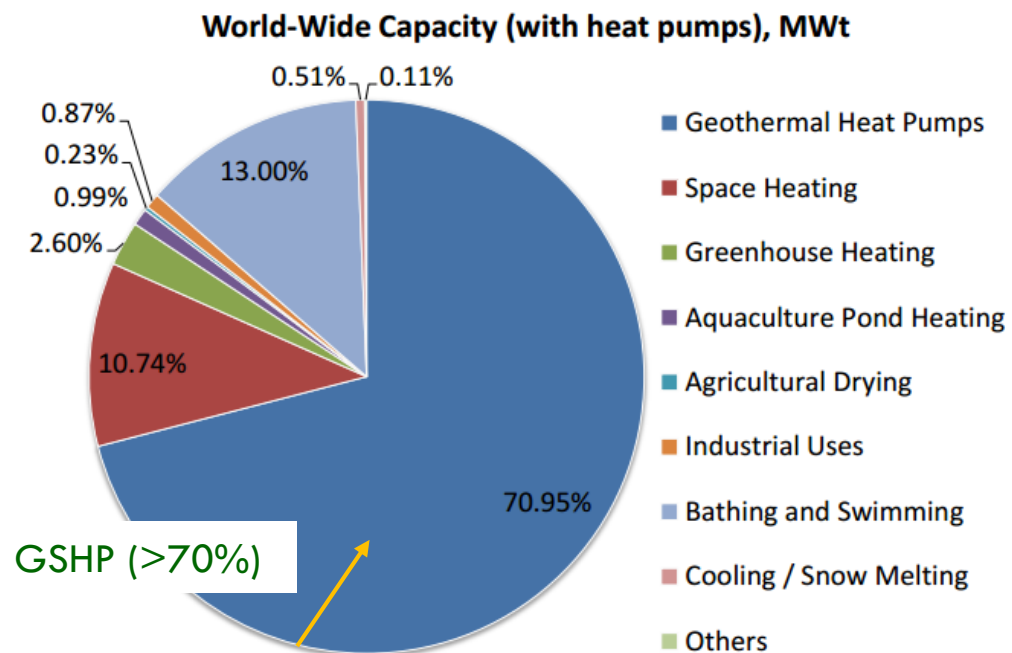
Data from (Bertani,2015) & (Lund&Boyd,2015)

# DIRECT USES OF GEOTHERMAL ENERGY

Geothermal direct applications worldwide in 2015 (Lund&Boyd,2015)

## Capacity

## Energy



# DIRECT USES OF GEOTHERMAL ENERGY

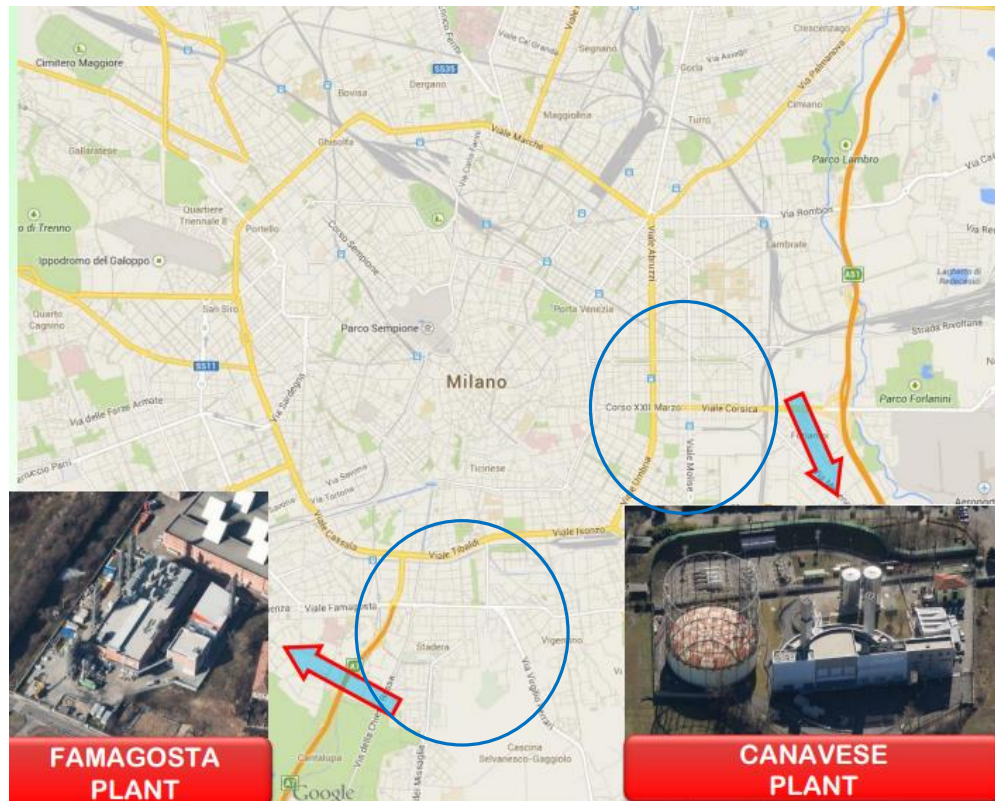
Sector of application	Capacity MW <sub>th</sub>			Energy TJ/yr		
	TOTAL	GSHP	DHs	TOTAL	GSHP	DHs
Space heating	725	550	78	4 607	3 211	683
Thermal balneology	421	-	-	3 698	-	-
Agriculture uses	69	14	-	725	82	-
Fish farming	122	-	-	1 927	-	-
Industrial process heat + minor uses	18	4	-	108	25	-
<b>TOTAL</b>	<b>1,355</b>	<b>568</b>	<b>92</b>	<b>11,065</b>	<b>3,318</b>	<b>-</b>

## Development of the different sectors of direct uses in Italy (2010-2014)



# DIRECT USES OF GEOTHERMAL ENERGY

## District Heating Systems (Milan, IT)



### Operative parameters:

Technologies: CHP + GSHP + Boilers

GSHPs heating capacity: **2 x 15.5 MW**

Heat source: **groundwater**

Groundwater operative Temp (in/out): 15-7.6 °C

Aquifer depth: 12-35 and 7-8 m

Groundwater flow: 1,150 m<sup>3</sup>/h

End-user loop temperature (in/out): 65.0 / 90.0 °C

Heating water flow: 546 m<sup>3</sup> /h

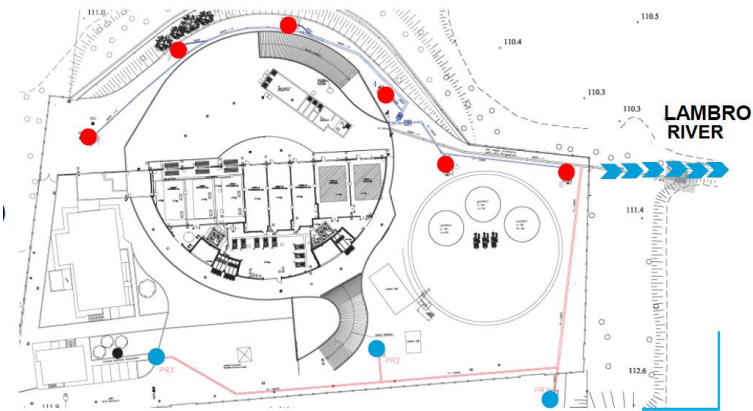
Operating since: 2009 and 2012

# DIRECT USES OF GEOTHERMAL ENERGY



# DIRECT USES OF GEOTHERMAL ENERGY

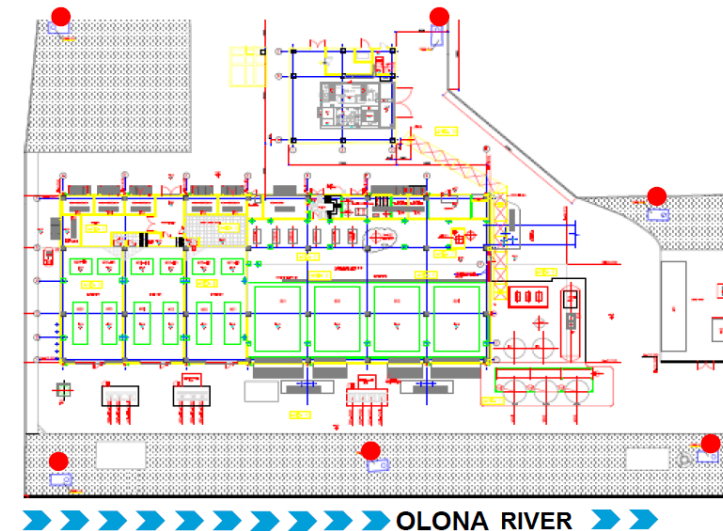
## Canavese wells



- Production wells
- Injection wells

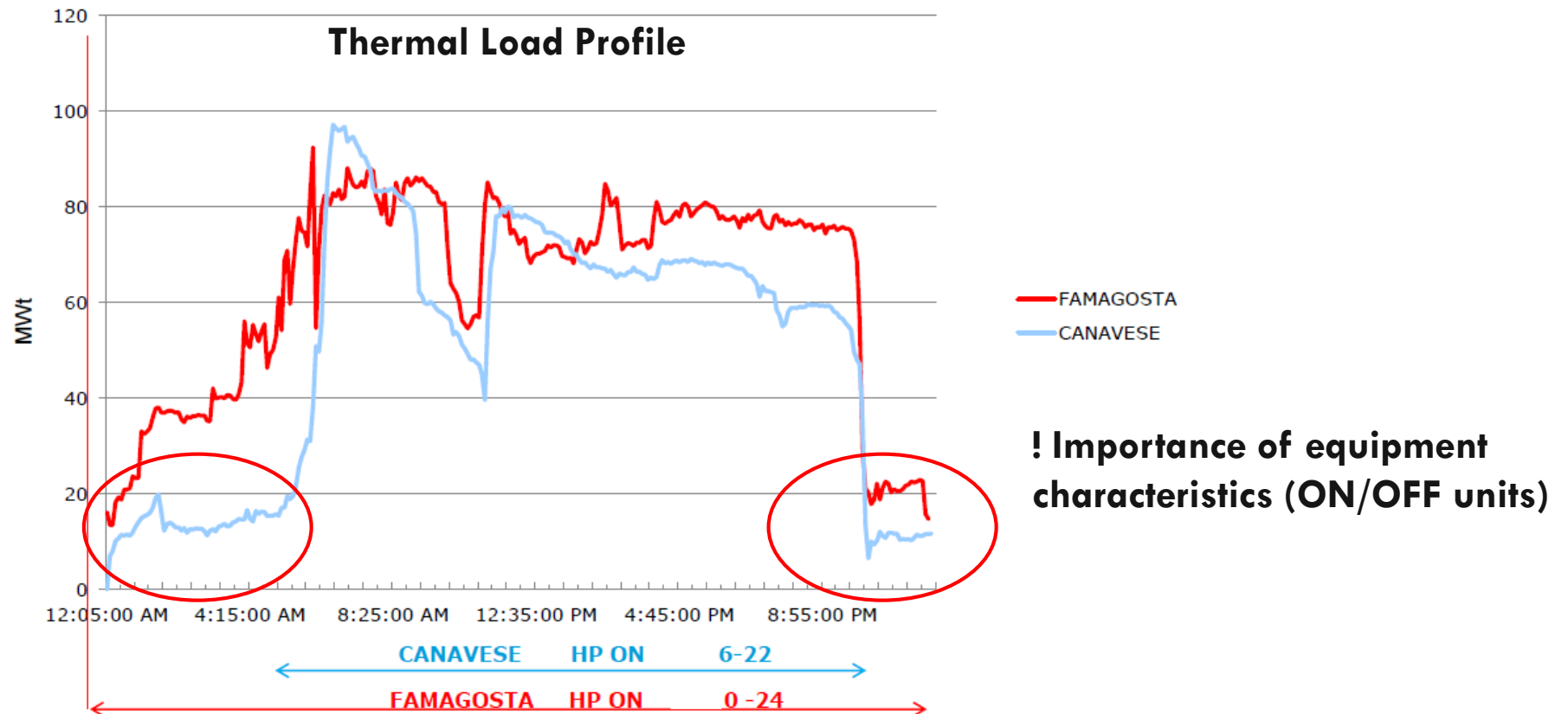
Aquifer depth: 12-35 m  
Nominal flow rate: 1000 m<sup>3</sup>/h

## Famagosta wells



Aquifer depth: 7-8 m  
Nominal flow rate: 1000 m<sup>3</sup>/h

# DIRECT USES OF GEOTHERMAL ENERGY





# DIRECT USES OF GEOTHERMAL ENERGY

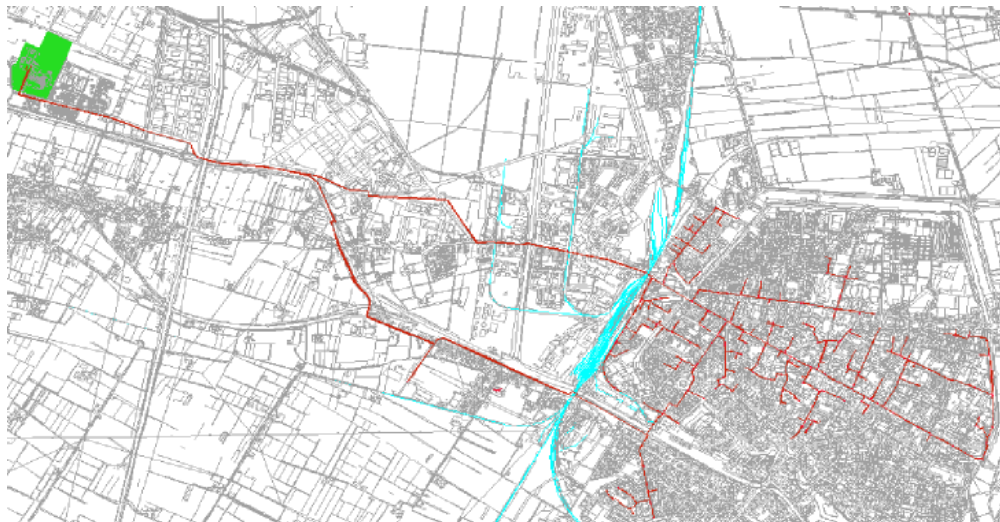
[GWh]	2011	2012	2013
Total heat delivered by TLR	732.529	756.823 (+ 3%)	839.786 (+11%)
Heat delivered by GWHPs (Reference point #2)	48.392	56.559 (+ 17%)	61.538 (+ 9%)
Seasonal COP	2.64	2.64	2.65
Geothermal Energy use	30.061	35.135 (+ 17%)	38.316 (+ 9%)

**! Importance of end-user loop temperature**

- The evolution of the geothermal energy use is related to the load profile

# DIRECT USES OF GEOTHERMAL ENERGY

## District Heating Systems (Ferrara, IT)



### Operative parameters:

Total capacity: 155 MW<sub>th</sub>

Geothermal capacity: 14 MW<sub>th</sub>

Operating temperature of the DH: 90 – 60 °C

Temperature of the geothermal fluid: 100-90 °C

DH length: ~56 km

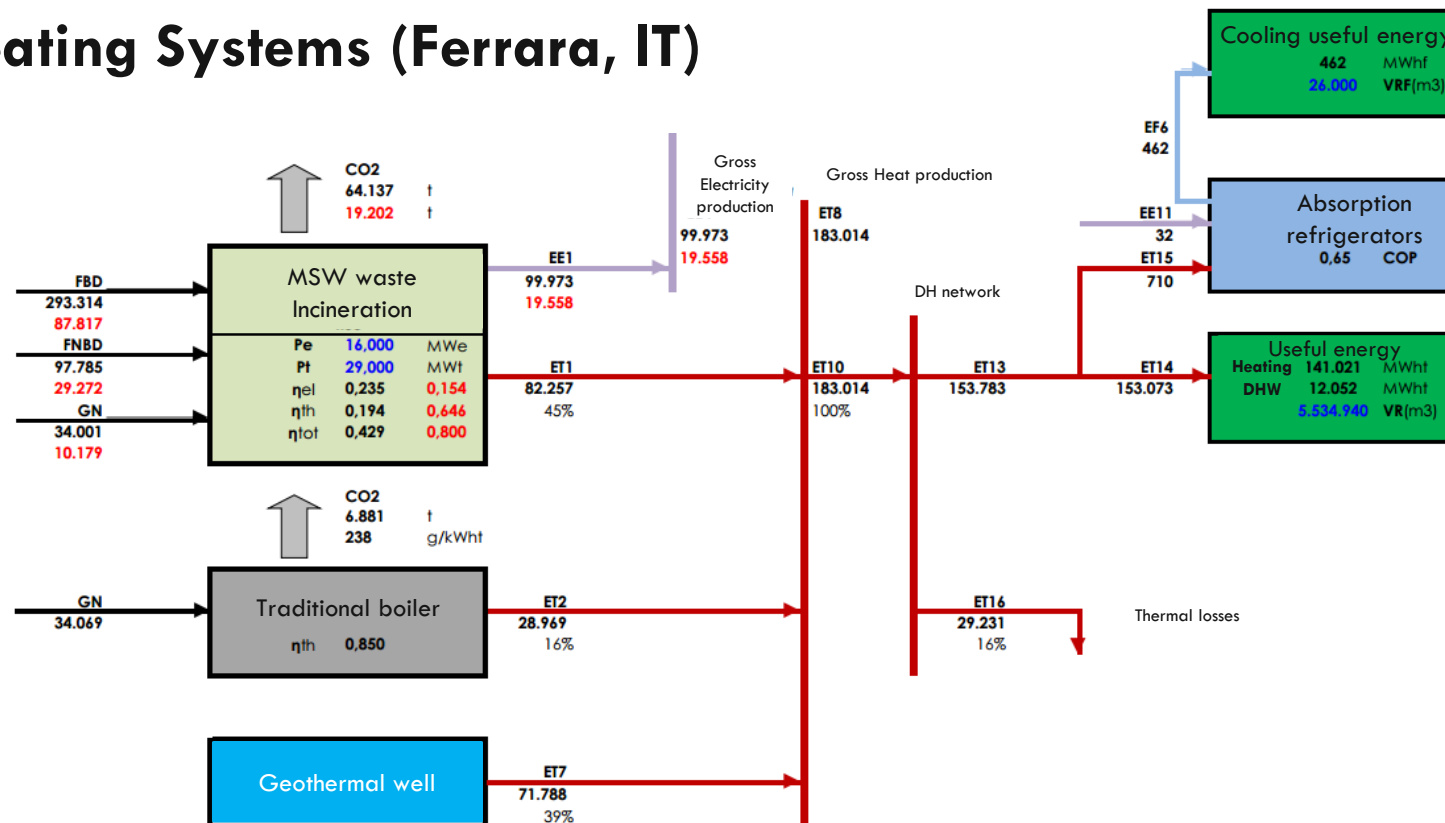
Total heated volumetry: 5.5 x 10<sup>6</sup> m<sup>3</sup>

Total thermal energy delivered to final users: >150 GWh/y ≈ 540 TJ/y

Total geothermal energy delivered:  
72 GWh/260 TJ/y (gross) 60 GWh/216 TJ/y (net)

# DIRECT USES OF GEOTHERMAL ENERGY

## District Heating Systems (Ferrara, IT)



# DIRECT USES OF GEOTHERMAL ENERGY

## Geothermal greenhouse (Piancastagnaio, IT)



The largest Italian and European greenhouse compound fed by geothermal energy is located in Mt. Amiata region, downstream of Enel's power plants.

Core business is tropical ornamental plants.

The main operation data in 2012 were as follows:

- Surface area: 230,000 m<sup>2</sup>
- Capacity installed: 35 MW<sub>th</sub>
- Geo-energy used : 450 TJ/y



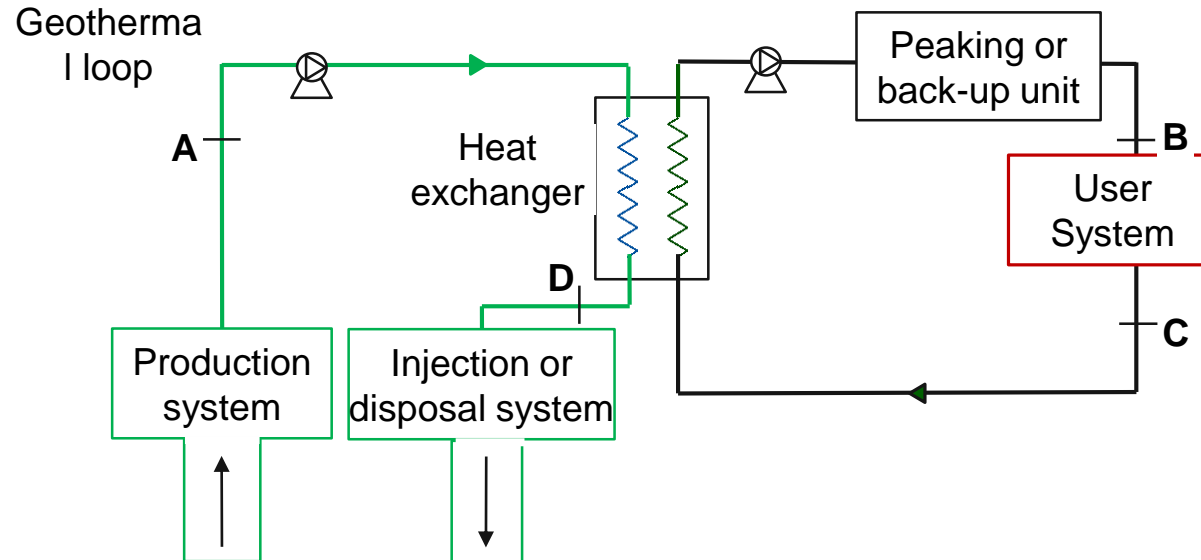
# DIRECT USES OF GEOTHERMAL ENERGY



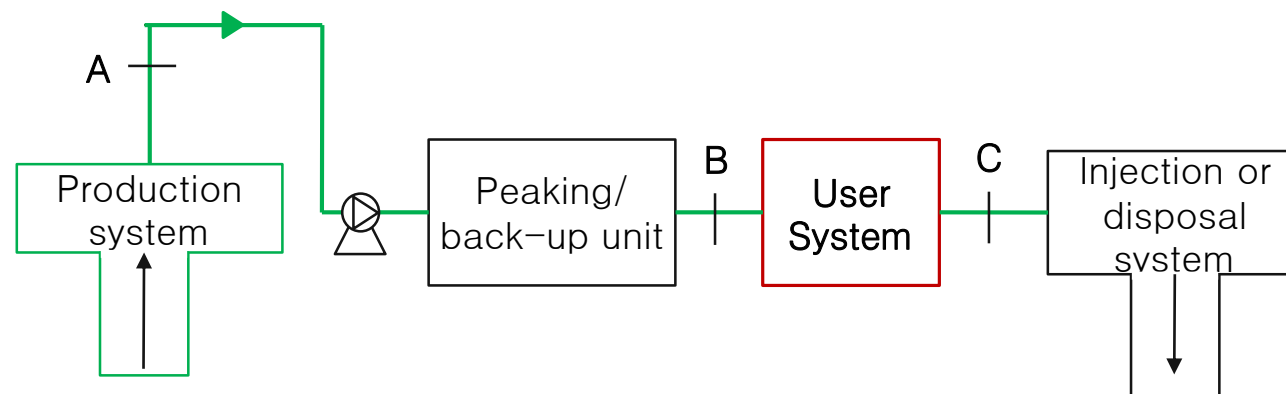
	Euganean district <i>Veneto</i>	Ischia <i>Campania</i>
Total users [10 <sup>6</sup> people]	3.5	1
Water used [m <sup>3</sup> x10 <sup>6</sup> ]	28	8
Water temperature [°C]	38-75	45-100
Energy used [T]/yr]	1 200	350

	Montecatini Terme <i>Tuscany</i>	Terme dei Papi <i>Latium</i>
Total users [10 <sup>6</sup> people]	1.6	1
Water used [m <sup>3</sup> x10 <sup>6</sup> ]	3.2	6
Water temperature [°C]	30	49-58
Energy used [T]/yr]	90	240

# DIRECT USES OF GEOTHERMAL ENERGY



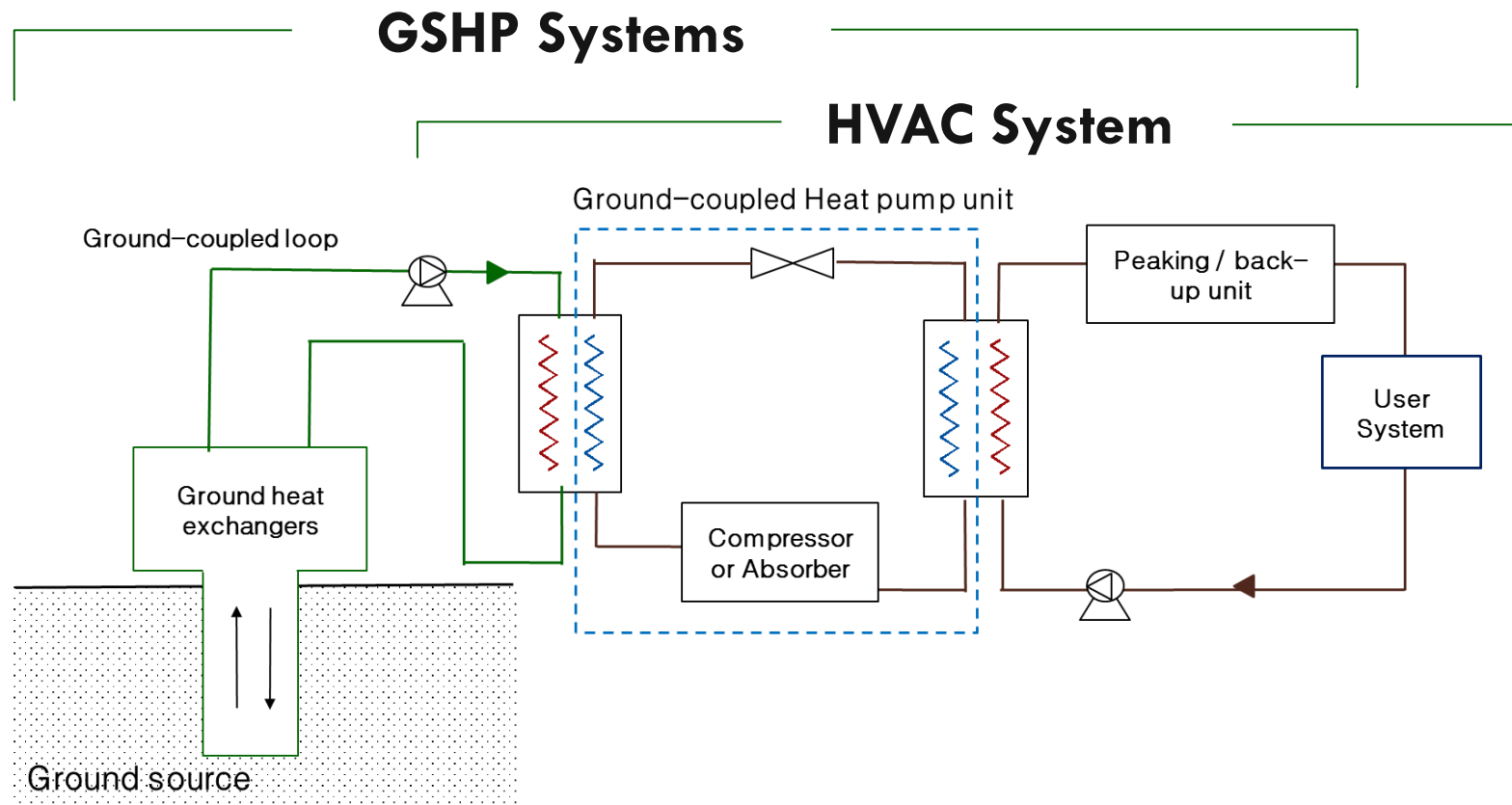
**Direct use system with heat exchanger**



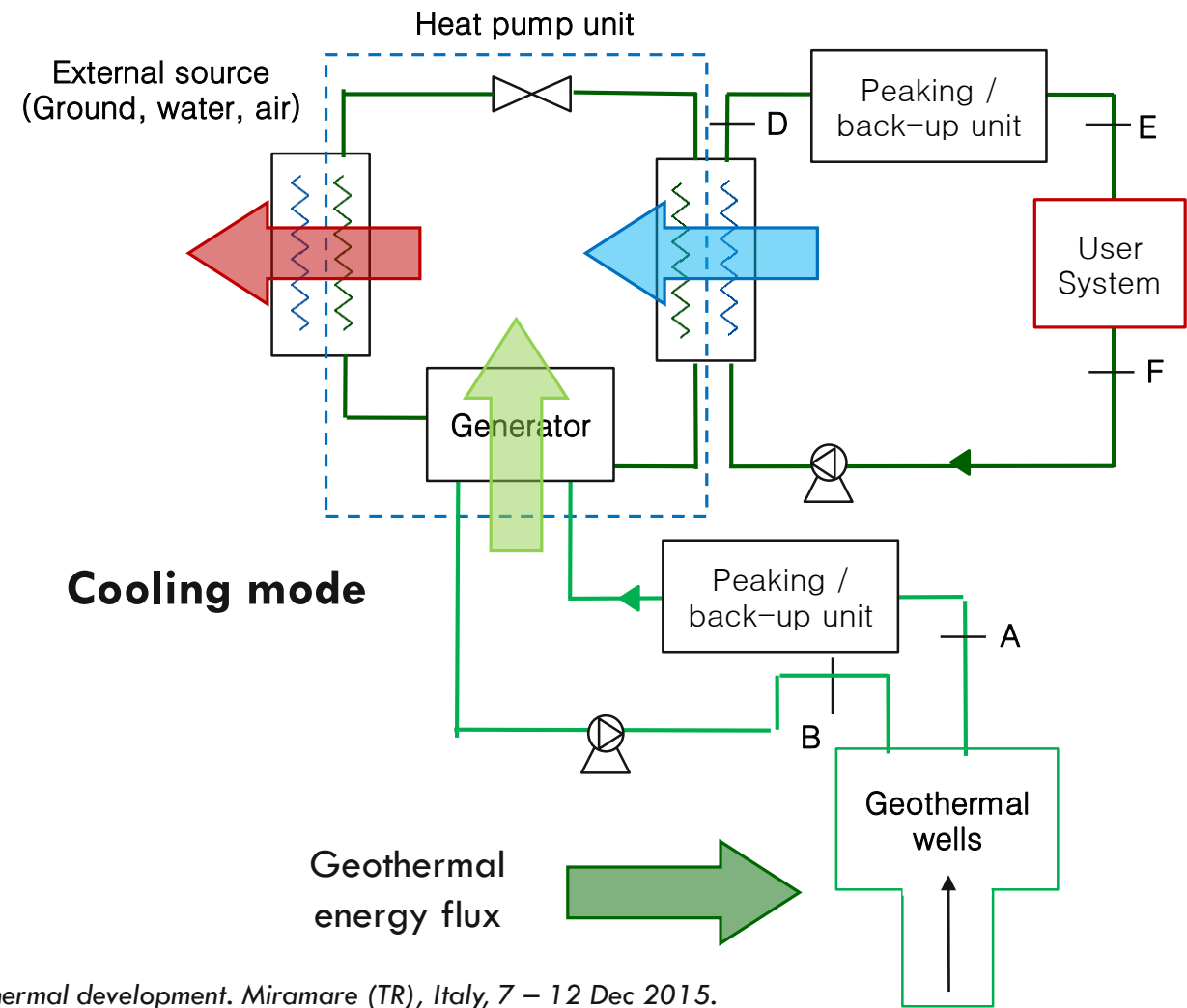
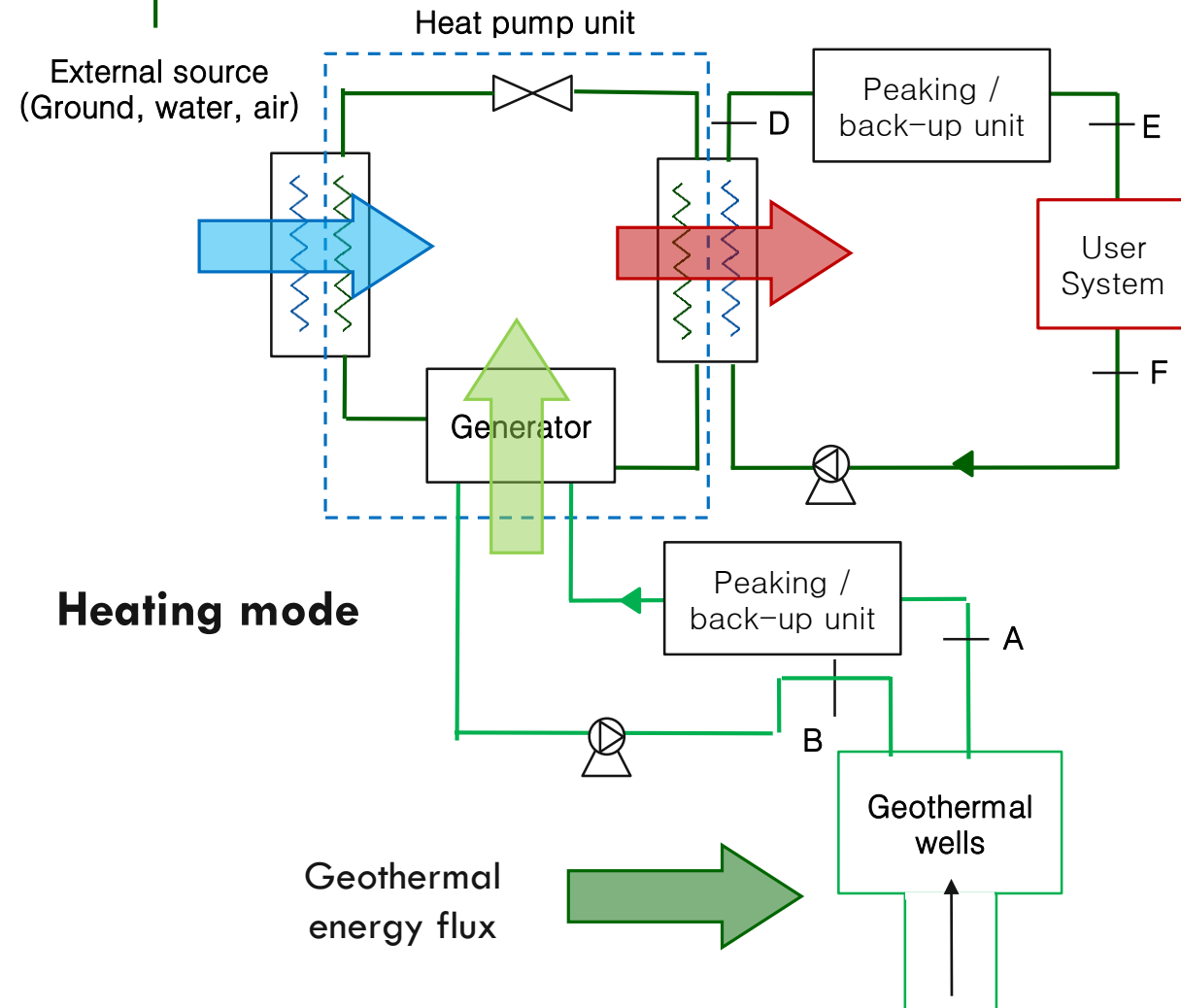
**Direct use without heat exchanger (e.g. balneology applications)**

# DIRECT USES OF GEOTHERMAL ENERGY

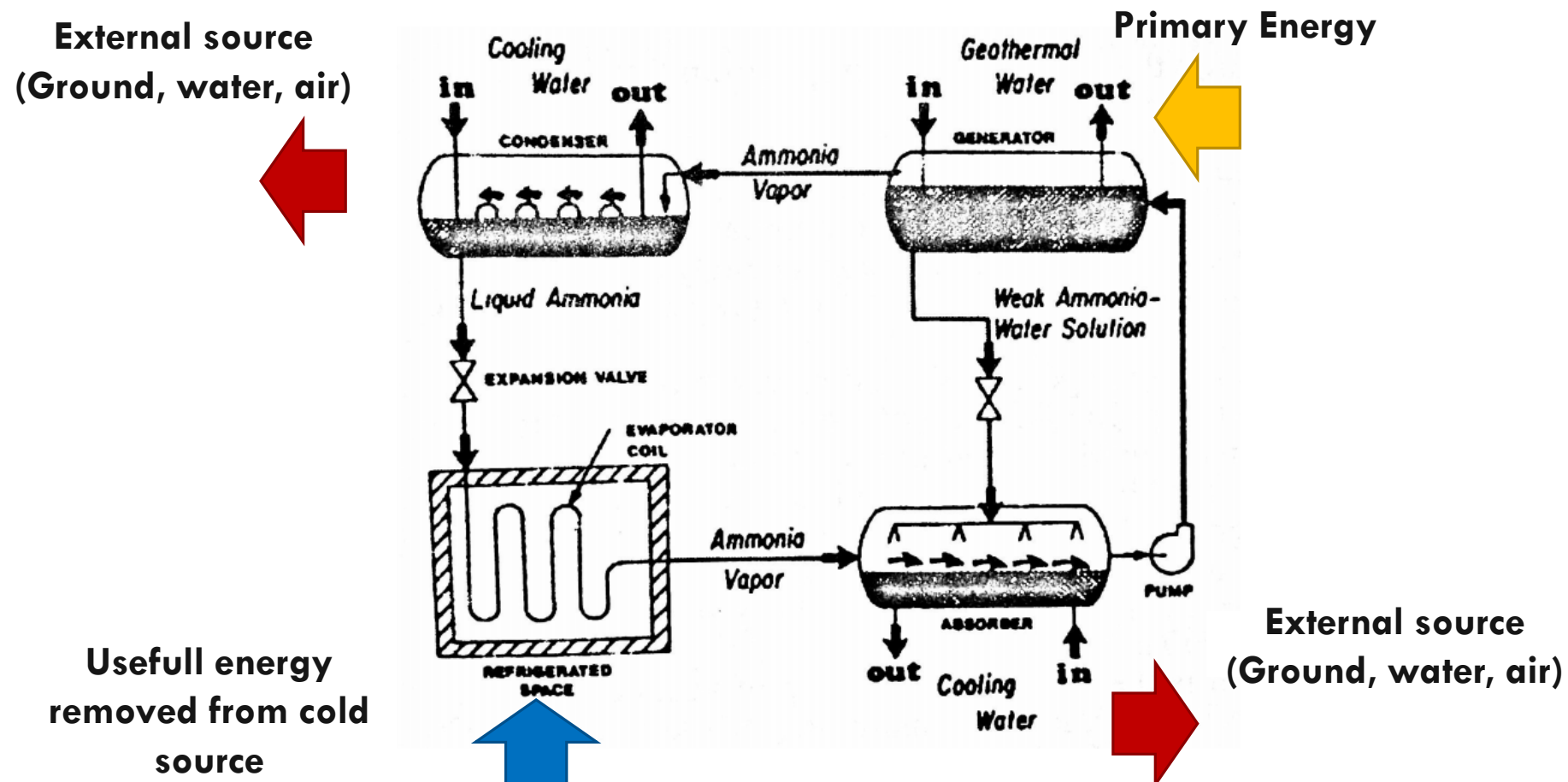
## GSHPs: equipment layout



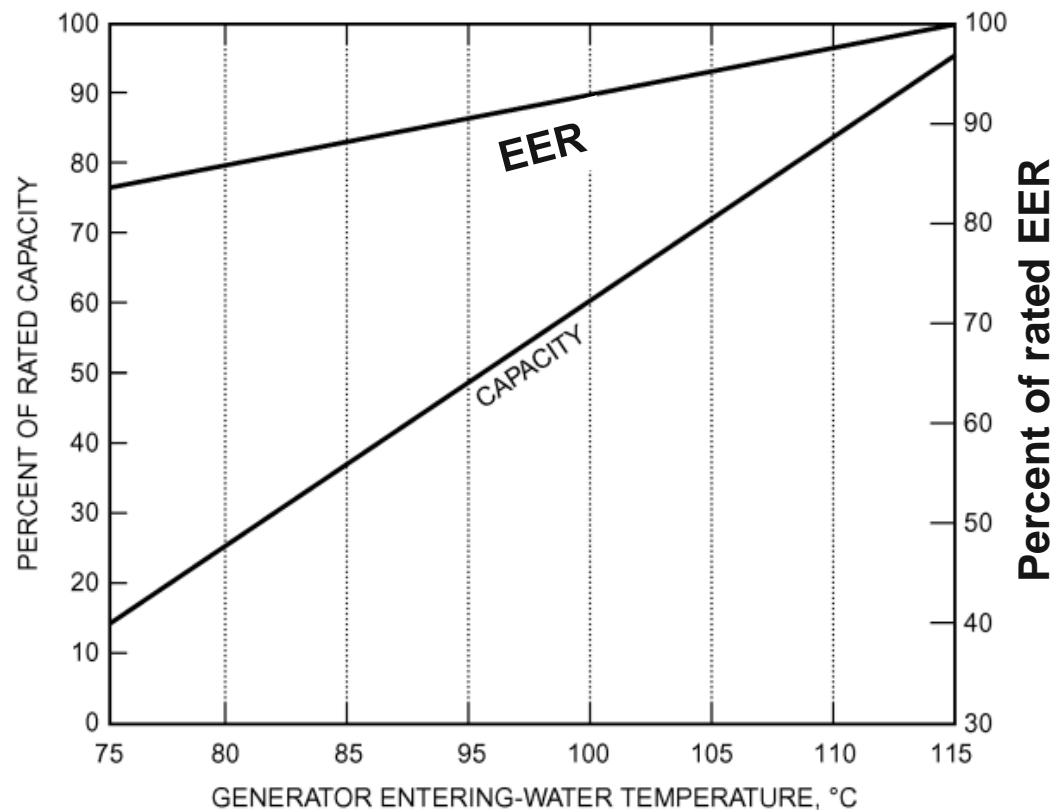
# DIRECT USES OF GEOTHERMAL ENERGY



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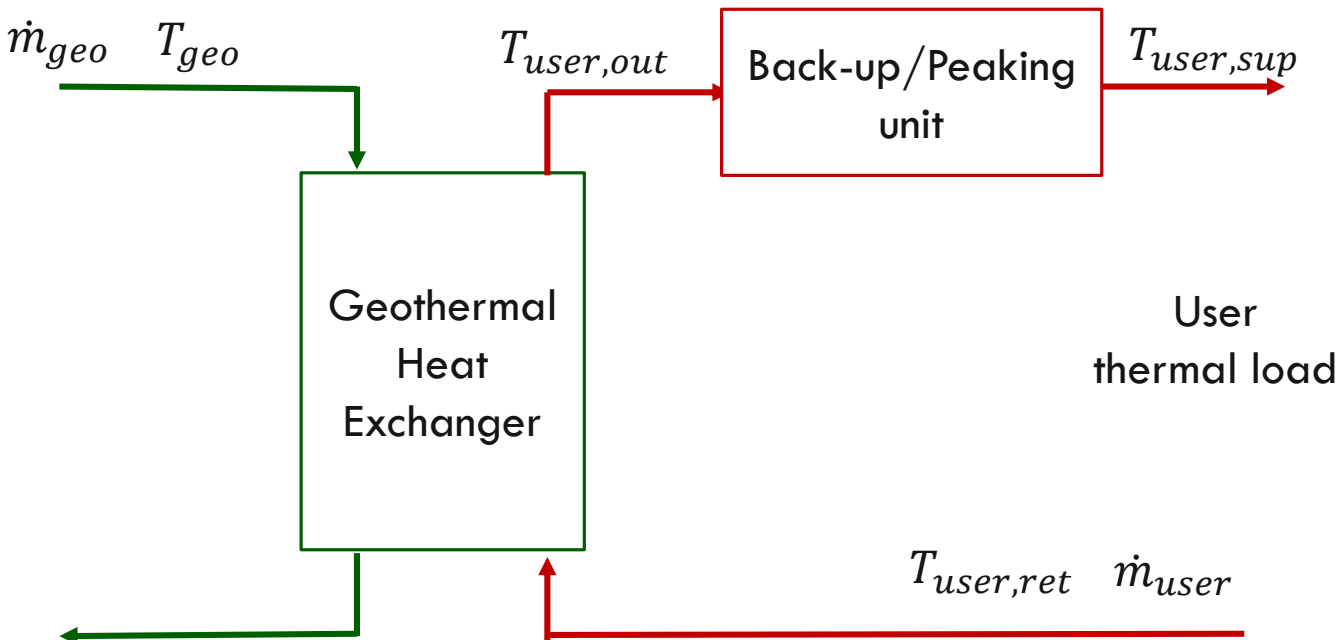
## Typical Lithium Bromide Absorption Chiller Performance Versus Temperature

!PER of Absorption Chillers  $\approx 0.6$   
 !PER of vapor-compression unit  $\approx 1.4 - 1.8$

!EER of Absorption Chillers  $\approx 0.6$   
 !EER of vapor-compression unit  $\approx 3.5 - 5.5$

! Thermal energy cost should be  $\sim 6$  times less than electricity costs

# DIRECT USES OF GEOTHERMAL ENERGY



## ! Rough analysis / ! First-order evaluation

$C_{f,bk}$  - \$/kWh Unitary costs of standard fuel (avoided energy consumption)

$L$  - kWh Annual energy demand

$\dot{m}_{geo}, T_{geo}$  Geo-resource characteristics

$T_{user,ret}$  Operational return temperature from user loop

$\epsilon$  Geo Hex effectiveness

# INVESTMENT ASSESSMENT OF DIRECT USES SYSTEMS



$$T_{geo} > T_{user,ret}$$



A – Radiators

$$T_{user,ret} \approx 50 - 70 \text{ } ^\circ\text{C}$$

B – Fancoils

$$T_{user,ret} \approx 30 - 40 \text{ } ^\circ\text{C}$$

C – Radiant floor

$$T_{user,ret} \approx 20 - 30 \text{ } ^\circ\text{C}$$

B





# DIRECT USES OF GEOTHERMAL ENERGY

## Heat exchanger basic theory

*Capacity rate ratio:*

$$C^* = \frac{C_{\min}}{C_{\max}} \quad (0 \leq C^* \leq 1)$$

*Exchanger heat transfer effectiveness:*

$$\epsilon = \frac{q}{q_{\max}} \quad (0 \leq \epsilon \leq 1) \quad \begin{array}{ll} q_{\max} = C_c(T_1 - t_1) & (C_c < C_h) \\ q_{\max} = C_h(T_1 - t_1) & (C_h < C_c) \end{array}$$

# DIRECT USES OF GEOTHERMAL ENERGY

## Heat exchanger basic theory

*Number of transfer units:*

$$N_{tu} \equiv \frac{US}{C_{\min}} = \frac{1}{C_{\min}} \int_S U dS$$

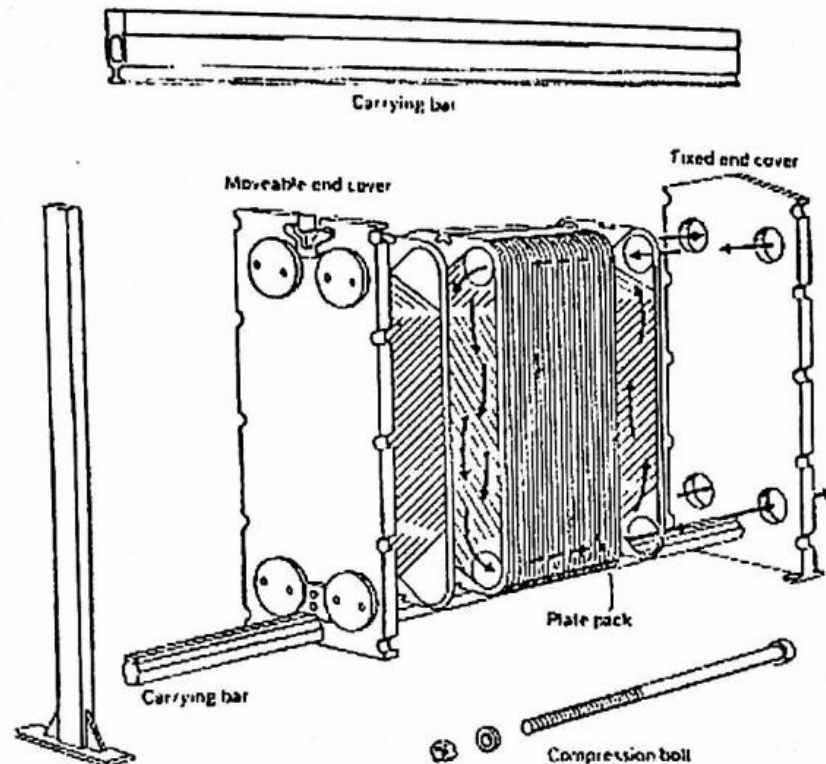
*Actual heat transfer performances*

$$\epsilon = \frac{q}{q_{\max}} = \frac{C_h(T_2 - T_1)}{C_{\min}(T_1 - t_1)} = \frac{C_c(t_2 - t_1)}{C_{\min}(T_1 - t_1)} \quad \epsilon = f(C^*, N_{tu}, \text{flow arrangement})$$

# DIRECT USES OF GEOTHERMAL ENERGY

## PLATE AND FRAME HEAT EXCHANGERS

(Yesin, 1997)



### Advantages:

Low space required («performance density»):  $100-200 \text{ m}^2/\text{m}^3$

Low temperature approach: 1-2 K

High overall heat transfer coefficient:  
**3000-8000 W/(m<sup>2</sup> K)**

Low corrosion rate: <0.05 mm/yr

### General disadvantages :

Work pressure: < 25 bar

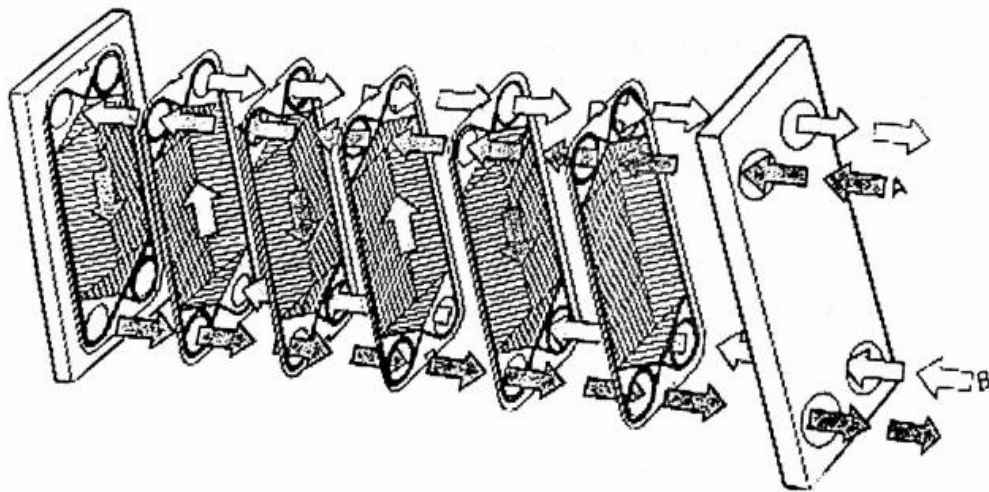
Work temperature: < 200 °C

**! Suitable solution for geothermal applications**

# DIRECT USES OF GEOTHERMAL ENERGY

## PLATE AND FRAME HEAT EXCHANGERS

(Yesin, 1997)



### Indicative data:

**Frame Material:** Carbon Steel

**Bolt Material:** High tensile steel

**Heating Surface Area:** 0.1-2200 m<sup>2</sup>

**Number of Plates:** 30 – 500

**Fluid Flow Rates:** 4-3600 m<sup>3</sup>/h

**Diameter of Connections:** 12-500 mm

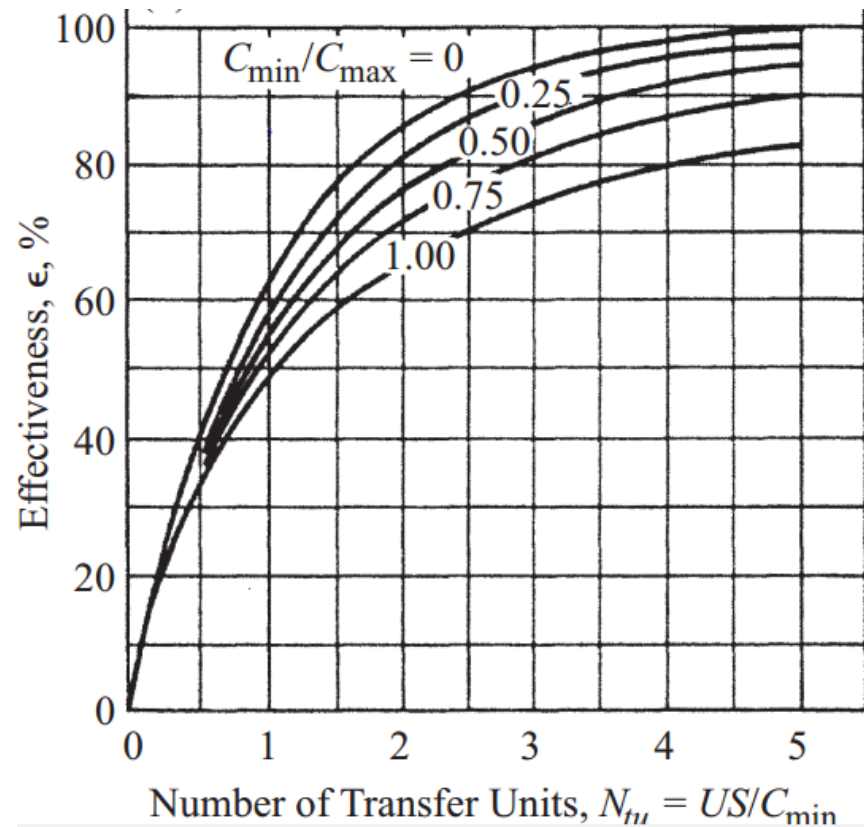
**Plate Thickness:** 0.5 - 1.2 mm

**Overall Heat Transfer Coefficient:** 3000 - 7000 W/m<sup>2</sup>/K

**NTU:** 0.3 – 4

**Pressure drop:** 30 kPa per NTU

# DIRECT USES OF GEOTHERMAL ENERGY



## Costs:

An example of a typical correlation between HE cost and HE surface:

$$C = 401 A^{0.4887} \quad \text{stainless steel}$$

$$C = 612 A^{0.4631} \quad \text{titanium}$$

C - \$

(Haslego & Polley, 2002)

A - Surface ft<sup>2</sup>

## Optimal design criterion

According to heat transfer physics, large **heat transfer surfaces** result in better **performances** (till saturation), but also additional **installation and operative costs** (head losses)

# DIRECT USES OF GEOTHERMAL ENERGY

## Pump power

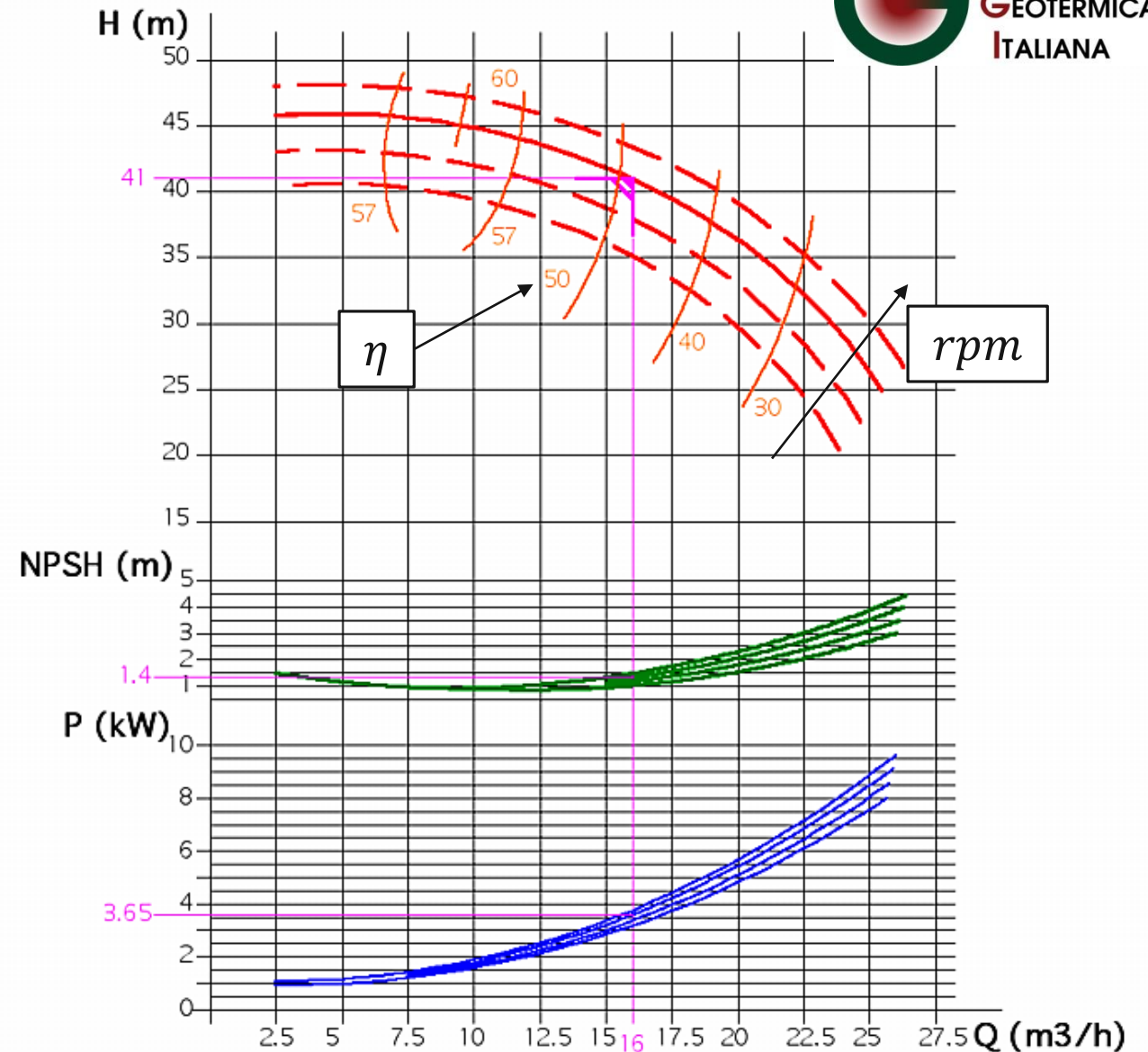
Hydraulic power

$$W_{id} = \rho \dot{Q} H g = \left[ \frac{\text{kg}}{\text{m}^3} \right] \left[ \frac{\text{m}^3}{\text{s}} \right] [\text{m}] \left[ \frac{\text{m}}{\text{s}^2} \right] = [\text{W}]$$

Electric input power

$$W_{in} = \frac{W_{id}}{\eta}$$

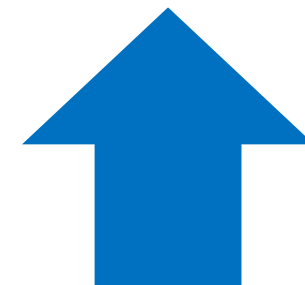
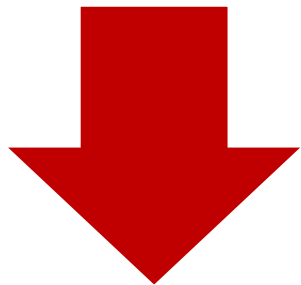
Indicative $\eta$ values	$W_{in}$ - kW	$\eta$
Circulator pumps	<0.1	0.1-0.25
	0.1 – 0.5	0.2 – 0.4
	0.5 – 2.5	0.3 – 0.5
Electro-mechanic pumps	<1.5	0.3-0.6
	1.5-7.5	0.35 – 0.75
	7.5 - 45	0.4 – 0.75



# DIRECT USES OF GEOTHERMAL ENERGY

High levels of exploitation result in an excessive alteration of the ground temperature resulting in GHP efficiency decrease (i.e. high operative costs)

Large heat transfer surfaces are required to minimize the impact of heat removal/injection from the source (i.e. high installation costs)



Low levels of exploitation do not take advantage of a favorable thermal source, reducing overall system efficiency (i.e. high operative costs)



# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

$$CR = \frac{\text{Useful energy}}{\text{Nominal capacity}} \propto \frac{\text{Energy (Economic) savings}}{\text{Installation costs}}$$

## Primary energy savings

Thermal load is delivered with **lower primary energy consumption** than alternative technologies

**Back-ups and auxiliaries** performances should be considered

Main parameters affecting direct geothermal applications performances are:

Temperature of geothermal fluid

Pumpung energy

Temperature of the ground source and end-user loop

**Capacity ratio** (i.e. thermal load evolution)

## Economic profitability

Installation costs:

- Equipment **retail and drilling costs**

Operative costs:

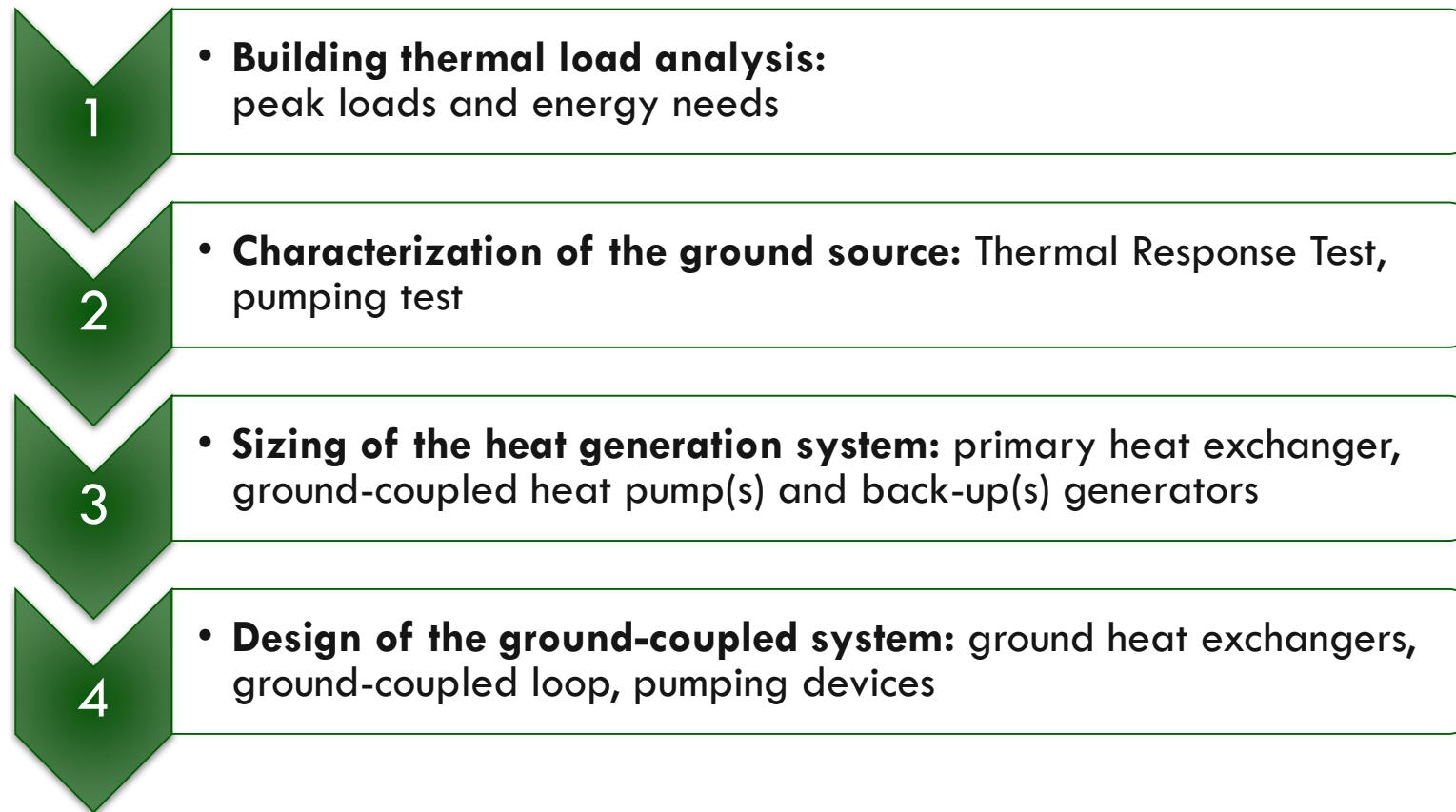
- **Energy savings**
- **Prices/Fares** of electricity and natural gas

Other non-technical parameters:

- **Inflation** of energy prices
- Evolution of retail prices (i.e. market situation)
- **Operators fees**
- Possible **financial incentives**



# TRADITIONAL/HANDBOOK DESIGN PROCEDURE



# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

## TRADITIONAL/HANDBOOK DESIGN PROCEDURE FOR GSHPs

1. Calculate reference cooling and heating loads, and estimate off-peak loads;
2. Evaluate annual heat extraction from and rejection to the ground through an estimation of seasonal COP, seasonal EER, and equivalent full load hour in cooling and heating mode
3. Select operative temperatures of the circulating fluid within the BHEs
4. Select ground-coupled heat pump(s) according to a proper share of cooling and/or heating loads
5. Design pipework apparatus aiming at minimizing duct costs and hydraulic losses
6. Conduct site survey to determine ground thermal properties and drilling conditions
7. Determine and evaluate possible BHE field arrangements that are likely to be optimum for the specific building and site (bore depth, separation distance, completion methods, annulus grout/fill, and header arrangements);
8. Determine ground heat exchanger dimensions;
9. Iterate and optimize to evaluate alternative operative temperatures, flow rates, BHEs arrangement, etc;
10. Design end user-loop
11. Select auxiliaries (e.g. pumps). If pumping energy exceeds 8 % of the total system demand different loop layouts should be investigated.

# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

## ASHRAE method

ASHRAE method is the worldwide reference methodology for BHEs sizing (ASHRAE 2011)

ASHRAE method uses two similar equations to evaluate the necessary BHE depth in heating and cooling mode. The final borehole size corresponds to the larger one.

$$H_{BHE,H} = \frac{\dot{Q}_a R_{g,a} + (\dot{Q}_{lh} - \dot{W}_h) (R_b + PLF_m R_{g,m} + R_{g,d} F_{sc})}{T_g^0 - \frac{T_{w,in} + T_{w,out}}{2} - T_p}$$

$$H_{BHE,C} = \frac{\dot{Q}_a R_{g,a} + (\dot{Q}_{lc} - \dot{W}_c) (R_b + PLF_m R_{g,m} + R_{g,d} F_{sc})}{T_g^0 - \frac{T_{w,in} + T_{w,out}}{2} - T_p}$$

# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

(UNI, 2012)

## Horizontal GCHPs

$$L_{h,p} = \frac{\dot{Q}_{g,h_D} \times (R_p + R_g \times P_m \times S_m \times F_h)}{\theta_{g,L} - \left(\frac{\theta_{wi} + \theta_{wo}}{2}\right)_{h_D}}$$

**R<sub>p</sub>**: ducts thermal resistance

**R<sub>g</sub>**: effective ground thermal resistance

**P<sub>m</sub>**: correction factor due to pipe diameter

$$L_{c,p} = \frac{\dot{Q}_{g,c_D} \times (R_p + R_g \times P_m \times S_m \times F_c)}{\theta_{g,H} - \left(\frac{\theta_{wi} + \theta_{wo}}{2}\right)_{c_D}}$$

**S<sub>m</sub>**: correction factor due to trenches distance

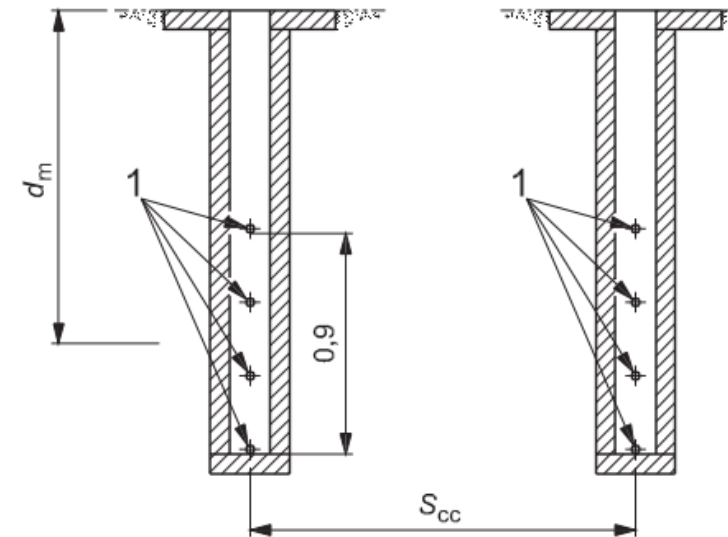
**F<sub>h,c</sub>**: Part load factor during the design month

# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

(UNI, 2012)

Thermal conductivity	Ground resistance	$S_m$				
		# trenches	$(S_{cc})$ (m)			
$\lambda_g$ W/(m K)	$R_g$ (m K)/W		3,35	2,74	2,13	1,52
0,35	4,22	2	1,01	1,03	1,07	1,15
		4	1,02	1,05	1,11	1,24
		6	1,02	1,05	1,12	1,27
0,87	1,89	2	1,04	1,07	1,12	1,21
		4	1,06	1,11	1,2	1,38
		6	1,06	1,12	1,23	1,44
1,30	1,31	2	1,05	1,09	1,15	1,23
		4	1,08	1,14	1,24	1,43
		6	1,09	1,15	1,27	1,5
1,73	1,00	2	1,06	1,1	1,16	1,25
		4	1,1	1,17	1,27	1,47
		6	1,12	1,18	1,31	1,55
2,42	0,73	2	1,07	1,11	1,17	1,26
		4	1,11	1,18	1,3	1,5
		6	1,13	1,2	1,35	1,6

1 Pipes  
dm  $\approx$  2 m (indicative)



# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

## Groundwater wells - TRADEOFF

An open-loop system design focuses on **well pumping power** and **heat pump/heat transfer performances**

As groundwater flow increases, **more favorable average temperatures** occur within the heat exchanger (i.e. reduced temperature drop)

As groundwater flow increases, **pump power requirements increase.**

At some point, additional increases in groundwater flow result in a greater increase in well pump power than the resulting heat pump efficiency decreases

The key strategy in open-loop system design is **identifying the point of maximum system performance** with respect to heat pump and well pump power requirements.

# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

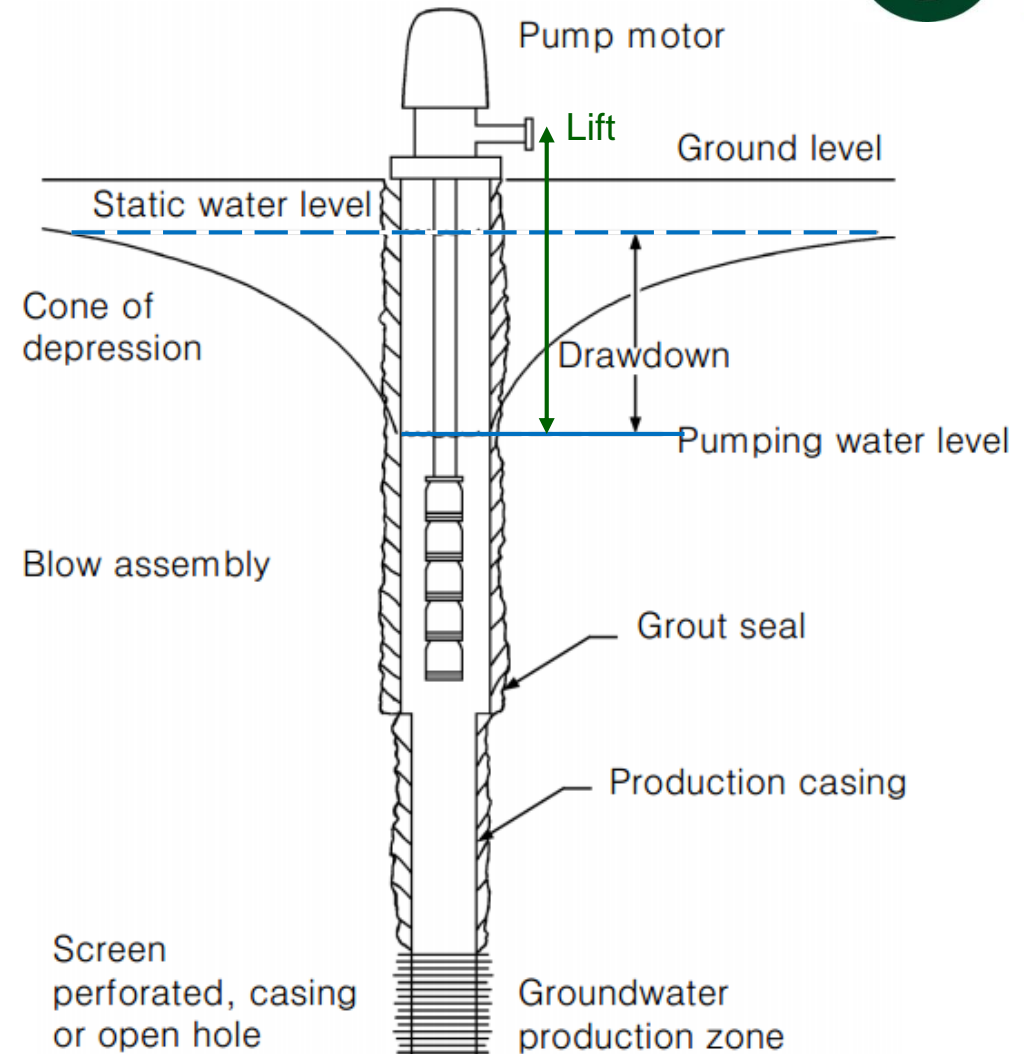
*Static water level (SWL)* is the level that exists under static (non-pumping) conditions

*Pumping water level (PWL)* is the level that exists under specific pumping conditions. It depends on pumping flow rates, well, and aquifer characteristics.

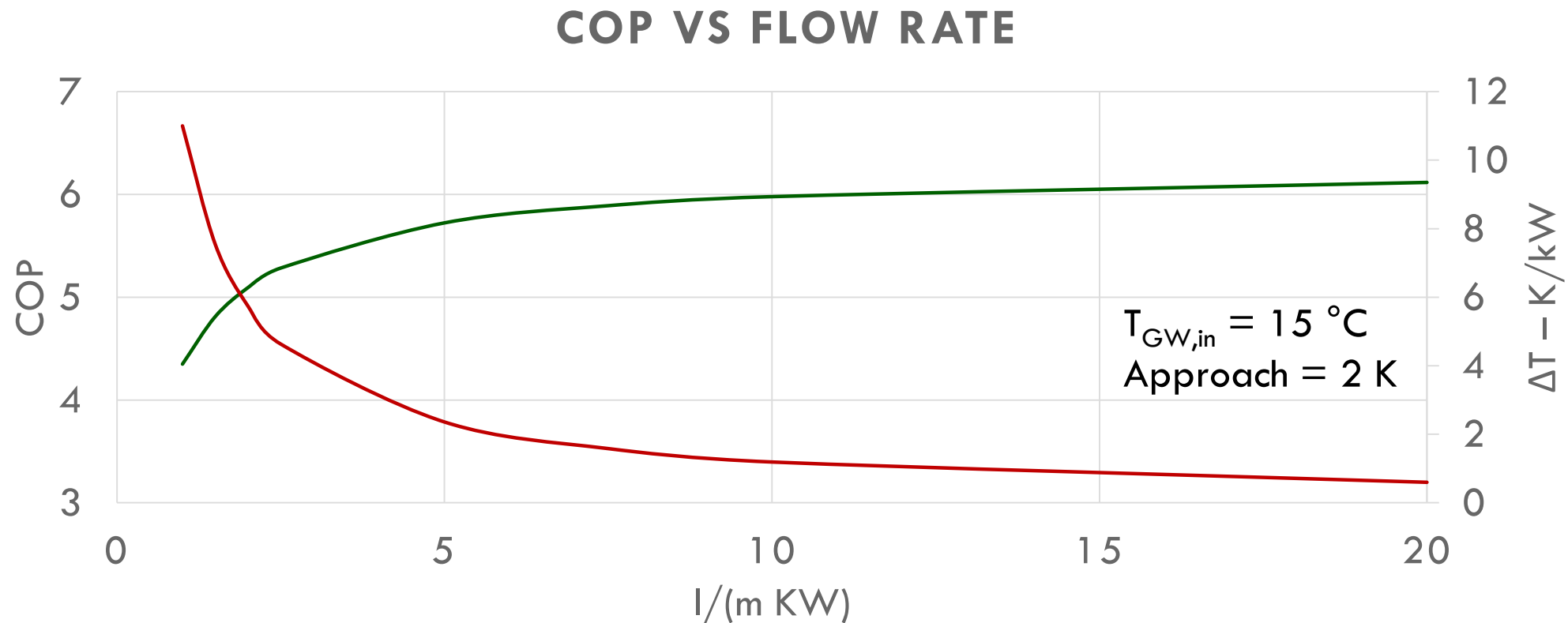
*Drawdown ( $s_w$ )* is the difference between the SWL and the PWL.

The *specific capacity* of a well is given by the pumping rate per meter of drawdown,  $l s^{-1} m^{-1}$

**Total pump head** is composed of four primary components: **lift**, column friction, surface requirements, and injection head due to aquifer conditions and water quality.

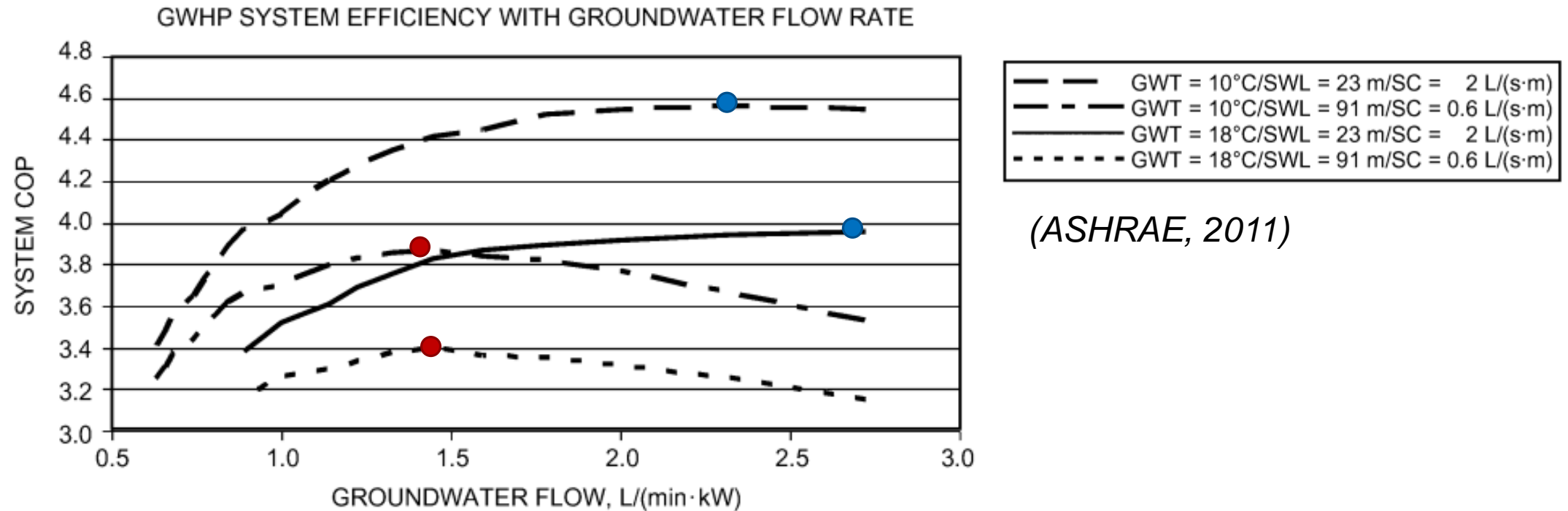


# TRADITIONAL/HANDBOOK DESIGN PROCEDURE





# TRADITIONAL/HANDBOOK DESIGN PROCEDURE



# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

## CURRENT DRAWBACKS

- ✓ Probable **oversizing** due to traditional engineering «precautionary principle»
- ✓ **Uncertainty** on final operative **performances**
- ✓ **Unfavorable cost-benefit ratio** among energy/economic savings and initial investment
- ✓ Several **competitor technologies** with similar performances, but more established design and installation methodologies
- ✓ **Lack of formation and specialization** among operators and authorities
- ✓ **Lack of communication among operators** (geologist, drillers, H&C system designers)
- ✓ **Lack of optimized design approach** in order to maximize system performances with respect of initial expenditure (CBA approach)

# ADVANCED/OPTIMIZED DESIGN

**Traditional engineering design process** is based on the classical “**precautionary principle**” to ensure the meeting of project specifications.

The latter point is obtained by **oversizing** the main equipment, on the basis of the worse operative situation, and the **installation of additional back-up devices**.

Modern engineering design approach is not aimed only at sizing system components to meet project specifications and constraints, but it seeks the **optimal design and management strategies** in terms of **energetic and economic performances**.

The latter looks for rigorous methods of decision making, such as **optimization methods**, which are based on the **predictions of the operative performances of the future project**.

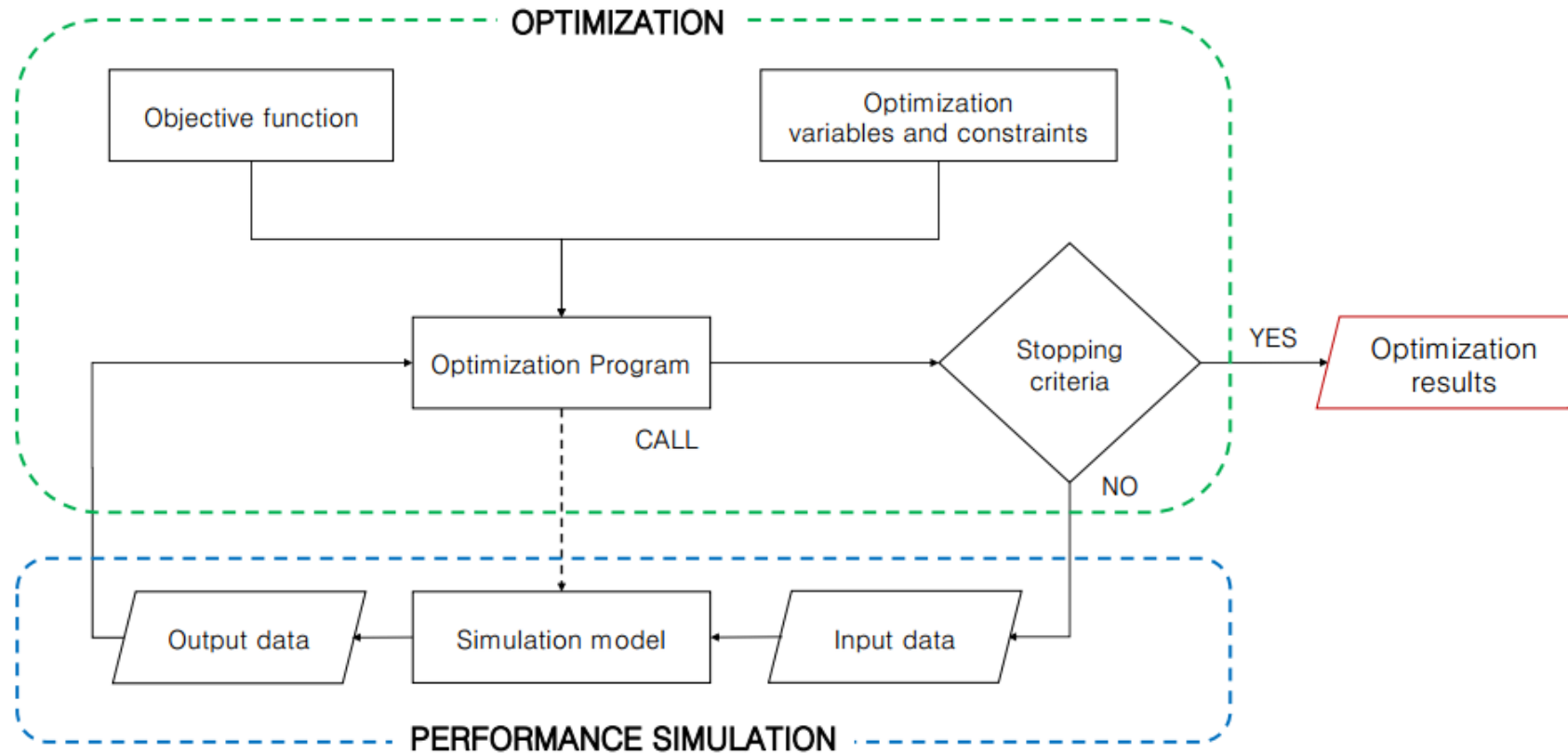
The accurate evaluation of the energy fluxes during the operative period is a mandatory input for any **cost-benefit analysis**.

# ADVANCED/OPTIMIZED DESIGN

The **optimal design configuration can be achieved through a holistic simulation** of the overall equipment on the basis of a proper modeling of the physical mechanisms involved and including mutual interactions among different components.

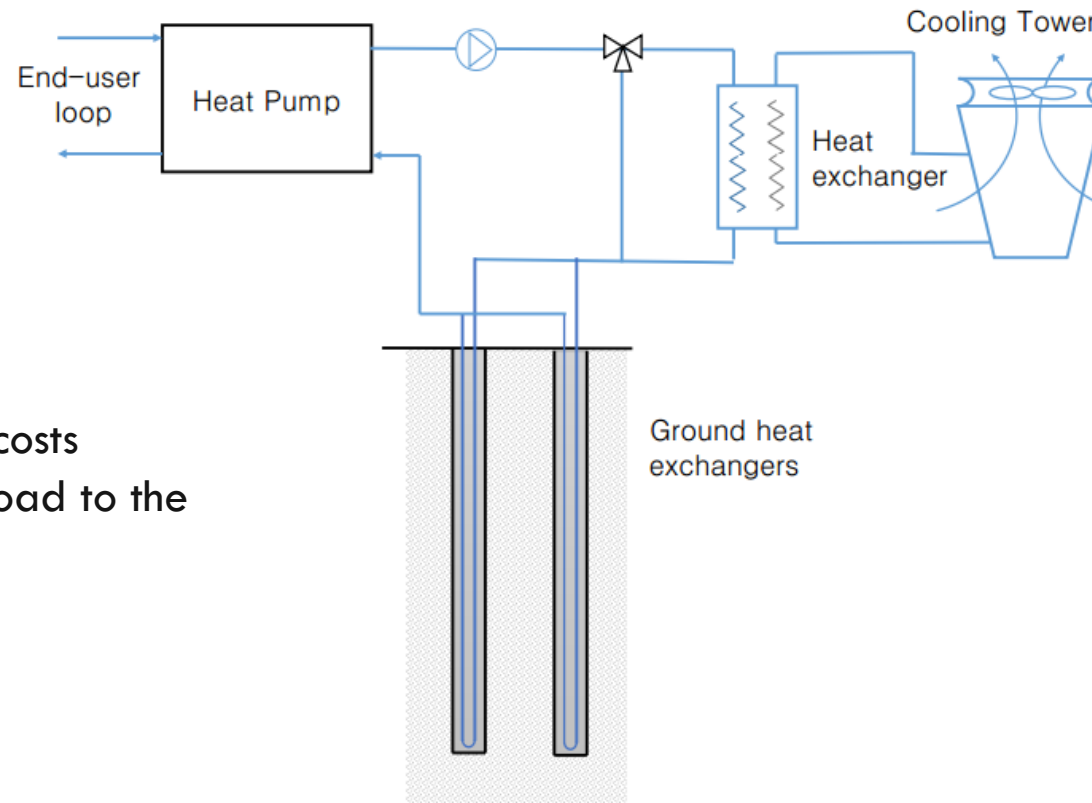
The **design of direct use systems** (GSHPs included) is a paradigmatic case to apply the above-mentioned considerations. Independently from the specific configuration adopted, these systems always require a **proper synergy among “geothermal devices” and back-ups in order to limit installation costs and ensure appropriate economic and energy savings**, together with the sustainable exploitation of the ground source.

# ADVANCED/OPTIMIZED DESIGN



# TRADITIONAL/HANDBOOK DESIGN PROCEDURE

## Hybrid systems



### Potential benefits:

1. Lower installation costs
2. Net-zero energy load to the ground source
3. Peak load

# ADVANCED/OPTIMIZED DESIGN

**A simple case study:** Heating system made of GSHP and Air-source HP (back-up)

$$COP_{GSHP} = \frac{T_l}{T_l - T_g(t)} \eta^{II} \quad \text{(GSHP unit performance)}$$

$$COP_{AHP} = \frac{T_l}{T_l - T_a(t)} \eta^{II} \quad \text{(Back-up performance)}$$

$$L(t) = \max [A_l \cdot \cos(2\pi/\omega_l t); 0] \quad \text{(Building thermal load profile)}$$

$$T_a(t) = \bar{T}_a - A_a \cdot \cos(2\pi/\omega_a t) \quad \text{(External air temperature profile)}$$

$$T_g(t) = T_g^0 + \int_0^t W(t - \beta) \frac{d\dot{q}}{d\beta}(\beta) d\beta \quad \text{(Ground temperature evolution)}$$

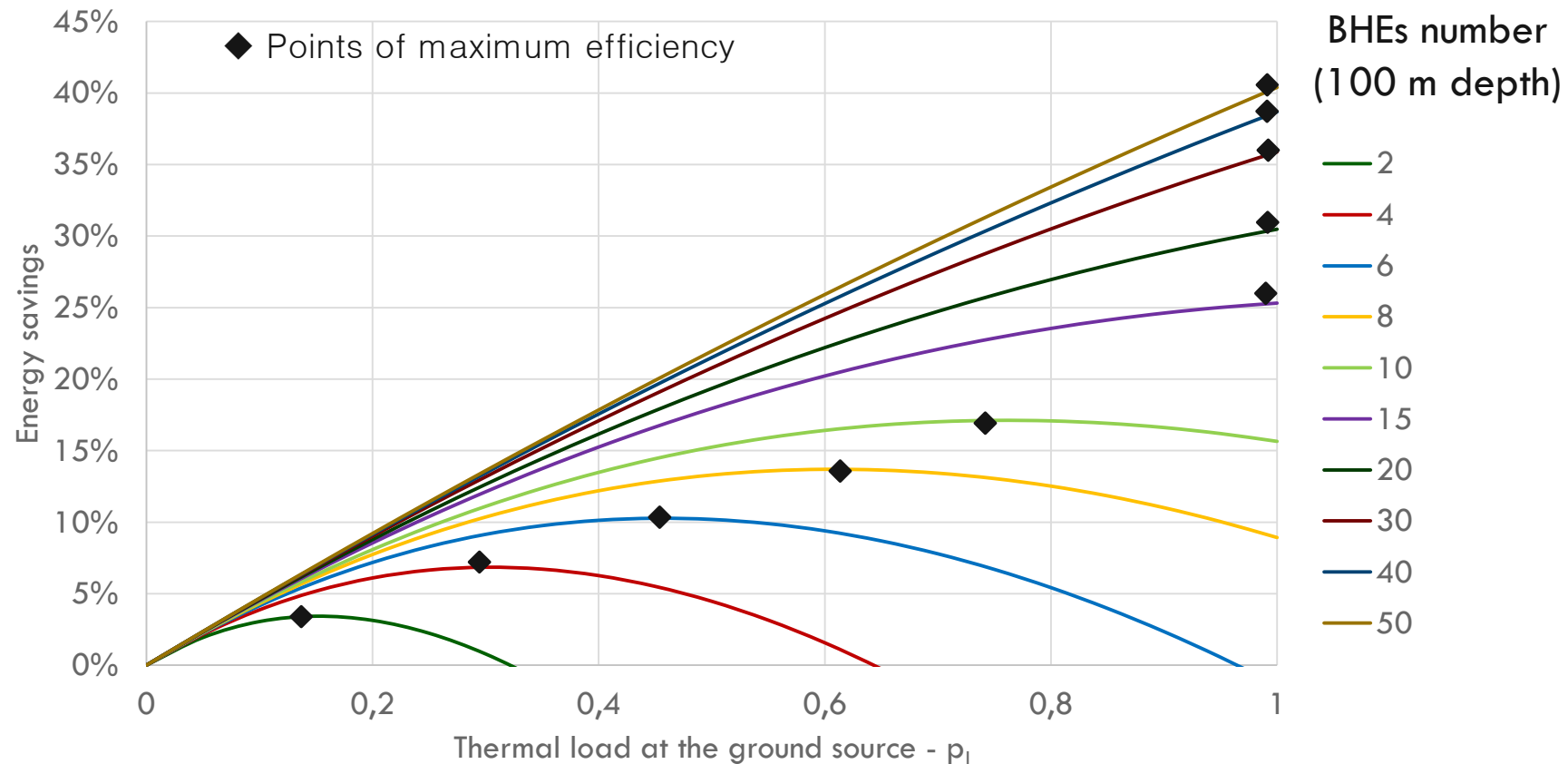
$$W(t) = \frac{1}{2\pi\lambda_g} \int_{\frac{R_{BHE}}{2\sqrt{\alpha_g t}}}^{+\infty} \frac{e^{-\beta^2}}{\beta} d\beta \quad \text{(Infinite line source model)}$$

$$\dot{q}(t) = \frac{p_l L(t)}{N_{BHE} H} \left( \frac{COP_{GSHP}(t) - 1}{COP_{GSHP}(t)} \right) \quad \text{(Energy balance of the BHE field)}$$



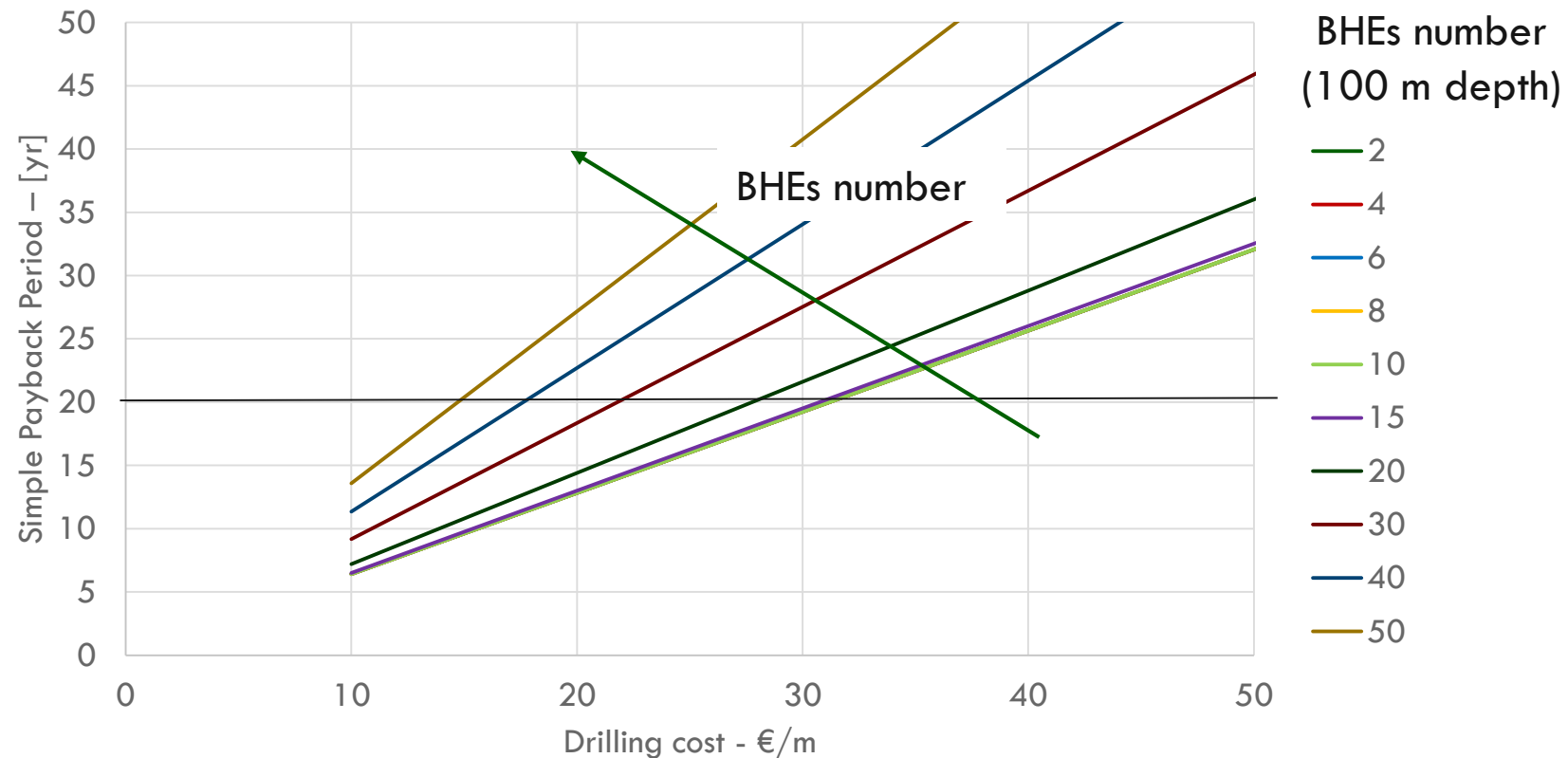
# ADVANCED/OPTIMIZED DESIGN

Energy savings with respect to an exclusive-AHP solution



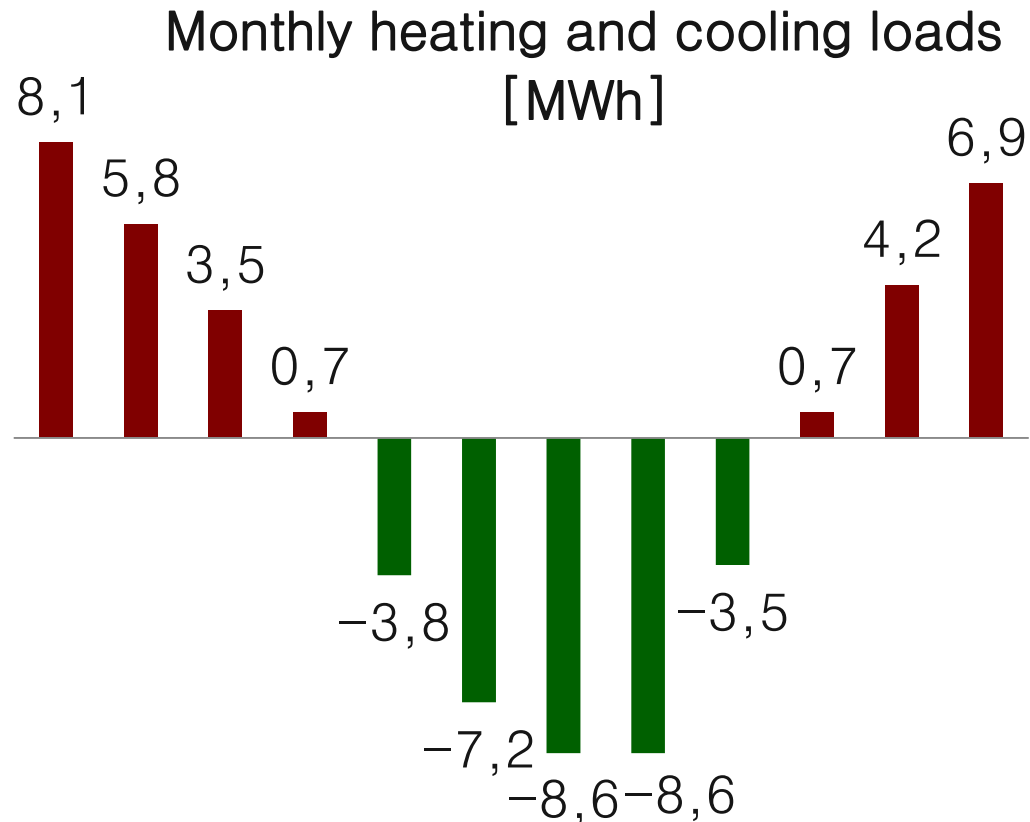
# ADVANCED/OPTIMIZED DESIGN

**Rough economic analyses of optimal configurations**



# ADVANCED/OPTIMIZED DESIGN

## Load profile



## Declared Capacities (kW) of the examined heat pumps (EN 14511:2008)

		Conf#1	Conf#2	Conf#3	Conf#4
GHP	Heating DC	35	10.7	12.1	-
	Cooling DC	40.5	12.1	8.88	-
Boiler		-	23.9	23.9	33.5
Air chiller		-	29.1	33.5	44.2

- **CONF#1:** GHP sized on the peak load
- **CONF#2:** GHP sized on the average power demand of the design months
- **CONF#3:** GHP sized on the seasonal average power demand
- **CONF#4:** No GSHP solution

# ADVANCED/OPTIMIZED DESIGN

## Technical parameters

- ✓ Electrically-driven heat pumps
- ✓ Double U-loops arrangement of BHEs
- ✓ Thermo-physical properties
  - *Ground thermal conductivity*      1.7 W/(m·K)
  - *Ground thermal diffusivity*      0.68 mm<sup>2</sup>/s
  - *BHE diameter*                              15 cm
  - *BHE pipe diameter*                      2.62-3.2 cm
  - *Spacing between BHEs*                8 m
  - *Grouting thermal conductivity*      1.7 W/(m·K)
  - *BHE thermal resistance*                0.062 m·K/W

## Economic parameters

### Energy Fees - €/kWh

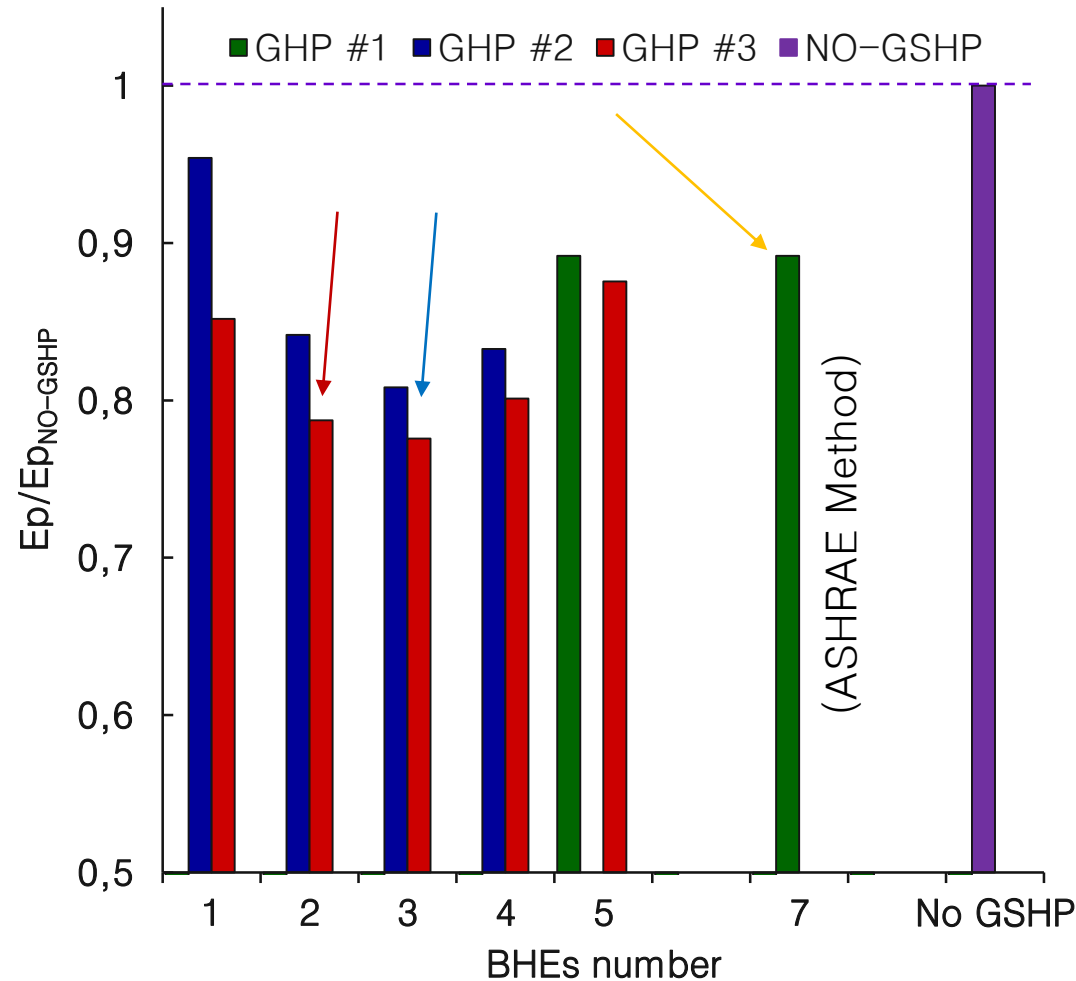
Unit price of electrical energy	0.20
Unit price of natural gas	0.08

### Retail prices – k€

GHP #1	18.5	Boiler #2	4.0	Air unit #2	8.5
GHP #2	5.2	Boiler #3	4.6	Air unit #3	10.0
GHP #3	4.0	Boiler #4	5.0	Air unit #4	14.0

\*Prices are purely indicative.

# ADVANCED/OPTIMIZED DESIGN



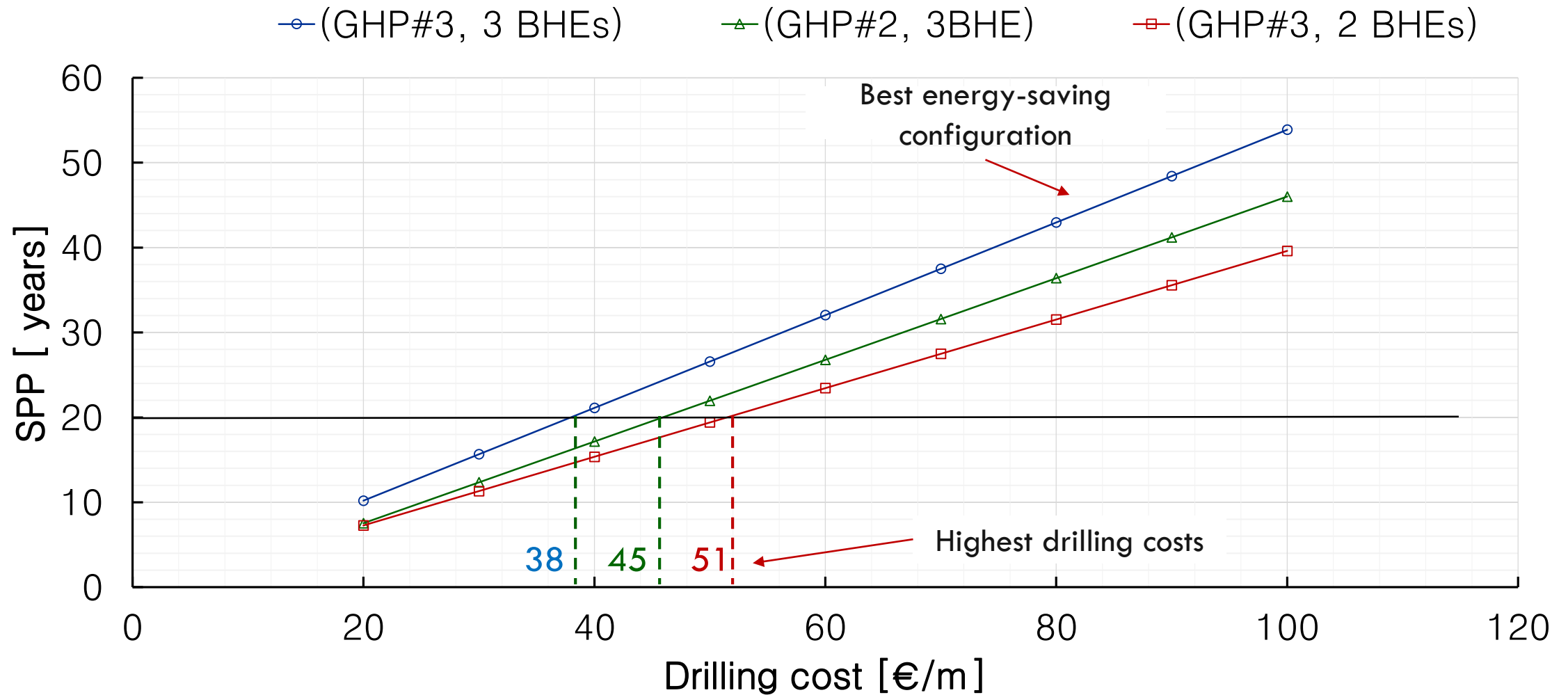
## Remarks:

- ✓ Energy savings normalized with respect to NO-GSHP solution (1183 MWh)
- ✓ GHP#1 needs 5 boreholes to cover the building load alone
- ✓ GHP#3 – 3 BHEs is the best configuration, savings ~22.5% of primary energy
- ✓ GHP#3 – 2 BHEs leads to similar savings (~21.5%) with one less BHE

# ADVANCED/OPTIMIZED DESIGN

	GHP#2 – 3 BHEs	GHP#3 – 3 BHEs	GHP#3 – 2 BHEs	GHP#1 – 7 BHEs (ASHRAE)
<b>Total length of BHEs [m]</b>	100 x 3	100 x 3	100 x 2	100 x 7
$f_H$ (heating season)	0.94	0.85	0.65	1
$f_C$ (cooling season)	0.84	0.23	0.23	1
<b>SCOP</b>	3.42	3.46	3.59	2.53
<b>SEER</b>	3.52	3.55	3.50	3.40
$CR$ (winter/summer)	0.39 / 0.65	0.61 / 0.56	0.47 / 0.56	0.14 / 0.24
<b>Condensing boiler efficiency</b>	1.09	1.09	1.09	-
<b>SEER Air chiller</b>	1.88	3.33	3.33	-
$CR$ Air chiller	0.29	0.81	0.81	-
<b>Heat flow per unit length (winter/summer) [W/m]</b>	19.4 / 34.5	17.2/20.6	19.7/31.6	7.3/10.3
<b>Primary energy consumption (after 20 years) [MWh]</b>	956 (-19.2%)	917 (-22.5%)	931 (-21.3%)	1 055 (-10.8%)

# ADVANCED/OPTIMIZED DESIGN





# ADVANCED/OPTIMIZED DESIGN

	GHP #2 – 3 BHEs			GHP #3 – 3 BHEs			GHP #3 – 2 BHEs		
Drilling cost	SPP	NPV [k€]	PI	SPP	NPV [k€]	PI	SPP	NPV [k€]	PI
20 €/m	8	7.8	0.33	10	5.4	0.22	7	6.3	0.28
40 €/m	17	1.8	0.06	21	<0	<0	15	2.3	0.09
60 €/m	27	<0	<0	32	<0	<0	23	<0	<0
80 €/m	36	<0	<0	43	<0	<0	32	<0	<0
100 €/m	46	<0	<0	54	<0	<0	40	<0	<0

## Acronyms

- ❑ **SPP:** simple payback period
- ❑ **NPV:** net present value after 20 years of operation
- ❑ **PI:** performance index after 20 years of operation

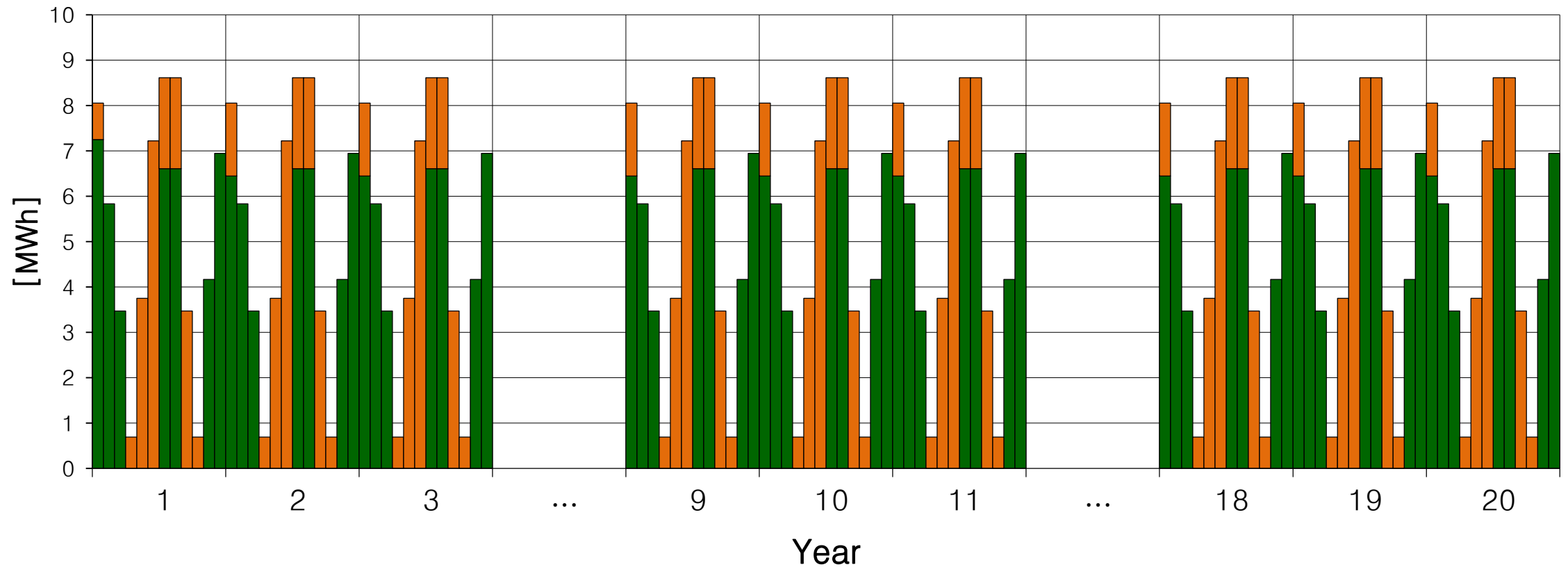
## Note:

- ✓ The 20-year period corresponds to the assumed **operative life of the GHP unit**; it does not refer to the overall GSHP system.
- ✓ **The BHEs field can still operate**, thanks to the optimized sizing and control strategy that **ensure the sustainability of the ground source.**

# ADVANCED/OPTIMIZED DESIGN

■ GSHP ■ Back-up generators

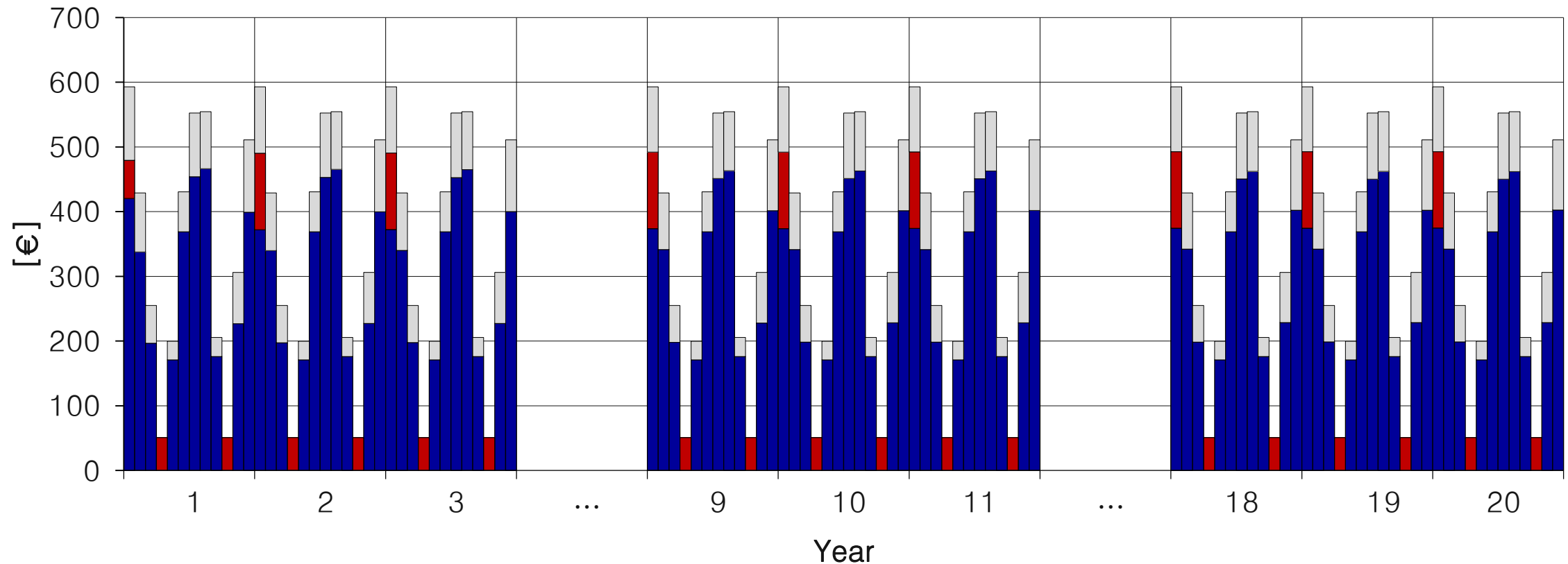
(HP3, 3 BHEs)



# ADVANCED/OPTIMIZED DESIGN

■ Electric energy ■ Natural Gas ■ Saving

(HP3, 3 BHEs)



(Savings with respect to the «NO-GSHP» solution)

# ADVANCED/OPTIMIZED DESIGN

## Economic performance indexes

SPP – Simple payback period (yrs)

PP – Payback period (yrs)

NV – Net value (€)

NPV – Net present value (€)

Profitability indexes – NPV per investment cost

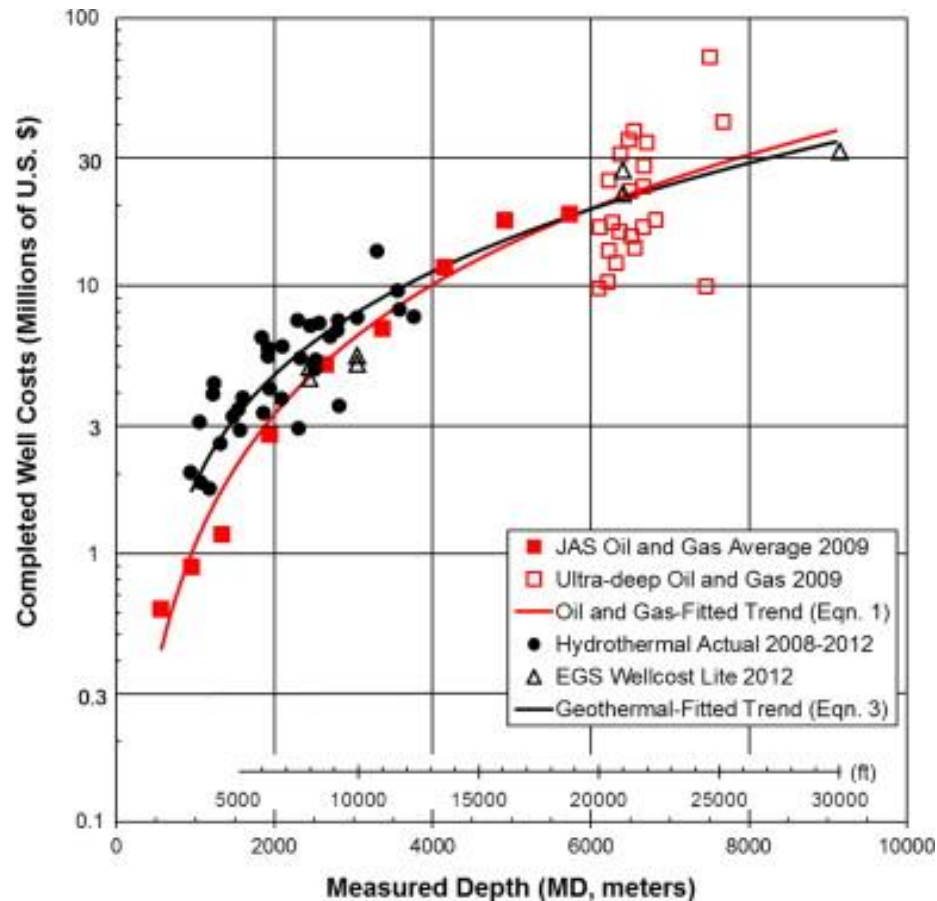
IRR – Internal rate of return

## Economic/energetic performance indexes

COSE - Cost of saved energy (\$/kWh)

Capital cost of saved energy (kWh/\$)

# INVESTMENT ASSESSMENT OF DIRECT USES SYSTEMS



**Shallow boreholes:**

50 – 100 €/m

**Geothermal well costs:**

$$C_{well} = 1.72 \times 10^{-7} (D)^2 + 2.3 \times 10^{-3} - 0.62$$

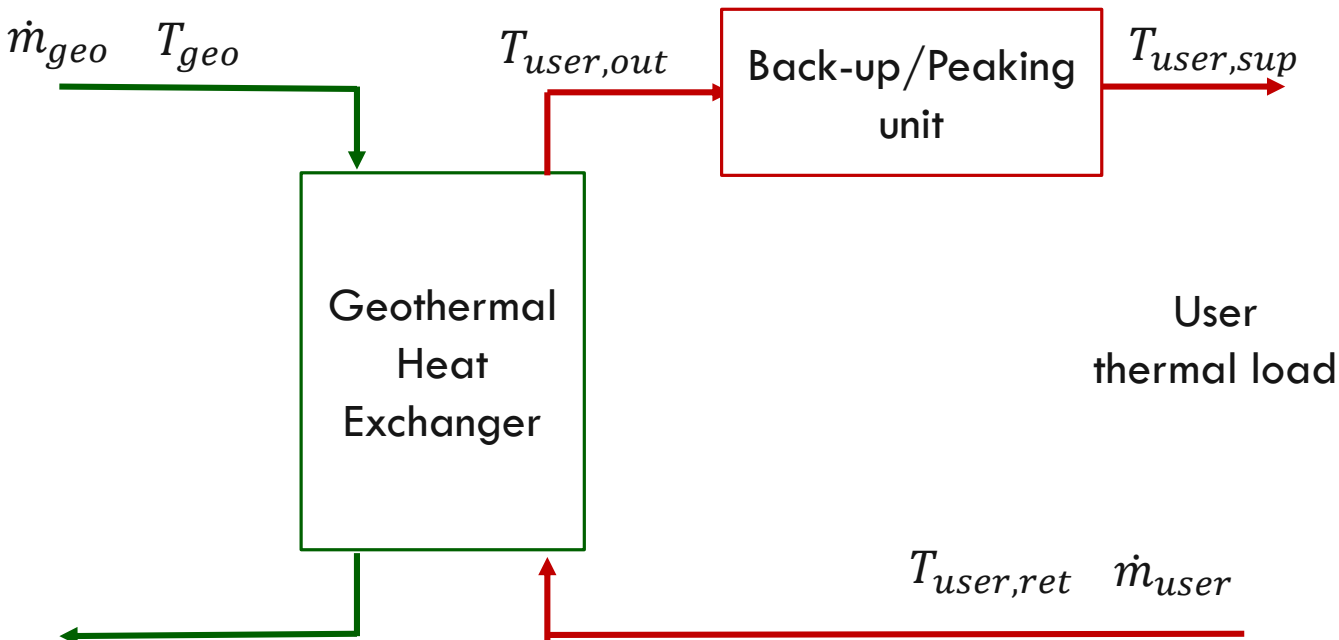
$C_{well}$  - M\$

$D$  - m

(Lukawski et al, 2014)

**! Rule of thumb 1 km → 1 M\$**

# INVESTMENT ASSESSMENT OF DIRECT USES SYSTEMS



## ! Rough analysis / ! First-order evaluation

$c_{f,bk}$  - \$/kWh Unitary costs of standard fuel (avoided energy consumption)

$L$  - kWh Annual energy demand

$\dot{m}_{geo}, T_{geo}$  Geo-resource characteristics

$T_{user,ret}$  Operational return temperature from user loop

$\epsilon$  Geo Hex effectiveness

$$\frac{c_{f,bk} [L - \dot{m}_{geo} c_{geo} (T_{geo} - T_{user,ret}) \epsilon (C^*, NTU)] - \Delta C_{maint} - \Delta C_{aux}}{C_{well} + C_{GHE}(\epsilon) + C_{pipeline}} > 0$$

# DIRECT USES/HEAT PUMPS

***Do less, do it best!!***

THANKS FOR YOUR KIND ATTENTION!!!

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# DIRECT USES/HEAT PUMPS

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